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NATIONAL ENERGY BOARD  
ENGINEERING BRANCH  
OCT 1 8 1991

**WELL SUMMARY**  
**FOR**  
**COLUMBIA GAS DEVELOPMENT OF CANADA**  
**COLUMBIA et al KOTANEELEE YT-I-48**



**WELL SUMMARY**  
**FOR**  
**COLUMBIA GAS DEVELOPMENT OF CANADA**  
**COLUMBIA et al KOTANEELEE YT-I-48**

**CONTENTS**

- 1. WELL DATA**
- 2. INTERVAL/TOTAL CONSUMPTION & COST**
- 3. DISCUSSION BY INTERVAL**
- 4. CONCLUSIONS & RECOMMENDATIONS**
- 5. DRILLING MUD PROPERTIES SUMMARY**
- 6. MUD REPORTS**

**PREPARED BY**

**INTERNATIONAL DRILLING FLUIDS**  
**TECHNICAL SERVICES DEPARTMENT**

**JULY 1991**

**COLUMBIA GAS DEVELOPMENT OF CANADA**

**COLUMBIA et al KOTANEELEE YT-I-48**

**WELL DATA**

**RIG:** KENTING HI-TOWER #07  
**DATE SPURRED:** RE-ENTRY APRIL 29, 1991  
**DATE RIG RELEASED:** JUNE 24, 1991  
**TOTAL DEPTH:** 3915m  
**TOTAL DAYS:** 58

CASING	DEPTH	FLUID TYPE	DAYS	INTERVAL COST	
				PROGRAMMED	ACTUAL
178mm (Liner)	3273m	Gel/Chemical/Wtd	26	\$ 12,040.00	\$ 27,242.50
127mm	3915m	Polymer/Wtd	32	70,340.00	117,875.80
		<b>WELL TOTAL</b>		<b>\$ 82,380.00</b>	<b><u>\$ 145,118.30</u></b>

**OPERATOR REPRESENTATIVE:** Mr. Harold Rugg  
Mr. Bob Toole  
Mr. Neil Bliss

**CONTRACTOR REPRESENTATIVE:** Mr. Jim Signer  
Mr. Phil Bosomworth

**IDF ENGINEER:** Mr. Rick Reinhart  
Mr. Jim Wieler

**All costs based on field estimates  
and at published book price.**

INTERNATIONAL DRILLING FLUIDS - 266-0722

**COLUMBIA GAS DEVELOPMENT OF CANADA**

**COLUMBIA et al KOTANEELEE YT-I-48**

**MATERIAL CONSUMPTION BY INTERVAL**

**HOLE SIZE: 178mm CASING**

**FLUID TYPE: GEL/CHEMICAL/WTD**

<b>PRODUCT</b>	<b>UNIT SIZE</b>	<b>QUANTITY</b>	<b>UNIT PRICE</b>	<b>TOTAL COST</b>
Gel	100lb	390	\$ 10.00	\$ 3,900.00
Barite	40kg	1629	12.50	20,362.00
Caustic Soda	50lb	30	30.00	900.00
Soda Ash	40kg	12	20.00	240.00
Sulban	19kg	6	250.00	1,500.00
Sodium Bicarbonate	100lb	5	40.00	140.00
Sawdust	sacks	28	5.00	137.20

**INTERVAL TOTAL \$ 27,242.50**

**COLUMBIA GAS DEVELOPMENT OF CANADA**

**COLUMBIA et al KOTANEELEE YT-I-48**

**MATERIAL CONSUMPTION BY INTERVAL**

**HOLE SIZE: 152mm**

**FLUID TYPE: POLYMER/WTD**

<b>PRODUCT</b>	<b>UNIT SIZE</b>	<b>QUANTITY</b>	<b>UNIT PRICE</b>	<b>TOTAL COST</b>
Barite	40kg	2260	\$ 12.50	\$ 28,250.00
Caustic Soda	50lb	44	30.00	1,320.00
Soda Ash	40kg	28	20.00	560.00
Sulban	19kg	14	250.00	3,500.00
Lime	25kg	20	8.58	171.60
Sawdust	sacks	160	5.00	800.00
Kwikseal	40lb	75	26.00	1,950.00
<b>IDF-FLR</b>	50lb	45	160.00	7,200.00
Drispac S. Lo	50lb	56	162.40	9,094.40
ASP-721	20L	56	135.00	7,560.00
<b>IDVIS D</b>	25kg	40	420.00	16,800.00
PTS-200	20L	69	260.00	17,940.00
X-Cide	6lb	40	140.00	5,600.00
Sodium Sulfit	50lb	30	49.00	1,470.70
Defoamer	20L	19	150.00	2,850.00
Flo Plex	50lb	21	125.00	2,625.00
Glass Beads	50lb	36	80.00	2,880.00
<b>IDF FCL</b>	25kg	10	32.00	320.00
Visplex	25kg	1	225.00	225.00
Celloflake	25lb	40	23.10	924.00
Mica	25kg	20	15.89	317.80
DFLC	25lb	31	178.00	5,518.00
<b>INTERVAL TOTAL</b>				<b>\$ 117,875.80</b>

**COLUMBIA GAS DEVELOPMENT OF CANADA**

**COLUMBIA et al KOTANEELEE YT-I-48**

**MATERIAL CONSUMPTION BY INTERVAL**

**TOTALS FOR WELL**

<b>PRODUCT</b>	<b>UNIT SIZE</b>	<b>QUANTITY</b>	<b>UNIT PRICE</b>	<b>TOTAL COST</b>
Mica	25kg	20	\$ 15.89	\$ 317.80
Gel	100lb	390	10.00	3,900.00
Barite	40kg	3889	12.50	48,612.50
Caustic Soda	50lb	74	30.00	2,220.00
Soda Ash	40kg	40	20.00	800.00
Sulban	19kg	20	250.00	5,000.00
Sodium Bicarbonate	100lb	5	40.00	200.00
Sawdust	sacks	188	5.00	940.00
Lime	25kg	20	8.58	171.60
Kwikseal	40lb	56	26.00	1,950.00
<b>IDF-FLR</b>	50lb	45	160.00	7,200.00
Drispac	50lb	56	162.40	9,094.40
ASP-721	20L	56	135.00	7,560.00
<b>IDVIS D</b>	25kg	40	420.00	16,800.00
PTS-200	20L	69	260.00	17,940.00
<b>IDF FCL</b>	25kg	10	32.00	320.00
X-Cide	6lb	40	140.00	5,600.00
Sodium Sulfite	50lb	30	49.00	1,470.00
Defoamer	20L	19	150.00	2,850.00
Glass Beads	50lb	36	80.00	2,880.00
Visplex	25kg	1	225.00	225.00
Flo Plex	50lb	21	125.00	2,625.00
Celloflake	25lb	40	23.10	924.00
DFLC	25lb	31	178.00	5,518.00

**WELL TOTAL**

**\$ 145,118.30**

## COLUMBIA GAS DEVELOPMENT OF CANADA

### COLUMBIA et al KOTANEELEE YT-I-48

#### DISCUSSION BY INTERVALS

**HOLE SIZE:** 178mm CASING

**MUD TYPE:** GEL/CHEMICAL (Weighted)

Mixed 90m<sup>3</sup> of kill mud at 1200kg/m<sup>3</sup>. Displaced the hole to mud and built volume increasing the yeild point to a level high enough to suspend the Barite. The possibility of H<sub>2</sub>S required raising and controlling the pH at 11.0 with Caustic Soda. Also pre-treated with 1.6kg/m<sup>3</sup> of Sulban (H<sub>2</sub>S Scavenger). Mixed a Barite pill prior to each trip (45 sacks) which continued to increase the density. Controlled the density at 1200kg/m<sup>3</sup> with water dilution at 20/L min. when circulating. Due to the high bottom hole temperature of approximately 350<sup>o</sup>F the viscosity at the shaker was 20 to 40 sec/L higher than at the suction. Set a bridge plug at 3331 metres. Whipstock packer at 3277 metres, logged and ran in with mill. Milled a window in the 178mm casing. Kicked off and drilled 152mm hole to 3290 metres.

**HOLE SIZE:** 152mm

**MUD TYPE:** POLYMER (Weighted)

Pre-mixed a weighted Polymer system on May 25, 1991. Displaced the hole over to the Polymer system and built volume and condition the mud. Drilled ahead, mixing 1 jug of X-Cide and 3 pails PTS-200 daily to prevent the Polymers from breaking down due to the high bottom hole temperature (350<sup>o</sup>F+). Maintained the viscosity at 35-45 s/L using **IDVIS D** and ASP-721. Controlled pH at 10.5 using Caustic Soda. The Yield point was 10 (Pa) until 3435 metres and then started to climb to 14. Increased H<sub>2</sub>O additions and added 27 sacks **IDF FCL** to lower the yield point. ASP-721 additions were stopped on June 8th at 3530 metres and resumed on June 17th at 3680. The fluid loss climbed from 10mL to 37mL. Used Drispac S. Lo and **IDF-FLR** to control the filtrate. Fluid loss was very unstable until additions of Flo Plex (3.7kg/m<sup>3</sup>) at 3800 metres. Fluid loss dropped below 8mL.

While drilling from 3784 metres - 3822 metres, the hole took approximately 8m<sup>3</sup> fluid. Prior to a trip out with Bit #17, a 14m<sup>3</sup> L.C.M. pill was spotted in the annulus. No further losses were encountered while drilling. TD was 3915 metres. Logged and ran 127mm liner. Lost approximately 21m<sup>3</sup> while running liner. Pumped L.C.M. and by passed shaker screens while circulating prior to cementing.

## **COLUMBIA GAS DEVELOPMENT OF CANADA**

### **COLUMBIA et al KOTANEELEE YT-I-48**

#### **CONCLUSIONS AND RECOMMENDATIONS**

**HOLE SIZE: 178mm CASING**

**MUD TYPE: GEL/CHEMICAL (Weighted)**

Pre-mixed a weighted Gel system prior to drilling out the bridge plug. The density was raised to 1200kg/m<sup>3</sup> due to expected gas pressures. Maintained the pH at 10.5-11.0 and pre-treated with .6kg/m<sup>3</sup> Sulban due to the possibility of H<sub>2</sub>S. This mud system was used to cut a window in the casing at 3273 metres with no problems.

**HOLE SIZE: 152mm**

**MUD TYPE: POLYMER**

Pre-mixed and displaced the hole with a weighted Polymer system after the window was cut in the casing. The Polymer system was used to prevent any damage to the producing formation. The density was controlled in the 1180-1210kg/m<sup>3</sup> range due to the possibility of high formation pressures. The hole was directionally drilled to stay away from the old hole. Fished for cones at 3664 metres and 3695 metres. The hole was in good shape and no problems were encountered other than the difficulty keeping the fluid loss down. Flo Plex was added to lower fluid loss below 12mL and no further problems were reported.

**COLUMBIA GAS DEVELOPMENT OF CANADA**

**COLUMBIA et al KOTANEELEE YT-I-48**

**PROGRAMMED PRODUCT COST DISCUSSION**

<b>Programmed Product Cost</b>	<b>\$ 82,380.00</b>
<b>Actual Cost</b>	<b>\$ 145,118.30</b>

**PRODUCT COST SUMMARY vs PROGRAMMED COST**

<b>Product</b>	<b>Programmed Usage</b>	<b>Actual Usage</b>	<b>Cost Difference</b>	<b>Reason For Use</b>
Bentonite	200	390	\$ 1,900.00	viscosity
Barite	1800	3889	26,112.50	density
Bicarbonate	50	5	(1,800.00)	cement contamination
Caustic Soda	42	74	960.00	pH control
<b>IDBOND (ASP 721)</b>	50	56	810.00	shale control
<b>IDF FCL</b>	40	10	(960.00)	thinner
Soda Ash	5	40	700.00	water hardness control
X-Cide 207	20	40	2,800.00	Biocide
<b>IDF-FLR (Drispac)</b>	60	101	6,560.00	fluid loss
DFLC	30	31	178.00	thinner
<b>IDVIS D</b>	25	40	6,300.00	viscosity
<b>PTS 200</b>	80	69	(2,860.00)	temperature stability
Mica	--	20	317.80	LCM
Sulban	--	20	5,000.00	H <sub>2</sub> S Scavenger
Sawdust	--	188	940.00	LCM
Lime	--	20	171.60	camp use
Kwik-Seal	--	56	1,950.00	LCM
Sodium Sulphite	--	30	1,470.00	polymer stability
<b>DEFOAMER</b>	--	19	2,850.00	gas entrapment
Glass Beads	--	36	2,880.00	torque reducer
<b>VISPLEX</b>	--	1	225.00	viscosity
<b>FLOPLEX</b>	--	21	2,625.00	fluid loss
Celloflake	--	40	924.00	LCM

## COLUMBIA GAS DEVELOPMENT OF CANADA

### COLUMBIA et al KOTANEELEE YT-I-48

## PRODUCT USE DISCUSSION

### WORKOVER

The product cost for the workover section of the re-entry was \$15,000.00 over our estimated program cost. This overrun was due to the time spent on this section (estimated 4 days, actual 26 days) and the Barite used for trip pills during this time (\$12,000.00). Extra Bentonite, Caustic Soda and four pails of Sulban accounted for the balance of the cost in excess of the estimate.

### RE-DRILL

The re-drill section of the project was accomplished within the programmed time frame, but the product cost was \$47,500.00 above the programmed estimate. Barite use was again the biggest reason as about \$14,000.00 over the programmed estimate was used. Trip pills and lost circulation accounted for the use. The centrifuge was used to reduce the density as it climbed above levels required for pressure control due to the many trip pills used.

Fluid loss control was the only drilling fluid problem experienced on this well. The programmed combination of **IDF-FLR**, **Drispac**, **PTS 200** and **Sodium Sulphite** could not stabilize the fluid loss once bottom hole temperatures climbed to the expected high levels. **FLOPLEX** was brought to location and used to stabilize the fluid loss. Fluid loss control contributed to \$7,800.00 of the cost over programmed estimate.

Lost circulation while drilling and running liner accounted for \$4,200.00 of lost circulation material and losses of \$7,200.00 of mud. The mud was on standby in a premix tank on location, but the cost to build the additional volume had not been included in our estimate.

Glass Beads were used to reduce torque between the casing and drillstring when kicking off (\$2,880.00). Scavenger to control hydrogen sulphide (\$5,000.00), Biocide to ensure bacteria did not become a problem (\$2,800.00 above estimate) and **DEFOAMER** to reduce gas entrapment (\$2,850.00) accounted for the balance of the cost over programmed estimate.

## COLUMBIA GAS DEVELOPMENT OF CANADA

### COLUMBIA et al KOTANEELEE YT-I-48

#### FUTURE AREA WELLS or RE-ENTRIES

#### PROGRAM RECOMMENDATIONS

1. The Polymer system is the best system to use on main hole or on a re-entry section in this area. It provides shale stability if these sections are in open hole, does not flocculate due to the high bottom hole temperatures and provides even cleaning ability through the different annular sizes. In addition, it appears that no formation damage was done as the well cleaned up and is producing as expected.
2. Programs for fluid loss control in the area will have to include product equivalent to **FLOPLEX** in the Polymer system. Conventional fluid loss polymers along with polymer stabilizers could not control the fluid loss adequately.
3. The balance between losses or gains from the producing formation appear to be very close, whole mud loss occurred both drilling and when running the casing. Although the losses were not severe on this well potential for serious problems exist and should be planned for. High mud weight to fight pressure may contribute to losses that would cause a serious well control problem.
4. Use a storage shed for mud products on location. Product bags were on location for over three (3) months and the shrink wrap started to break down. Product loss could have been a greater problem if the weather turned worse.

**COLUMBIA GAS DEVELOPMENT OF CANADA**

**COLUMBIA et al KOTANEELEE YT-1-48**

**MATERIAL SUPPLY RECORD**

<b>PRODUCT</b>	<b>RECEIVED</b>	<b>RETURNED</b>	<b>USED</b>	<b>COST</b>	<b>TOTAL</b>
Mica	20	0	20	\$ 15.89	\$ 317.80
Gel	665	275	390	10.00	3,900.00
Caustic Soda	210	136	74	30.00	2,220.00
Barite	6196	2307	3889	12.50	48,612.50
Soda Ash	40	0	40	20.00	800.00
Sulban	100	80	20	250.00	5,000.00
Lime	20	0	20	8.58	171.60
Sodium Bicarbonate	60	55	5	40.00	200.00
Sawdust	288	100	188	4.90	940.00
<b>IDF-FLR</b>	80	35	45	160.00	7,200.00
Drispac S. Lo	80	24	56	162.40	9,094.40
ASP-721	80	24	56	135.00	7,560.00
<b>IDVIS D</b>	80	40	40	420.00	16,800.00
PTS-200	158	89	69	260.00	17,940.00
<b>IDF FCL</b>	60	50	10	32.00	320.00
X-Cide	42	2	40	140.00	5,600.00
Sodium Sulfito	30	0	30	49.00	1,470.00
Kwikseal	150	75	75	26.00	1,950.00
Defoamer	20	1	19	150.00	2,850.00
Visplex	10	9	1	225.00	225.00
Celloflake	40	0	40	23.10	924.00
Glass Beads	64	28	36	80.00	2,880.00
Flo Plex	56	35	21	125.00	2,625.00
DFLC	35	4	31	178.00	5,518.00
				<b>MATERIAL COST</b>	<b>\$ 145,118.30</b>
				<b>ENGINEER COST</b>	<b>\$ 21,375.00</b>
				<b>SHRINKWRAPS</b>	<b>\$ 3,060.00</b>
				<b>FREIGHT</b>	<b>\$ 30,852.50</b>
				<b>PALLETS</b>	<b>\$ 3,084.00</b>
				<b>LOADING &amp; UNLOADING</b>	<b>\$ 693.54</b>
				<b>POLY TARP</b>	<b>\$ 150.00</b>
				<b>FREIGHT ADJUSTMENT</b>	<b>\$ 2,831.81</b>
				<b>G.S.T.</b>	<b>\$ 14,791.80</b>
				<b>TOTAL COST</b>	<b><u>\$ 221,930.25</u></b>





















# International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WT. GEL CAUSTIC

WELL NAME COLUMBIA et al KOPALAK AREA Y-5-E-48

STOCK POINT FT. ST. JOHN Contractor KENTING #7

ENGINEERS J.M. WHEELER

Day No.	DATE	DEPTH	MUD PROPERTIES																				OPERATION REMARKS		
			WEIGHT PPG				VISCOSITY				GEL				Filtrate Analysis				RETORT						
			Sec./L	A.V. cps	P.V. cps	Y.P. Pa	10	0	FLUID LOSS .30 Min cc's	CAKE mm	H.T.H.P. cc's	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m <sup>3</sup>	POTASH kg/m <sup>3</sup>	ID BOND kg/m <sup>3</sup>	"N"		"K"	
18	05-16	3200	1190	56	25	20	5	3	10.5	2.0	-	16.7	750	TR.	1.4	-	.07	.002	70						PRESSURE TEST CEMENT
19	05-17	3274	1185	48	26	22	4	1	12.4	2.0		10.8	750	TR.	1.4		.07	TR.	66						LOGGING & RAN IN TO MILL
20	05-18	3274	1190	62	36	28	8	3	12.6	2.0		11.0	750	TR.	1.4		.07	TR.	70						C.R.
21	05-19	3274	1195	62	39	30	9	3	12.6	2.0		11.0	750	TR.	1.3		.07	TR.	70						MILLING WINDOW
22	05-20	3276	1190	53	35	28	7	1	13.0	2.0		11.0	750	TR.	1.3		.07	TR.	70						MILLING
23	05-21	3277	1190	53	35	28	7	1	13.0	2.0		11.0	750	TR.	1.3		.07	.001	70						"
24	05-22	3277	1195	53	35	28	7	1	12.8	2.0		10.5	700	TR.	1.2		.075	.001	70						"
25	05-23	3279	1205	57	41	32	9	3	12.0	2.0		11.0	650	TR.	1.1		.08	.002	75						"
26	05-24	3290	1210	60	44	34	10	3	12.4	2.0		10.5	600	TR.	1.0		.085	TR.	75						DRUG 152 mm HOLE, DISPLAYED
27	05-25	3308	1185	40	16	10	6	3	11.0	.05		10.0	150	TR.	.50		.045	.001	-	.50					HOLE TO A POLYMER SYSTEM
28	05-26	3334	1190	39	20	10	10	3	8.0	.05		10.0	150	TR.	.40		.06	.002	-	.75					DRUG 152 mm HOLE.
29	05-27	3354	1190	37	20	10	10	3	8.0	.05		10.5	150	TR.	.45		.07	.003	-	1.1					" " "
30	05-28	3400	1185	37	20	10	10	3	8.0	.05		10.5	150	TR.	.45		.065	.003	-	1.2					DRUG 152 mm HOLE

REMARKS: - 05-16 PRESSURE TEST 05-17/18 SET BRIDGE PLUG AT 3331 m SET WITH Packer AT 3277 m LOGGED & RAN IN WITH MILL. AFTER MILLING WAS COMPLETED, DRILLED 152 mm HOLE TO 3290 m, AND THE HOLE WAS DISPLAYED TO A WT. POLYMER SYSTEM. DENSITY - 1180 - 1200 kg/m<sup>3</sup>. THE YIELD PT. WAS RAISED TO 8-10 (Pa) USING IDVLS D + ASP-721. VIS. - 35-40 s/L. PH - 10-10.5. FLUIDLOSS BELOW 15 ml.





# International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED POLYMER SYSTEM

WELL NAME COLUMBIA ET AL AREA KOTANEELEK

STOCK POINT FT. ST. JOHN Contractor KENTING #07

ENGINEERS RICK REINHART

(5)

Day No.	DATE	DEPTH	MUD PROPERTIES																		OPERATION REMARKS		
			WEIGHT PPG		VISCOSITY					GEL		FILTRATE ANALYSIS				RETORT		OTHER					
			SEC/L	A.V. CPS	P.V. CPS	Y.P. PA	10	30	FLUID LOSS 30 Min cc's	CAKE mm	H.T.H.P. CC'S	PH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m <sup>3</sup>	POTASH kg/m <sup>3</sup>		ID BOND kg/m <sup>3</sup>	ASPHALT
38	06-05	3481	1175	41	26	75	11	2.5	17.0	1.0	-	10.5	280	20	.85	-	.065	.001	10	.5	0	120	JUNE-05 DRILL AHEAD.
	06-05	3492	1175	41	25	15	10	2.5	16.5	1.0	-	10.5	280	20	.9	-	.065	.001	10	.6	0	120	CONDITION MUD.
																							JUNE-06 DRILL w/ MUD
39	06-06	3494	1180	42	26	15	11	2.5	12.0	1.0	-	10.5	250	20	.85	-	.068	.001	11	.7	0	120	MOTOR, To 3495 M.
		3495	1180	42	27	16	11	2.5	11.5	1.0	-	10.5	350	25	.85	-	.068	.002	11	.8	0	150	CONDITION MUD, WORK ON FLUID LOSS. MIXING
40	06-07	3497	1180	45	32	20	12.5	2.5	15.5	1.5	-	10.5	250	20	.9	-	.068	.002	10	.8	0	160	DRISPAC. LOUIS. FILTER
	06-07	3510	1180	43	28.5	18	11.5	2.5	13	1.5	-	10.5	250	20	1.0	-	.068	.002	10	.8	0	150	CAKE IS MUCH FIRMER,
	06-07	3524	1175	43	29	18	11	2.5	12	1.0	-	10.5	250	20	.85	-	.066	.015	10	.8	0	150	NOT JUST SOLIDS.
																							HOIST BIT #6 FOR
41	06-08	3544	1175	42	27	17	10	2.5	12.5	1.5	-	10.5	250	20	.85	-	.066	.001	10	.7	0	130	NEW MUD MOTOR.
																							MIXING DRISPAC. LOW.
42	06-09	3552	1175	45	30	19	11	2.5	13	1.0	-	11.0	300	30	1.3	-	.065	.001	10	.7	0	165	FLUID LOSS IS STAYING
																							"12 TO 13 CM"

REMARKS: JUNE-07 Run in BIT #7. GAS ON BOTTOMS UP IS @ 9,000 UNITS + AFTER TRIP. THE VISCOSITY IS UP TO 45 SEC/L YIELD @ 12.5 PA. FLUID LOSS @ 15.5 CM<sup>3</sup>. THESE UNSTABLE PROPERTIES ARE LIKELY DUE TO EXTRA ADDITIONS OF ASP. 721 STOP ASP. 721. MIXING D.E.C.L. @ .5 KG/M<sup>3</sup>. AFTER MIXING D.E.C.L. Run WATER @ 20 L/MIN. JUNE-08 DRILL AHEAD w/ STEERING TOOL @ 2 1/2 m/HR. HOIST BIT #7 @ 3550 M. JUNE-09 Run in BIT #8 w/ STABILIZERS. REAM FROM 3470 TO 3550 METERS. MIXED 3 BAGS OF DRISPAC-LOUIS. THIS RAISED THE VISCOSITY FROM 43 TO 46 SEC/L + ALSO RAISED THE FLUID LOSS. LIKELY DUE TO THE HIGH CONCENTRATION OF POLYMERS. (CONT.) DUE TO Run WATER AS THE MUD IS DEHYDRATED. DUE TO THE HIGH CONC. OF POLYMERS.





# International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED POLYMER

WELL NAME COLUMBIA ETAL AREA KATANELEF  
 STOCK POINT FT. ST. JOHN Contractor KENTINE #07  
 ENGINEERS ALIC REINHART

①

Day No.	DATE	DEPTH	MUD PROPERTIES																		OPERATION REMARKS				
			WEIGHT PPG		VISCOSITY			GEL		Filtrate Analysis				RETORT		BENTONITE			POLYMER						
			sec./l	A.V. cps	P.V. cps	YP. Pa	10	FLUID LOSS 30 Min cc's	CAKE mm	H.T.H.P. cc's	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>		kg/m <sup>3</sup>			
46	06-13	3636	1200	45	30	21	9	1.5	2	20	1.0	-	10.5	300	100	1.0	TTC	.083	.002	10	125	4.5	0	0	JUNE-13 PRESSURE TEST. Run in DIT #10
47	06-14	3654	1205	43	27	20	25	1.5	2	17	1.2	-	10.5	300	80	1.3	TTC	.085	.002	10	125	4.8	5	1.4	(SHGIL H2S) on DITMS. OP
	06-14	3565	1210	44	28	20	8	1.5	2	18	1.0	-	10.5	300	40	1.8	TTC	.09	.002	10	100	5.0	0	1.4	MIX 1.4 KG/M <sup>3</sup> SILDAN. FLUID LOSS WENT UP TO
48	06-15	3664	1215	44	29	21	8	1.5	2	18.5	1.2	-	10.5	300	50	1.6	TTC	.093	.002	10	120	5.0	0	1.4	20 CM <sup>3</sup> . TREAT OUT 120
	06-15	3667	1215	43	28.5	22	25	1.5	2	22	1.0	-	10.5	300	60	1.5	TTC	.093	.002	10	130	5.0	0	1.4	MILL (ALLOW W/SODA ASH (PRE-MIX L.C.M. MUD IN
49	06-16	3672	1200	43	27.5	20	25	1.5	2	26	1.0	-	10.5	350	40	1.5	TTC	.085	.002	12	130	4.5	0	1.2	PRE-MIX TANK.) VISCOSITY
																									0.50 SEC/L. W/ L.O. VIS-D
50	06-17	3681	1190	45	29	22	7	1.5	2	29	1.2	-	10.5	350	40	1.5	TTC	.075	.002	12	130	5.0	0	1.3	+ FLR. REG. ADD 15 M <sup>3</sup>
	06-17	3685	1195	43	26	20	6	1.5	2	33	1.5	-	10.5	400	40	1.5	-	.08	.002	15	130	6.0	0	1.0	FROM ACTIVE SYSTEM TO LOWER MAIN TANK
																									VOLUME.

REMARKS: JUNE 14 RAISE MUD DENSITY IN PRE-MIX TANK TO 1210 KG/M<sup>3</sup>. HOIST DIT #10 @ 3664 METERS. LOST 3 CONES, Run in + MILL on CONES, HOIST MILL.  
 JUNE-15 Run in DIT #11 (CLEAR TO BTM. WORK TANK SUR. HOIST DIT #11 @ 3667 M. THE FLUID LOSS IS STILL CLADING, LIKELY DUE TO ASP-721 USED UP. HIGH FLUID LOSS MAY BE NORMAL FOR THIS SYSTEM WHEN MIXING PDS-200 COATING POLYMERS. FILTER CAKE IS FIRM.  
 JUNE-16 Run in DIT #12 DRILL TO 3672 M. BEAM + WORK STABILIZED. HOIST DIT #12 Run in DIT #13  
 JUNE-17 CONDITION MUD. HOIST DIT @ 3681 M. Run in w/ BIT #14. BEAM 10 M. TO BTM. MIXING ASP-721 TO LOWER FLUID LOSS.



# International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED AQUEOUS

WELL NAME COLUMBIA ETAL AREA KOTANEKLEK

STOCK POINT FT. ST. JOHN Contractor KENTING #7

ENGINEERS REIL REINHART / JIM WIELER

(8)

Day No.	DATE	DEPTH	MUD PROPERTIES																		OPERATION REMARKS										
			WEIGHT DATA						VISCOSITY			GEL		FILTRATE ANALYSIS				RETORT				BENTONITE		POTASH		SULPHATES		ID BOND		TOTAL SOLIDS	
			Wt. ppm	sec. dl	A.V. cps	P.V. cps	Y.P. Pa	10	30	mm	H.T.H.P. cc's	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	kg/m <sup>3</sup>	kg/m <sup>3</sup>		kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>	kg/m <sup>3</sup>
51	06-18	369.3	1190	40	23.5	19	4.5	1.5	37	1.5	-	10.5	400	40	1.5	-	.078	.002	15	130	6	0	1.0	JUNE-18 DRILL TO 369.5							
"		369.5	1195	41	24	19	5	1.5	35	1.5	5.0	10.5	350	40	1.5	-	.08	.002	15	130	7	0	1.0	HOIST BIT #15. LOST							
"		369.5	1193	43	25.5	20	5.5	1.5	20	0.8	-	10.3	350	30	1.4	-	.08	.002	13	100	7.5	0	1.0	CONES ON BOTTOM.							
52	06-19	370.5	1200	43	24	19	5	1.5	25	1.0	-	10.3	350	30	1.4	-	.085	.002	14	110	7.5	-	1.0	RUN IN W/ MAGNET							
"	06-19	373.3	1195	43	26	20	6	1.5	15	0.8	-	10.5	350	TR.	1.4	-	.085	.003	-	100	9.0	NEG.	-	1.0	WORK MAGNET + HOIST.						
53	06-20	377.2	1210	43	26	20	6	1.2	19.4	0.8	-	10.5	350	TR.	1.4	-	.09	.004	-	110	9.5	"	-	1.0	THE FLUID LOSS IS						
54	06-21	379.0	1210	44	30	24	6	1.2	24.0	0.8	-	10.5	350	TR.	1.3	-	.09	.004	-	115	9.5	"	-	1.0	STARTING TO COME						
	06-21	380.2	1195	44	30	24	6	1.2	17.0	0.8	-	11.0	350	TR.	1.5	-	.08	.003	-	120	9.5	"	-	1.0	DOWN AND FILTER CAKE						
55	06-22	384.3	1195	46	28	22	6	1.2	7.6	0.5	-	10.5	350	TR.	1.4	-	.08	.003	-	130	10	"	-	1.0	IS TIGHT, DUE TO						
56	06-23	385.0	1205	46	30	24	6	1.2	7.0	0.5	-	10.5	350	TR.	1.4	-	.08	.004	-	120	9.5	"	-	1.0	ADDITIONS OF ASP-721						
57	06-24	391.5	1205	44	26	20	6	1.2	6.6	0.5	-	10.5	350	TR.	1.5	-	.08	.004	-	120	10.0	"	-	1.0	FLUID LOSS DROPPED FROM						
58	06-25	391.5	1210	46	29	22	7	1.2	7.6	0.5	-	11.0	350	TR.	1.8	-	.08	.002	-	120	10.0	"	-	1.0	24 m' TO BELOW B.M. AFF						
59	06-27	391.5	1210	46	25	20	5	1.2	11.0	0.8	-	11.0	350	TR.	1.8	-	.08	-	-	120	9.0	"	-	1.0	1.3 lb/BBL. FLO PEX WAS ADDED TO SYSTEM.						

REMARKS: - LOST APPROX. 8 m<sup>3</sup> FLUID TO HOLE WHILE DRUG. FROM 3784 - 3802 M. PRIOR TO TRIP OUT FOR BIT #17. A 14 m<sup>2</sup> L.C.M. PILL WAS SPOTTED IN ANNULUS NO FURTHER LOSSES WERE ENCOUNTERED. DRILLED 152 mm HOLE TO 391.5 m (T.D.) & LOGGED. RAN 127 mm LINER TO 391.5 m. LOST APPROX. 21 m<sup>3</sup> MUD TO HOLE WHILE RUNNING LINER. PUMPED L.C.M. & BYPASSED SHAKER WHILE C.R. PRIOR TO CEMENTING.



International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 02/03/2001
REPORT No. 101
SPUD DATE RE E. T. B.

WELL NAME ... LOCATION VT T US
OPERATOR ... CONTRACTOR ...
REPORT FOR Mr. ... REPORT FOR Mr. ...

Table with 5 columns: ASSEMBLY, CASING, MUD Vol. (m³), PUMP OUTPUT, ANNULAR VEL. m./min. Includes rows for BIT SIZE, DRILL PIPE, DRILL COLLARS, OTHER.

Table with 3 columns: HOLE DATA, DESANDER/DESTILTER, DRILLING FLUID SPECIFICATIONS. Includes rows for MUD TYPE, HOLE COND., DEVIATION, CURRENT OP.

EQUIPMENT: [ ] DEGASSER [ ] DESILTER [ ] DESANDER [ ] CENTRIFUGE [ ] DOUBLE DECK OR HIGH SPEED SHAKER

Table with 2 main sections: MUD PROPERTIES and MATERIALS INVENTORY & COST. Includes rows for TIME SAMPLE TAKEN, PRESENT DEPTH, FLOWLINE TEMPERATURE, DENSITY, etc.

COMMENTS:
1. Viscosity 45-50 sec 10 ml 7 FPL 245 sec 10 ml
2. Mud ... 119-1000 ...
3. ... 10 ... 15 ...

STOCK POINT ... I.D.F. ENGINEER ...
PHONE ... MOBILE # ...



# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 01/23/91  
 REPORT No. 815  
 SPUD DATE 01/23/91

WELL NAME W-101 STAIRWAY 2000 FT LOCATION W-7-118

OPERATOR W. J. BIRD CONTRACTOR W. J. BIRD

REPORT FOR Mr. W. J. BIRD REPORT FOR Mr. W. J. BIRD

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>4500</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>20</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>2000</u>	m³/STK. <u>0.150</u>	OPPOSITE D.C.
DRILL COLLARS <u>mm</u>	INTER. <u>15.754</u>	TOTAL <u>10500</u>	S.P.M. <u>5</u>	PUMP PRESS. <u>4100</u>
OTHER	OTHER	STANDBY	m³/min. <u>10</u>	CIRC. TIME <u>150</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>CEL 1190</u>	FLOWLINE WT.	kg/m³	MUD WT. <u>1190</u>	kg/m³	
HOLE COND.	UNDERFLOW WT.	kg/m³	VISCOSITY <u>45</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m³	FILTRATE	cm³/30 min.	
CURRENT OP.	UNDERFLOW RATE	m³/min.	pH <u>10.5-11.0</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL.  PIT

TIME SAMPLE TAKEN	MUD PROPERTIES			MATERIALS INVENTORY & COST				
	INITIAL	RECEIVED	USED	BALANCE	COST	PREVIOUS COST	STARTING VOLUME	
PRESENT DEPTH (m)	<u>1100</u>							
FLOWLINE TEMPERATURE (°C)	<u>25.45</u>							
DENSITY (kg/m³)	<u>4500</u>							
FUNNEL VISCOSITY (s/L)	<u>1190</u>							
APPARENT VISCOSITY (mPa.s)	<u>44</u>							
PLASTIC VISCOSITY (mPa.s)	<u>345</u>							
YIELD POINT (Pa)	<u>7</u>							
GELS 0/10 min. (Pa)	<u>45</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>140</u>							
FILTER CAKE (mm)	<u>200</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>810</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>70</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>800</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.10</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.05</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>9.0</u>							
MBT (Kg/m³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>50</u>							
ELECTRICAL STABILITY (V)	<u>-</u>							
OIL/WATER RATIO	<u>-</u>							
CaCl₂ w/w%	<u>-</u>							
"n"/"k" <u>100/300</u>	<u>40/50</u>							

COMMENTS:

1. MUD TYPE CEL 1190 - 1190 KG/M3, 45 SEC/FUNNEL, 7.00 VOL. LOSS

2. CEL 1190 - 1000 KG/M3, 45 SEC/FUNNEL, 7.00 VOL. LOSS

3. MUD TYPE CEL 1190 - 1190 KG/M3, 45 SEC/FUNNEL, 7.00 VOL. LOSS

4. CEL 1190 - 1000 KG/M3, 45 SEC/FUNNEL, 7.00 VOL. LOSS

5. MUD TYPE CEL 1190 - 1190 KG/M3, 45 SEC/FUNNEL, 7.00 VOL. LOSS

6. CEL 1190 - 1000 KG/M3, 45 SEC/FUNNEL, 7.00 VOL. LOSS

STOCK POINT ST. NELSON I.D.F. ENGINEER BOB BIRD

PHONE 500 222 2222 MOBILE 500 222 2222

THE INFORMATION IN THIS REPORT IS BASED ON OUR EXPERIENCE, REPRESENTS OUR BEST JUDGEMENT IN THE MATTER AND IS INTENDED TO BE HELPFUL, BUT WE CANNOT ASSUME RESPONSIBILITY FOR ANY LOSS OR ACCIDENT THAT MAY RESULT FROM ITS USE. FURTHERMORE, NOTHING CONTAINED HEREIN SHALL BE CONSTRUED AS A RECOMMENDATION TO USE ANY PRODUCT IN CONFLICT WITH EXISTING PATENTS COVERING ANY MATERIALS OR USE



DRILLING FLUID REPORT

DATE 10/05/1991
REPORT No. 503
SPUD DATE 08/29/91

WELL NAME GULFSTREAM OF KATALEEF LOCATION WT. T. 49
OPERATOR GULFSTREAM CO. OPERATOR, IT CONTRACTOR KR. T. 116 # 007
REPORT FOR Mr. HAROLD BULL REPORT FOR Mr. T. J. ...

Table with 5 columns: ASSEMBLY, CASING, MUD Vol. (m³), PUMP OUTPUT, ANNULAR VEL. m./min. Includes rows for BIT SIZE, DRILL PIPE, DRILL COLLARS, and OTHER.

Table with 3 columns: HOLE DATA, DESANDER/DESTILTER, DRILLING FLUID SPECIFICATIONS. Includes rows for MUD TYPE, HOLE COND., DEVIATION, and CURRENT OP.

EQUIPMENT: [ ] DEGASSER [ ] DESILTER [ ] DESANDER [ ] CENTRIFUGE [ ] DOUBLE DECK OR HIGH SPEED SHAKER

Large table with columns: TIME SAMPLE TAKEN, PRESENT DEPTH, FLOWLINE TEMPERATURE, DENSITY, FUNNEL VISCOSITY, APPARENT VISCOSITY, PLASTIC VISCOSITY, YIELD POINT, GELS 0/10 min., pH STRIP, FILTRATE, FILTER CAKE, ALK, TOTAL HARDNESS, SAL, SAND CONTENT, SOLIDS CONTENT, OIL/WATER CONT., MBT, ELECTRICAL STABILITY, OIL/WATER RATIO, CaCl2 w/w%, and "n"/"k" content. Includes sub-tables for MUD PROPERTIES and MATERIALS INVENTORY & COST.

COMMENTS:
1. USE T. 116 # 007 TO KEEP THE MUD ...
2. ...
3. ...

STOCK POINT FT. NELSON I.D.F. ENGINEER PHILIP ...
PHONE ... MOBILE # ...





# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE May 01 1991  
 REPORT No. 404  
 SPUD DATE April 29 91

WELL NAME CONTRACTOR'S WELLS LOCATION WT-T-48

OPERATOR CONTRACTOR'S WELLS CONTRACTOR KEATING  
 REPORT FOR Mr. WATSON REPORT FOR Mr. T. SIGNED

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>149mm</u>	COND.	TANKS <u>55.0</u>	PUMP SIZE <u>114x44</u>	OPPOSITE D.P. <u>58</u>
DRILL PIPE <u>59</u> mm	SURFACE	HOLE <u>12.0</u>	m <sup>3</sup> /STK. <u>0.155</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>443</u>	TOTAL <u>115.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>11000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>25</u>	CIRC. TIME <u>15</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T 100 10 10</u>	FLOWLINE WT. kg/m <sup>3</sup>	MUD WT. <u>1150</u> kg/m <sup>3</sup>
HOLE COND. <u>100</u>	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>10</u> s/L
DEVIATION <u>T 100 10 10</u>	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>1.0</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>10000</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>7000</u>		CEL	215		11	205	100.00
FLOWLINE TEMPERATURE (°C) <u>50</u>		CEL	138		7	131	60.00
DENSITY (kg/m <sup>3</sup> ) <u>1180</u>		CEL	4291		79	4212	987.50
FUNNEL VISCOSITY (s/L) <u>98.80</u>							
APPARENT VISCOSITY (mPa.s) <u>475</u>							
PLASTIC VISCOSITY (mPa.s) <u>30</u>							
YIELD POINT (Pa) <u>175</u>							
GELS 0/10 min. (Pa) <u>714</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>11.5</u>							
FILTER CAKE (mm) <u>15</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L) <u>500</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>		PREVIOUS COST	<u>15</u>	STARTING VOLUME			
ELECTRICAL STABILITY (V)		DAILY COST	<u>114</u>	VOL. BUILT	<u>714</u>		
OIL/WATER RATIO		CUM. COST	<u>16</u>	VOL. LOST ON SURFACE			
CaCl <sub>2</sub> w/w%		CUM. ENG. COST	<u>1500</u>	VOL. LOST SUB SURFACE			
"n"/"k" <u>90/100</u>				END VOLUME			
				CUM. VOL. BUILT			

COMMENTS: 1. All solids are within limits.  
2. Filtrate is 1.0 cm<sup>3</sup>/30 min.  
3. Mud weight is 1150 kg/m<sup>3</sup>.  
4. Viscosity is 10 s/L.  
5. Yield point is 175 Pa.  
6. Gels are 714 Pa.  
7. Filter cake is 15 mm.  
8. Sand content is 0%.  
9. Solids content is 0%.  
10. Oil/water ratio is 100/100.  
11. MBT is 500 mg/L.  
12. Electrical stability is 0 V.  
13. CaCl<sub>2</sub> is 500 mg/L.  
14. "n"/"k" is 90/100.

STOCK POINT IT NE 5000 I.D.F. ENGINEER [Signature]  
 PHONE [Number] PHONE [Number] MOBILE # [Number]



# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 02.03.1991  
 REPORT No. 405  
 SPUD DATE 01.09.91

WELL NAME WELL 101-101-01 LOCATION T-48

OPERATOR CONCRETE DEVELOPMENT CONTRACTOR KENTING HO

REPORT FOR Mr. ALAN BROWN REPORT FOR Mr. T. S. S. S. S.

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>140</u>	COND.	TANKS <u>5</u>	PUMP SIZE <u>111/4x4 1/2</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>52</u>	m <sup>3</sup> /STK. <u>1.15</u>	OPPOSITE D.C. <u>50</u>
DRILL COLLARS <u>130</u> mm	INTER <u>130x4430</u>	TOTAL <u>115</u>	S.P.M. <u>47</u>	PUMP PRESS. <u>12000</u>
OTHER	OTHER <u>130</u>	STANDBY	m <sup>3</sup> /min. <u>5504</u>	CIRC. TIME <u>190</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>1.5% CMC 1.0% BENTONITE</u>	FLOWLINE WT. kg/m <sup>3</sup>	MUD WT. <u>1150</u> kg/m <sup>3</sup>
HOLE COND. <u>1.5% CMC 1.0% BENTONITE</u>	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>60</u> s/L
DEVIATION <u>1.5% CMC 1.0% BENTONITE</u>	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>110</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>1.5% CMC 1.0% BENTONITE</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL.  PIT  SOFT MUD PROPERTIES: MAKING MATERIALS INVENTORY & COST

TIME SAMPLE TAKEN	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>2700</u>			<u>47</u>		<u>575.00</u>
FLOWLINE TEMPERATURE (°C) <u>23.00</u>					
DENSITY (kg/m <sup>3</sup> ) <u>1210</u>					
FUNNEL VISCOSITY (s/L) <u>15</u>					
APPARENT VISCOSITY (mPa.s) <u>34</u>					
PLASTIC VISCOSITY (mPa.s) <u>20</u>					
YIELD POINT (Pa) <u>1000</u>					
GELS 0/10 min. (Pa) <u>310</u>					
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>				
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>110</u>					
FILTER CAKE (mm) <u>1.5</u>					
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>9/11</u>				
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>20</u>					
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>500</u>					
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.05</u>				
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.05</u>				
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.05</u>				
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>0.5</u>				
ELECTRICAL STABILITY (V)					
OIL/WATER RATIO <u>10/100</u>					
CaCl <sub>2</sub> w/w% <u>0.1</u>					
"n"/"k" <u>15/20</u>					
PREVIOUS COST <u>11.500</u>					
DAILY COST <u>500.00</u>					
CUM. COST <u>12.500</u>					
CUM. ENG. COST <u>15.500</u>					
STARTING VOLUME					
VOL. BUILT <u>7.100</u>					
VOL. LOST ON SURFACE <u>1</u>					
VOL. LOST SUB SURFACE <u>1.5</u>					
END VOLUME					
CUM. VOL. BUILT					

COMMENTS: WATER TANKS FULL & READY TO USE

I AS FOUND AT YOUR SITE & CHEMICALS IN WATER  
WAS 1.5% FULL  
WAS 1.5% FULL  
WAS 1.5% FULL  
WAS 1.5% FULL

STOCK POINT ST. NEW I.D.F. ENGINEER ALAN BROWN  
 PHONE 040 000 000 MOBILE # 01 2 1

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# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE MAY 09 1991  
 REPORT No. 406  
 SPUD DATE APR 29 91

WELL NAME W. 113030 W. 113030 LOCATION W. 7-48

OPERATOR W. 113030 W. 113030 CONTRACTOR KEATING INC

REPORT FOR Mr. HAROLD BULL REPORT FOR Mr. TIM SINGER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>140mm</u>	COND.	TANKS <u>55.0</u>	PUMP SIZE <u>11x14x11</u>	OPPOSITE D.P. <u>4/4</u>
DRILL PIPE <u>59</u> mm	SURFACE	HOLE <u>60</u>	m <sup>3</sup> /STK. <u>0.159</u>	OPPOSITE D.C. <u>77</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>400</u>	TOTAL <u>115.0</u>	S.P.M. <u>28</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>5.744</u>	CIRC. TIME <u>730</u>

HOLE DATA	DESANDER/DESTILER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>7-113030-111</u>	FLOWLINE WT. <u>1.195</u> kg/m <sup>3</sup>	MUD WT. <u>1150-1150</u> kg/m <sup>3</sup>
HOLE COND. <u>2515</u>	UNDERFLOW WT.	VISCOSITY <u>10.5</u> s/L
DEVIATION <u>2.2</u>	OVERFLOW WT.	FILTRATE <u>10</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>2515</u>	UNDERFLOW RATE	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	14:00	14:00	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	2515	2515	CEL	313				
FLOWLINE TEMPERATURE (°C)	27.0	27.0	OPPOSITE	5147		88	5259	1100.00
DENSITY (kg/m <sup>3</sup> )	1200	1195						
FUNNEL VISCOSITY (s/L)	68	75						
APPARENT VISCOSITY (mPa.s)	275							
PLASTIC VISCOSITY (mPa.s)	27							
YIELD POINT (Pa) <u>0.25</u>	55							
GELS 0/10 min. (Pa)	214							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	10.5	10						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	10.6							
FILTER CAKE (mm)	1.5-4.0							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	81.9							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	40							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	550							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	0.07							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	0.75							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	9.75		PREVIOUS COST	16.500	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	75		DAILY COST	1100.00	VOL. BUILT			
ELECTRICAL STABILITY (V)	-		CUM. COST	15.000	VOL. LOST ON SURFACE	7.12		
OIL/WATER RATIO <u>11-1.1</u>	0		CUM. ENG. COST	15.000	VOL. LOST SUB SURFACE	1.0		
CaCl <sub>2</sub> w/w% <u>0.5</u>					END VOLUME			
"n" "k" <u>6.0/200</u>	6.125				CUM. VOL. BUILT			

COMMENTS: 1. 113030 W. 113030

1. 113030 W. 113030  
2. 113030 W. 113030  
3. 113030 W. 113030

STOCK POINT FT. NELSON I.D.F. ENGINEER John K. Bennett  
 PHONE 503-338-1111 MOBILE # 503-338-1111

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# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 11/10/91  
 REPORT No. 807  
 SPUD DATE 08/29/91

WELL NAME WELL 1212 FT 01 K20000000 LOCATION VT 7-48  
 OPERATOR WELL 1212 GAS DEVELOPMENT CONTRACTOR KENTING #07  
 REPORT FOR Mr. \_\_\_\_\_ REPORT FOR Mr. TIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/2</u>	COND.	TANKS <u>12.0</u>	PUMP SIZE <u>114 x 4.1</u>	OPPOSITE D.P. <u>58</u>
DRILL PIPE <u>58</u> mm	SURFACE	HOLE <u>10.0</u>	m <sup>3</sup> /STK. <u>0.28</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170</u> mm	INTERICE <u>4121</u>	TOTAL <u>12.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>11000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>19</u>	CIRC. TIME <u>180</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WATER BASED</u>	FLOWLINE WT. <u>1190</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1190</u> kg/m <sup>3</sup>
HOLE COND. <u>17.0</u>	UNDERFLOW WT.	VISCOSITY <u>55.25</u> s/L
DEVIATION <u>1.0</u>	OVERFLOW WT.	FILTRATE <u>10</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>25.0</u>	UNDERFLOW RATE	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>2515</u>		<u>CEI</u>	<u>363</u>		<u>70</u>	<u>298</u>	<u>25000</u>
FLOWLINE TEMPERATURE (°C) <u>28.00</u>		<u>10424</u>	<u>196</u>		<u>7</u>	<u>194</u>	<u>6000</u>
DENSITY (kg/m <sup>3</sup> ) <u>1190</u>		<u>5000</u>	<u>55</u>		<u>70</u>	<u>375</u>	<u>9800</u>
FUNNEL VISCOSITY (s/L) <u>25</u>							
APPARENT VISCOSITY (mPa.s) <u>215</u>							
PLASTIC VISCOSITY (mPa.s) <u>75</u>							
YIELD POINT (Pa) <u>12500</u>							
GELS 0/10 min. (Pa) <u>310</u>							
pH STRIP <input type="checkbox"/> -METER <input type="checkbox"/>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>10.5</u>							
FILTER CAKE (mm) <u>1.5</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>40</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>200</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>							
ELECTRICAL STABILITY (V) <u>-</u>							
OIL/WATER RATIO <u>1.0</u>							
CaCl <sub>2</sub> w/w% <u>4</u>							
"n"/"k" <u>1.0/2.0</u>							
PREVIOUS COST		15000				STARTING VOLUME	
DAILY COST		4450				VOL. BUILT	<u>7.00</u>
CUM. COST		15445				VOL. LOST ON SURFACE	
CUM. ENG. COST		3275				VOL. LOST SUB SURFACE	
						END VOLUME	
						CUM. VOL. BUILT	

COMMENTS:  
AS SPUD ON 08/29/91 AT 11:00 AM  
WELL 1212 AT 10:00 AM WITH

STOCK POINT VT ST TOWN I.D.F. ENGINEER Rich McQuinn  
 PHONE \_\_\_\_\_ PHONE 508 238 1000 MOBILE # 515 111

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# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE NOV 11 1991  
 REPORT No. 428  
 SPUD DATE 09/15/91

WELL NAME W. 1/4 SEC. 35 T. 12 N. R. 10 E. S. 15 LOCATION UT 7-45

OPERATOR CONCRETE CONSTRUCTION CONTRACTOR KEATINGE HCP

REPORT FOR Mr. W. J. ... REPORT FOR Mr. T. J. ...

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>5 1/8</u>	COND.	TANKS <u>1500</u>	PUMP SIZE <u>114 x 114</u>	OPPOSITE D.P. <u>45</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>1000</u>	m <sup>3</sup> /STK. <u>0.135</u>	OPPOSITE D.C. <u>70</u>
DRILL COLLARS <u>100</u> mm	INTER. <u>100-200</u>	TOTAL <u>1500</u>	S.P.M. <u>30</u>	PUMP PRESS. <u>7000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>0.087</u>	CIRC. TIME <u>30</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>Water based</u>	FLOWLINE WT. <u>800</u> kg/m <sup>3</sup>	MUD WT. <u>1190</u> kg/m <sup>3</sup>
HOLE COND. <u>100</u>	UNDERFLOW WT.	VISCOSITY <u>120-90</u> s/L
DEVIATION <u>100</u>	OVERFLOW WT.	FILTRATE <u>10-15</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>100</u>	UNDERFLOW RATE	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>2430</u>							
PRESENT DEPTH (m) <u>3540</u>		<u>DRITE 5059</u>		<u>17</u>	<u>499</u>	<u>827.50</u>	
FLOWLINE TEMPERATURE (°C) <u>37.0</u>		<u>IRITE 194</u>		<u>3</u>	<u>19.7</u>	<u>60.00</u>	
DENSITY (kg/m <sup>3</sup> ) <u>1700</u>							
FUNNEL VISCOSITY (s/L) <u>90</u>							
APPARENT VISCOSITY (mPa.s) <u>45</u>							
PLASTIC VISCOSITY (mPa.s) <u>30</u>							
YIELD POINT (Pa) <u>15</u>							
GELS 0/10 min. (Pa) <u>11</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>10.5</u>							
FILTER CAKE (mm) <u>1.5</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>5/10</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>40</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>500</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/> <u>0.05</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/> <u>0.05</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/> <u>0.40</u>		PREVIOUS COST <u>10.45</u>		STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> -1% <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>15</u>		DAILY COST <u>900.00</u>		VOL. BUILT <u>710.45</u>			
ELECTRICAL STABILITY (V) <u>-</u>		CUM. COST <u>1020.00</u>		VOL. LOST on SURFACE			
OIL/WATER RATIO <u>10/1</u>		CUM. ENG. COST <u>2050</u>		VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <u>0.02</u>				END VOLUME <u>6.00</u>			
"n"/"k" <u>0.01/0.02</u>				CUM. VOL. BUILT			

COMMENTS:  
REF TO LOG FOR LATER FINDING OF LOSS OF GELS  
TO BE TAKEN INTO ACCOUNT  
REF TO LOG FOR LOSS OF GELS  
TO BE TAKEN INTO ACCOUNT

STOCK POINT ST ST TOWN I.D.F. ENGINEER ...  
 PHONE ... PHONE ... MOBILE# ...





# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 02/17/91  
 REPORT No. #10  
 SPUD DATE 02/17/91

WELL NAME WELL 101A FT 101A LOCATION ST T 42  
 OPERATOR INTERNATIONAL DRILLING FLUIDS CORP CONTRACTOR KENTLINE 7107  
 REPORT FOR Mr. WILLIAM T. GAGG REPORT FOR Mr. TIM SHERER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>15 1/4</u>	COND. <u>15.0</u>	TANKS <u>15.0</u>	PUMP SIZE <u>114V/100L</u>	OPPOSITE D.P. <u>49</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>15.0</u>	m <sup>3</sup> /STK. <u>0.138</u>	OPPOSITE D.C. <u>75</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>15.0</u>	TOTAL <u>15.0</u>	S.P.M. <u>41</u>	PUMP PRESS. <u>9100</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>0.796</u>	CIRC. TIME

HOLE DATA	DESANDER/DESILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T 101A</u>	FLOWLINE WT. <u>1.12</u> kg/m <sup>3</sup>	MUD WT. <u>1.12</u> kg/m <sup>3</sup>
HOLE COND. <u>15.0</u>	UNDERFLOW WT. <u>100</u> kg/m <sup>3</sup>	VISCOSITY <u>70.50</u> s/L
DEVIATION <u>15.0</u>	OVERFLOW WT. <u>100</u> kg/m <sup>3</sup>	FILTRATE <u>10.15</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>15.0</u>	UNDERFLOW RATE <u>100</u> m <sup>3</sup> /min.	pH <u>11.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>22:30</u>							
PRESENT DEPTH (m) <u>7500</u>		<u>100.0</u>	<u>456.7</u>		<u>33</u>	<u>40.79</u>	<u>417.50</u>
FLOWLINE TEMPERATURE (°C) <u>30.0</u>							
DENSITY (kg/m <sup>3</sup> ) <u>1.12</u>	<u>1.12</u>						
FUNNEL VISCOSITY (s/L) <u>130</u>							
APPARENT VISCOSITY (mPa.s) <u>50.5</u>							
PLASTIC VISCOSITY (mPa.s) <u>38</u>							
YIELD POINT (Pa) <u>145</u>							
GELS 0/10 min. (Pa) <u>216</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>11.5</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>15.0</u>						
FILTER CAKE (mm) <u>18.600</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>111.0</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>800</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>100</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.8</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>9.3</u>	PREVIOUS COST	<u>19.10</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> -1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>150</u>	DAILY COST	<u>41.50</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>-</u>	CUM. COST	<u>7.00</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO	<u>0</u>	CUM. ENG. COST	<u>41.50</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w%	<u>4</u>			END VOLUME			
"n" / "k"	<u>100/100</u>			CUM. VOL. BUILT			

COMMENTS:  
 I KEEP A CLOSE WATCH ON THE FLUID TO SEE  
 FOR ANY CHANGE IN VISCOSITY  
 2. FOR THE 15.0 LITERS OF FLUID SAMPLED TO BE  
 TAKEN FROM THE SURFACE  
 THANKS

STOCK POINT ST T 42 I.D.F. ENGINEER WILLIAM T. GAGG  
 PHONE 714 941-1111 PHONE 714 941-1111 MOBILE # 15 11



# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 07/17/1991  
 REPORT No #11  
 SPUD DATE 09/29/91

WELL NAME WINDY HILL LOCATION VT. T. 42

OPERATOR WINDY HILL DEVELOPMENT CONTRACTOR KENTING #07

REPORT FOR Mr. WINDY HILL REPORT FOR Mr. TIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/2</u> mm	COND.	TANKS <u>7200</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>49</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>1000</u>	m <sup>3</sup> /STK. <u>0.125</u>	OPPOSITE D.C. <u>95</u>
DRILL COLLARS <u>150</u> mm	INTERFERS <u>7800</u>	TOTAL <u>17200</u>	S.P.M. <u>47</u>	PUMP PRESS. <u>7000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>5796</u>	CIRC. TIME <u>730</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WINDY HILL</u>	FLOWLINE WT. <u>1190</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1200</u> kg/m <sup>3</sup>			
HOLE COND. <u>WINDY HILL</u>	UNDERFLOW WT. <u>105</u> kg/m <sup>3</sup>	VISCOSITY <u>55</u> s/L			
DEVIATION <u>WINDY HILL</u>	OVERFLOW WT. <u>105</u> kg/m <sup>3</sup>	FILTRATE <u>10</u> cm <sup>3</sup> /30 min.			
CURRENT OP.	UNDERFLOW RATE <u>105</u> m <sup>3</sup> /min.	pH <u>10.5-11.0</u>			

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL.  PIT  MUD PROPERTIES CHANGED MATERIALS INVENTORY & COST

TIME SAMPLE TAKEN	PRESENT DEPTH (m)	FLOWLINE TEMPERATURE (°C)	DENSITY (kg/m <sup>3</sup> )	FUNNEL VISCOSITY (s/L)	APPARENT VISCOSITY (mPa.s)	PLASTIC VISCOSITY (mPa.s)	YIELD POINT (Pa)	GELS 0/10 min. (Pa)	pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	FILTER CAKE (mm)	ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	ELECTRICAL STABILITY (V)	OIL/WATER RATIO	CaCl <sub>2</sub> w/w%	"n"/"k"	PREVIOUS COST	DAILY COST	CUM. COST	CUM. ENG. COST	STARTING VOLUME	VOL. BUILT	VOL. LOST ON SURFACE	VOL. LOST SUB SURFACE	END VOLUME	CUM. VOL. BUILT		
10:00	3740	7700	1195	54	70	76	4	113	10.5	115	18000	1117	70	800	0.7	0.7	9.7	62	-	0	2	1.174	21000	53100	74100	45000	61350	21000	21000	0	0	61350		

COMMENTS:  
KEEP A CLOSE WATCH FOR LOSS OF CEMENT  
ONCE CEMENT IS SETTED  
RE-START AT 30 LITERS PER MIN. FOR 1 HOUR  
TIM SIGNER

STOCK POINT VT. ST. JOHN F.C. I.D.F. ENGINEER PAUL BERNHART  
 PHONE 802-251-1111 PHONE 802-251-1111 MOBILE 802-251-1111



# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE NOV 14 1991  
 REPORT No. H 17  
 SPUD DATE 080 79 91

WELL NAME COLUMBIA GAS DEVELOPMENT LOCATION VT. T. 48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING #07  
 REPORT FOR Mr. HAROLD BROWN REPORT FOR Mr. T. L. SIGHELI

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE # <u>1 1/2</u>	COND.	TANKS <u>700</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>400</u>	m <sup>3</sup> /STK. <u>0.178</u>	OPPOSITE D.C. <u>20</u>
DRILL COLLARS <u>150</u> mm	INTER <u>158-2800</u>	TOTAL <u>1000</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>2000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>5934</u>	CIRC. TIME <u>7-8</u>

HOLE DATA	DESANDER/DESILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T. L. SIGHELI</u>	FLOWLINE WT. <u>1190</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1200</u> kg/m <sup>3</sup>
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>100</u> kg/m <sup>3</sup>	VISCOSITY <u>55</u> s/L
DEVIATION <u>1.000</u>	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>10-15</u> cm <sup>3</sup> /30 min.
CURRENT OP.	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2240</u>			GFL	<u>215</u>		<u>200</u>	<u>238</u>	<u>250</u>
FLOWLINE TEMPERATURE (°C)	<u>90</u>	<u>400</u>		ADITE	<u>619L</u>		<u>1718</u>	<u>4958</u>	<u>15 750</u>
DENSITY (kg/m <sup>3</sup> )	<u>1190</u>	<u>1190</u>		ADITE	<u>210</u>		<u>19</u>	<u>190</u>	<u>540</u>
FUNNEL VISCOSITY (s/L)	<u>55</u>	<u>55</u>		ADITE	<u>100</u>		<u>4</u>	<u>96</u>	<u>240</u>
APPARENT VISCOSITY (mPa.s)	<u>30</u>			ADITE	<u>288</u>		<u>28</u>	<u>260</u>	<u>175</u>
PLASTIC VISCOSITY (mPa.s)	<u>25</u>			ADITE	<u>190</u>		<u>1</u>	<u>191</u>	<u>200</u>
YIELD POINT (Pa)	<u>5</u>								
GELS 0/10 min. (Pa)	<u>110</u>								
pH STRIP <input type="checkbox"/> -METER <input type="checkbox"/>	<u>11.0</u>								
FILTRATE <input type="checkbox"/> -API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>110</u>								
FILTER CAKE (mm)	<u>1.8</u>								
ALK <input type="checkbox"/> -(PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1-1.3</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>20</u>								
SAL <input type="checkbox"/> NACl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>800</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>100</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>100</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>50</u>			PREVIOUS COST	<u>200</u>		STARTING VOLUME		
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>50</u>			DAILY COST	<u>200</u>		VOL. BUILT		
ELECTRICAL STABILITY (V)	<u>-</u>			CUM. COST	<u>200</u>		VOL. LOST on SURFACE		
OIL/WATER RATIO	<u>0</u>			CUM. ENG. COST	<u>4800</u>		VOL. LOST SUB SURFACE		
CaCl <sub>2</sub> w/w%	<u>0</u>						END VOLUME		
"n"/"k"	<u>10/20</u>						CUM. VOL BUILT		

COMMENTS:  
 I WOULD A FINE LATER FOR A LARGER PIT 600' IF WE WERE TO GET DOWN TO 50 SECT. BY 10' IN FACT WE WERE TO 11' IN FACT.  
 T. H. BROWN

STOCK POINT VT. ST. TOWN I.D.F. ENGINEER ALAN P. RICHMOND  
 PHONE 508 238 1111 PHONE 508 238 1111 MOBILE # 508 238 1111

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DRILLING FLUID REPORT

DATE 01/15/91
REPORT No. #113
SPUD DATE 09/29/91

WELL NAME ... LOCATION ...

OPERATOR ... CONTRACTOR ...

REPORT FOR Mr. ... REPORT FOR Mr. ...

Table with columns: ASSEMBLY, CASING, MUD Vol. (m³), PUMP OUTPUT, ANNULAR VEL. m./min. Rows include BIT SIZE, DRILL PIPE, DRILL COLLARS, OTHER.

Table with columns: HOLE DATA, DESANDER/DESILTER, DRILLING FLUID SPECIFICATIONS. Rows include MUD TYPE, HOLE COND., DEVIATION, CURRENT OP., FLOWLINE WT., UNDERFLOW WT., OVERFLOW WT., UNDERFLOW RATE, MUD WT., VISCOSITY, FILTRATE, pH.

EQUIPMENT: [ ] DEGASSER [ ] DESILTER [ ] DESANDER [ ] CENTRIFUGE [ ] DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. [ ] PIT [ ] MUD PROPERTIES MATERIALS INVENTORY & COST

Table with columns: TIME SAMPLE TAKEN, PRESENT DEPTH (m), FLOWLINE TEMPERATURE (°C), DENSITY (kg/m³), FUNNEL VISCOSITY (s/L), APPARENT VISCOSITY (mPa.s), PLASTIC VISCOSITY (mPa.s), YIELD POINT (Pa), GELS 0/10 min. (Pa), pH STRIP [ ] METER [ ], FILTRATE [ ] API [ ] HT HP (cm³), FILTER CAKE (mm), ALK [ ] (PF/MF) [ ] (PM/LIME), TOTAL HARDNESS [ ] Ca [ ] (mg/L), SAL [ ] NaCl [ ] Cl [ ] (mg/L), SAND CONTENT (%) [ ] (Ø) [ ], SOLIDS CONTENT (%) [ ] (Ø) [ ], OIL/WATER CONT. (%) [ ] (Ø) [ ], MBT (Kg/m³) [ ] /% [ ] OIL RET [ ], ELECTRICAL STABILITY (V), OIL/WATER RATIO, CaCl₂ w/w%, "n"/"k". Includes MATERIALS INVENTORY & COST sub-table.

COMMENTS: To ...

STOCK POINT ... I.D.F. ENGINEER ... PHONE ... MOBILE # ...





DRILLING FLUID REPORT

DATE 91-05-17  
 REPORT No. 15  
 SPUD DATE 91-04-29

WELL NAME <u>COLUMBIA #1 KATANFELCE</u>		LOCATION <u>V-T-T-40</u>	
OPERATOR <u>COLUMBIA GAS DEVELOPMENT</u>		CONTRACTOR <u>KATANFELCE #7</u>	
REPORT FOR Mr. <u>HAROLD BORG / 255 TRAIL</u>		REPORT FOR Mr. <u>PHILIP J. C. MULLER</u>	
ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS	PUMP SIZE <u>114 x 406</u>
DRILL PIPE <u>69 mm</u>	SURFACE	HOLE	m <sup>3</sup> /STK. <u>0.118</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>177.8 / 230</u>	TOTAL	S.P.M. <u>45</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>0.5</u>
HOLE DATA		DESANDER/DESTILTER	
MUD TYPE <u>CEL CAUSTIC</u>		FLOWLINE WT.	kg/m <sup>3</sup>
HOLE COND.		UNDERFLOW WT.	kg/m <sup>3</sup>
DEVIATION		OVERFLOW WT.	kg/m <sup>3</sup>
CURRENT OP.		UNDERFLOW RATE	m <sup>3</sup> /min.
			pH <u>10.5</u>

EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER	
SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/>	MUD PROPERTIES
TIME SAMPLE TAKEN <u>22:00</u>	
PRESENT DEPTH (m)	
FLOWLINE TEMPERATURE (°C)	
DENSITY (kg/m <sup>3</sup> ) <u>1185</u>	
FUNNEL VISCOSITY (s/L) <u>48</u>	
APPARENT VISCOSITY (mPa.s) <u>27</u>	
PLASTIC VISCOSITY (mPa.s) <u>22</u>	
YIELD POINT (Pa) <u>4</u>	
GELS 0/10 min. (Pa) <u>112</u>	
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>10.5</u>	
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>124</u>	
FILTER CAKE (mm) <u>2.0</u>	
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>1.4/32</u>	
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>	
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>750</u>	
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/> <u>TR.</u>	
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/> <u>87</u>	
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/> <u>93</u>	
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>65</u>	
ELECTRICAL STABILITY (V)	
OIL/WATER RATIO <u>1:3</u> <u>AKG.</u>	
CaCl <sub>2</sub> w/w%	
"n"/"k"	

MATERIALS	MATERIALS INVENTORY & COST				
	INITIAL	RECEIVED	USED	BALANCE	COST
PREVIOUS COST	<u>21,504</u>				
DAILY COST					
CUM. COST					
CUM. ENG. COST	<u>6000</u>				
STARTING VOLUME					
VOL. BUILT					
VOL. LOST ON SURFACE					
VOL. LOST SUB SURFACE					
END VOLUME					
CUM. VOL. BUILT					

COMMENTS:

Control Density at 1100 kg/m<sup>3</sup> using

Portland PM at 10.5 using caustic.

Red to Green H<sub>2</sub>O for pH.

Keep V.C. at 50-55 slt using

STOCK POINT <u>FT ST. JOHN</u>	I.D.F. ENGINEER <u>JIM WIELER</u>
PHONE <u>765-4332</u>	PHONE AT LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-18  
 REPORT No. 16  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA of a1 KOTANEELEE LOCATION Y-T-I-48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING #7  
 REPORT FOR Mr. POP TIDDLE REPORT FOR Mr. PHIL KOSMIDITH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # 152	COND.	TANKS 70	PUMP SIZE 14 x 406	OPPOSITE D.P.
DRILL PIPE 99 mm	SURFACE	HOLE 52	m <sup>3</sup> /STK. .0118	OPPOSITE D.C.
DRILL COLLARS 120 mm	INTER 177.8	TOTAL 120	S.P.M. 37	PUMP PRESS.
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. .436	CIRC. TIME 200

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE GEL CAUSTIC	FLOWLINE WT.	kg/m <sup>3</sup>	MUD WT. 1190	kg/m <sup>3</sup>	
HOLE COND. OK	UNDERFLOW WT.	kg/m <sup>3</sup>	VISCOSITY 50-55	s/L	
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE 12	cm <sup>3</sup> /30 min.	
CURRENT OP. C.R.	UNDERFLOW RATE	m <sup>3</sup> /min.	pH 10.5		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES			MATERIALS INVENTORY & COST			
TIME SAMPLE TAKEN	15:00							
PRESENT DEPTH (m)	3274			MATERIALS BARITE	INITIAL	RECEIVED	USED 35	BALANCE
FLOWLINE TEMPERATURE (°C)	30							COST 438
DENSITY (kg/m <sup>3</sup> )	1190							
FUNNEL VISCOSITY (s/L)	62							
APPARENT VISCOSITY (mPa.s)	36							
PLASTIC VISCOSITY (mPa.s)	28							
YIELD POINT (Pa)	8							
GELS 0/10 min. (Pa)	2/3							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	11.0							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	12.6							
FILTER CAKE (mm)	2.0							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	1.4/2.3							
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	TR.							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	150							
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	TR.							
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	27							
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.93			PREVIOUS COST 21.554	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	70			DAILY COST 438	VOL. BUILT			
ELECTRICAL STABILITY (V)	-			CUM. COST 21.992	VOL. LOST on SURFACE			
OIL/WATER RATIO H <sub>2</sub> O	NEG.			CUM. ENG. COST 6375	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w%					END VOLUME			
"n"/"k"					CUM. VOL. BUILT			

COMMENTS: SET BRIDGE PLUG AT 3331 m  
 SET WH. P. STACK BACKER - 3277 m  
 LOGGED - PAN IN TO FULL  
 HOLD DENSITY AT 1190 kg/m<sup>3</sup> WITH BARITE.  
 PH AT 10.5 WITH CAUSTIC.  
 KEEP V.S. AT 50-55 s/L USING GEL.  
 RUN 20 LINES H<sub>2</sub>O PER MIN.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER  
 PHONE 785-4222 PHONEM LOCATION MOBILE #

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# DRILLING FLUID REPORT

DATE 91-05-19  
 REPORT No. 17  
 SPUD DATE 91-04-27

INTERNATIONAL DRILLING FLUIDS

WELL NAME COLUMBIA #1 of KOTANEELER LOCATION Y-J-I-48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING #7  
 REPORT FOR Mr. Bob Toole REPORT FOR Mr. Phil Rosenthal

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND. <u>75</u>	TANKS <u>53</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>89 mm</u>	SURFACE <u>53</u>	HOLE <u>53</u>	m <sup>3</sup> /STK. <u>0.118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120 mm</u>	INTER. <u>177.8</u>	TOTAL <u>127</u>	S.P.M. <u>5</u>	PUMP PRESS <u>877MS UP=90</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>59</u>	CIRC. TIME <u>2.5 ±</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>GEL CAUSTIC</u>	FLOWLINE WT.	kg/m <sup>3</sup>	MUD WT. <u>1190</u>	kg/m <sup>3</sup>	
HOLE COND. <u>CASED</u>	UNDERFLOW WT.	kg/m <sup>3</sup>	VISCOSITY <u>50-60</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE <u>12</u>	cm <sup>3</sup> /30 min.	
CURRENT OP. <u>MILL</u>	UNDERFLOW RATE	m <sup>3</sup> /min.	pH <u>11.0</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES				MATERIALS INVENTORY & COST				
TIME SAMPLE TAKEN	<u>05:00</u>		<u>23:30</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2274</u>		<u>2274</u>	<u>BARITE</u>			<u>70</u>		<u>875</u>
FLOWLINE TEMPERATURE (°C)	<u>35</u>		<u>39</u>						
DENSITY (kg/m <sup>3</sup> )	<u>1195</u>		<u>1190</u>						
FUNNEL VISCOSITY (s/L)	<u>62</u>		<u>53</u>						
APPARENT VISCOSITY (mPa.s)	<u>39</u>		<u>35</u>						
PLASTIC VISCOSITY (mPa.s)	<u>30</u>		<u>28</u>						
YIELD POINT (Pa)	<u>9</u>		<u>7</u>						
GELS 0/10 min. (Pa)	<u>212</u>		<u>113</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>		<u>11.0</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>12.6</u>		<u>13.0</u>						
FILTER CAKE (mm)	<u>2.0</u>		<u>2.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.3/2.3</u>		<u>1.3/2.4</u>						
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>		<u>TR.</u>						
SAL <input type="checkbox"/> NaCl <input checked="" type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>150</u>		<u>150</u>						
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>TR.</u>		<u>TR.</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>07</u>		<u>07</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>93</u>		<u>93</u>	PREVIOUS COST	<u>21,993</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 7% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>70</u>		<u>70</u>	DAILY COST	<u>875</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>-</u>		<u>-</u>	CUM. COST	<u>22,867</u>	VOL. LOST on SURFACE			
OIL/WATER RATIO <u>H<sub>2</sub>O</u>	<u>NEG.</u>		<u>NEG.</u>	CUM. ENG. COST	<u>6750</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w%						END VOLUME			
"n"/"k"						CUM. VOL. BUILT			

COMMENTS: MILLING WINDOW

CONTROL DENSITY AT 1190 kg/m<sup>3</sup> USING BARITE.

KEEP PH AT 11.0 WITH CAUSTIC.

HOLD VIS. AT 50-55 SL W/ GEL.

NOTE: IF VAC DUMPS RUN WATER.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER TIM WHEELER  
 PHONE 785-4222 PHONEDN LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-20  
 REPORT No. 18  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA #1 / KOTANEELEE LOCATION Y-J-5-4B  
 OPERATOR COLUMBIA GAS DEVELO. CONTRACTOR KENTING #7  
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. PHIL BOSEM WORTH

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>87</u> mm	SURFACE	HOLE <u>52</u>	m³/STK. <u>0.118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120</u> mm	INTER. <u>171.6/3074</u>	TOTAL <u>122</u>	S.P.M. <u>40</u>	PUMP PRESS.
OTHER	OTHER	STANDBY	m³/min. <u>.473</u>	CIRC. TIME

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. GEL/CAUSTIC</u>	FLOWLINE WT. kg/m³	MUD WT. <u>1190</u> kg/m³
HOLE COND. <u>CASED</u>	UNDERFLOW WT. kg/m³	VISCOSITY <u>50-55</u> s/L
DEVIATION	OVERFLOW WT. kg/m³	FILTRATE <u>12</u> cm³/30 min.
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE m³/min.	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>03:30</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3276</u>							
FLOWLINE TEMPERATURE (°C) <u>38</u>							
DENSITY (kg/m³) <u>1190</u>							
FUNNEL VISCOSITY (s/L) <u>53</u>							
APPARENT VISCOSITY (mPa.s) <u>35</u>							
PLASTIC VISCOSITY (mPa.s) <u>28</u>							
YIELD POINT (Pa) <u>7</u>							
GELS 0/10 min. (Pa) <u>113</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>12.0</u>						
FILTER CAKE (mm) <u>2.0</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.3/2.4</u>						
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>750</u>						
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.001</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.07</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.93</u>	PREVIOUS COST	<u>22,867</u>	STARTING VOLUME			
MBT (Kg/m³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>70</u>	DAILY COST	<u>-</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)		CUM. COST	<u>22,867</u>	VOL. LOST on SURFACE			
OIL/WATER RATIO <u>1/25</u>	<u>NEG.</u>	CUM. ENG. COST	<u>7125</u>	VOL. LOST SUB SURFACE			
CaCl₂ w/w%				END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: MILLING

CONTROL DENSITY AT 1190 kg/m³ WITH BARITE.

PH AT 11.0 USING CAUSTIC.

HOLD VIS AT 50-55 s/L WHEEL.

NOTE: IF VIS. CUMBS RUN H₂O

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER  
 PHONE 785-4222 PHONE ON LOCATION MOBILE #



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-21  
 REPORT No. 19  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA of KOTANEELKE LOCATION Y-J-I-48  
 OPERATOR COLUMBIA GAS DEVELOP. CONTRACTOR KENTING H.T. #7  
 REPORT FOR Mr. Rob TADLE REPORT FOR Mr. PHIL BOLANIKATH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND. <u>70</u>	TANKS <u>70</u>	PUMP SIZE <u>14 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52</u>	m <sup>3</sup> /STK. <u>0.118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120</u> mm	INTER <u>170R/3274</u>	TOTAL <u>122</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>875.10 = 110</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>472</u>	CIRC. TIME <u>260</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>W. GEL/CAUSTIC</u>	FLOWLINE WT. kg/m <sup>3</sup>	MUD WT. <u>1190</u> kg/m <sup>3</sup>
HOLE COND.	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>50-55</u> s/L
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>12</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> DPT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>02:30</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3277</u>		<u>BARITE</u>			<u>35</u>		<u>438</u>
FLOWLINE TEMPERATURE (°C) <u>37</u>							
DENSITY (kg/m <sup>3</sup> ) <u>1190</u>							
FUNNEL VISCOSITY (s/L) <u>53</u>							
APPARENT VISCOSITY (mPa.s) <u>35</u>							
PLASTIC VISCOSITY (mPa.s) <u>28</u>							
YIELD POINT (Pa) <u>7</u>							
GELS 0/10 min. (Pa) <u>113</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>11.0</u>							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>13.0</u>							
FILTER CAKE (mm) <u>2.0</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>1.3/2.3</u>							
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CaCl <sub>2</sub> (mg/L) <u>750</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>0.01</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>0.7</u>							
WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>93</u>		PREVIOUS COST <u>22,267</u>	STARTING VOLUME				
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>70</u>		DAILY COST <u>438</u>	VOL. BUILT				
ELECTRICAL STABILITY (V) <u>-</u>		CUM. COST <u>23,305</u>	VOL. LOST ON SURFACE				
OIL/WATER RATIO <u>H<sub>2</sub>S</u> <u>NEG.</u>		CUM. ENG. COST <u>7500</u>	VOL. LOST SUB SURFACE				
CaCl <sub>2</sub> w/w%			END VOLUME				
"n"/"k"			CUM. VOL. BUILT				

COMMENTS: MILLING.

CONTROL DENSITY AT 1190 kg/m<sup>3</sup> USING BARITE.  
KEEP PH AT 11.0 WITH CAUSTIC.  
HOLD VIS. AT 50-60 SIL USING GEL.  
IF VIS. RUMBS OVER 60 SIL RUN H<sub>2</sub>O

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELEK  
 PHONE 785-4222 PHONE AT LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-22  
 REPORT No. 20  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA #1 KOTANSELEE

LOCATION V J I - 48

OPERATOR COLUMBIA GAS DEVELOPMENT

CONTRACTOR KENTING HI-TOWER #7

REPORT FOR Mr. BOB TOOLE

REPORT FOR Mr. PHIL BOSMILWORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # /	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>40</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52</u>	m <sup>3</sup> /STK. <u>0118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120</u> mm	INTER <u>178/3274</u>	TOTAL <u>122</u>	S.P.M. <u>43</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>.507</u>	CIRC. TIME <u>240</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. BLD CAUSTIC</u>	FLOWLINE WT. kg/m <sup>3</sup>	MUD WT. <u>1190</u> kg/m <sup>3</sup>
HOLE COND. <u>CRSD</u>	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>50-55</u> s/L
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>12</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5-11.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>09:30</u>	<u>3277</u>	<u>BARITE</u>			<u>70</u>		<u>875</u>
FLOWLINE TEMPERATURE (°C) <u>37</u>							
DENSITY (kg/m <sup>3</sup> ) <u>1195</u>							
FUNNEL VISCOSITY (s/L) <u>53</u>							
APPARENT VISCOSITY (mPa.s) <u>35</u>							
PLASTIC VISCOSITY (mPa.s) <u>28</u>							
YIELD POINT (Pa) <u>7</u>							
GELS 0/10 min. (Pa) <u>113</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>12.8</u>						
FILTER CAKE (mm) <u>2.0</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0/2.0</u>						
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>700</u>						
SAND CONTENT (%) <input type="checkbox"/> (1) <input checked="" type="checkbox"/> (2)	<u>.001</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (1) <input checked="" type="checkbox"/> (2)	<u>.075</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (1) <input checked="" type="checkbox"/> (2)	<u>.925</u>	PREVIOUS COST	<u>23,305</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 7% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>70</u>	DAILY COST	<u>875</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>-</u>	CUM. COST	<u>24,180</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>1.5</u>	<u>NEG.</u>	CUM. ENG. COST	<u>7075</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w%				END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: MILLING Runs. UP 100 M.M.

1) HOLD DENSITY AT 1190 Kg/m<sup>3</sup> WITH BARITE.

2) KEEP PH AT 10.5-11.0 USING CAUSTIC.

3) CONTROL VIS. AT 50-55 SL W/ GEL.

4) NOTE: IF VIS. CUMBS OVER 60 SL RUN H<sub>2</sub>O.

STOCK POINT FL. ST. JOHN

PHONE 785-4225

I.D.F. ENGINEER JIM WIELER

PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-23  
 REPORT No. 21  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA et al KOTANEEICE LOCATION YJI-48

OPERATOR COLUMBIA GAS LEVEL CONTRACTOR KENTING HI-TOWER #7

REPORT FOR Mr. BAD TOULE REPORT FOR Mr. PHIL BOSMORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND.	TANKS <u>75</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>44</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120</u> mm	INTER <u>170/3274</u>	TOTAL <u>127</u>	S.P.M. <u>45</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>.531</u>	CIRC. TIME <u>240</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. GEL CAUSTIC</u>	FLOWLINE WT.	kg/m <sup>3</sup>	MUD WT. <u>1190</u>	kg/m <sup>3</sup>	
HOLE COND. <u>OK</u>	UNDERFLOW WT.	kg/m <sup>3</sup>	VISCOSITY <u>50-55</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE <u>12</u>	cm <sup>3</sup> /30 min.	
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE	m <sup>3</sup> /min.	pH <u>10.5-11.0</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL.  PIT

MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>27:00</u>	<u>3279</u>	<u>BARITE</u>			<u>70</u>		<u>875</u>
FLOWLINE TEMPERATURE (°C)	<u>38</u>		<u>GEL</u>			<u>25</u>		<u>250</u>
DENSITY (kg/m <sup>3</sup> )	<u>1205</u>		<u>CAUSTIC</u>			<u>1</u>		<u>30</u>
FUNNEL VISCOSITY (s/L)	<u>57</u>							
APPARENT VISCOSITY (mPa.s)	<u>41</u>							
PLASTIC VISCOSITY (mPa.s)	<u>32</u>							
YIELD POINT (Pa)	<u>9</u>							
GELS 0/10 min. (Pa)	<u>2/3</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>12.0</u>							
FILTER CAKE (mm)	<u>2.0</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.1/2.2</u>							
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>650</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.000</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.08</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.92</u>		PREVIOUS COST	<u>24,180</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>75</u>		DAILY COST	<u>1155</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>-</u>		CUM. COST	<u>25,335</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>H<sub>2</sub>O</u>	<u>NEG.</u>		CUM. ENG. COST	<u>8,250</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w%					END VOLUME			
"n"/"k"					CUM. VOL. BUILT			

COMMENTS: MILLING. 80MGS. UP - 100 MIN.

1) CONTROL DENSITY AT 1190 kg/m<sup>3</sup> USING BARITE.

2) KEEP PH AT 10.5-11.0 WITH CAUSTIC.

3) HOLD VIS. AT 50-55 SL. w/REL.

4) RUN 15 LITRES H<sub>2</sub>O PER MIN. IF VIS. OVER 60 SL.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER

PHONE 785-4222 PHONE ON LOCATION MOBILE #

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# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 91-05-24  
 REPORT No. 23  
 SPUD DATE 91-04-29

WELL NAME COLUMBA 2nd KOTANJEFF

LOCATION Y.T. 1-48

OPERATOR COLUMBA GAS FIELD

CONTRACTOR YENTING - HIT #7

REPORT FOR Mr. Tom Tolle

REPORT FOR Mr. John M. Smith

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS	PUMP SIZE <u>110 x 40L</u>	OPPOSITE D.P.
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE	m <sup>3</sup> /STK. <u>0.18</u>	OPPOSITE D.C.
DRILL COLLARS <u>130 mm</u>	INTER. <u>178/177</u>	TOTAL	S.P.M.	PUMP PRESS.
OTHER	OTHER	STANDBY	m <sup>3</sup> /min.	CIRC. TIME

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. Gelcauser</u>	FLOWLINE WT. kg/m <sup>3</sup>	MUD WT. <u>1190</u> kg/m <sup>3</sup>
HOLE COND.	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>45-50</u> s/L
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>&lt; 10</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>REC.</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>14:30</u>	<u>04:30</u>	<u>KARITE</u>			<u>25</u>		<u>300</u>
FLOWLINE TEMPERATURE (°C)	<u>37</u>	<u>—</u>	<u>CEL</u>			<u>10</u>		<u>100</u>
DENSITY (kg/m <sup>3</sup> )	<u>1210</u>	<u>1010</u>						
FUNNEL VISCOSITY (s/L)	<u>60</u>	<u>42</u>						
APPARENT VISCOSITY (mPa.s)	<u>44</u>	<u>14</u>						
PLASTIC VISCOSITY (mPa.s)	<u>34</u>	<u>8</u>						
YIELD POINT (Pa)	<u>10</u>	<u>6</u>						
GELS 0/10 min. (Pa)	<u>312</u>	<u>113</u>						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.0</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>2</sup> )	<u>13.4</u>	<u>10.0</u>						
FILTER CAKE (mm)	<u>3.0</u>	<u>0.5</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0/2.1</u>	<u>55/95</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>78</u>	<u>—</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>600</u>	<u>300</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>TR.</u>	<u>—</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.85</u>	<u>—</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>2.15</u>	<u>—</u>	PREVIOUS COST	<u>235</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>45</u>	<u>—</u>	DAILY COST	<u>400</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>1</u>	<u>—</u>	CUM. COST	<u>235</u>	VOL. LOST on SURFACE			
OIL/WATER RATIO	<u>1:1</u>	<u>—</u>	CUM. ENG. COST	<u>8125</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w%	<u>—</u>	<u>—</u>			END VOLUME			
"n"/"k"					CUM. VOL. BUILT			

COMMENTS: DRILLED 153 m HOLE TO 3290 m.  
FOUND LEAK OFF TEST DIPPED TANKS TO MIX PUMPED SYSTEM.

ADD 3 L. 500 ml H<sub>2</sub>O + MIX TANK AT 15 MIN. 5x TO OBTAIN 100 ml 45-50 S/L  
ADD 3 TANKS 1000L AT 30 MIN. 1 tank.  
MIX PARTS TO RAISE DENSITY TO 1200 kg/m<sup>3</sup> 1 S/L MIN.

STOCK POINT ST. ST. JOHN D.F. ENGINEER JM [Signature]  
 PHONE 745-4222 PHONE AND LOCATION MOBILE #

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# International Drilling Fluids Corporation

## DRILLING FLUID REPORT

DATE 91-05-25  
 REPORT No. 22  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA AT KOTAKSELE LOCATION Y.T. 1-02  
 OPERATOR COLUMBIA GAS DEV. CONTRACTOR KENTON H.T. #7  
 REPORT FOR Mr. Bob Tomie REPORT FOR Mr. PHIL ROSE

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>188 / 153</u>	COND. <u>174/2074</u>	TANKS <u>50</u>	PUMP SIZE <u>114 x 436</u>	OPPOSITE D.P. <u>49</u>
DRILL PIPE <u>89 mm</u>	SURFACE <u>174/2074</u>	HOLE <u>45</u>	m³/STK. <u>0.112</u>	OPPOSITE D.C. <u>11' 0"</u>
DRILL COLLARS <u>120 mm</u>	INTER.	TOTAL <u>95</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m³/min. <u>59</u>	CIRC. TIME <u>165"</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>POLYMER</u>	FLOWLINE WT. kg/m³	MUD WT. <u>1190-1200</u> kg/m³
HOLE COND.	UNDERFLOW WT. kg/m³	VISCOSITY <u>45-50</u> s/L
DEVIATION	OVERFLOW WT. kg/m³	FILTRATE <u>410-</u> cm³/30 min.
CURRENT OP. <u>DRILL</u>	UNDERFLOW RATE m³/min.	pH <u>10-10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN	PRESENT DEPTH (m)	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
	<u>23:00</u>	<u>3300</u>	BARITE	<u>4300</u>		<u>200</u>	<u>3060</u>	<u>8750</u>
	<u>22</u>	<u>1185</u>	GEL	<u>305</u>			<u>305</u>	
	<u>40</u>	<u>16</u>	CALCIC	<u>100</u>		<u>3</u>	<u>197</u>	<u>90</u>
	<u>10</u>	<u>6</u>	BICARB	<u>5</u>			<u>55</u>	
	<u>213</u>	<u>10.0</u>	SUBST	<u>260</u>		<u>10</u>	<u>250</u>	<u>49</u>
	<u>10.0</u>	<u>05</u>	SULPH	<u>26</u>			<u>96</u>	
	<u>150</u>	<u>001</u>	SDA SH	<u>20</u>		<u>2</u>	<u>36</u>	<u>78</u>
	<u>05</u>	<u>045</u>	XGMS	<u>42</u>		<u>2</u>	<u>40</u>	<u>380</u>
	<u>150</u>	<u>001</u>	ASP. 701	<u>80</u>		<u>8</u>	<u>72</u>	<u>800</u>
	<u>05</u>	<u>001</u>	SD. S.H.	<u>30</u>			<u>30</u>	
	<u>05</u>	<u>001</u>	FLR	<u>80</u>		<u>4</u>	<u>76</u>	<u>128</u>
	<u>05</u>	<u>001</u>	IDUIS	<u>80</u>		<u>13</u>	<u>67</u>	<u>5400</u>
			PREVIOUS COST	<u>25,735</u>	STARTING VOLUME			
			DAILY COST	<u>19,235</u>	VOL. BUILT			
			CUM. COST	<u>44,370</u>	VOL. LOST ON SURFACE			
			CUM. ENG. COST	<u>2,000</u>	VOL. LOST SUB SURFACE			
					END VOLUME			
					CUM. VOL. BUILT			

COMMENTS: DRILL 152 m HOLE DISBURSED HOLE TO COLLAR SURFACE  
AT 3300 m

CONTROL VISCOSITY AT 1180 kg/m³ USING BARITE (2-3 ml/sk)  
KEEP PH AT 10-10.5 WITH CALCIC (2.5% CIR.)  
HOLD VISC. AT 40-45 s/L USING LIME D, ASP-701 + FLR.  
IF VISC. DROPS BELOW 30 s/L ADD 5 SK. IDUIS D  
ADD 2-3 BALS ASP-701 FLUXES TO HRT.  
CONTROL FLUID LOSS BELOW 10 ml WITH FLR. 4 SK/CIR.  
RUN 10-15 LINES H. RES. P.M.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER TIM WIELER  
 PHONE 785-432-744 PHONE ON LOCATED MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-26  
 REPORT No. 24  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA et al KOTANEELEE LOCATION V.T. I-48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. # 7  
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. PHIL BASMORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # 1 1/2	COND.	TANKS 64	PUMP SIZE 114 x 406	OPPOSITE D.P. 49
DRILL PIPE 89 mm	SURFACE	HOLE 46	m <sup>3</sup> /STK. .0118	OPPOSITE D.P. 75
DRILL COLLARS 120 mm	INTER 17A/3213	TOTAL 110	S.P.M.	PUMP PRESS. 10,000
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. .59	CIRC. TIME 180 ±

HOLE DATA		DESANDER/DESILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE POLYMER	FLOWLINE WT.	kg/m <sup>3</sup>	MUD WT. 1150 - 1180	kg/m <sup>3</sup>	
HOLE COND. OK	UNDERFLOW WT.	kg/m <sup>3</sup>	VISCOSITY 36 - 45	s/L	
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE 212	cm <sup>3</sup> /30 min.	
CURRENT OP. DRG.	UNDERFLOW RATE	m <sup>3</sup> /min.	pH 10-10.5		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN 14:30				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) 3330				PARITE	3868		205	3663	2562
FLOWLINE TEMPERATURE (°C) 44				GEL	305			305	
DENSITY (kg/m <sup>3</sup> ) 1190				CAUSTIC	147			187	
FUNNEL VISCOSITY (s/L) 39				DUST	250			250	
APPARENT VISCOSITY (mPa.s) 20				ASP-721	72		3	69	300
PLASTIC VISCOSITY (mPa.s) 10				XG.DF	40			40	
YIELD POINT (Pa) 10				FLR	76		4	72	
GELS 0/10 min. (Pa) 2/3				FW'S D	67		11	56	4620
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.0			SOD. SULF.	30		2	28	100
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	8.0			DEFORMER	20		2	18	213
FILTER CAKE (mm) .05				PTS-200	64		1	63	260
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	40/70								
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	TR.								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	150								
SAND CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	.002								
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.06								
OH <sup>-</sup> WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.94			PREVIOUS COST	41,370			STARTING VOLUME	
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>				DAILY COST	815			VOL. BUILT	
ELECTRICAL STABILITY (V) H <sub>2</sub> S	NEG.			CUM. COST	49,485			VOL. LOST ON SURFACE	
ASP OIL/WATER RATIO POLYMER	.75			CUM. ENG. COST	4375			VOL. LOST SUB SURFACE	
CaCl <sub>2</sub> w/w%	=							END VOLUME	
"n"/"k"	=							CUM. VOL. BUILT	

COMMENTS: DRG. 152 mm HOLE.

1) ALLOW DENSITY TO DROP BACK TO 1150 kg/m<sup>3</sup>.

2) KEEP PH AT 10-10.5 USING CAUSTIC. 2 SX. 1 CIR.

3) CONTROL VISC. AT 36-42 s/L WITH ADJUS + ASP-721. ADD 2 PAILS ASP-721 EVERY 12 HRS. WHILE DRG. ADD SLOWLY.

4) RUN 10-15 LITRES H<sub>2</sub>O PER MIN.

5) MIX 2 SX. SOD. SULFITE DAILY. ADD TO H<sub>2</sub>O IN CHEM. BDL \* TOP W/ DIESEL.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER TIM WIEBER  
 PHONE 785-4332 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91.05.27  
 REPORT No. 25  
 SPUD DATE 91.04.29

WELL NAME COLUMBIA of KOTANEELER LOCATION Y.T. I-48  
 OPERATOR COLUMBIA GAS BEVEL. CONTRACTOR KENTING H.T. #7  
 REPORT FOR Mr. Phil Trole REPORT FOR Mr. Phil Easonworth

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>152</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE <u>178/3273</u>	HOLE <u>47</u>	m³/STK. <u>.0118</u>	OPPOSITE D.C. <u>BTM. # 75 ±</u>
DRILL COLLARS <u>120 mm</u>	INTER.	TOTAL <u>117</u>	S.P.M. <u>53</u>	PUMP PRESS. <u>11,000</u>
OTHER	OTHER	STANDBY	m³/min. <u>.62</u>	CIRC. TIME <u>195</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>POLYMER</u>	FLOWLINE WT.	kg/m³	MUD WT. <u>1180</u>	kg/m³	
HOLE COND. <u>OK.</u>	UNDERFLOW WT.	kg/m³	VISCOSITY <u>35.40</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m³	FILTRATE <u>12</u>	cm³/30 min.	
CURRENT OP. <u>DRILG.</u>	UNDERFLOW RATE	m³/min.	pH <u>10.10.5</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>23:30</u>				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3354</u>				BARITE	<u>3663</u>			<u>3663</u>	
FLOWLINE TEMPERATURE (°C) <u>44</u>				CAUSTIC	<u>187</u>		<u>2</u>	<u>185</u>	<u>60</u>
DENSITY (kg/m³) <u>1190</u>				ASP 721	<u>69</u>		<u>1</u>	<u>68</u>	<u>100</u>
FUNNEL VISCOSITY (s/L) <u>37</u>				SOD. SUL.	<u>28</u>		<u>2</u>	<u>26</u>	<u>100</u>
APPARENT VISCOSITY (mPa.s) <u>20</u>									
PLASTIC VISCOSITY (mPa.s) <u>10</u>									
YIELD POINT (Pa) <u>10</u>									
GELS 0/10 min. (Pa) <u>213</u>									
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>10.5</u>									
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³) <u>8.0</u>									
FILTER CAKE (mm) <u>.05</u>									
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>.451.95</u>									
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>									
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L) <u>150</u>									
SAND CONTENT (%) <input type="checkbox"/> (20) <u>.003</u>									
SOLIDS CONTENT (%) <input type="checkbox"/> (20) <u>.07</u>									
OIL/WATER CONT. (%) <input type="checkbox"/> (20) <u>.93</u>				PREVIOUS COST	<u>49,485</u>	STARTING VOLUME			
MBT (Kg/m³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>				DAILY COST	<u>260</u>	VOL. BUILT			
ELECTRICAL STABILITY (V) <u>NEG.</u>				CUM. COST	<u>49,745</u>	VOL. LOST on SURFACE			
OIL/WATER RATIO				CUM. ENG. COST	<u>9750</u>	VOL. LOST SUB SURFACE			
CaCl₂ w/w% ASP <u>POWDER</u> <u>1.1</u>						END VOLUME			
"n"/"k"						CUM. VOL. BUILT			

COMMENTS: DRILG. 152 mm HOLE.  
CONTROL DENSITY AT 1180 kg/m³.  
KEEP PH AT 10.10.5 USING CAUSTIC. 2 SX / CIR.  
MAINTAIN VIC. AT 35-40 s/L WITH IRVINS + ASP-721. ADD 2 PAILS ASP-721 EVERY 12 HRC.  
ADD 1 SX. SOD. SULFIDE DAILY. ADD TO H₂O IN CHEM. PAIL → TO W/RESER.  
RUN 5-6 LITRES H₂O PER MIN.

STOCK POINT IT. ST. SOHN I.D.F. ENGINEER JIN WIEGER  
 PHONE 785.41222 PHONE AT LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-28  
 REPORT No. 26  
 SPUD DATE 91-04-29

WELL NAME COLUMBIA #1 KOTANELEE

LOCATION Y.T. - I - 48

OPERATOR COLUMBIA GAS DEVELOP.

CONTRACTOR KENTING H.T. #7

REPORT FOR Mr. BOB TOOLE

REPORT FOR Mr. PHIL BOSOMWORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # 152	COND.	TANKS 72	PUMP SIZE 114 x 406	OPPOSITE D.P. 51
DRILL PIPE 89 mm	SURFACE	HOLE 48	m <sup>3</sup> /STK. 0.118	OPPOSITE D.P. 80
DRILL COLLARS 120 mm	INTER 178/3273	TOTAL 120	S.P.M. 53	PUMP PRESS. 12.500
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. 63	CIRC. TIME 125

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE WT. POLYMER	FLOWLINE WT.		kg/m <sup>3</sup>	MUD WT. 1180	kg/m <sup>3</sup>
HOLE COND. OK.	UNDERFLOW WT.		kg/m <sup>3</sup>	VISCOSITY 35.40	s/L
DEVIATION	OVERFLOW WT.		kg/m <sup>3</sup>	FILTRATE 12	cm <sup>3</sup> /30 min.
CURRENT OP. DRUG.	UNDERFLOW RATE		m <sup>3</sup> /min.	pH 10-10.5	

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN 23:30				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) 3400				ASP-721	68		3	65	300
FLOWLINE TEMPERATURE (°C) 45				SOD. SULF.	26		1	25	50
DENSITY (kg/m <sup>3</sup> ) 1185				XCIDR	40		1	39	140
FUNNEL VISCOSITY (s/L) 31				PTC-200	63		2	61	320
APPARENT VISCOSITY (mPa.s) 20									
PLASTIC VISCOSITY (mPa.s) 10									
YIELD POINT (Pa) 10									
GELS 0/10 min. (Pa) 213									
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	8.0								
FILTER CAKE (mm)	.05								
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	45/1.1								
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	TR.								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	150								
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.003								
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.065								
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.935			PREVIOUS COST	47,745		STARTING VOLUME		
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>				DAILY COST	10.10		VOL. BUILT		
ELECTRICAL STABILITY (V) H <sub>2</sub> S	NEG.			CUM. COST	50,755		VOL. LOST ON SURFACE		
OIL/WATER RATIO ASP-721	1.2			CUM. ENG. COST	10,125		VOL. LOST SUB SURFACE		
CaCl <sub>2</sub> w/w% 600/300	40/30						END VOLUME		
"n"/"k"							CUM. VOL. BUILT		

COMMENTS: DRUG. 152 mm HOLE.

HOLD DENSITY IN THE 1180 kg/m<sup>3</sup> RANGE.

KEEP PH AT 10-10.5 USING CAUSTIC. 2.5x/CIR.

MAINTAIN V.S. AT 35-40 S/L WITH ID/IS + ASP-721. ADD 1-2 ASP-721 EVERY 12 HRS.

ADD 1.5x. SOD. SULFITE + 1 GAL XCIDR DAILY.

RUN 5.6 LITRES H<sub>2</sub>O PER MIN.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WHEELER  
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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# DRILLING FLUID REPORT

DATE MAY 29 91  
 REPORT No. # 27  
 SPUD DATE APR. 29 91

INTERNATIONAL DRILLING FLUIDS

WELL NAME COLUMBIA FTAL KOTANEEFEE LOCATION VT. J-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07  
 REPORT FOR Mr. POP TOLE REPORT FOR Mr. TIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE # <u>3 1/8</u>	COND.	TANKS <u>77</u>	PUMP SIZE <u>175x406</u>	OPPOSITE D.P. <u>56</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57</u>	m³/STK. <u>.0167</u>	OPPOSITE D.C. <u>98</u>
DRILL COLLARS <u>170</u> mm	INTER <u>158-222</u>	TOTAL <u>125</u>	S.P.M. <u>40</u>	PUMP PRESS <u>17,000</u>
OTHER <u>748-307</u>	OTHER	STANDBY	m³/min. <u>.668</u>	CIRC. TIME <u>190</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>1180</u> kg/m³	MUD WT. <u>1180</u> kg/m³
HOLE COND. <u>CLEAN 18m.</u>	UNDERFLOW WT <u>70</u> kg/m³	VISCOSITY <u>35-40</u> s/L
DEVIATION <u>To L.T.</u>	OVERFLOW WT.	FILTRATE <u>Flow 10</u> cm³/30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE	pH <u>10.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/> Suction		MUD PROPERTIES <u>SHAKER</u>		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2405</u>	<u>2405</u>		CARBITE	<u>2663</u>		<u>25</u>	<u>2638</u>	<u>217.50</u>
FLOWLINE TEMPERATURE (°C)	<u>24.00</u>	<u>25.00</u>		ASP-721	<u>65</u>		<u>1</u>	<u>64</u>	<u>100.00</u>
DENSITY (kg/m³)	<u>1180</u>	<u>1185</u>		X-CIDE	<u>39</u>		<u>1</u>	<u>38</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>38</u>	<u>41</u>		SULFITE	<u>35</u>		<u>1</u>	<u>24</u>	<u>49.70</u>
APPARENT VISCOSITY (mPa.s)	<u>20</u>								
PLASTIC VISCOSITY (mPa.s)	<u>10</u>								
YIELD POINT (Pa)	<u>10</u>								
GELS 0/10 min. (Pa)	<u>214</u>								
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>								
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>9.0</u>								
FILTER CAKE (mm)	<u>.05 SOFT.</u>								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.518</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>30</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>								
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.001</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.065</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.935</u>								
MBT (Kg/m³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>								
ELECTRICAL STABILITY (V) <u>H.S.</u>	<u>0</u>								
OIL/WATER RATIO <u>0.251</u>	<u>.6 KG/m³</u>								
CaCl₂ w/w % <u>SULFITES</u>	<u>190</u>								
"n"/"k" <u>Lead/Con</u>	<u>40/30</u>								
PREVIOUS COST	<u>50.755</u>								
DAILY COST	<u>203.79</u>								
CUM. COST	<u>51.257</u>								
CUM. ENG. COST	<u>10.500</u>								
STARTING VOLUME									
VOL. BUILT									
VOL. LOST ON SURFACE									
VOL. LOST SUB SURFACE									
END VOLUME									
CUM. VOL. BUILT									

COMMENTS: MAINTAIN SYSTEM AS FOLLOWS:  
1. DENSITY = 1180 KG/M³ NOT BELOW 1150 KG/M³  
2. VISCOSITY = 35-40 SEC/10. NOT BELOW 25 SEC/10 IF PEG. MIX 2 BAGS 12 OZS - 1 = 100 PPM V. BAG!  
3. PH = 10.0 L1 CAUSTIC SOLID = 2 BAGS A CIRC. WHEN REQD.  
4. SLOWLY ADD 1-2 BAGS ASP-721 EVERY 17 HRS. WHEN DRILL SHALE  
5. MIX 1 TUB X-CIDE DAILY + FLOW 2 BAGS MIX 1 Sulfite Sulfite  
6. Add WATER = 5-6 LITRES / MIN WHEN CIRCULATING!

STOCK POINT FT. ST JOHN I.D.F. ENGINEER BUCK REINHART  
 PHONE 785-4222 PHONE FAR Room 001 MOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 01A-20-1991
REPORT No. H 28
SPUD DATE 01A-29-91

WELL NAME COLONIA FT AL KOTANEE LEE

LOCATION YT T 48

OPERATOR COLONIA GAS DEVELOPMENT

CONTRACTOR KEATING H.T. CO.

REPORT FOR Mr. PAT TOOLE

REPORT FOR Mr. JIM SINGER

Table with 5 columns: ASSEMBLY, CASING, MUD Vol. (m³), PUMP OUTPUT, ANNULAR VEL. m./min. Includes rows for BIT SIZE, DRILL PIPE, DRILL COLLARS, OTHER, COND., SURFACE, INTER, OTHER, TANKS, HOLE, TOTAL, STANDBY, PUMP SIZE, m³STK., S.P.M., m³/min., OPPOSITE D.P., OPPOSITE D.C., PUMP PRESS., CIRC. TIME.

Table with 3 main sections: HOLE DATA, DESANDER/DESTILTER, DRILLING FLUID SPECIFICATIONS. Includes rows for MUD TYPE, HOLE COND., DEVIATION, CURRENT OP, FLOWLINE WT, UNDERFLOW WT, OVERFLOW WT, UNDERFLOW RATE, MUD WT., VISCOSITY, FILTRATE, pH.

EQUIPMENT: DEGASSER, DESILTER, DESANDER, CENTRIFUGE, DOUBLE DECK OR HIGH SPEED SHAKER

Table with 2 main sections: MUD PROPERTIES, MATERIALS INVENTORY & COST. Includes rows for TIME SAMPLE TAKEN, PRESENT DEPTH, FLOWLINE TEMPERATURE, DENSITY, FUNNEL VISCOSITY, APPARENT VISCOSITY, PLASTIC VISCOSITY, YIELD POINT, GELS, pH STRIP, FILTRATE, FILTER CAKE, ALK, TOTAL HARDNESS, SAL, SAND CONTENT, SOLIDS CONTENT, OIL/WATER CONT., MBT, ELECTRICAL STABILITY, OIL/WATER RATIO, CaCl2, 'n'/'k'.

COMMENTS: 1. MUD DENSITY = 1170 - 1180 KG/M³. NOT BELOW 1170 KG/M³. 2. VISCOSITY = 25-40 SEC/CL. NOT BELOW 25 SEC/CL. 3. PH = 10.0. USE PLASTIC SOLID = 2 LBS. B. (100.0). 4. SLOWLY ADD 1.0 L PAIL OF ASP. 2.0 L F.F.F. 9 HOURS. 5. MIX 1 JUG OF X-CIDE 1.0 CHEL. L.F.L. (1.0) 190 ML DAILY. 6. FEED 1 TON DAILY MIX 1.0 LBS OF SOLID SULPHATE. 7. PUMP WATER 2.0 LITRES (1.0) WHEN CIRCULATING. 8. PRIOR TO TRIPPING ISOLATE SECTION TANK. MIX 1.0 LBS OF P.T.S. 200. PUMP THIS DOWN THE HOLE AND REPLACE IT WITH 1.0 LBS OF 15 MINUTES, THEN...

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KEVIN KEINHART
PHONE 785-4557 PHONE EAR ROAD OUTMOBILE # 1.

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE MAY 31 1996  
 REPORT No. # 79  
 SPUD DATE APR. 29.91

WELL NAME COLUMBIA FT AL KOTANEELEF LOCATION YT. I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENNING # 07

REPORT FOR Mr. POP TOOLE REPORT FOR Mr.

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/8" 15.875"</u>	COND.	TANKS <u>72 m<sup>3</sup></u>	PUMP SIZE <u>1" x 4 1/2"</u>	OPPOSITE D.P. <u>57</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>52 m<sup>3</sup></u>	m <sup>3</sup> /STK. <u>.0167</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170 mm</u>	INTER <u>8.225"</u>	TOTAL <u>124 m<sup>3</sup></u>	S.P.M. <u>41</u>	PUMP PRESS. <u>14,500</u>
OTHER <u>1 1/2" 19.625"</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.6847</u>	CIRC. TIME <u>180</u>

HOLE DATA	DESANDER/DESILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>29 m<sup>3</sup></u> kg/m <sup>3</sup>	MUD WT. <u>1180</u> kg/m <sup>3</sup>
HOLE COND.	UNDERFLOW WT. <u>60 m<sup>3</sup></u> kg/m <sup>3</sup>	VISCOSITY <u>35-40</u> s/L
DEVIATION <u>VAR. OF ICE FACE</u>	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>410</u> cm <sup>3</sup> /30 min.
CURRENT OP <u>EDU. AHEAD</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u> MUD PROPERTIES		INVENTORY MATERIALS INVENTORY & COST <sup>o</sup> <u>16:00 HRS</u>					
TIME SAMPLE TAKEN	<u>10:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2470</u>	GEL	<u>465</u>		<u>255</u>	<u>210</u>	<u>3550.<sup>00</sup></u>
FLOWLINE TEMPERATURE (°C)	<u>47.0</u>	BARITE	<u>6196</u>		<u>2582</u>	<u>3612</u>	<u>32,287.<sup>50</sup></u>
DENSITY (kg/m <sup>3</sup> )	<u>1185</u>	CAUSTIC	<u>710</u>	<u>(7)</u>	<u>29</u>	<u>181</u>	<u>870.<sup>00</sup></u>
FUNNEL VISCOSITY (s/L)	<u>38</u>	SOAPASH	<u>40</u>		<u>5</u>	<u>25</u>	<u>100.<sup>00</sup></u>
APPARENT VISCOSITY (mPa.s)	<u>77</u>	SULFAN	<u>100</u>		<u>4</u>	<u>96</u>	<u>840.<sup>00</sup></u>
PLASTIC VISCOSITY (mPa.s)	<u>11</u>	EM-CARE	<u>60</u>		<u>5</u>	<u>55</u>	<u>200.<sup>00</sup></u>
YIELD POINT (Pa)	<u>11</u>	FUR-10	<u>80</u>	<u>(3)</u>	<u>7</u>	<u>73</u>	<u>1130.<sup>00</sup></u>
GELS 0/10 min. (Pa)	<u>3/4</u>	ASP-771	<u>80</u>		<u>15</u>	<u>65</u>	<u>1500.<sup>00</sup></u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10</u>	IRUS-D	<u>80</u>		<u>28</u>	<u>52</u>	<u>11,260.<sup>00</sup></u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>15</u>	PTS-200	<u>64</u>		<u>8</u>	<u>56</u>	<u>2080.<sup>00</sup></u>
FILTER CAKE (mm)	<u>.15 GOOD</u>	X-CIDE	<u>47</u>	<u>(1)</u>	<u>35</u>	<u>7</u>	<u>980.<sup>00</sup></u>
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>41.6</u>	NE-SWIT	<u>30</u>		<u>6</u>	<u>24</u>	<u>298.<sup>75</sup></u>
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>70</u>	DEF-FOAM	<u>70</u>		<u>2</u>	<u>17</u>	<u>409.<sup>50</sup></u>
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>700</u>	SAN-IND-1	<u>288</u>	<u>(12)</u>	<u>50</u>	<u>238</u>	<u>245.<sup>00</sup></u>
SAND CONTENT (%) <input checked="" type="checkbox"/> (0) <input type="checkbox"/>	<u>.001</u>	600R	<u>44</u>		<u>23</u>	<u>200R</u>	<u>28</u>
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.07</u>	100R	<u>70</u>		<u>AR-4</u>	<u>FR</u>	<u>3</u>
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.92</u>	PREVIOUS COST	<u>52,584.<sup>00</sup></u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	DAILY COST	<u>2654.<sup>00</sup></u>	VOL. BUILT <u>741.45</u>			
ELECTRICAL STABILITY (V) <u>10</u>	<u>0</u>	CUM. COST	<u>56,240.<sup>00</sup></u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO: <u>180</u>	<u>180</u>	CUM. ENG. COST	<u>11,250.<sup>00</sup></u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <u>ASP-771</u>	<u>.5 KG/L</u>			END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS:

1 MIX 4 BAGS OF FUR-10 @ 45 MILLS / BAG.

2 FUR-10 W/ CAUSTIC SOAP AS REQD.

3 Slowly Pumped 1 BAR OF ASP-771 EVERY 8 HOURS.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER ALICIA REINHART

PHONE 885-4777 PHONE FOR ROOM & MOBILE # 21

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE MAY 21 1991  
 REPORT No. # 79A  
 SPUD DATE APR 79 91

WELL NAME COLUMBIA ET AL KOTANELEE LOCATION VT. I-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING #107  
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/8" IS 2000</u>	COND.	TANKS <u>5000</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>59</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57 M</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>107</u>
DRILL COLLARS <u>120</u> mm	INTERIOR <u>377</u>	TOTAL <u>177 M</u>	S.P.M. <u>60</u>	PUMP PRESS. <u>13400</u>
OTHER <u>CHAS 196</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.708</u>	CIRC. TIME <u>175-180</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>T. POLYMER</u>	FLOWLINE WTA <u>0.00</u>	<u>39</u> kg/m <sup>3</sup>	MUD WT. <u>1180</u> kg/m <sup>3</sup>		
HOLE COND. <u>HAIR 1800 PLANT</u>	UNDERFLOW WT. <u>0.55</u>	kg/m <sup>3</sup>	VISCOSITY <u>37-40</u> s/L		
DEVIATION <u>MIX LEADS</u>	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE <u>610.0</u> cm <sup>3</sup> /30 min.		
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE	m <sup>3</sup> /min.	pH <u>10.0</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>19:30</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2425</u>			PARITE	<u>349</u>		<u>35</u>	<u>363</u>	<u>437.50</u>
FLOWLINE TEMPERATURE (°C)	<u>4300</u>			CAUSTIC	<u>184</u>		<u>7</u>	<u>187</u>	<u>60.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1180</u>			ASP 721	<u>65</u>		<u>3</u>	<u>62</u>	<u>300.00</u>
FUNNEL VISCOSITY (s/L)	<u>38</u>			SOP ASH	<u>26</u>		<u>1</u>	<u>35</u>	<u>30.00</u>
APPARENT VISCOSITY (mPa.s)	<u>77</u>			LD. VIS-D	<u>56</u>		<u>4</u>	<u>57</u>	<u>1680.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>12</u>			PTS-300	<u>58</u>		<u>7</u>	<u>56</u>	<u>570.00</u>
YIELD POINT (Pa)	<u>10</u>			X-CIDE	<u>38</u>		<u>3</u>	<u>35</u>	<u>470.00</u>
GELS 0/10 min. (Pa)	<u>2517</u>			FIB-LO	<u>77</u>		<u>3</u>	<u>69</u>	<u>480.00</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.7</u>			DISP-LO	<u>80</u>		<u>1</u>	<u>79</u>	<u>167.40</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>9.6</u>			SACRIBIT	<u>260</u>		<u>27</u>	<u>228</u>	<u>107.80</u>
FILTER CAKE (mm)	<u>.1 FAIR!</u>								
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>61.9</u>			LEADS	<u>90.00</u>				
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>70</u>			CAEPHIT	<u>80.00</u>				
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	<u>700</u>								
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.0015</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.068</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.932</u>								
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>8</u>			PREVIOUS COST	<u>57,974</u>	STARTING VOLUME			
ELECTRICAL STABILITY (V) <u>H=0</u>	<u>0</u>			DAILY COST	<u>4187.5</u>	VOL. BUILT			
OIL/WATER RATIO <u>SEP 751</u>	<u>.6</u>			CUM. COST	<u>57,012</u>	VOL. LOST on SURFACE			
CaCl <sub>2</sub> w/w% <u>SULPHITES</u>	<u>175</u>			CUM. ENG. COST	<u>11,750</u>	VOL. LOST SUB SURFACE			
"n"/"k"						END VOLUME			
						CUM. VOL. BUILT			

COMMENTS: AS SOON AS THE GLASS LEADS GET HERE! MIX 10 BAGS AT 18 MINUTES A BAG. ALSO MIX 7 BAGS OF DISPAC-LO @ 90 MIN/BAG. AND MIX 7 BAGS I.D. VIS-D @ 90 MIN/BAG. - MIX 3 PAILS OF ASP-721 @ 4 HOURS A PAIL, THEN 1 PAIL EVERY 2 HRS. - FH @ 10 W/1 BAG CAUSTIC SOLA OVER 1 CIRC. OR AS REQ'D. - MIX 1 TON X-CIDE ONCE A DAY. - MIX 1 BAG SOLUNA SULPHITE EVERY TWO DAYS. - BRICK TO THIPPING ISOLATE SECTION TANK. MIX 3 PAILS OF PTS-300 @ 5 MIN/PAIL & PUMP DOWN THE HOLE AND DISPLACE W/ MUD FOR 15 MINUTES. - WHEN MIXING PILL IN PILL TANK ADD 1/2 - 1/3 PAIL OF DEFOAMER BRICK TO MIXING TANK. - MUD DENSITY @ 1180 KG/M<sup>3</sup>. MOVE GUIDS AROUND ALL THE TIME!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KIRK REINHART  
 PHONE 785-4322 PHONE FAR ROOM MOBILE SIDE



# DRILLING FLUID REPORT

DATE JUNE 01 1991  
 REPORT No. #120  
 SPUD DATE APR - 29 - 91

INTERNATIONAL DRILLING FLUIDS

WELL NAME COLUMBIA ET AL KOTANFFIEF LOCATION VT. T-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07  
 REPORT FOR Mr. POP TOOLE REPORT FOR Mr. TIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>3.157 in</u>	COND.	TANKS <u>69.0</u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>45</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57.5</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>78</u>
DRILL COLLARS <u>170</u> mm	INTER <u>15.3333</u>	TOTAL <u>121.5</u>	S.P.M. <u>45</u>	PUMP PRESS. <u>10,000</u>
OTHER <u>THA-195</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.531</u>	CIRC. TIME <u>700</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. kg/m <sup>3</sup>	MUD WT. <u>1180-1185</u> kg/m <sup>3</sup>
HOLE COND.	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>28.40</u> s/L
DEVIATION <u>WELL W/STEAD</u>	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>110</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>TOOL</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.0</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/> SHAKER	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>19:00</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>2435</u>		GEL <u>710</u>			1	309	10.00
FLOWLINE TEMPERATURE (°C) <u>40.00</u>		CARITE <u>343</u>			25	2588	212.50
DENSITY (kg/m <sup>3</sup> ) <u>1187</u>		CAUSTIC <u>187</u>			1	181	30.00
FUNNEL VISCOSITY (s/L) <u>43</u>		ASP-721 <u>67</u>			2	59	300.00
APPARENT VISCOSITY (mPa.s) <u>29</u>		X-CIDE <u>35</u>			1	24	140.00
PLASTIC VISCOSITY (mPa.s) <u>15</u>		DRISPAK <u>79</u>			2	27	324.80
YIELD POINT (Pa) <u>14</u>		IL-GIS-D <u>57</u>			2	50	840.00
GELS 0/10 min. (Pa) <u>215</u>		EFFOAM <u>17</u>			1	16	136.50
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.3</u>	PTS-300 <u>56</u>			2	57	780.00
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>9.0</u>		PEARS			10		800.00
FILTER CAKE (mm) <u>1.600 in</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>61.9</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>70</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>750</u>							
SAND CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	<u>.001</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	<u>.073</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input type="checkbox"/>	<u>.977</u>						
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 7% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>9</u>						
ELECTRICAL STABILITY (V) <u>H.25</u>	<u>0</u>						
OIL/WATER RATIO <u>ASP-721</u>	<u>.8</u>						
CaCl <sub>2</sub> w/w% <u>SULPHITES</u>	<u>160</u>						
"n"/"k"							

COMMENTS: DENSITY = 1180-1180 KCL. HOWE HIGH GELS (EXCEPT SHAKER)  
2 BBL WATER @ 5 LITERS / MIN. FOR 1 CIRC. EVERY 17 HOURS.  
3 VISCOSITY = 28.40 SEC/11  
4 FLOW 10 LITERS CAUSTIC SOLA. OVER 1 FULL CIRC. WHEN REQ'D  
5 SLOWLY ADD 1/2 PAIL OF ASP-721 EVERY 2 HOURS.  
6 MIX 1 JUG OF X-CIDE. ONCE A DAY!  
7 MIX 1 LAG OF SOLUBLE SULPHITE EVERY TWO LAYS.  
8 PRIOR TO TRIPPING: ISOLATE SECTION TANK, MIX 2 PAILS  
OF PTS-300 @ 5 MIN. PAIL 2 PUMP FLOW IN HOLE + DISPLACE  
W/ H<sub>2</sub>O FOR 15 MINUTES.  
9 WHEN MIXING PAIL 10. PULL TANK AND V<sub>2</sub> TO 1/2 PAIL OF  
EFFOAM. PRIOR TO MIXING CARITE.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART  
 PHONE 888-4777 PHONE FAR ROCKY MOUNTAIN MOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 07 1991  
 REPORT No. # 31  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FT AL KATANELEE LOCATION Y T - I - 48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07  
 REPORT FOR Mr. POP TOOLE REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/4 - 157 mm</u>	COND.	TANKS <u>69 m<sup>3</sup></u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>57 m<sup>3</sup></u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>178.2222</u>	TOTAL <u>127 m<sup>3</sup></u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9,000</u>
OTHER <u>THA - 195</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.59</u>	CIRC. TIME <u>210</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>1195</u> kg/m <sup>3</sup>	MUD WT. <u>1180-1185</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1195</u> kg/m <sup>3</sup>	VISCOSITY <u>38-40</u> s/L	
HOLE COND.	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>210</u> cm <sup>3</sup> /30 min.			
DEVIATION	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.0</u>			

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/> SHAKER	MUD PROPERTIES			MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	2451	2454	2444	LARITE	2588		30	2558	275.00
FLOWLINE TEMPERATURE (°C)	42°C		39°C	PTS-200	52		3	50	780.00
DENSITY (kg/m <sup>3</sup> )	1195	1195	1195	SAPPHIRE	24		1	23	49.70
FUNNEL VISCOSITY (s/L)	41	41	42	OFFICER	16		1	15	126.50
APPARENT VISCOSITY (mPa.s)	26.5	26	(28)	GLASS	65		10	45	800.00
PLASTIC VISCOSITY (mPa.s)	15	15	15						
YIELD POINT (Pa)	11.5	11	13.5						
GELS 0/10 min. (Pa)	25.5	21.3	21.4						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5								
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	9.5								
FILTER CAKE (mm)	1.600								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	9/11.4								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	30								
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	250								
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	.001								
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	.075								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	.925								
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	10								
ELECTRICAL STABILITY (V) <u>H<sub>2</sub>S</u>	0								
OIL/WATER RATIO <u>pp. 731</u>	.7								
CaCl <sub>2</sub> w/w% <u>SULPHATES</u>	180								
"n"/"k"									

COMMENTS: DENSITY: 1180-1190 KG/M<sup>3</sup>. MUD MORE MUD CURED. EXCEPT SHAKER TANKS.  
 2 RING WATER - 5 LITRES/MIN FOR 1 CIRC. FOR 13 HOURS.  
 VISCOSITY: 38 TO 40 SEC/L.  
 PH = 10 (CAUSTIC SOAP OVER 1 FULL CIRC. WHEN REQD.)  
 3 SLOWLY RUN TO 1 PAIR OF ASP. 731 FOR 13 HOURS.  
 1 MIX 1 JOB OF X-LIME ONCE A DAY.  
 1 PAIR TO TRIPPING: ISOLATE SECTION, TANK, MIX 3 PAILS OF PTS-200 & 5 MIN PAIL PUMP DOWN HOLE & DISPLACE FOR 15 MINUTES.  
 2 WHEN MIXING ALL IN PAIL TANK, ADD 1/2 PAIL OF TREFORMER FROM TRIPPING LARITE.

STOCK POINT FT. ST JOHN I.D.F. ENGINEER RICK KEINHART  
 PHONE 785.4727 PHONE FAR ROOM OPPOSITE # 1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 04 1991  
 REPORT No. # 32  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FTAL KOTANEE LEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. 07

REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>5.157 (2 1/8)</u>	COND.	TANKS <u>75 M<sup>3</sup></u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>54.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>53 M<sup>3</sup></u>	m <sup>3</sup> /STK. <u>0.118</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>130</u> mm	INTER <u>178 M<sup>3</sup></u>	TOTAL <u>178 M<sup>3</sup></u>	S.P.M. <u>55</u>	PUMP PRESS. <u>8500</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>649</u>	CIRC. TIME <u>200</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>ST. POLYMER</u>	FLOWLINE WT <u>40 M<sup>3</sup></u> kg/m <sup>3</sup>	MUD WT. <u>1180-1190</u> kg/m <sup>3</sup>			
HOLE COND. <u>HARD REAMING</u>	UNDERFLOW WT <u>62</u> kg/m <sup>3</sup>	VISCOSITY <u>38-40</u> s/L			
DEVIATION <u>3417-3476 M.</u>	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>110</u> cm <sup>3</sup> /30 min.			
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.0-10.5</u>			

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>02:30</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>2459</u>			<u>TARITE</u>	<u>3558</u>		<u>30</u>	<u>3528</u>	<u>275.00</u>
FLOWLINE TEMPERATURE (°C) <u>4200</u>			<u>PTS-200</u>	<u>50</u>		<u>3</u>	<u>47</u>	<u>780.00</u>
DENSITY (kg/m <sup>3</sup> ) <u>1190</u>			<u>X-CILE</u>	<u>34</u>		<u>1</u>	<u>33</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L) <u>41</u>			<u>DEFOAM</u>	<u>15</u>		<u>1</u>	<u>14</u>	<u>136.50</u>
APPARENT VISCOSITY (mPa.s) <u>76.5</u>								
PLASTIC VISCOSITY (mPa.s) <u>15</u>								
YIELD POINT (Pa) <u>11.5</u>								
GELS 0/10 min. (Pa) <u>313</u>								
pH STRIP METER <input type="checkbox"/> <u>10.3</u>								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> ) <u>14.0</u>								
FILTER CAKE (mm) <u>.5 FAIR</u>								
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>71.9</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>20</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>250</u>								
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.001</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.077</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.978</u>								
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>11</u>								
ELECTRICAL STABILITY (V) <u>11.5 (MILL) ON STAG. OP!</u>								
OIL/WATER RATIO <u>SP. 7.31</u> <u>1.6</u>								
CaCl <sub>2</sub> w/w% <u>SULPHITES</u> <u>150</u>								
"n"/"k"								

COMMENTS: DENSITY = 1180-1190 KG/M<sup>3</sup> NOISE GAINS EXCEPT SHAKER TANK  
20 LITRES WATER = 20 LITRES MIL. UNTIL VISCOSITY IS BELOW 40  
3 VISCOSITY = 27-29 SEC/L.  
4 PM-10.5 W/ CAUSTIC SODA 1 LAG A CIRC. WHEN REC'D.  
5 Slowly Run 1st PAIR OF DESP. 1 FUR. 1 1/2 HOURS.  
1 MIX 1 JUG OF X-CILE, ONCE A DAY.  
2 PUMP TO MIXING PILL 1st PILL TANK, MIX 1/2 PAIL + CF DEFOAMER  
3 PUMP TO TRIPRING & ISOLATE LAST TWO TANKS, MIX 3 PAILS  
OF PTS-200'S MIL. 1st PAIL 1st EACH TANK, (4 PAILS TOTAL)  
PUMP POUND HOLE FOR 30 MIN. + 1st PAIL W/ MIL. FOR 10 MIN.  
AS SOON AS YOU GET LACK ON BOTTOM W/ IT #6.  
1 Run WATER = 20 MIL LITRE, MIX 2 LAGS OF LINSPEC-LO  
15 MIL. 1 LAG, MIX 1 LAG OF SOLID SULPHITE!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK BELLHART  
 PHONE 785-4372 PHONE FAR ROOM 00 MOBILE # 1

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I.D.F.C. - 015 (3)



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-05-91  
 REPORT No. # 33  
 SPUD DATE APR-79-91

WELL NAME COLOMBIA FT AL KOTANEELKE LOCATION YT-I-48

OPERATOR COLOMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07

REPORT FOR Mr. POP TOOLE REPORT FOR Mr. JILL SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>6.1520mm</u>	COND.	TANKS <u>75 m<sup>3</sup></u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>54.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>53 m<sup>3</sup></u>	m <sup>3</sup> /STK. <u>0.188</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>120</u> mm	INTERFER. <u>3270</u>	TOTAL <u>178 m<sup>3</sup></u>	S.P.M. <u>55</u>	PUMP PRESS. <u>12.500</u>
OTHER <u>THA-193</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>6.49</u>	CIRC. TIME <u>200</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WTP. <u>0.01</u> kg/m <sup>3</sup>	MUD WT. <u>1180</u>	kg/m <sup>3</sup>		
HOLE COND. <u>BY 15.8 JETS</u>	UNDERFLOW WT. <u>1.0</u> kg/m <sup>3</sup>	VISCOSITY <u>38.40</u>	s/L		
DEVIATION	OVERFLOW WTP. <u>0.01</u> kg/m <sup>3</sup>	FILTRATE <u>2.10</u>	cm <sup>3</sup> /30 min.		
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>0.28</u> (l./m.)/min.	pH <u>10-10.5</u>			

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>04:00</u>				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3468</u>				PARITE	<u>3528</u>		<u>30</u>	<u>3498</u>	<u>375.00</u>
FLOWLINE TEMPERATURE (°C)	<u>43.0</u>				FTS-200	<u>47</u>		<u>4</u>	<u>43</u>	<u>1040.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1180</u>				X-CIDE	<u>33</u>		<u>1</u>	<u>32</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>41</u>				PLASTIC	<u>181</u>		<u>1</u>	<u>180</u>	<u>30.00</u>
APPARENT VISCOSITY (mPa.s)	<u>36</u>				DEFOR.	<u>14</u>		<u>1</u>	<u>13</u>	<u>126.50</u>
PLASTIC VISCOSITY (mPa.s)	<u>15</u>									
YIELD POINT (Pa)	<u>11</u>									
GELS 0/10 min. (Pa)	<u>2/2.5</u>									
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>									
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>10.5</u>									
FILTER CAKE (mm)	<u>1.0 GOOD!</u>									
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>8/1.1</u>									
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L)	<u>30</u>									
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>350</u>									
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.001</u>									
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.068</u>									
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.932</u>									
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>									
ELECTRICAL STABILITY (V/H <sub>2</sub> S)	<u>0</u>									
OIL/WATER RATIO <u>0.721</u>	<u>5</u>									
CaCl <sub>2</sub> w/w% <u>SULPHATES</u>	<u>135</u>									
"n"/"k"										

COMMENTS: 1. FLOWLINE WTP. 0.01, MUD WT. 1180, VISCOSITY 38.40, FILTRATE 2.10, pH 10.5, YIELD POINT 11, GELS 0/10 2/2.5, SAND .001, SOLIDS .068, OIL/WATER .932, MBT 10, ELECTRICAL STABILITY 0, OIL/WATER RATIO 0.721, CaCl2 135.  
2. PREP AREA 4, CODE 22  
3. 2000-30, 2000-37, 2000-52  
4. PREVIOUS COST 4,259.1, STARTING VOLUME  
5. DAILY COST 1721.5, VOL. BUILT THA-193  
6. CUM. COST 15,980.68, VOL. LOST ON SURFACE  
7. CUM. ENG. COST 12,500.00, VOL. LOST SUB SURFACE  
8. END VOLUME  
9. CUM. VOL. BUILT

STOCK POINT FT ST JOHN I.D.F. ENGINEER KICK BEINHART  
 PHONE 785-4220 PHONE FAR ROOM MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 05 91  
 REPORT No. # 24  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FTAL KOTANEELEE LOCATION VT-I-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #307  
 REPORT FOR Mr. POPE TOOLE NEIL PLESS-JOHN A. REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/2 7/16</u>	COND.	TANKS <u>75.5</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>54.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52.5</u>	m³/STK. <u>0.188</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170</u> mm	INTER <u>17803773</u>	TOTAL <u>179 m³</u>	S.P.M. <u>55</u>	PUMP PRESS. <u>11,000</u>
OTHER <u>THA 193 m</u>	OTHER	STANDBY	m³/min. <u>649</u>	CIRC. TIME <u>300</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>ANIL. 001 @ 40.5 m³/kg/m³</u>	MUD WT. <u>1175-1180</u> kg/m³
HOLE COND. <u>(2 X 15.8 JETS)</u>	UNDERFLOW WT <u>DTA. 1.6 @ 65 m³/kg/m³</u>	VISCOSITY <u>38-40</u> s/L
DEVIATION <u>10° N @ 3474</u>	OVERFLOW WT.	FILTRATE <u>L10</u> cm³/30 min.
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

TIME SAMPLE TAKEN	MUD PROPERTIES		MATERIALS INVENTORY & COST					
			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2492</u>	<u>2481</u>	DISPAC 10	<u>27</u>		<u>7</u>	<u>70</u>	<u>1126.80</u>
FLOWLINE TEMPERATURE (°C)	<u>46°C</u>	<u>47°C</u>	SULPHITE	<u>23</u>		<u>1</u>	<u>22</u>	<u>49.70</u>
DENSITY (kg/m³)	<u>1175</u>	<u>1175</u>	ASP-771	<u>59</u>		<u>3</u>	<u>56</u>	<u>300.00</u>
FUNNEL VISCOSITY (s/L)	<u>41</u>	<u>41</u>	X-CIDE	<u>23</u>		<u>1</u>	<u>21</u>	<u>140.00</u>
APPARENT VISCOSITY (mPa.s)	<u>25</u>	<u>26</u>						
PLASTIC VISCOSITY (mPa.s)	<u>15</u>	<u>15</u>						
YIELD POINT (Pa)	<u>10</u>	<u>11</u>						
GELS 0/10 min. (Pa)	<u>312.5</u>	<u>212.5</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>10.5</u>	<u>13.0</u>						
FILTER CAKE (mm)	<u>1.0</u>	<u>1.0</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>911.2</u>	<u>8511.7</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>70</u>	<u>70</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>750</u>	<u>750</u>	PR = 2 AR = 2					
SAND CONTENT (%) <input type="checkbox"/> (O) <input checked="" type="checkbox"/>	<u>.001</u>	<u>.001</u>	3000 = 30 3000 = 35					
SOLIDS CONTENT (%) <input type="checkbox"/> (O) <input checked="" type="checkbox"/>	<u>.065</u>	<u>.065</u>	ACOL = 50					
OIL/WATER CONT. (%) <input type="checkbox"/> (O) <input checked="" type="checkbox"/>	<u>.935</u>	<u>.935</u>						
MBT (Kg/m³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	PREVIOUS COST <u>65,980.45</u>					
ELECTRICAL STABILITY (V) <u>H:5</u>	<u>0</u>	<u>0</u>	DAILY COST <u>1126.80</u>					
OIL/WATER RATIO <u>ASP-771</u>	<u>.6</u>	<u>.5</u>	CUM. COST <u>67,607.25</u>					
CaCl₂ w/w% <u>SULPHITES</u>	<u>170</u>	<u>170</u>	CUM. ENG. COST <u>13,500.00</u>					
"n"/"k"			STARTING VOLUME					
			DAILY COST					
			CUM. COST					
			CUM. ENG. COST					
			STARTING VOLUME					
			VOL. BUILT					
			VOL. LOST ON SURFACE					
			VOL. LOST SUB SURFACE					
			END VOLUME					
			CUM. VOL. BUILT					

COMMENTS: 1. DENSITY @ 1180 KG/L. HOLE MUD GIVES EXCEPT IN SHAKER TANK!  
 2. VISCOSITY @ 38-40 SEC/L FROM WATER @ 5 L/MIN. 10 MIN. EVERY 15 MIN.  
 3. PH @ 10.5 W/ PLASTIC SOLID LEAG A CIRC. WHEN REQD.  
 4. Slowly pour 1/2 1 PAIL OF ASP-771 EVERY 15 MIN.  
 5. MIX 1 JUG OF X-CIDE ONCE A DAY!  
 6. PRIOR TO MIXING FILL IN PILL TANK: MIX 1/2 PAIL + DEFORMER!  
 7. PRIOR TO TRIPPING ISOLATE LAST TWO TANKS: MIX 2 PAILS OF PTS-500 @ 5 MIN 1 PAIL IN EACH TANK. (4 PAILS TOTAL)  
 Pump Down HOLE FOR 30/MIN. AND DISPLACE W/ MUD FOR 10 MINUTES.  
 8. IF MUD DENSITY DROPS BELOW 1150. KG/L MIX 50 SXS LIME AT 4 MINUTE LEAG.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KICK REINHART  
 PHONE 785-4777 PHONE FAR ROOM 0 MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 06 1991  
 REPORT No. #35  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FTAL KOTANFELEE LOCATION VT-I-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07  
 REPORT FOR Mr. NEIL RUSS REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1.57mm</u>	COND.	TANKS <u>77.13</u>	PUMP SIZE / <u>14x406</u>	OPPOSITE D.P. <u>55</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>54m</u>	m <sup>3</sup> /STK. <u>0118</u>	OPPOSITE D.C. <u>95</u>
DRILL COLLARS <u>170</u> mm	INTER <u>15.27m</u>	TOTAL <u>131m</u>	S.P.M. <u>55</u>	PUMP PRESS. <u>12,500</u>
OTHER <u>EMD 194m</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.649</u>	CIRC. TIME <u>300</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>41m<sup>3</sup> kg/m<sup>3</sup></u>	MUD WT. <u>1175-1180</u> kg/m <sup>3</sup>
HOLE COND.	UNDERFLOW WT. <u>65m<sup>3</sup> kg/m<sup>3</sup></u>	VISCOSITY <u>38-40</u> s/L
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>L10</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>16:30</u>	<u>11:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2495</u>	<u>2494</u>	<u>DAKITE</u>	<u>2498</u>		<u>207</u>	<u>2468</u>	<u>462.50</u>
FLOWLINE TEMPERATURE (°C)	<u>45°C</u>	<u>45°C</u>	<u>ASP-721</u>	<u>56</u>		<u>1</u>	<u>55</u>	<u>100.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1180</u>	<u>1180</u>	<u>X-CHE</u>	<u>21</u>		<u>1</u>	<u>30</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>42</u>	<u>42</u>	<u>GRAHITE</u>	<u>22</u>		<u>1</u>	<u>21</u>	<u>49.70</u>
APPARENT VISCOSITY (mPa.s)	<u>27</u>	<u>26</u>	<u>PTS-200</u>	<u>42</u>		<u>4</u>	<u>29</u>	<u>1040.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>16</u>	<u>15</u>	<u>DRIFAC-10</u>	<u>70</u>		<u>4</u>	<u>65</u>	<u>649.60</u>
YIELD POINT (Pa)	<u>11</u>	<u>11</u>	<u>GRAHITE</u>	<u>-</u>		<u>2</u>	<u>-</u>	
GELS 0/10 min. (Pa)	<u>2/2.5</u>	<u>2/2</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>11.5</u>	<u>12.0</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.85/1.2</u>	<u>.85/1.2</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>30</u>	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>750</u>	<u>700</u>	<u>BR=3</u>	<u>GR=4</u>	<u>100R=21</u>			
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.002</u>	<u>.001</u>	<u>200R=31</u>	<u>300R=38</u>	<u>400R=54</u>			
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.068</u>	<u>.068</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.937</u>	<u>.932</u>	PREVIOUS COST	<u>67,607.18</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>11</u>	<u>11</u>	DAILY COST	<u>2441.80</u>	VOL. BUILT		<u>TH 2.111</u>	
ELECTRICAL STABILITY (V) <u>0</u>	<u>0</u>	<u>0</u>	CUM. COST	<u>70,048.98</u>	VOL. LOST on SURFACE		<u>1</u>	
OIL/WATER RATIO <u>.75</u>	<u>.7</u>	<u>.7</u>	CUM. ENG. COST	<u>13,875.58</u>	VOL. LOST SUB SURFACE		<u>1</u>	
CaCl <sub>2</sub> w/w% <u>150</u>	<u>170</u>	<u>170</u>			END VOLUME			
"n"/"k" TOTAL POLYMER <u>3.5 KG/100</u>					CUM. VOL. BUILT			

COMMENTS: 1 DENSITY = 1175-1180 KG/M<sup>3</sup>. MOVE MUD FROM EXCEPT 100 SHAKER TANK, IF DENSITY GOES BELOW 1170 KG/M<sup>3</sup> MIX 50 SXS OF DAKITE - 4 MINUTES A PAG.  
 2 VISCOSITY = 38-40 SEC/100ML. RUN WATER - 5 L/MIN. 1000 L EACH 12 HRS.  
 3 PH = 10.5 ON CAUSTIC SOLAG LAG A CIRC. WHEN REQ'D.  
 4 Run 1st PAIR OF ASP-721 EVERY 12 HOURS.  
 5 MIX 1 TUB OF X-CHE, ONCE A DAY.  
 6 PRIOR TO MIXING PULL 1st PAIL TANKS: MIX 1/2 PAIL DEFCAMER  
 7 PRIOR TO TRIPPING ISOLATE LAST TWO TANKS: MIX 1/2 PAIL OF PTS-200 IN EACH TANK - 5 MIN PAIL. (4 PAILS TOTAL)  
 PUMP DOWN HOLE FOR 20 MIN. PAIL. REPLACE WITH HOLE FOR 10 MINUTES.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART  
 PHONE 785-4777 PHONE FAR ROOM 0 MOBILE 41

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 07 91  
 REPORT No. # 36  
 SPUD DATE APR 29 91

WELL NAME COLUMPIA FTAL KOTANEE LEE LOCATION VT. J-48  
 OPERATOR COLUMPIA GAS DEVELOPMENT CONTRACTOR KENTING H. T. #07  
 REPORT FOR Mr. NEIL RUSS REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>7.15" bit</u>	COND.	TANKS <u>77 m<sup>3</sup></u>	PUMP SIZE <u>20x40</u>	OPPOSITE D.P. <u>56</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>54 m<sup>3</sup></u>	m <sup>3</sup> /STK. <u>.0167</u>	OPPOSITE D.C. <u>98</u>
DRILL COLLARS <u>120</u> mm	INTER <u>58-3353</u>	TOTAL <u>131 m<sup>3</sup></u>	S.P.M. <u>40</u>	PUMP PRESS. <u>11,500</u>
OTHER <u>THE 194 m</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.648</u>	CIRC. TIME <u>700</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>1175-1180</u> kg/m <sup>3</sup>	MUD WT. <u>1175-1180</u> kg/m <sup>3</sup>
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>17.0</u> kg/m <sup>3</sup>	VISCOSITY <u>28-40</u> s/L
DEVIATION	OVERFLOW WT. <u>BOTTOM OF HOLE</u> kg/m <sup>3</sup>	FILTRATE <u>10-12</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>215</u> m <sup>3</sup> /min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>23:30</u>	<u>19:00</u>	<u>11:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3524</u>	<u>3510</u>	<u>3497</u>	X-CIDE	<u>30</u>		<u>1</u>	<u>29</u>	<u>140.00</u>
FLOWLINE TEMPERATURE (°C)	<u>43.0</u>	<u>43.0</u>	<u>41.0</u>	SULPHITE	<u>21</u>		<u>1</u>	<u>20</u>	<u>49.70</u>
DENSITY (kg/m <sup>3</sup> )	<u>1175</u>	<u>1180</u>	<u>1180</u>	DEFL	<u>30</u>		<u>12</u>	<u>18</u>	<u>2126.00</u>
FUNNEL VISCOSITY (s/L)	<u>43</u>	<u>43</u>	<u>45</u>	INDUSPAC-10	<u>66</u>		<u>3</u>	<u>63</u>	<u>487.20</u>
APPARENT VISCOSITY (mPa.s)	<u>29</u>	<u>29.5</u>	<u>32.5</u>	GLASS					
PLASTIC VISCOSITY (mPa.s)	<u>18</u>	<u>18</u>	<u>20</u>	DEALS	<u>45</u>		<u>5</u>	<u>40</u>	<u>400.00</u>
YIELD POINT (Pa)	<u>11</u>	<u>11.5</u>	<u>12.5</u>						
GELS 0/10 min. (Pa)	<u>2/2</u>	<u>2/2</u>	<u>2.5/2</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>12.0</u>	<u>12</u>	<u>15.5</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.5</u>	<u>1.5</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>85/1.2</u>	<u>1.0/1.4</u>	<u>.9/1.4</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>20</u>	<u>20</u>	<u>20</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>250</u>	<u>250</u>	<u>250</u>	3R=3	6R=4	10OR=22			
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.0015</u>	<u>.003</u>	<u>.002</u>	20OR=32	30OR=40	60OR=58			
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.066</u>	<u>.068</u>	<u>.068</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.924</u>	<u>.922</u>	<u>.922</u>	PREVIOUS COST <u>70,048.7</u>	STARTING VOLUME				
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	<u>10</u>	DAILY COST <u>2212.90</u>	VOL. BUILT <u>THAN 115</u>				
ELECTRICAL STABILITY (V) <input checked="" type="checkbox"/>	<u>0</u>	<u>0</u>	<u>0</u>	CUM. COST <u>73,261.60</u>	VOL. LOST ON SURFACE <u>1</u>				
OIL/WATER RATIO <input checked="" type="checkbox"/> (2) <input type="checkbox"/>	<u>.8</u>	<u>.8</u>	<u>.8</u>	CUM. ENG. COST <u>14,750</u>	VOL. LOST SUB SURFACE <u>1</u>				
CaCl <sub>2</sub> w/w % <input checked="" type="checkbox"/>	<u>150</u>	<u>150</u>	<u>160</u>		END VOLUME				
"n" <input checked="" type="checkbox"/> TOTAL FLOWER	<u>3.0</u>	<u>3.0</u>	<u>3.0</u>		CUM. VOL. BUILT				

COMMENTS: LE-SIT-1175-1180 KCL MUD. MUD GOOD. EXCEPT 10  
SHAKER TANK. IF DENSITY GOES UP TO 1150 KCL, 1.14 X 50 SX  
WHITE AT 4 MINUTES A TAG,  
3 LITERS OF 28-40 SEC. 100 WATER 5 LITERS LIME,  
PH 10.5 W/ CAUSTIC SOLID 91 TAG A CIRC. WHEN REQ'D.  
4 STAP ADDITION OF ASP. 23L  
5 MIX 1 JOB X-CIDE AND 1 TAG NA+ SULPHITE ONCE A DAY  
6 PRIOR TO MIXING PULL 1 PAIL TANK. MIX 1/2 PAIL DEFLAMER!  
7 PAIL TO TRIPPING 2 LITERS LAST TWO TANKS. MIX 2 PAILS  
OF FTS-200 10 EACH TANK 5 MIN 1 PAIL. PUMP DOWN HOLE  
FOR 40 MINUTES. ALL THE PUMP FILLS

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART  
 PHONE 785-4722 PHONE FAR ROOM MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 08 1991  
 REPORT No. # 37  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FT AL KUTANEELEE LOCATION VT - I - 48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07  
 REPORT FOR Mr. NEIL FLISS REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>7.157 mm</u>	COND.	TANKS <u>85.17</u>	PUMP SIZE <u>175x406</u>	OPPOSITE D.P. <u>50.5</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>55 mm</u>	m <sup>3</sup> /STK. <u>.0167</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>8.7373</u>	TOTAL <u>140 m</u>	S.P.M. <u>26</u>	PUMP PRESS. <u>12,000</u>
OTHER <u>PHB 194 m</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.6013</u>	CIRC. TIME <u>730</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE: <u>ST. POLYMER</u>	FLOWLINE WT. <u>106.45 m<sup>3</sup></u>	kg/m <sup>3</sup>	MUD WT. <u>1175-1180</u>	kg/m <sup>3</sup>	
HOLE COND.	UNDERFLOW WT. <u>7.1 m<sup>3</sup></u>	kg/m <sup>3</sup>	VISCOSITY <u>40 SEC/10</u>	s/L	
DEVIATION <u>10 1/4°</u>	OVERFLOW WT. <u>ETAL. HOLE TEMP</u>	kg/m <sup>3</sup>	FILTRATE <u>10-12</u>	cm <sup>3</sup> /30 min.	
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>215 CF</u>	m <sup>3</sup> /min.	pH <u>10.5</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>11:00</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3544</u>			<u>EMERITE</u>	<u>2461</u>		<u>35</u>	<u>2426</u>	<u>437.50</u>
FLOWLINE TEMPERATURE (°C)	<u>42°C</u>			<u>X-CIDE</u>	<u>29</u>		<u>1</u>	<u>28</u>	<u>140.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1175</u>			<u>DEFORM</u>	<u>12</u>		<u>1</u>	<u>12</u>	<u>136.50</u>
FUNNEL VISCOSITY (s/L)	<u>47</u>			<u>SUBHITE</u>	<u>20</u>		<u>1</u>	<u>19</u>	<u>49.50</u>
APPARENT VISCOSITY (mPa.s)	<u>27</u>			<u>FTS-200</u>	<u>29</u>		<u>4</u>	<u>35</u>	<u>1040.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>17</u>								
YIELD POINT (Pa)	<u>10</u>								
GELS 0/10 min. (Pa)	<u>2/2.5</u>								
pH STRIP 2" METER <input type="checkbox"/>	<u>10.5</u>								
FILTRATE 2 API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>12.5</u>								
FILTER CAKE (mm)	<u>.5 TIGHT!</u>								
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.85/1.1</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>30</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>250</u>								
SAND CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	<u>.001</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	<u>.066</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input type="checkbox"/>	<u>.924</u>								
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>								
ELECTRICAL STABILITY (V) <input type="checkbox"/>	<u>0</u>								
OIL/WATER RATIO ASP. <u>221</u>	<u>.7</u>								
CaCl <sub>2</sub> w/w% <u>SUBPHITES</u>	<u>130</u>								
"n" <u>STAL POLYMER</u>	<u>3.5 KG/L</u>								

COMMENTS:

A: SOON AS YOU GET BACK AND PATTEN W/ BIT #8!  
1 RUN WATER @ 70 LITRES/MIN. FOR 1 CIRCULATION. THEN  
SLOW THE WATER DOWN TO 5 LITRES/MINUTE.  
2 MIX 1 BAG OF X-CIDE AND THEN 1 BAG OF SODIUM SULPHITE.  
3 AFTER 1 FULL CIRCULATION MIX 3 BAGS OF DRISPAK  
LOW AT 70 MINUTES A BAG!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICKE REINHART  
 PHONE 785-4722 PHONE FAR ROOM OUNBLE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 09 1991  
 REPORT No. # 28  
 SPUD DATE APR - 29 91

WELL NAME <u>COLOMPIA FTAL KOTANEELEE</u>		LOCATION <u>VT-I-48</u>						
OPERATOR <u>COLOMPIA GAS DEVELOPMENT</u>		CONTRACTOR <u>KENTING H.T. #07</u>						
REPORT FOR Mr. <u>NEIL PLISS</u>		REPORT FOR Mr. <u>JIM SIGNED</u>						
ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.				
BIT SIZE <u>8.125</u>	COND.	TANKS <u>80</u>	PUMP SIZE <u>177x406</u>	OPPOSITE D.P. <u>60</u>				
DRILL PIPE <u>59</u> mm	SURFACE	HOLE <u>55</u>	m <sup>3</sup> /STK. <u>0.167</u>	OPPOSITE D.C. <u>105</u>				
DRILL COLLARS <u>130</u> mm	INTER <u>178.0000</u>	TOTAL <u>135</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>10,000</u>				
OTHER <u>SHA</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>0.7181</u>	CIRC. TIME <u>190</u>				
HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS				
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>45</u> kg/m <sup>3</sup>	MUD WT. <u>1190</u> kg/m <sup>3</sup>	VISCOSITY <u>40</u> SEC/11 s/L					
HOLE COND.	UNDERFLOW WT <u>65</u> kg/m <sup>3</sup>	OVERFLOW WT <u>11</u> kg/m <sup>3</sup>		FILTRATE <u>10-12</u> cm <sup>3</sup> /30 min.				
DEVIATION	UNDERFLOW RATE <u>2150</u> m <sup>3</sup> /min.	pH <u>10.5</u>						
CURRENT OP <u>FILLING</u>								
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER								
SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	70:00	15:00	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	3559	3557	BARITE	2471		100	2371	1750.00
FLOWLINE TEMPERATURE (°C)	44.0	47.0	SULPHITE	19		1	18	49.70
DENSITY (kg/m <sup>3</sup> )	1180	1170	DFCL	18		6	17	1068.00
FUNNEL VISCOSITY (s/L)	43	45	DRISPAC	12		7	60	487.70
APPARENT VISCOSITY (mPa.s)	28	30						
PLASTIC VISCOSITY (mPa.s)	18	19						
YIELD POINT (Pa)	10	11						
GELS 0/10 min. (Pa)	212.5	212						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.7	11.0						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	15	12.0						
FILTER CAKE (mm)	1.0 Firm.	1.0						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	11/1.4	1.2/2.1						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	30	30						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	250	300	DR = 3	LR = 4	100 DR = 20			
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	.001	.001	200 DR = 30	200 DR = 28	600 DR = 56			
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	.07	.065						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	.92	.925	PREVIOUS COST	25,065	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % OIL RET <input type="checkbox"/>	10	11	DAILY COST	2854.9	VOL BUILT			
ELECTRICAL STABILITY (V/M)	0	0	CUM. COST	27,930	LOST on SURFACE			
OIL/WATER RATIO (KOH)	.7	.7	CUM. ENG. COST	15,000	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <u>CLIFONES</u>	170	175			END VOLUME			
"n"/"k" <u>TAL KOTANEELEE</u>	4	4			CUM. VOL. BUILT			
COMMENTS: DENSITY = 1190 KG/M <sup>3</sup> MORE HOLE CUMS EXCEPT 10 SHAKER TANK. IF DENSITY 60% BELOW 1185 KG/M <sup>3</sup> , MIX 50.5% BARITE AT 4 MINUTES A BAG! - VISCOSITY = 40 SEC/11, ADD WATER = 5 LITRES 1 MIN. - PH = 10.5 DO NOT ADD ANY MORE CAUSTIC FOR NOW! - 4 STB ADDITIONS OF DR-300 AND DRISPAC 10. - 2 STB ADDITIONS OF HTS-300 FOR NOW! - MIX 1 JOG OF X-CIDE A DAY - ALSO ALL 1 JOG OF X-CIDE THROUGH TRIPPING! - ADD TO MIXING FILLING FILL TANK, MIX 1/2 BAG OF DEFAMER!								
STOCK POINT <u>FT. ST JOHN</u>			I.D.F. ENGINEER					
PHONE <u>888.4777</u>			PHONE			MOBILE #		

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-10-1991  
 REPORT No. # 39  
 SPUD DATE APR-29-91

WELL NAME COLUMBIA ET AL KOTANEELEE LOCATION VT-1-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07

REPORT FOR Mr. NEIL PLISS REPORT FOR Mr. TILL SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>8.157 in</u>	COND.	TANKS <u>85.1</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>55.5</u>	m <sup>3</sup> /STK. <u>0.119</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>130</u> mm	INTER <u>78-3375</u>	TOTAL <u>140.5</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>7500</u>
OTHER <u>HA-196, 1.</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.59</u>	CIRC. TIME <u>330</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>ST. POLYMER</u>	FLOWLINE WT <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>
HOLE COND.	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>
DEVIATION <u>7/4° 3561</u>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE <u>275°F-1070°</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>275°F-1070°</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>275°F-1070°</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>275°F-1070°</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>275°F-1070°</u> m <sup>3</sup> /min.

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES				MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>16:00</u>	<u>09:30</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST		
PRESENT DEPTH (m)	<u>3587</u>	<u>3580</u>	<u>PARITE</u>	<u>3226</u>		<u>85</u>	<u>3741</u>	<u>1067.50</u>		
FLOWLINE TEMPERATURE (°C)	<u>4500</u>	<u>4400</u>	<u>DFLC</u>	<u>17</u>		<u>7</u>	<u>5</u>	<u>1746.00</u>		
DENSITY (kg/m <sup>3</sup> )	<u>1195</u>	<u>1190</u>	<u>X-CIDE</u>	<u>28</u>		<u>1</u>	<u>27</u>	<u>140.00</u>		
FUNNEL VISCOSITY (s/L)	<u>47</u>	<u>47</u>	<u>DISPAC 10</u>	<u>60</u>		<u>2</u>	<u>57</u>	<u>487.20</u>		
APPARENT VISCOSITY (mPa.s)	<u>77</u>	<u>26</u>								
PLASTIC VISCOSITY (mPa.s)	<u>18</u>	<u>17</u>								
YIELD POINT (Pa)	<u>9</u>	<u>9</u>								
GELS 0/10 min. (Pa)	<u>1.512</u>	<u>1.512</u>								
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.7</u>	<u>10.7</u>								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>15.5</u>	<u>16</u>								
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.0</u>								
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0/1.2</u>	<u>1.0/1.2</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>	<u>30</u>								
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>	<u>300</u>	<u>PR=2</u>	<u>LR=2</u>	<u>1000R=19</u>					
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.0015</u>	<u>.0015</u>	<u>700R=28</u>	<u>300R=26</u>	<u>1000R=54</u>					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.078</u>	<u>.075</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.972</u>	<u>.975</u>	PREVIOUS COST	<u>77.920</u>	STARTING VOLUME					
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST	<u>7925.2</u>	VOL. BUILT	<u>1 HAWK</u>				
ELECTRICAL STABILITY (V) <u>H7S</u>	<u>0</u>	<u>0</u>	CUM. COST	<u>80.856</u>	VOL. LOST ON SURFACE	<u>7</u>				
OIL/WATER RATIO <u>P.S.P. 771</u>	<u>.7</u>	<u>.7</u>	CUM. ENG. COST	<u>15.375</u>	VOL. LOST SUB SURFACE	<u>1</u>				
CaCl <sub>2</sub> w/w% <u>SUBPHITES</u>	<u>150</u>	<u>150</u>			END VOLUME	<u>1</u>				
"n"/"k" TOTAL POLYMER	<u>4.0 KG/L</u>	<u>4.0</u>			CUM. VOL. BUILT	<u>1</u>				

COMMENTS: MUD DENSITY = 1190-1195 KG/M<sup>3</sup>: IF DENSITY GOES BELOW 1185 KG/M<sup>3</sup> MIX 50 SXS PARITE @ 4 MIN. / BAG. & RAISE DENSITY TO 1220 KG/M<sup>3</sup> PUMP TO 2650 M. CHECK W/ FING. VISCOSITY @ 40-42 SEC/1 LITRE WATER @ 5 LITRE / MIN. PH @ 10.5. DO NOT ADD CAUSTIC FOR NOW! STOP ADDITION OF ASP. 771! ONCE A DAY MIX 1 JUG OF X-CIDE: ALSO 1X-CIDE POUCH TO TRIP! & CONTIN. FILL 10 SXS @ 15-17 CM @ 0.13 DISPAC-10 @ 75 MIN / BAG! PUMP TO MIXING PILLING PILL TANK. MIX 1/2 PAIL DEFOAMER. PUMP TO TRIP: IF YOU ARE GOING TO PRESSURE TEST! MIX 4 PAILS OF PTS-200. ISOLATE LAST TWO TANKS. MIX 2 PAILS W/ EACH TANK! PUMP FOR 40 MINUTES. THEN PUMP PILL!

STOCK POINT ET. ST. JOHN I.D.F. ENGINEER RICK KENNEDY  
 PHONE 785-4772 PHONE FOR ROOM MOBILE LINE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 11 1991  
 REPORT No. # 40  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA ET AL KOTANEE LEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07

REPORT FOR Mr. \_\_\_\_\_ REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>9.157 IN</u>	COND.	TANKS <u>85.1</u>	PUMP SIZE <u>114x400</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>56.1</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120</u> mm	INTER <u>158-250</u>	TOTAL <u>141.1</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9500</u>
OTHER <u>THA 196.1</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.59</u>	CIRC. TIME <u>230</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>T. POLYMER</u>	FLOWLINE WT <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1195</u> kg/m <sup>3</sup>
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	UNDERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>
DEVIATION <u>JETS 3X10.3</u>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>	OVERFLOW WT <u>1190-1195</u> kg/m <sup>3</sup>
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>1190-1195</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>1190-1195</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>1190-1195</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>1190-1195</u> m <sup>3</sup> /min.	UNDERFLOW RATE <u>1190-1195</u> m <sup>3</sup> /min.

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>21:00</u>	<u>09:30</u>						
FLOWLINE TEMPERATURE (°C)	<u>36.09</u>	<u>35.98</u>	SULPHITE	<u>18</u>		<u>1</u>	<u>17</u>	<u>49.70</u>
DENSITY (kg/m <sup>3</sup> )	<u>44.00</u>	<u>40.00</u>	X-CIDE	<u>27</u>		<u>1</u>	<u>26</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>1190</u>	<u>1195</u>						
APPARENT VISCOSITY (mPa.s)	<u>42</u>	<u>44</u>						
PLASTIC VISCOSITY (mPa.s)	<u>74.5</u>	<u>78</u>						
YIELD POINT (Pa)	<u>17</u>	<u>19</u>						
GELS 0/10 min. (Pa)	<u>7.5</u>	<u>9</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>1.512</u>	<u>1.512</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>10.5</u>	<u>10.5</u>						
FILTER CAKE (mm)	<u>16.5</u>	<u>15.7</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0 TIGHT</u>	<u>.5</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>911.3</u>	<u>911.3</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>50</u>	<u>60</u>						
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>300</u>	<u>300</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.007</u>	<u>.0015</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.075 (TRACE)</u>	<u>.075</u>						
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>.925 (OIL)</u>	<u>.925</u>	PREVIOUS COST	<u>80.856</u>		STARTING VOLUME		
ELECTRICAL STABILITY (M) H <sub>2</sub> S	<u>11</u>	<u>10</u>	DAILY COST	<u>189.70</u>		VOL. BUILT	<u>TRAIL 115</u>	
OIL/WATER RATIO ASP. 721	<u>0</u>	<u>0</u>	CUM. COST	<u>81.045</u>		LOST ON SURFACE	<u>1</u>	
CaCl <sub>2</sub> w/w% <u>5.17</u>	<u>.6</u>	<u>.6</u>	CUM. ENG COST	<u>15.250</u>		LOST SUB SURFACE	<u>1</u>	
"n"/"K" RTAI <u>130</u>	<u>130</u>	<u>130</u>				END VOLUME		
"n"/"K" RTAI <u>4.0</u>	<u>4.0</u>	<u>4.0</u>				CUM. VOL. BUILT		

COMMENTS: 1) MUD DENSITY 1190-1195 KG/M<sup>3</sup> IF DENSITY GOES BELOW 1185 KG/M<sup>3</sup> MIX 50 SXS BARITE @ 4 MIN/1 BAG.  
 2) VISCOSITY 42-45 SEC/CL. KUD WATER 5 LITRES/1 MIN.  
 3) PH 10.5: DO NOT ADD PLASTIC FOR NOW!  
 4) STOP ALL TITRATIONS OF ASP-721  
 5) MIX 1 JUG OF X-CIDE CONC. A DAY!  
 6) CONTINUED FLUID LOSS 15-17 CM. W/3 DRISFAC-LO OVER 1 CIRC.  
 7) PRIOR TO MIXING FILL IN PILL TANKS MIX 1/2 PAIL DEFORMER.  
 8) PRIOR TO TRIP: IF YOU ARE GOING TO PRESSURE TEST, MIX 4 PAILS OF PTE-200 + 1 JUG X-CIDE ISOLATE LAST TWO TANKS, MIX 2 PAILS PTE 200 IN EACH TANK, MIX 1/2 JUG X-CIDE IN EACH TANK, PUMP FOR 40 MIN, THEN PUMP PILL!  
 STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KIKI KENNHART  
 PHONE 785-4222 PHONE FAR ROOM ABOVE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 17 1991  
 REPORT No. # 41  
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FT AL KUTANEE LEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTINE H.T. #7

REPORT FOR Mr. PORTER NEIL BLISS REPORT FOR Mr. PHIL ROSEBROUGH

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m³/min.
BIT SIZE / # <u>9.157 IN</u>	COND.	TANKS <u>84.17</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>56.17</u>	m³/STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>170</u> mm	INTER <u>178-277</u>	TOTAL <u>140.17</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9.000</u>
OTHER <u>PMA-196 M</u>	OTHER	STANDBY	m³/min. <u>.59</u>	CIRC. TIME <u>730</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>WT. 46.17</u> kg/m³	MUD WT. <u>1190-1195</u> kg/m³
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>PT. 1.00</u> 80 MIN kg/m³	VISCOSITY <u>45 SEC 10</u> s/L
DEVIATION <u>8° @ 2610 M</u>	OVERFLOW WT <u>EST. CH. TEMP</u> kg/m³	FILTRATE <u>15-17</u> cm³/30 min.
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE <u>275°F</u> m³/min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>14:00</u> <u>2630</u>	<u>08:00</u> <u>2673</u>	<u>PARITE</u>	<u>3741</u>		<u>90</u>	<u>351</u>	<u>1125.00</u>
FLOWLINE TEMPERATURE (°C)	<u>42°</u>	<u>41°</u>	<u>DRISPAK</u>	<u>57</u>		<u>8</u>	<u>49</u>	<u>1299.20</u>
DENSITY (kg/m³)	<u>1195</u>	<u>1185</u>	<u>FT-700</u>	<u>35</u>		<u>4</u>	<u>31</u>	<u>1040.00</u>
FUNNEL VISCOSITY (s/L)	<u>44</u>	<u>43</u>	<u>X-CIDE</u>	<u>26</u>		<u>2</u>	<u>74</u>	<u>780.00</u>
APPARENT VISCOSITY (mPa.s)	<u>27.5</u>	<u>26</u>						
PLASTIC VISCOSITY (mPa.s)	<u>19</u>	<u>18</u>						
YIELD POINT (Pa)	<u>8.5</u>	<u>8</u>						
GELS 0/10 min. (Pa)	<u>1.5/2</u>	<u>1.5/2</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.</u>	<u>10.2</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>15.8</u>	<u>16.0</u>						
FILTER CAKE (mm)	<u>.5</u>	<u>.8</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.85/1.2</u>	<u>.8/1.3</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L)	<u>80</u>	<u>80</u>						
SAL. <input type="checkbox"/> NACL <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	<u>300</u>	<u>300</u>	<u>BR-1</u>	<u>AR-2</u>	<u>100R-17</u>			
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.007</u>	<u>.007</u>	<u>200R-27</u>	<u>300R-26</u>	<u>100R-55</u>			
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.08</u>	<u>.072</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.92</u>	<u>.927</u>	PREVIOUS COST	<u>81,045.89</u>	STARTING VOLUME			
MBT (Kg/m³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST	<u>3744.30</u>	VOL. BUILT	<u>7 HANKS</u>		
ELECTRICAL STABILITY (V) <u>MS</u>	<u>0</u>	<u>0</u>	CUM. COST	<u>84,790.19</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>CP-251</u>	<u>.6</u>	<u>.6</u>	CUM. ENG. COST	<u>16,125.00</u>	VOL. LOST SUB SURFACE			
CaCl₂ w/w% <u>SULPHITES</u>	<u>100</u>	<u>100</u>			END VOLUME			
"n"/"k" <u>TOTAL POLYMER</u>	<u>4.2</u>	<u>4.2</u>			CUM. VOL. BUILT			

COMMENTS:

AS SOON AS YOU GET BACK ON BOTTOM W/ BIT #10  
1 RWD WATER @ 10 LITRES/MINUTE FOR 1 CIRCULATION?  
2 RWD 100 L BAG OF SODIUM SULPHITE OVER 1 CIRCULATION?

STOCK POINT FT. ST. JOHN  
 PHONE 785-4222

I.D.F. ENGINEER ARIC REINHART  
 PHONE FAR ROOM OUBSIDE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 12, 1991

REPORT No. # 47

SPUD DATE FEB. 29, 91

WELL NAME COLEAS FT. ALKATENE FLEFF LOCATION VT-1-48

OPERATOR COLEAS GAS DEVELOPMENT CONTRACTOR KENTING H.T. #7

REPORT FOR Mr. BOB TOOLE - NEW PLISS REPORT FOR Mr. PAUL ESCOFFIER

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>10-15/16</u>	COND.	TANKS <u>70 m<sup>3</sup></u>	PUMP SIZE <u>114 X 406</u>	OPPOSITE D.P. <u>535</u>
DRILL PIPE <u>99</u> mm	SURFACE	HOLE <u>56 m<sup>3</sup></u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>93</u>
DRILL COLLARS <u>120</u> mm	INTER <u>50-277</u>	TOTAL <u>126 m<sup>3</sup></u>	S.P.M. <u>54</u>	PUMP PRESS. <u>11,000</u>
OTHER <u>THA - 200 m<sup>3</sup></u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>6.277</u>	CIRC. TIME <u>200</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>W.T. Polymer</u>	FLOWLINE WT. <u>46 m<sup>3</sup></u> kg/m <sup>3</sup>	MUD WT. <u>1195-1200</u> kg/m <sup>3</sup>	HOLE COND <u>CCCC</u>	UNDERFLOW WT. <u>70 m<sup>3</sup></u> kg/m <sup>3</sup>	VISCOSITY <u>45 SECIL</u> s/L
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE <u>15.17</u> cm <sup>3</sup> /30 min.	CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE
		m <sup>3</sup> /min.	pH <u>10.5</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
<input checked="" type="checkbox"/>	<u>JUNE 14 05:00</u>	<u>19:30</u>						
PRESENT DEPTH (m)	<u>3654</u>	<u>3636</u>	F.L.R.	<u>79</u>		<u>4</u>	<u>75</u>	<u>640.00</u>
FLOWLINE TEMPERATURE (°C)	<u>41°C</u>	<u>38°C</u>	W.L.W.C.	<u>50</u>		<u>3</u>	<u>47</u>	<u>1760.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1305</u>	<u>1300</u>	SULPHITE	<u>17</u>		<u>1</u>	<u>16</u>	<u>49.70</u>
FUNNEL VISCOSITY (s/L)	<u>43</u>	<u>45</u>	WASH	<u>25</u>		<u>1</u>	<u>24</u>	<u>20.00</u>
APPARENT VISCOSITY (mPa.s)	<u>27.5</u>	<u>30</u>						
PLASTIC VISCOSITY (mPa.s)	<u>20</u>	<u>21</u>						
YIELD POINT (Pa)	<u>7.5</u>	<u>9</u>						
GELS 0/10 min. (Pa)	<u>1.5/2</u>	<u>1.5/2</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>17</u>	<u>20</u>						
FILTER CAKE (mm)	<u>1.7</u>	<u>1.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.2/1.7</u>	<u>1.0/1.2</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>90</u>	<u>100</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>	<u>300</u>						
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.002</u>	<u>.003</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.085</u> (oil)	<u>.083</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.915</u> (water)	<u>.917</u>	PREVIOUS COST	<u>84,790.</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST	<u>1969.70</u>	VOL. BUILT	<u>THANKS</u>		
ELECTRICAL STABILITY (V) <input checked="" type="checkbox"/> (5 HGH) <input type="checkbox"/> (10 FT) <input type="checkbox"/> (0 FT)	<u>1.4</u> (KGL)	<u>1.35</u>	CUM. COST	<u>86,759.70</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO	<u>1.4</u> (KGL)	<u>1.35</u>	CUM. ENG. COST	<u>16,500.</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <input checked="" type="checkbox"/> (PHITE)	<u>1.35</u>	<u>1.35</u>			END VOLUME			
"n"/"k" TOTAL POLYMER	<u>4.8</u>	<u>4.5</u>			CUM. VOL. BUILT			

COMMENTS: 1) DENSITY 1190-1195 KGL/M<sup>3</sup> - KEEP MONITORING MUD GUNTS!  
IF DENSITY COEF. BELOW 1190 KGL/M<sup>3</sup> MIX 50 GALS OF 4 MINUTE LAG!  
2) VISCOSITY 45 SECIL PLUS WATER - 5 LITRES/MIN. WHEN CIRC.  
3) MIX 1 TON OF X-CIDE ONCE A DAY MIX 1 SULPHITE A DAY!  
4) HAVE PRE-MIX TANK 3/4 FULL, RAISE DENSITY TO 1270 KGL/M<sup>3</sup>  
MIX 300 TO 250 SX - 1/2 MINUTE A LAG!

5) 10 MAIN SYSTEMS 11X TONIGHT 10 PAILS OF SOLID - 20 MIN  
PAIL 2 PALS SOLID ASH + 2 PALS OF DISPAC-10.

6) KEEP VISCOSITY 1.0 PRE-MIX 55 SECIL. 1 L LAG F.L.R  
ONLY IF REGIL. DO NOT ADD ANY WATER TO PRE-MIX.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KICK REINHART  
 PHONE 785-4777 PHONE FAIRBORN OUTMOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 14 1991  
 REPORT No. # 43  
 SPUD DATE APR 29 91

WELL NAME COIGAS ETAL KOTANEE LEE LOCATION VT. I-48  
 OPERATOR COLOMBIA GAS DEVELOPMENT CONTRACTOR KENTING HT. 7  
 REPORT FOR Mr. POD TOUF-NEIL PLISS REPORT FOR Mr. FHIL GOSCHLWORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE # <u>10.155 IN</u>	COND.	TANKS <u>70.17</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57.17</u>	m <sup>3</sup> /STK. <u>0.118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>130</u> mm	INTER <u>58.3273</u>	TOTAL <u>177.17</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>10,000</u>
OTHER <u>PMA-300</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>0.59</u>	CIRC. TIME <u>215</u>

HOLE DATA		DESANDER/DESTILER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>LT. POLYMER</u>	FLOWLINE WTA <u>1200</u> kg/m <sup>3</sup>	MUD WT. <u>1205-1310</u> kg/m <sup>3</sup>			
HOLE COND. <u>GOOD</u>	UNDERFLOW WTD <u>78</u> kg/m <sup>3</sup>	VISCOSITY <u>45</u> s/L			
DEVIATION	OVERFLOW WT. <u>HOLE D.P. 0</u> kg/m <sup>3</sup>	FILTRATE <u>15-18</u> cm <sup>3</sup> /30 min.			
CURRENT OP <u>HEAT FIT #10</u>	UNDERFLOW RATE <u>11,000</u> m <sup>3</sup> /min.	pH <u>10.5</u>			

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/> <u>SHALE</u>	MUD PROPERTIES <u>PRE-MIX</u>		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>13:30</u>	<u>13:30</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2664</u>		LARITE	<u>3151</u>		<u>435</u>	<u>7716</u>	<u>5477.50</u>
FLOWLINE TEMPERATURE (°C)	<u>38.00</u>		FLR	<u>65</u>		<u>3</u>	<u>62</u>	<u>480.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1310</u>	<u>1210</u>	DISPAC	<u>49</u>		<u>7</u>	<u>42</u>	<u>1126.80</u>
FUNNEL VISCOSITY (s/L)	<u>44</u>	<u>51</u>	SULPHATE	<u>24</u>		<u>6</u>	<u>28</u>	<u>120.00</u>
APPARENT VISCOSITY (mPa.s)	<u>78</u>	<u>34</u>	SULPHATE	<u>96</u>		<u>10</u>	<u>86</u>	<u>2100.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>30</u>	<u>20</u>						
YIELD POINT (Pa)	<u>8</u>	<u>14.5</u>						
GELS 0/10 min. (Pa)	<u>1.5/2</u>	<u>2/4</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>18</u>	<u>8.5</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.8/2.3</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.007</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.09</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.91</u>							
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>							
ELECTRICAL STABILITY (V) <u>H2S</u>	<u>0</u>							
OIL/WATER RATIO <u>SULPHATE</u>	<u>1.4 KG/L</u>							
CaCl <sub>2</sub> w/w% <u>SULPHATE</u>	<u>100 MG/L</u>							
"n"/k <u>TOTAL POLYMER</u>	<u>5 KG/L</u>							

COMMENTS: 1. MUD DENSITY = 1205 KG/M<sup>3</sup>. KEEP MUD GUNS HOIVING!  
IF DENSITY GOES BELOW 1200 KG/M<sup>3</sup>: MIX 50 LARITE + 4 BAGS OF  
AS SOON AS YOU GET BACK ON BOTTOM W/ FIT #11!  
1. RUN WATER = 10 LITERS/LINE. FEEL 1 CIRCULATION.  
2. RUN 1X CIRC OVER 1 FULL CIRC. THEN RUN 1 SULPHATE.  
3. AFTER BOTTOMS UP MIX 4 BAGS DISPAC + 10 SS MIN/L BAG.  
4. KEEP VISCOSITY IN PRE-MIX = 55 SEC/L. MIX 1/2 BAG OF  
FLR-BEG. AS REQ'D.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KIKI REINHART  
 PHONE 785-4777 PHONE FAR ROOM OUT MOBILE # #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-15-1991  
 REPORT No. # 44  
 SPUD DATE APR-29-91

WELL NAME COLGAS ETAL KOTANE E LEE LOCATION VT-I-48  
 OPERATOR COLGAS ETAL GAS DEVELOPMENT CONTRACTOR KENTING HI-TOWER  
 REPORT FOR Mr. POP TOOLE-NEIL BLISS REPORT FOR Mr. PHIL ROSONI/CORLITH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2 MILL</u>	COND.	TANKS <u>73</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>150</u> mm	INTER <u>58-3372</u>	TOTAL <u>130 m<sup>3</sup></u>	S.P.M. <u>50</u>	PUMP PRESS <u>10,000</u>
OTHER <u>THA-300</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.59</u>	CIRC. TIME <u>215</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>ST. POLYMER</u>	FLOWLINE WT. <u>APPROX 001</u> kg/m <sup>3</sup>	<u>46 m<sup>3</sup></u>	MUD WT. <u>1205-1210</u> kg/m <sup>3</sup>		
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>APPROX 001</u> kg/m <sup>3</sup>	<u>78 m<sup>3</sup></u>	VISCOSITY <u>45</u> s/L		
DEVIATION	OVERFLOW WT. <u>APPROX 001</u> kg/m <sup>3</sup>	<u>55 m<sup>3</sup></u>	FILTRATE <u>15-17</u> cm <sup>3</sup> /30 min.		
CURRENT OP. <u>MILL AND CONES</u>	UNDERFLOW RATE	m <sup>3</sup> /min.	pH <u>10.5</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	01:30			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	3664								
FLOWLINE TEMPERATURE (°C)	27.00								
DENSITY (kg/m <sup>3</sup> )	1215								
FUNNEL VISCOSITY (s/L)	44								
APPARENT VISCOSITY (mPa.s)	29								
PLASTIC VISCOSITY (mPa.s)	21								
YIELD POINT (Pa)	8								
GELS 0/10 min. (Pa)	1.517								
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	18.5								
FILTER CAKE (mm)	1.2 FUR.								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	1.6/2.0								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	50								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	300								
SAND CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	.002								
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/>	.092								
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input type="checkbox"/>	.907								
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	10								
ELECTRICAL STABILITY (V) <u>H<sub>2</sub>S</u>	0								
OIL/WATER RATIO <u>SULFON</u>	1.4 KG/ML								
CaCl <sub>2</sub> w/w% <u>SULPHITES</u>	120								
"n"/"k" TOTAL <u>BLUNDER 5 KG/ML</u>									
PREVIOUS COST	96,034.80			STARTING VOLUME					
DAILY COST				VOL BUILT					
CUM. COST				VOL. LOST ON SURFACE					
CUM. ENG. COST	17,750			VOL. LOST SUB SURFACE					
				END VOLUME					
				CUM. VOL BUILT					

COMMENTS:  
 1. AS SPUD AT 400 GFT LACK OF BOTTOM W/ BIT # 11  
 2. RAN WATER @ 10 LITRES/MIN. FOR 1 CIRCULATION  
 3. RAN 1/2 BAG OF SOLUBLE SULPHITE OVER 1 FULL CIRCULATION  
 4. AFTER BOTTOMS DROPPED MIX 4 BAGS OF DISPAC-LOW  
 @ 55 MINUTES 1 BAG!  
 5. KEEP VISCOSITY IN PRE-MIX @ 55 SEC/L. MIX 1/2 BAG  
 OF FLR. REMAIN IF REQ'D.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KILIK REINHART  
 PHONE 785-4222 PHONE FAR ROOM MOBILE # 1

THE INFORMATION IN THIS REPORT IS BASED ON OUR EXPERIENCE, REPRESENTS OUR BEST JUDGEMENT IN THE MATTER AND IS INTENDED TO BE HELPFUL BUT WE CANNOT ASSUME RESPONSIBILITY FOR ANY LOSS OR ACCIDENT THAT MAY RESULT FROM ITS USE. FURTHERMORE, NOTHING CONTAINED HEREIN SHALL BE CONSTRUED AS A RECOMMENDATION TO USE ANY PRODUCT IN CONFLICT WITH EXISTING PATENTS COVERING ANY MATERIALS OR USE



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 15 1991  
 REPORT No. #44A  
 SPUD DATE APR 29 91

WELL NAME COLEMAN GAS DEVELOPMENT LOCATION VT-I-48

OPERATOR COLEMAN GAS DEVELOPMENT CONTRACTOR KENTING HI TOWER 7

REPORT FOR Mr. FOR TOLLE - NEIL PLISS REPORT FOR Mr. PHIL COSEWORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / #11- <u>1 7/8" ID</u>	COND.	TANKS <u>72 m<sup>3</sup></u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57 m<sup>3</sup></u>	m <sup>3</sup> /STK. <u>.0018</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>130</u> mm	INTER <u>3333</u>	TOTAL <u>130 m<sup>3</sup></u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9200</u>
OTHER <u>THAC</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.59</u>	CIRC. TIME <u>215</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>L.T. POLYMER</u>	FLOWLINE WT <u>ANIN. VOL. 46 m<sup>3</sup></u> kg/m <sup>3</sup>	MUD WT <u>1305-1310 KG.</u> kg/m <sup>3</sup>	VISCOSITY <u>45</u> s/L		
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>ETA. UP 78 m<sup>3</sup></u> kg/m <sup>3</sup>	FILTRATE <u>15-17</u> cm <sup>3</sup> /30 min.			
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	pH <u>10.5</u>			
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE m <sup>3</sup> /min.				

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>19:00</u>		<u>PARITE 2716</u>			<u>70</u>	<u>246</u>	<u>875.00</u>
FLOWLINE TEMPERATURE (°C)	<u>26.7</u>		<u>X-CIDE 74</u>			<u>2</u>	<u>22</u>	<u>780.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>36.0</u>		<u>SIPHITE 16</u>			<u>2</u>	<u>14</u>	<u>99.40</u>
FUNNEL VISCOSITY (s/L)	<u>1215</u>		<u>DISPAC 42</u>			<u>3</u>	<u>39</u>	<u>487.20</u>
APPARENT VISCOSITY (mPa.s)	<u>43</u>		<u>FIR-REG 67</u>			<u>1</u>	<u>61</u>	<u>160.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>79.5</u>							
YIELD POINT (Pa)	<u>27</u>							
GELS 0/10 min. (Pa)	<u>7.5</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>15/2</u>							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>10.5</u>							
FILTER CAKE (mm)	<u>27</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0 TIGHT!</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L)	<u>1.5/1.9</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>60</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>300</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.002</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.092</u>							
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>.907</u>		PREVIOUS COST <u>96,034</u>	STARTING VOLUME				
ELECTRICAL STABILITY (V) <u>10</u>	<u>10</u>		DAILY COST <u>1901.60</u>	VOL. BUILT <u>THAC 115</u>				
OIL/WATER RATIO <u>1.4 KG/L</u>	<u>0</u>		CUM. COST <u>97,935.60</u>	VOL. LOST ON SURFACE <u>1</u>				
CaCl <sub>2</sub> w/w% <u>130</u>			CUM. ENG. COST <u>17,250</u>	VOL. LOST SUB SURFACE <u>1</u>				
"n" <u>5 KG/M<sup>3</sup></u>				END VOLUME				
				CUM. VOL. BUILT				

COMMENTS:

AS SOON AS YOU GET TO BOTTOM W/ BIT #13!

1 RUN THE CENTRIFUGE FOR 1 FULL CIRCULATION!

2 MIX 5 BAGS DISPAC-10 AT 45 MINUTES A BAG!

3 MIX 1 JUG OF X-CIDE OVER 1 FULL CIRCULATION!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KICKE REINHART

PHONE 785-4322 PHONE FOR ROOM ON MOBILE #1

THE INFORMATION IN THIS REPORT IS BASED ON OUR EXPERIENCE, REPRESENTS OUR BEST JUDGEMENT IN THE MATTER AND IS INTENDED TO BE HELPFUL, BUT WE CANNOT ASSUME RESPONSIBILITY FOR ANY LOSS OR ACCIDENT THAT MAY RESULT FROM ITS USE. FURTHERMORE, NOTHING CONTAINED HEREIN SHALL BE CONSTRUED AS A RECOMMENDATION TO USE ANY PRODUCT IN CONFLICT WITH EXISTING PATENTS COVERING ANY MATERIALS OR USE.



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 16 1991  
 REPORT No. # 45  
 SPUD DATE APR 29 91

WELL NAME COI GAS ET AL KOTANEE LEE LOCATION VT-1-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING HITOWER  
 REPORT FOR Mr. POE TOOLE-NEIL BUSS REPORT FOR Mr. PHIL CASAMUZZI

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2 15mm</u>	COND.	TANKS <u>23.0</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>51.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57.1</u>	m <sup>3</sup> /STK. <u>.0018</u>	OPPOSITE D.C. <u>90</u>
DRILL COLLARS <u>130</u> mm	INTER <u>9-2752</u>	TOTAL <u>130m<sup>3</sup></u>	S.P.M. <u>52</u>	PUMP PRESS. <u>9200</u>
OTHER <u>HT 2000</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.6136</u>	CIRC. TIME <u>210</u>

HOLE DATA		CENTRIFUGER/DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. PULVER</u>	FLOWLINE WT. <u>1215 to 1300</u> kg/m <sup>3</sup>	MUD WT. <u>1300</u> kg/m <sup>3</sup>	HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>2730</u> kg/m <sup>3</sup>	VISCOSITY <u>45</u> s/L
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE <u>670</u> cm <sup>3</sup> /30 min.	CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER		pH <u>10.5</u>			

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/> <u>SHALLOW</u>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>10:00</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3672</u>			LADITE	<u>246</u>		<u>35</u>	<u>2611</u>	<u>437.50</u>
FLOWLINE TEMPERATURE (°C)	<u>37.00</u>			DRISPAK	<u>29</u>		<u>5</u>	<u>34</u>	<u>817.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1300</u>			X-CIDE	<u>22</u>		<u>1</u>	<u>21</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>42</u>			FTS-200	<u>21</u>		<u>4</u>		<u>1040.00</u>
APPARENT VISCOSITY (mPa.s)	<u>27.5</u>								
PLASTIC VISCOSITY (mPa.s)	<u>20</u>								
YIELD POINT (Pa)	<u>7.5</u>								
GELS 0/10 min. (Pa)	<u>1.5/2</u>								
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>								
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>36</u>								
FILTER CAKE (mm)	<u>1.0 FIRM.</u>								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.5/1.9</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>250</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.007</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.085</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.915</u>								
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>12</u>								
ELECTRICAL STABILITY (V) <input type="checkbox"/>	<u>0</u>								
OIL/WATER RATIO <input type="checkbox"/>	<u>1.3 KOLM</u>								
CaCl <sub>2</sub> w/w% <input type="checkbox"/>	<u>130</u>								
"n"/"k" <input type="checkbox"/>	<u>4.5</u>								
PREVIOUS COST <u>97,925.60</u>				STARTING VOLUME					
DAILY COST <u>3439.50</u>				VOL. BUILT <u>THAN 1/2</u>					
CUM. COST <u>100,365.10</u>				VOL. LOST ON SURFACE <u>1/2</u>					
CUM. ENG. COST <u>17,675.00</u>				VOL. LOST SUB SURFACE <u>1/2</u>					
				END VOLUME					
				CUM. VOL. BUILT					

COMMENTS:  
AS SOON AS YOU GET ON BOTTOM W/ BIT #12!  
W/ RUN WATER @ 5 LITRES/MIN. FOR 1 CIRCULATION!  
2 MIX 5 BAGS DRISPAK-10 AT 45 MINUTES A BAG!  
2 MIX 1 BAG OF ASP. 221 OVER 1 FULL CIRCULATION!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RIK BERNHART  
 PHONE 785-4377 PHONE FAR 1000 MOBILE # #1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-17-91  
 REPORT No. # 46  
 SPUD DATE APR-29-91

WELL NAME COLUMBIA GAS DEVELOPMENT LOCATION YT-T-48  
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING HI-TECH #7  
 REPORT FOR Mr. FOR TIGLE - NEW PLISS REPORT FOR Mr. PHIL ROSSWORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>12.15 # mm</u>	COND.	TANKS <u>23m</u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>57m</u>	m <sup>3</sup> /STK. <u>0.118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>158-3373</u>	TOTAL <u>120.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9500</u>
OTHER <u>THA 200L</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>.59</u>	CIRC. TIME <u>715</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>L.T. FULMER</u>	FLOWLINE WT.	kg/m <sup>3</sup>	MUD WT. <u>1200</u>	kg/m <sup>3</sup>	
HOLE COND. <u>GOOD</u>	UNDERFLOW WT.	kg/m <sup>3</sup>	VISCOSITY <u>45</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE <u>230</u>	cm <sup>3</sup> /30 min.	
CURRENT OP <u>HT PIT #13</u>	UNDERFLOW RATE	m <sup>3</sup> /min.	pH <u>10.5</u>		

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>04:00</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3681</u>			<u>INVENTORY JUNE-16 @ 20:00 HRS.</u>					
FLOWLINE TEMPERATURE (°C)	<u>35.0</u>			SODA ASH	<u>78</u>		<u>4</u>	<u>74</u>	<u>80.00</u>
DENSITY (kg/m <sup>3</sup> )	<u>1190</u>			ASP-721	<u>55</u>		<u>1</u>	<u>54</u>	<u>100.00</u>
FUNNEL VISCOSITY (s/L)	<u>45</u>			FTS-200	<u>27</u>		<u>2</u>	<u>25</u>	<u>570.00</u>
APPARENT VISCOSITY (mPa.s)	<u>39</u>			X-CILE	<u>21</u>		<u>1</u>	<u>20</u>	<u>140.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>27</u>			SULPHITE	<u>14</u>		<u>1</u>	<u>13</u>	<u>49.70</u>
YIELD POINT (Pa)	<u>7</u>			DEFAC-1	<u>17</u>		<u>3</u>	<u>9</u>	<u>409.50</u>
GELS 0/10 min. (Pa)	<u>1.513</u>			DRISPAC	<u>34</u>		<u>2</u>	<u>32</u>	<u>374.80</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>			DFLC	<u>5</u>		<u>2</u>	<u>3</u>	<u>356.00</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>28</u>			SANDUST	<u>228</u>		<u>28</u>	<u>200</u>	<u>186.20</u>
FILTER CAKE (mm)	<u>1.2 FINE</u>			LINE	<u>20</u>		<u>4</u>	<u>16</u>	<u>24.40</u>
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.5/1.9</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L)	<u>40</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>350</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>0.07</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>0.75</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.25</u>			PREVIOUS COST	<u>100.365</u>		STARTING VOLUME		
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>17</u>			DAILY COST	<u>2490.49</u>		VOL. BUILT	<u>THA-115</u>	
ELECTRICAL STABILITY (V) <u>H=5</u>	<u>0</u>			CUM. COST	<u>102855.20</u>		VOL. LOST ON SURFACE		
OIL/WATER RATIO <u>SULPHITE</u>	<u>1.2</u>			CUM. ENG. COST	<u>18.000</u>		VOL. LOST SUB SURFACE		
CaCl <sub>2</sub> w/w% <u>SULPHITE</u>	<u>130</u>						END VOLUME		
"n"/"k" <u>TOTAL RUNNER</u>	<u>5.0 KG/M<sup>3</sup></u>						CUM. VOL. BUILT		

COMMENTS:  
AS SOON AS YOU GET OUR BOTTOM HOLE PIT # 14!  
1 BAG WATER @ 10 LITRES/LINE FOR 1 CIRCULATION!  
MIX 4 BAGS OF DRISPAC 10 @ 55 MIN/1 BAG!  
MIX 1 - 1 BAG OF ASP-721 OVER 1 FULL CIRCULATION!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK BELLHART  
 PHONE 785-4222 PHONE FAL ROCK OILFIELD #1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 17 1991  
 REPORT No. # 46A  
 SPUD DATE APR 29 91

WELL NAME COLEGA ETAL KITANELEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING HITOWER 7

REPORT FOR Mr. BOB TOOLE - NEIL CLISE REPORT FOR Mr. PHIL BOGALWORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>4.152 1200?</u>	COND.	TANKS <u>69.5</u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>51.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57.5</u>	m <sup>3</sup> /STK. <u>0118</u>	OPPOSITE D.C. <u>90</u>
DRILL COLLARS <u>120</u> mm	INTER <u>158.2773</u>	TOTAL <u>177.17</u>	S.P.M. <u>52</u>	PUMP PRESS. <u>9500</u>
OTHER <u>THA-300M.</u>	OTHER	STANDBY	m <sup>3</sup> /min. <u>6136</u>	CIRC. TIME <u>710</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>1190-1300</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1300</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1300</u> kg/m <sup>3</sup>	VISCOSITY <u>45</u> s/L	
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>76</u> m <sup>3</sup> /min	VISCOSITY <u>45</u> s/L			
DEVIATION	OVERFLOW WT. <u>76</u> m <sup>3</sup> /min	FILTRATE <u>cm<sup>3</sup>/30 min.</u>			
CURRENT OF <u>DRILLING</u>	UNDERFLOW RATE <u>76</u> m <sup>3</sup> /min	pH <u>10.5</u>			
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER					

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	04:00	01:00	20:00	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	3695	3695	3685	BARITE	7611		35	2576	427.50
FLOWLINE TEMPERATURE (°C)	40°	40°	39°	X-IDE	30		3	17	470.00
DENSITY (kg/m <sup>3</sup> )	1195	1190	1195	DRISPAK	33		8	74	1799.70
FUNNEL VISCOSITY (s/L)	41	40	43	ASP-721	54		3	51	300.00
APPARENT VISCOSITY (mPa.s)	74	73.5	76	F.L.R.	61		1	60	160.00
PLASTIC VISCOSITY (mPa.s)	19	19	20						
YIELD POINT (Pa)	5	4.5	6						
GELS 0/10 min. (Pa)	111.5	111.5	151.2						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5	10.5	10.5						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	35	37	33						
FILTER CAKE (mm)	1.538T	1.5	1.5						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	1.5/2.0	1.5/2.0	1.5/2.1						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L)	40	40	40						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl (mg/L)	350	400	400	30-1	60-1	100-1	12		
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	.007	.007	.007	200R=21	300R=39	600R=48			
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	.08	.078	.08						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	.92	.923	.93	PREVIOUS COST	2855.	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	15	15	15	DAILY COST	2616.50	VOL. BUILT	THANKS		
ELECTRICAL STABILITY (V) <u>H.2.S</u>	0	0	0	CUM. COST	105,472	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>SULLAN</u>	1.0	1.0	1.0	CUM. ENG. COST	18,000.	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <u>SULFITE</u>	130	130	130			END VOLUME			
"n" <u>TOTAL POLYMER</u>	7	7	7			CUM. VOL. BUILT			

COMMENTS:

AS SOON AS YOU GET BACK ON BOTTOM W/ PIT #15!

FINISH RUNNING IN THE ASP-721 IN CHEM. F.L. OVER 70 MIN.

RUN IN THE LAST BAG OF F.L.R. REG. OVER 70 MIN.

RUN IN WATER AT 5 LITRES/MINUTE.

RUN IN 3 BAGS OF ASP-721 @ 70 LITRE BAG?

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KEVIN KEIGHTANT

PHONE 785-4777 PHONE FAR ROOM MOBILE #1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 19, 1991  
 REPORT No. # 48  
 SPUD DATE APR. 29, 91

WELL NAME COLGAS ETAL KETAMEELEE LOCATION YT-I-48  
 OPERATOR COLGAS DEVELOPMENT CONTRACTOR KENTING HITOWER 7  
 REPORT FOR Mr. Bob Toole-Nell Pluss REPORT FOR Mr. Mike Foschworth

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>4.5-1.5 in</u>	COND.	TANKS <u>72</u>	PUMP SIZE <u>114x404</u>	OPPOSITE D.P. <u>51.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>58</u>	m³/STK. <u>.0118</u>	OPPOSITE D.C. <u>90</u>
DRILL COLLARS <u>170</u> mm	INTERSECT <u>2777</u>	TOTAL <u>120</u>	S.P.M. <u>52</u>	PUMP PRESS.
OTHER <u>LHA-300</u>	OTHER	STANDBY	m³/min. <u>.6136</u>	CIRC. TIME <u>210</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. Polymer</u>	FLOWLINE WT. <u>46.5</u> kg/m³	MUD WT. <u>1190-1700</u> kg/m³	VISCOSITY <u>45</u> s/L		
HOLE COND. <u>Good</u>	UNDERFLOW WT. <u>76</u> kg/m³	FILTRATE <u>215</u> cm³/30 min.			
DEVIATION	OVERFLOW WT. kg/m³	pH <u>10.5</u>			
CURRENT OF DRILLING	UNDERFLOW RATE m³/min.				

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH-SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>08:00</u>				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3705</u>									
FLOWLINE TEMPERATURE (°C) <u>36°C</u>									
DENSITY (kg/m³) <u>1200</u>									
FUNNEL VISCOSITY (s/L) <u>43</u>									
APPARENT VISCOSITY (mPa.s) <u>24</u>									
PLASTIC VISCOSITY (mPa.s) <u>19</u>									
YIELD POINT (Pa) <u>5</u>									
GELS 0/10 min. (Pa) <u>111.5</u>									
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.3</u>								
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>25</u>								
FILTER CAKE (mm) <u>1.0 FIRM.</u>									
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.4/20</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>30</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>250</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.007</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.085</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.915</u>								
MBT (Kg/m³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>14</u>								
ELECTRICAL STABILITY (V) <u>0</u>	<u>M61L</u>								
OIL/WATER RATIO <u>1.0</u>	<u>KG/L</u>								
CaCl₂ w/w% <u>110</u>	<u>M61L</u>								
"n" "k" TOTAL Polymer <u>7.5</u>	<u>KG/L</u>								
PREVIOUS COST <u>109.78</u>									
DAILY COST									
CUM. COST									
CUM. ENG. COST <u>18.75</u>									
STARTING VOLUME									
VOL. BUILT									
VOL. LOST on SURFACE									
VOL. LOST SUB SURFACE									
END VOLUME									
CUM. VOL. BUILT									

COMMENTS:

1. Run WATER @ 5 LITRE/MIN.

2. AFTER MIXING THE NEXT 3 ASP. 2 21% IF THE VISCOSITY IS 45 SEC/L OR LESS, MIX 3 MORE PAILS.

3. PRIOR TO NEXT TRIP: ISOLATE LAST TWO TANKS MIX 4 PAILS OF PTS-300, 2 PAILS IN EACH TANK. DISPLACE FOR 40 MINUTES AND PUMP FILL.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART  
 PHONE 85-4333 PHONE FAR Rockville MD 301-477-4111

THE INFORMATION IN THIS REPORT IS BASED ON OUR EXPERIENCE. REPRESENTS OUR BEST JUDGEMENT IN THE MATTER AND IS INTENDED TO BE HELPFUL. BUT WE CANNOT ASSUME RESPONSIBILITY FOR ANY LOSS OR ACCIDENT THAT MAY RESULT FROM ITS USE. FURTHERMORE, NOTHING CONTAINED HEREIN SHALL BE CONSTRUED AS A RECOMMENDATION TO USE ANY PRODUCT IN CONFLICT WITH EXISTING PATENTS COVERING ANY MATERIALS OR USE.



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-19  
 REPORT No. 49  
 SPUD DATE 91-04-29

WELL NAME COLCAS at KOTANEELEF LOCATION YT - I - 48  
 OPERATOR COLUMBIA GAS DEVELOP. CONTRACTOR KENTINS H.T. #7  
 REPORT FOR Mr. BOB TADLE / NEIL BLISS REPORT FOR Mr. PHIL BOSMORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>15 / 152</u>	COND.	TANKS <u>72</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>58</u>	m <sup>3</sup> /STK. <u>0118</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>178/3273</u>	TOTAL <u>130</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9,000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>.6</u>	CIRC. TIME <u>215 ±</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>BTRMS W = 80</u> kg/m <sup>3</sup>	MUD WT. <u>1190-1200</u> kg/m <sup>3</sup>
HOLE COND. <u>OK.</u>	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>40-45</u> s/L
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>15</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>CIR</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST									
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST				
PRESENT DEPTH (m)	<u>22:30</u>		<u>BAR. TE</u>			<u>35</u>		<u>438</u>				
FLOWLINE TEMPERATURE (°C)	<u>3733</u>		<u>ASP-721</u>			<u>10</u>		<u>1000</u>				
DENSITY (kg/m <sup>3</sup> )	<u>40</u>		<u>SOD. SUL.</u>			<u>1</u>		<u>50</u>				
FUNNEL VISCOSITY (s/L)	<u>1195</u>		<u>X.C.O.F.</u>			<u>2</u>		<u>280</u>				
APPARENT VISCOSITY (mPa.s)	<u>43</u>		<u>FLR</u>			<u>5</u>		<u>960</u>				
PLASTIC VISCOSITY (mPa.s)	<u>26</u>		<u>PTS-200</u>			<u>4</u>		<u>1040</u>				
YIELD POINT (Pa)	<u>20</u>		<u>INDVIS</u>			<u>2</u>		<u>840</u>				
GELS 0/10 min. (Pa)	<u>6</u>		<u>K. SEAL</u>	<u>PREV</u>		<u>10</u>		<u>238</u>				
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.5</u>		<div style="border: 1px solid black; padding: 5px; display: inline-block;"> <table border="1"> <tr> <td>600/300</td> <td>52/32</td> </tr> <tr> <td>200/100</td> <td>23/14</td> </tr> <tr> <td>6/3</td> <td>1.5/1</td> </tr> </table> </div>				600/300	52/32	200/100	23/14	6/3	1.5/1
600/300	52/32											
200/100	23/14											
6/3	1.5/1											
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>10.5</u>											
FILTER CAKE (mm)	<u>15.0</u>											
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.8</u>											
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>1.4/5.0</u>											
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CaCl <sub>2</sub> (mg/L)	<u>TR.</u>											
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>350</u>											
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.003</u>											
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.085</u>											
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>.915</u>		PREVIOUS COST	<u>109,782</u>	STARTING VOLUME							
ELECTRICAL STABILITY (V) <u>H<sub>2</sub>S</u> <u>N2G.</u>	<u>—</u>		DAILY COST	<u>4846</u>	VOL. BUILT							
OIL/WATER RATIO <u>SULFITE</u> <u>100</u>			CUM. COST	<u>114,628</u>	VOL. LOST ON SURFACE							
CaCl <sub>2</sub> w/w% <u>TOTAL POLYMER</u> <u>9. Kg/m<sup>3</sup></u>			CUM. ENG. COST	<u>1,125</u>	VOL. LOST SUB SURFACE							
"n"/"k"					END VOLUME							
					CUM. VOL. BUILT							

COMMENTS: DRILLED TO 3733 m + TRIP FOR BIT.  
CONTROL DENSITY AT 1195-1200 kg/m<sup>3</sup>. RUN 5 LITRES H<sub>2</sub>O PER MIN.  
KEEP PH AT 10.5 USING CAUSTIC.  
MAINTAIN VIS. AT 40-45 s/L USING ASP-721 + FLR. ADD 3 ASP-721 EVERY 12 HRS.  
ADD 1 X.C.O.F. + 1 SK. SOD. SUL. DAILY.

STOCK POINT FT ST. JOHN THKS O.F. ENGINEER JIM CHELSEA  
 PHONE 785-4223 PHONE ON LOCATION MOBILE #



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-20  
 REPORT No. 30  
 SPUD DATE 91-04-29

WELL NAME COLGAS of KOTANELELE LOCATION VT I-48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. #7  
 REPORT FOR Mr. BOB TOOLE / NEIL BLISS REPORT FOR Mr. PHIL BOSMORTH

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>16 / 152</u>	COND.	TANKS <u>76</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>59</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>178 / 3273</u>	TOTAL <u>135</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9.000</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>.6</u>	CIRC. TIME <u>225 ±</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT.	MUD WT. <u>1200</u> kg/m <sup>3</sup>
HOLE COND. <u>OK</u>	UNDERFLOW WT.	VISCOSITY <u>40-45</u> s/L
DEVIATION	OVERFLOW WT.	FILTRATE <u>215</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>DRIG.</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN	<u>23:30</u>						
PRESENT DEPTH (m)	<u>3772</u>	<u>DRISAC</u>			<u>5</u>		<u>812</u>
FLOWLINE TEMPERATURE (°C)	<u>42</u>	<u>X-CIDE</u>			<u>1</u>		<u>140</u>
DENSITY (kg/m <sup>3</sup> )	<u>1210</u>	<u>ASP-721</u>			<u>3</u>		<u>300</u>
FUNNEL VISCOSITY (s/L)	<u>43</u>	<u>SOD. SULF.</u>			<u>1</u>		<u>50</u>
APPARENT VISCOSITY (mPa.s)	<u>26</u>						
PLASTIC VISCOSITY (mPa.s)	<u>20</u>						
YIELD POINT (Pa)	<u>6</u>						
GELS 0/10 min. (Pa)	<u>112</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>19.4</u>						
FILTER CAKE (mm)	<u>.8</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.4/5.0</u>						
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL (mg/L)	<u>350</u>	<u>600/300</u>	<u>52/32</u>				
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.004</u>	<u>200/1100</u>	<u>24/14</u>				
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.09</u>	<u>613</u>	<u>311</u>				
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.91</u>	PREVIOUS COST	<u>114,390</u>	STARTING VOLUME			
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u>	DAILY COST	<u>1302</u>	VOL. BUILT			
ELECTRICAL STABILITY (V) <u>H<sub>2</sub>S</u>	<u>NEG.</u>	CUM. COST	<u>115692</u>	VOL. LOST on SURFACE			
OIL/WATER RATIO <u>SULFITE</u>	<u>110</u>	CUM. ENG. COST	<u>19,500</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <u>POLYMER</u>	<u>9.5 Kg/m<sup>3</sup></u>			END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: DRIG. 152 mm HOLE.

- KEEP VISCOSITY AT 40-45 s/L USING ASP-721 + FLR. 3 ASP-721 EVERY 12 HRS.
- HOLD DENSITY AT 1200 Kg/m<sup>3</sup>. RUN 5 LITRES H<sub>2</sub>O PER MIN.
- ADD 1 X-CIDE + 1SX. SOD. SULFITE DAILY.
- ADD 3 Pts. 200 PRIOR TO TRIP.

STOCK POINT FT. ST. JOHN JHRS I.D.F. ENGINEER JIM WELER  
 PHONE 785-4222 PHONE ON LOCATION MOBILE #



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-21  
 REPORT No. 51  
 SPUD DATE 91-04-29

WELL NAME COLGAS of a KOTANEFLER LOCATION VT F-48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. #7  
 REPORT FOR Mr. BOB TORRE / NEIL RUSSELL REPORT FOR Mr. PHIL BOSOMWORTH

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>17 /</u>	COND.	TANKS <u>74</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>60</u>	m³/STK. <u>0116</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>178/3273</u>	TOTAL <u>134</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9700</u>
OTHER	OTHER	STANDBY	m³/min. <u>.6</u>	CIRC. TIME <u>225±</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. kg/m³	MUD WT. <u>1190-1200</u> kg/m³
HOLE COND.	UNDERFLOW WT. kg/m³	VISCOSITY <u>40-45</u> s/L
DEVIATION <u>734 @ 3767 M 11 1/4"</u>	OVERFLOW WT. kg/m³	FILTRATE <u>2.15</u> cm³/30 min.
CURRENT OP. <u>DRUG.</u>	UNDERFLOW RATE m³/min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>22:00</u>	<u>02:00</u>	ASP-721			<u>2</u>		<u>200</u>
FLOWLINE TEMPERATURE (°C)	<u>3790</u>	<u>3802</u>	FLR			<u>5</u>		<u>800</u>
DENSITY (kg/m³)	<u>1210</u>	<u>1195</u>	WTS-200			<u>3</u>		<u>780</u>
FUNNEL VISCOSITY (s/L)	<u>44</u>	<u>44</u>	PARITE			<u>35</u>		<u>438</u>
APPARENT VISCOSITY (mPa.s)	<u>30</u>	<u>30</u>	CAUSTIC			<u>2</u>		<u>60</u>
PLASTIC VISCOSITY (mPa.s)	<u>24</u>	<u>24</u>						
YIELD POINT (Pa)	<u>6</u>	<u>6</u>						
GELS 0/10 min. (Pa)	<u>112</u>	<u>112</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>11.0</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>24</u>	<u>17.0</u>						
FILTER CAKE (mm)	<u>.8</u>	<u>.8</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.3/5.0</u>	<u>1.5/5.5</u>						
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>TR.</u>	<u>TR.</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>350</u>	<u>350</u>						
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.004</u>	<u>.003</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.09</u>	<u>.08</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.91</u>	<u>.92</u>	PREVIOUS COST	<u>115,692</u>	STARTING VOLUME			
MBT (Kg/m³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u>	<u>-</u>	DAILY COST	<u>2278</u>	VOL. BUILT			
ELECTRICAL STABILITY (V) <u>H<sub>2</sub>S</u>	<u>NEG.</u>	<u>NEG.</u>	CUM. COST	<u>117,970</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>SULFITE</u>	<u>115</u>	<u>120</u>	CUM. ENG. COST	<u>19,875</u>	VOL. LOST SUB SURFACE			
CaCl <sub>2</sub> w/w% <u>POLYMER (kg/l) 3</u>	<u>9.5</u>	<u>9.5</u>			END VOLUME			
"n"/"k"					CUM. VOL. BUILT			

COMMENTS: DRUG. 152 mm HOLE KAN CENTRIFUGE FOR 1 HR.

- 1) MAINTAIN VIS. AT 40-45 s/L USING ASP-721 + FLR.
- 2) HOLD DENSITY AT 1190-1200 kg/m³. RUN 5 LINES H<sub>2</sub>O PER MIN.
- 3) ADD 1 GALLON + 1 GAL. SOD. SULFITE DAILY.
- 4) ADD 3 ASP-721 EVERY 13 HRS.
- 5) KEEP PH AT 10.5 USING CAUSTIC.

STOCK POINT FT. ST. JOHN ENGINEER JIM WICKER  
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-22  
 REPORT No. 52  
 SPUD DATE 91-04-29

WELL NAME Colgas of Kotankelf LOCATION YT I 48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. # 7  
 REPORT FOR Mr. Bob Toole / Neil Bliss REPORT FOR Mr. Phil Basomworth

ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>17 / 152</u>	COND.	TANKS <u>72</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>61</u>	m <sup>3</sup> /STK. <u>.0118</u>	OPPOSITE D.C. <u>68</u>
DRILL COLLARS <u>120</u> mm	INTER <u>178 / 3273</u>	TOTAL <u>133</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9600</u>
OTHER	OTHER	STANDBY	m <sup>3</sup> /min. <u>.6</u>	CIRC. TIME <u>250 ±</u>

HOLE DATA	DESANDER/DESTILER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>BAMS WP = 85 MIN</u> kg/m <sup>3</sup>	MUD WT. <u>1190 - 1300</u> kg/m <sup>3</sup>
HOLE COND. <u>OK.</u>	UNDERFLOW WT. kg/m <sup>3</sup>	VISCOSITY <u>40-45</u> s/L
DEVIATION	OVERFLOW WT. kg/m <sup>3</sup>	FILTRATE <u>&lt; 15</u> cm <sup>3</sup> /30 min.
CURRENT OP. <u>CIR.</u>	UNDERFLOW RATE m <sup>3</sup> /min.	pH <u>10.5</u>

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>09:00</u>	<u>19:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3820</u>	<u>3843</u>	BARITE	<u>2468</u>		<u>35</u>	<u>2430</u>	<u>438</u>
FLOWLINE TEMPERATURE (°C)	<u>42</u>	<u>43</u>	FLOPLEX	<u>56</u>		<u>22</u>	<u>34</u>	<u>2750</u>
DENSITY (kg/m <sup>3</sup> )	<u>1195</u>	<u>1195</u>	FLR	<u>99</u>		<u>6</u>	<u>93</u>	<u>960</u>
FUNNEL VISCOSITY (s/L)	<u>46</u>	<u>46</u>	X-CIDE	<u>13</u>		<u>1</u>	<u>14</u>	<u>140</u>
APPARENT VISCOSITY (mPa.s)	<u>28</u>	<u>28</u>	ASP-721	<u>32</u>		<u>7</u>	<u>25</u>	<u>700</u>
PLASTIC VISCOSITY (mPa.s)	<u>22</u>	<u>22</u>	SOD. SULF.	<u>11</u>		<u>1</u>	<u>10</u>	<u>50</u>
YIELD POINT (Pa)	<u>6</u>	<u>6</u>	STANDUST	<u>200</u>		<u>70</u>	<u>130</u>	<u>343</u>
GELS 0/10 min. (Pa)	<u>112</u>	<u>112</u>	PTS-200	<u>18</u>			<u>18</u>	
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>	CAUSTIC	<u>178</u>			<u>178</u>	
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	<u>8.0</u>	<u>7.6</u>						
FILTER CAKE (mm)	<u>.5</u>	<u>.5</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>14 / 5.2</u>	<u>14 / 5.4</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>	<u>TR.</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <sup>-</sup> (mg/L)	<u>350</u>	<u>350</u>	600/300	<u>56/34</u>				
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.003</u>	<u>.003</u>	200/100	<u>26/14</u>				
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.08</u>	<u>.08</u>	0/13	<u>312</u>				
WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.92</u>	<u>.92</u>	PREVIOUS COST	<u>115.690</u>				
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u>	<u>-</u>	DAILY COST	<u>5381</u>				
ELECTRICAL STABILITY (V) <u>H<sub>2</sub>S</u>	<u>NEG.</u>	<u>NEG</u>	CUM. COST	<u>121,072</u>				
OIL/WATER RATIO <u>SULFITE</u>	<u>130</u>	<u>130</u>	CUM. ENG. COST	<u>19,875</u>				
CaCl <sub>2</sub> w/w% <u>POLYMER</u>	<u>10</u>	<u>10</u>						
"n"/"k"								

COMMENTS: CIR. PRIOR TO TRIP FOR BIT #17 LOST 8 m<sup>3</sup> FROM 3822-3844 m  
PUMPED 14 m<sup>3</sup> L.C.M. PILL PRIOR TO TRIP  
CONTROL DENSITY AT 1190-1300 kg/m<sup>3</sup>. RUN 5 LITRES H<sub>2</sub>O PER MIN.  
MAINTAIN PH AT 10.5 WITH CAUSTIC.  
HOLD V.S. AT 40-45 s/L USING ASP-721. ADD 3 PAILS EVERY 10 MIN.  
ADD 1 Ltr. SOD. SULFITE + 1 X-CIDE DAILY.  
PRIOR TO TRIP OUT TO LOG, MIX 7 PAILS PTS-200 + 2 X-CIDE.

STOCK POINT ST. JOHN I.D.F. ENGINEER JIM WIELER  
 PHONE 785-4222 PHONE AT LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-24  
 REPORT No. 54  
 SPUD DATE 91-04-29

WELL NAME	COLGAS of KOTANELEE		LOCATION	VT - I 48	
OPERATOR	COLUMBIA GAS DEVEL.		CONTRACTOR	KENTINE H.T. # 7	
REPORT FOR Mr.	BOB TADLE / NEIL SLICK		REPORT FOR Mr.	PHIL JOSEPH WORTH	
ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT	ANNULAR VEL. m./min.	
BIT SIZE / #	1 1/2	TANKS	75	PUMP SIZE	114 x 406
COND.	SURFACE	HOLE	62	m <sup>3</sup> /STK.	0.118
DRILL PIPE	69 mm	TOTAL	137	S.P.M.	50
DRILL COLLARS	120 mm	INTER	178/323	m <sup>3</sup> /min.	1.6
OTHER	OTHER	STANDBY		CIRC. TIME	230±

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE	W. POLYMER	FLOWLINE WT.	600/700 52/32	kg/m <sup>3</sup>	MUD WT.
HOLE COND.	OK.	UNDERFLOW WT.	200/100 24/14	kg/m <sup>3</sup>	VISCOSITY
DEVIATION	8° x 388 N34° E	OVERFLOW WT.	613 3/2	kg/m <sup>3</sup>	FILTRATE
CURRENT OP.	CIR.	UNDERFLOW RATE		m <sup>3</sup> /min	pH

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> OR <input type="checkbox"/>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	15:30			PARTE	2888		35	2353	438
FLOWLINE TEMPERATURE (°C)	39.5			FLR	35			35	
DENSITY (kg/m <sup>3</sup> )	44			ACIDE	13		1	12	140
FUNNEL VISCOSITY (s/L)	1205			ASP. 721	25		5	20	500
APPARENT VISCOSITY (mPa.s)	44			SOD. SUL.	9			9	
PLASTIC VISCOSITY (mPa.s)	26			SANDWST	130			130	
YIELD POINT (Pa)	20			MS-200	18		8	10	2080
GELS 0/10 min. (Pa)	6			CAUSTIC	173	173	6	167	180
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	11/2			IODINE	45		5	40	2100
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>3</sup> )	10.5			SUREAN	82			82	
FILTER CAKE (mm)	6.6			SFA ASH	18			18	
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	.5			LIME	16		5	11	43
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	1.5/5.5			DRISPAE	37		8	19	1300
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CaCl <sub>2</sub> (mg/L)	TR.			DEFAMER	6			6	
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	350			GL	310			310	
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.004			PREVIOUS COST	123,809				
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.08			DAILY COST	6781				
OIL-WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.08			CUM. COST	130,590				
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	.92			CUM. ENG. COST	20,625				
ELECTRICAL STABILITY (V)	N.G.			STARTING VOLUME					
OIL/WATER RATIO	N.G.			VOL. BUILT					
CaCl <sub>2</sub> w/w%	120	mg/L		VOL. LOST ON SURFACE					
"n"/"k"	POLYMER	10	kg/m <sup>3</sup>	VOL. LOST SUB SURFACE					
				END VOLUME					
				CUM. VOL. BUILT					

COMMENTS: T.D. 3915 m CIR. PRIOR TO TRIP OUT TO LOG.

MAINTAIN PH AT 10.5 USING CAUSTIC.

CONTROL DENSITY AT 1190-1200 kg/m<sup>3</sup>. RUN 5 LINES H<sub>2</sub>O WHEN OK.

Vis 40-45 s/L.

NOTE: PRIOR TO TRIP OUT TO RUN UNDER MUD 8 TRILS. MS-200 + 1 GAL X-CIDE.

STOCK POINT B. ST. TOWN  
 PHONE 785-9222  
 I.D.F. ENGINEER TIM WIELER  
 PHONE ON LOCATION MOBILE #

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I.D.F.C. - 015 (3)



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-25  
 REPORT No. 55  
 SPUD DATE 91-04-29

WELL NAME COLGAS #101 KOTANEFF LF LOCATION VT I-48  
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. #7  
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. PHIL ROSMOUTH

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL (m./min.)
BIT SIZE / # 1 1/2	COND.	TANKS 74	PUMP SIZE 114 x 406	OPPOSITE D.P. 51
DRILL PIPE 89 mm	SURFACE	HOLE 60	m³/STK. 0.118 (0.167)	OPPOSITE D.C. 88
DRILL COLLARS 120 mm	INTER 178/2272	TOTAL 136	S.P.M. 50	PUMP PRESS. 10,000
OTHER	OTHER	STANDBY	m³/min. .6 .6	CIRC. TIME 230

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE WT. POLYMER	FLOWLINE WT. 600300 58136 kg/m³	MUD WT. 1190-1200 kg/m³
HOLE COND. OK.	UNDERFLOW WT. 2001100 27116 kg/m³	VISCOSITY 40-45 s/L
DEVIATION	OVERFLOW WT. 613 312 kg/m³	FILTRATE <15 cm³/30 min.
CURRENT OP. CIR.	UNDERFLOW RATE m³/min.	pH 10.5

EQUIPMENT:  DEGASSER  DESILTER  DESANDER  CENTRIFUGE  DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	20.00			BARITE	2353		35	2318	438
FLOWLINE TEMPERATURE (°C)	39.5			FLR	35			35	
DENSITY (kg/m³)	41			XCIDE	12		2	10	280
FUNNEL VISCOSITY (s/L)	1210			ASP-201	20			20	
APPARENT VISCOSITY (mPa.s)	46			SOD. SUL.	9			9	
PLASTIC VISCOSITY (mPa.s)	29			SHUDDIST	130			130	
YIELD POINT (Pa)	22			M.S.-200	102		8	94	2080
GELS 0/10 min. (Pa)	7			CARBON	167		1	166	30
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	11.0			TDMS D	40			40	
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	7.6			SULFAN	82			82	
FILTER CAKE (mm)	.5			SODIUM ASH	18			18	
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	68/6.0			LIME	11			11	
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	78.			DRISPAK	19			19	
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL (mg/L)	350			DEFAMER	6			6	
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	.002			GEL	310			310	
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	.08			POLYTRAMP	.50			.50	
OH/WATER CONT. (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	.92			PREVIOUS COST	127,290			STARTING VOLUME	
MBT (Kg/m³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	—			DAILY COST	2826			VOL. BUILT	
ELECTRICAL STABILITY (V/H <sub>2</sub> S)	NEG.			CUM. COST	132,118			VOL. LOST ON SURFACE	
OIL/WATER RATIO SULFITE	120			CUM. ENG. COST	21,000			VOL. LOST SUB SURFACE	
CaCl <sub>2</sub> w/w% POLYMER	10							END VOLUME	
"n"/"k"								CUM. VOL. BUILT	

COMMENTS: T.D. 39.5 m LOGGED. NAB CLEAN OUT TRIP TO RUN LINER.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WILKER  
 PHONE 785-4333 PHONE ON LOCATION MOBILE #

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I.D.F.C. - 015 (3)



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-26/27  
 REPORT No. 56  
 SPUD DATE 91-04-29

WELL NAME <b>COLGAC #1 of KOTANEELE</b>		LOCATION <b>YT-I-48</b>	
OPERATOR <b>COLUMBIA GAS DEVELOPMENT</b>		CONTRACTOR <b>KENTING H.T. #7</b>	
REPORT FOR Mr. <b>BOE TADLE</b>		REPORT FOR Mr. <b>PHIL ROSSMURTH</b>	
ASSEMBLY	CASING	MUD Vol. (m <sup>3</sup> )	PUMP OUTPUT
BIT SIZE / #	COND.	TANKS	ANNULAR VEL. m./min.
DRILL PIPE mm	SURFACE	HOLE	PUMP SIZE <b>114 x 406</b>
DRILL COLLARS mm	INTER <b>178/3273</b>	TOTAL	m <sup>3</sup> /STK. <b>.018</b>
OTHER	OTHER <b>127/3915</b>	STANDBY	S.P.M.
HOLE DATA		DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <b>WT. POLYMER</b>	FLOWLINE WT.	kg/m <sup>3</sup>	MUD WT. kg/m <sup>3</sup>
HOLE COND. <b>OK</b>	UNDERFLOW WT.	kg/m <sup>3</sup>	VISCOSITY s/L
DEVIATION	OVERFLOW WT.	kg/m <sup>3</sup>	FILTRATE cm <sup>3</sup> /30 min.
CURRENT OP. <b>C.R.</b>	UNDERFLOW RATE	m <sup>3</sup> /min.	pH
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER			
SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES	
TIME SAMPLE TAKEN		MATERIALS INVENTORY & COST	
PRESENT DEPTH (m)		MATERIALS	INITIAL RECEIVED USED BALANCE COST
FLOWLINE TEMPERATURE (°C)		BARITE	33.8 10 2308 125
DENSITY (kg/m <sup>3</sup> )		FLR	35 35
FUNNEL VISCOSITY (s/L)		X-CIDE	10 3 7 420
APPARENT VISCOSITY (mPa.s)		ASP-721	21 21
PLASTIC VISCOSITY (mPa.s)		SOD-SUL	9 9
YIELD POINT (Pa)		SAUBUST	130 30 100 147
GELS 0/10 min. (Pa)		PTS-200	96 5 91 1300
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>		CAUSTIC	166 166
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm <sup>2</sup> )		EDWD	40 40
FILTER CAKE (mm)		SULFAN	82 82
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)		SOD ASH	18 18
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)		LIME	11 11
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)		IR-JAC	19 19
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>		DEFAMER	6 1 5 136
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>		GEL	310 10 300 100
OH/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>		POLYTEMP	50 50
MBT (Kg/m <sup>3</sup> ) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>		PREVIOUS COST	132118 STARTING VOLUME
ELECTRICAL STABILITY (V) H <sub>2</sub> S		DAILY COST	3172 VOL. BUILT
OIL/WATER RATIO <b>SULFITE</b>		CUM. COST	135290 VOL. LOST ON SURFACE
CaCl <sub>2</sub> w/w% <b>POLYMER</b>		CUM. ENG. COST	21250 VOL. LOST SUB SURFACE
"n"/"k"			END VOLUME
COMMENTS <b>RAN LINER (127 mm)</b>			CUM. VOL. BUILT
<b>LOST APPROX. 21 m<sup>3</sup> MUD TO HOLE</b>		BICARB	55 55
<b>WHILE RUNNING LINER PUMPED</b>		<del>RESIN</del>	-
<b>L.C.M. &amp; BYPASSED SHAKER WHILE</b>		DEFL	3 3
<b>CIR. TRIP TO CEMENTING.</b>		BEADS	32 32
		FCU	60 60
		POWTEMP	50 50
		K-SCAL	100 11 89 262
		TRFREE	4 4
		VISPLEX	10 2 8 500
		CaCO <sub>3</sub>	102 102
		CELLULOSE	20 8 12 185
		WALNUT	20 20
		FLOPLEX	34 34
STOCK POINT <b>AT ST JOHN</b>		I.D.F. ENGINEER <b>JIM WHEELER</b>	
PHONE <b>785-4222</b>		PHONE <b>ON LOCATION</b>	MOBILE #

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