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NATIONAL ENERGY BOARD
ENGINEERING BRANCH
OCT 18 1991

WELL SUMMARY
FOR
COLUMBIA GAS DEVELOPMENT OF CANADA
COLUMBIA et al KOTANEELEE YT-I-48



WELL SUMMARY
FOR
COLUMBIA GAS DEVELOPMENT OF CANADA
COLUMBIA et al KOTANEELEE YT-I-48

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PREPARED BY

INTERNATIONAL DRILLING FLUIDS
TECHNICAL SERVICES DEPARTMENT

JULY 1991

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

WELL DATA

RIG: KENTING HI-TOWER #07
DATE SPURRED: RE-ENTRY APRIL 29, 1991
DATE RIG RELEASED: JUNE 24, 1991
TOTAL DEPTH: 3915m
TOTAL DAYS: 58

CASING	DEPTH	FLUID TYPE	DAYS	INTERVAL COST	
				PROGRAMMED	ACTUAL
178mm (Liner)	3273m	Gel/Chemical/Wtd	26	\$ 12,040.00	\$ 27,242.50
127mm	3915m	Polymer/Wtd	32	70,340.00	117,875.80
WELL TOTAL				\$ 82,380.00	<u>\$ 145,118.30</u>

OPERATOR REPRESENTATIVE: Mr. Harold Rugg
Mr. Bob Toole
Mr. Neil Bliss

CONTRACTOR REPRESENTATIVE: Mr. Jim Signer
Mr. Phil Bosomworth

IDF ENGINEER: Mr. Rick Reinhart
Mr. Jim Wieler

**All costs based on field estimates
and at published book price.**

INTERNATIONAL DRILLING FLUIDS - 266-0722

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

MATERIAL CONSUMPTION BY INTERVAL

HOLE SIZE: 178mm CASING

FLUID TYPE: GEL/CHEMICAL/WTD

PRODUCT	UNIT SIZE	QUANTITY	UNIT PRICE	TOTAL COST
Gel	100lb	390	\$ 10.00	\$ 3,900.00
Barite	40kg	1629	12.50	20,362.00
Caustic Soda	50lb	30	30.00	900.00
Soda Ash	40kg	12	20.00	240.00
Sulban	19kg	6	250.00	1,500.00
Sodium Bicarbonate	100lb	5	40.00	140.00
Sawdust	sacks	28	5.00	137.20

INTERVAL TOTAL

\$ 27,242.50

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

MATERIAL CONSUMPTION BY INTERVAL

HOLE SIZE: 152mm

FLUID TYPE: POLYMER/WTD

PRODUCT	UNIT SIZE	QUANTITY	UNIT PRICE	TOTAL COST
Barite	40kg	2260	\$ 12.50	\$ 28,250.00
Caustic Soda	50lb	44	30.00	1,320.00
Soda Ash	40kg	28	20.00	560.00
Sulban	19kg	14	250.00	3,500.00
Lime	25kg	20	8.58	171.60
Sawdust	sacks	160	5.00	800.00
Kwikseal	40lb	75	26.00	1,950.00
IDF-FLR	50lb	45	160.00	7,200.00
Drispac S. Lo	50lb	56	162.40	9,094.40
ASP-721	20L	56	135.00	7,560.00
IDVIS D	25kg	40	420.00	16,800.00
PTS-200	20L	69	260.00	17,940.00
X-Cide	6lb	40	140.00	5,600.00
Sodium Sulfite	50lb	30	49.00	1,470.70
Defoamer	20L	19	150.00	2,850.00
Flo Plex	50lb	21	125.00	2,625.00
Glass Beads	50lb	36	80.00	2,880.00
IDF FCL	25kg	10	32.00	320.00
Visplex	25kg	1	225.00	225.00
Celloflake	25lb	40	23.10	924.00
Mica	25kg	20	15.89	317.80
DFLC	25lb	31	178.00	5,518.00
INTERVAL TOTAL				\$ 117,875.80

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

MATERIAL CONSUMPTION BY INTERVAL

TOTALS FOR WELL

PRODUCT	UNIT SIZE	QUANTITY	UNIT PRICE	TOTAL COST
Mica	25kg	20	\$ 15.89	\$ 317.80
Gel	100lb	390	10.00	3,900.00
Barite	40kg	3889	12.50	48,612.50
Caustic Soda	50lb	74	30.00	2,220.00
Soda Ash	40kg	40	20.00	800.00
Sulban	19kg	20	250.00	5,000.00
Sodium Bicarbonate	100lb	5	40.00	200.00
Sawdust	sacks	188	5.00	940.00
Lime	25kg	20	8.58	171.60
Kwikseal	40lb	56	26.00	1,950.00
IDF-FLR	50lb	45	160.00	7,200.00
Drispac	50lb	56	162.40	9,094.40
ASP-721	20L	56	135.00	7,560.00
IDVIS D	25kg	40	420.00	16,800.00
PTS-200	20L	69	260.00	17,940.00
IDF FCL	25kg	10	32.00	320.00
X-Cide	6lb	40	140.00	5,600.00
Sodium Sulfite	50lb	30	49.00	1,470.00
Defoamer	20L	19	150.00	2,850.00
Glass Beads	50lb	36	80.00	2,880.00
Visplex	25kg	1	225.00	225.00
Flo Plex	50lb	21	125.00	2,625.00
Celloflake	25lb	40	23.10	924.00
DFLC	25lb	31	178.00	5,518.00
WELL TOTAL				\$ 145,118.30

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

DISCUSSION BY INTERVALS

HOLE SIZE: 178mm CASING

MUD TYPE: GEL/CHEMICAL (Weighted)

Mixed 90m³ of kill mud at 1200kg/m³. Displaced the hole to mud and built volume increasing the yeild point to a level high enough to suspend the Barite. The possibility of H₂S required raising and controlling the pH at 11.0 with Caustic Soda. Also pre-treated with 1.6kg/m³ of Sulban (H₂S Scavenger). Mixed a Barite pill prior to each trip (45 sacks) which continued to increase the density. Controlled the density at 1200kg/m³ with water dilution at 20/L min. when circulating. Due to the high bottom hole temperature of approximately 350°F the viscosity at the shaker was 20 to 40 sec/L higher than at the suction. Set a bridge plug at 3331 metres. Whipstock packer at 3277 metres, logged and ran in with mill. Milled a window in the 178mm casing. Kicked off and drilled 152mm hole to 3290 metres.

HOLE SIZE: 152mm

MUD TYPE: POLYMER (Weighted)

Pre-mixed a weighted Polymer system on May 25, 1991. Displaced the hole over to the Polymer system and built volume and condition the mud. Drilled ahead, mixing 1 jug of X-Cide and 3 pails PTS-200 daily to prevent the Polymers from breaking down due to the high bottom hole temperature (350°F+). Maintained the viscosity at 35-45 s/L using **IDVIS D** and **ASP-721**. Controlled pH at 10.5 using Caustic Soda. The Yield point was 10 (Pa) until 3435 metres and then started to climb to 14. Increased H₂O additions and added 27 sacks **IDF FCL** to lower the yield point. **ASP-721** additions were stopped on June 8th at 3530 metres and resumed on June 17th at 3680. The fluid loss climbed from 10mL to 37mL. Used **Drispac S. Lo** and **IDF-FLR** to control the filtrate. Fluid loss was very unstable until additions of **Flo Plex** (3.7kg/m³) at 3800 metres. Fluid loss dropped below 8mL.

While drilling from 3784 metres - 3822 metres, the hole took approximately 8m³ fluid. Prior to a trip out with Bit #17, a 14m³ L.C.M. pill was spotted in the annulus. No further losses were encountered while drilling. TD was 3915 metres. Logged and ran 127mm liner. Lost approximately 21m³ while running liner. Pumped L.C.M. and by passed shaker screens while circulating prior to cementing.

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

CONCLUSIONS AND RECOMMENDATIONS

HOLE SIZE: 178mm CASING

MUD TYPE: GEL/CHEMICAL (Weighted)

Pre-mixed a weighted Gel system prior to drilling out the bridge plug. The density was raised to 1200kg/m³ due to expected gas pressures. Maintained the pH at 10.5-11.0 and pre-treated with .6kg/m³ Sulban due to the possibility of H₂S. This mud system was used to cut a window in the casing at 3273 metres with no problems.

HOLE SIZE: 152mm

MUD TYPE: POLYMER

Pre-mixed and displaced the hole with a weighted Polymer system after the window was cut in the casing. The Polymer system was used to prevent any damage to the producing formation. The density was controlled in the 1180-1210kg/m³ range due to the possibility of high formation pressures. The hole was directionally drilled to stay away from the old hole. Fished for cones at 3664 metres and 3695 metres. The hole was in good shape and no problems were encountered other than the difficulty keeping the fluid loss down. Flo Plex was added to lower fluid loss below 12mL and no further problems were reported.

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

PROGRAMMED PRODUCT COST DISCUSSION

Programmed Product Cost	\$ 82,380.00
Actual Cost	\$ 145,118.30

PRODUCT COST SUMMARY vs PROGRAMMED COST

Product	Programmed Usage	Actual Usage	Cost Difference	Reason For Use
Bentonite	200	390	\$ 1,900.00	viscosity
Barite	1800	3889	26,112.50	density
Bicarbonate	50	5	(1,800.00)	cement contamination
Caustic Soda	42	74	960.00	pH control
IDBOND (ASP 721)	50	56	810.00	shale control
IDF FCL	40	10	(960.00)	thinner
Soda Ash	5	40	700.00	water hardness control
X-Cide 207	20	40	2,800.00	Biocide
IDF-FLR (Drispac)	60	101	6,560.00	fluid loss
DFLC	30	31	178.00	thinner
IDVIS D	25	40	6,300.00	viscosity
PTS 200	80	69	(2,860.00)	temperature stability
Mica	--	20	317.80	LCM
Sulban	--	20	5,000.00	H ₂ S Scavenger
Sawdust	--	188	940.00	LCM
Lime	--	20	171.60	camp use
Kwik-Seal	--	56	1,950.00	LCM
Sodium Sulphite	--	30	1,470.00	polymer stability
DEFOAMER	--	19	2,850.00	gas entrapment
Glass Beads	--	36	2,880.00	torque reducer
VISPLEX	--	1	225.00	viscosity
FLOPLEX	--	21	2,625.00	fluid loss
Celloflake	--	40	924.00	LCM

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PRODUCT USE DISCUSSION

WORKOVER

The product cost for the workover section of the re-entry was \$15,000.00 over our estimated program cost. This overrun was due to the time spent on this section (estimated 4 days, actual 26 days) and the Barite used for trip pills during this time (\$12,000.00). Extra Bentonite, Caustic Soda and four pails of Sulban accounted for the balance of the cost in excess of the estimate.

RE-DRILL

The re-drill section of the project was accomplished within the programmed time frame, but the product cost was \$47,500.00 above the programmed estimate. Barite use was again the biggest reason as about \$14,000.00 over the programmed estimate was used. Trip pills and lost circulation accounted for the use. The centrifuge was used to reduce the density as it climbed above levels required for pressure control due to the many trip pills used.

Fluid loss control was the only drilling fluid problem experienced on this well. The programmed combination of **IDF-FLR**, **Drispac**, **PTS 200** and **Sodium Sulphite** could not stabilize the fluid loss once bottom hole temperatures climbed to the expected high levels. **FLOPLEX** was brought to location and used to stabilize the fluid loss. Fluid loss control contributed to \$7,800.00 of the cost over programmed estimate.

Lost circulation while drilling and running liner accounted for \$4,200.00 of lost circulation material and losses of \$7,200.00 of mud. The mud was on standby in a premix tank on location, but the cost to build the additional volume had not been included in our estimate.

Glass Beads were used to reduce torque between the casing and drillstring when kicking off (\$2,880.00). Scavenger to control hydrogen sulphide (\$5,000.00), Biocide to ensure bacteria did not become a problem (\$2,800.00 above estimate) and **DEFOAMER** to reduce gas entrapment (\$2,850.00) accounted for the balance of the cost over programmed estimate.

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

FUTURE AREA WELLS or RE-ENTRIES

PROGRAM RECOMMENDATIONS

1. The Polymer system is the best system to use on main hole or on a re-entry section in this area. It provides shale stability if these sections are in open hole, does not flocculate due to the high bottom hole temperatures and provides even cleaning ability through the different annular sizes. In addition, it appears that no formation damage was done as the well cleaned up and is producing as expected.
2. Programs for fluid loss control in the area will have to include product equivalent to **FLOPLEX** in the Polymer system. Conventional fluid loss polymers along with polymer stabilizers could not control the fluid loss adequately.
3. The balance between losses or gains from the producing formation appear to be very close, whole mud loss occurred both drilling and when running the casing. Although the losses were not severe on this well potential for serious problems exist and should be planned for. High mud weight to fight pressure may contribute to losses that would cause a serious well control problem.
4. Use a storage shed for mud products on location. Product bags were on location for over three (3) months and the shrink wrap started to break down. Product loss could have been a greater problem if the weather turned worse.

COLUMBIA GAS DEVELOPMENT OF CANADA

COLUMBIA et al KOTANEELEE YT-I-48

MATERIAL SUPPLY RECORD

PRODUCT	RECEIVED	RETURNED	USED	COST	TOTAL
Mica	20	0	20	\$ 15.89	\$ 317.80
Gel	665	275	390	10.00	3,900.00
Caustic Soda	210	136	74	30.00	2,220.00
Barite	6196	2307	3889	12.50	48,612.50
Soda Ash	40	0	40	20.00	800.00
Sulban	100	80	20	250.00	5,000.00
Lime	20	0	20	8.58	171.60
Sodium Bicarbonate	60	55	5	40.00	200.00
Sawdust	288	100	188	4.90	940.00
IDF-FLR	80	35	45	160.00	7,200.00
Drispac S. Lo	80	24	56	162.40	9,094.40
ASP-721	80	24	56	135.00	7,560.00
IDVIS D	80	40	40	420.00	16,800.00
PTS-200	158	89	69	260.00	17,940.00
IDF FCL	60	50	10	32.00	320.00
X-Cide	42	2	40	140.00	5,600.00
Sodium Sulfite	30	0	30	49.00	1,470.00
Kwikseal	150	75	75	26.00	1,950.00
Defoamer	20	1	19	150.00	2,850.00
Visplex	10	9	1	225.00	225.00
Celloflake	40	0	40	23.10	924.00
Glass Beads	64	28	36	80.00	2,880.00
Flo Plex	56	35	21	125.00	2,625.00
DFLC	35	4	31	178.00	5,518.00

MATERIAL COST	\$ 145,118.30
ENGINEER COST	\$ 21,375.00
SHRINKWRAPS	\$ 3,060.00
FREIGHT	\$ 30,852.50
PALLETS	\$ 3,084.00
LOADING & UNLOADING	\$ 693.54
POLY TARP	\$ 150.00
FREIGHT ADJUSTMENT	\$ 2,831.81
G.S.T.	\$ 14,791.80
TOTAL COST	<u>\$ 221,930.25</u>



International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED GEL CASSTIC SOLIDAO2

WELL NAME COLUMBIA ET AL AREA KOTANKELEE

STOCK POINT ET ST JOHN Contractor KENTING #7

ENGINEERS RICK REINHART

(1)

Day No.	DATE	DEPTH	MUD PROPERTIES																OPERATION REMARKS								
			WEIGHT PPG				VISCOSITY				GEL		Filtrate Analysis				RETORT			BENTONITE kg/m ³		H ₂ S MILL SOLIDAO (kg/m ³)		"N"		"X"	
			1	2	3	4	1	2	3	4	10	0	1	2	3	4	Ca ⁺⁺ ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE	H ₂ S MILL	SOLIDAO	"N"	"X"	
5	03-05	3545	1210	49	24	19	5	3	6	11.5	1.5	-	16.5	350	30	.3	-	.078	NO	50	0						APR-30 NIPPLE UP.
	03-05	3545	1190	44	24	20	4.5	2	3	14	2.0	-	11.0	800	20	.8	-	.07	NO	50	0						MAY-01 PRESSURE TEST.
								1	2																		MAY-02 PRESS. TEST.
7	05-05	3554	1205	49	28	25	3.5	2	3	9.0	1.5	-	10.7	600	20	.8	-	.078	NO	65	0						MIX KILL MUD TO
	05-05	3734	1200	60	33	26	2.5	3	2	10.0	1.5	-	10.7	700	20	.9	-	.075	002	90	0	.6					1200 KG/M ³ VISCOSITY
								2	4																		0.48 SEC/LL (90M ³)
8	06-05	3735	1195	80	42	30	12	4	2	10.5	1.5	-	10.5	800	30	.7	-	.073	002	80	0	.6					MAY-03 FINISH MIXING
								2	7																		KILL MUD, CIRCULATE
9	07-05	3735	1210	65	34	29	5	4	2	10	1.5	-	10.7	800	30	.9	-	.078	002	75	0	.5					TUBING AND DISPLACE
								2	4																		HOLE W/ KILL MUD.
11	09-05	3515	1200	68	32	27	5.5	4	2	10	1.5	-	10.5	850	40	.8	-	.075	002	75	0	.5					LAY DOWN TUBING
								2	4																		MAY-04 LAY DOWN
								2	4																		TUBING, MAKE UP AND
								2	4																		RUN IN W/ MILL.

REMARKS: - MAY-05 CIRCULATE AND MILL OUT BRIDGE PLUG CIRC. OUT AIR. (NO GAS) WASH PACKER TO BOTTOM. CIRC. BOTTOMS UP. NO GAS. RAISED PH TO 11.0 + PRE-MIXED .5 KG SOLIDAO

MAY-06 HOIST MILL, RUN IN WITH OVERSHOT, WORK OVER SHOT @ 3515 M. WOULD NOT GO PAST WHERE CASING PARTED. HOIST OVER SHOT.

MAY-07 RUN IN WITH SPEAR AND LATCH ONTO FISH. CHAIN OUT + RECOVER TAIL PIPE.

MAY-08 RUN IN W/ TAPERED MILL WORK OFF EDGES ON BOTTOM PART OF CASING WHERE IT PARTED @ 3515 METERS HOIST MILL AND RUN IN W/ WASH OVER PIPE

IT REQUIRES 35 TO 40 SXS DABITE FOR PILLS PRIOR TO TRIPPING.



International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WT. GEL CAUSTIC

WELL NAME ALMBA et al KOPANEE AREA Y-5-I-48

STOCK POINT FT. ST. JOHN Contractor KENTON #7

ENGINEERS J.M. WHEELER

Day No.	DATE	DEPTH	MUD PROPERTIES																		OPERATION REMARKS											
			WEIGHT (ppg)			VISCOSITY			GEL		CAKE			Filtrate Analysis			RETORT			BENTONITE			POTASH			ID BOND			"N"		"K"	
			sec./l	A.V. cps	P.V. cps	Y.P. Pa	10	0	FLUID LOSS 30 Min cc's	CAKE mm	H.T.H.P. cc's	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m ³	POTASH kg/m ³	ID BOND kg/m ³	"N"	"K"									
18	05-16	3274	1190	26	25	20	5	2	10.5	2.0	-	10.7	750	TR.	1.4	-	.07	.002	70													PRESSURE TEST CEMENT
19	05-17	3274	1185	42	26	22	4	1	12.4	2.0		10.5	750	TR.	1.4		.07	TR.	66													LOGGING & RAN IN TO MILL
20	05-18	3274	1190	62	36	28	8	2	10.6	2.0		11.0	750	TR.	1.4		.07	TR.	70													CIR.
21	05-19	3274	1195	62	39	30	9	2	10.6	2.0		11.0	750	TR.	1.3		.07	TR.	70													MILLING WINDOW
22	05-20	3276	1190	53	35	28	7	1	13.0	2.0		11.0	750	TR.	1.3		.07	TR.	70													MILLING
23	05-21	3277	1190	53	35	28	7	1	13.0	2.0		11.0	750	TR.	1.3		.07	.001	70													"
24	05-22	3277	1195	53	35	28	7	1	12.8	2.0		10.5	700	TR.	1.0		.075	.001	70													"
25	05-23	3279	1205	57	41	32	9	2	12.0	2.0		11.0	650	TR.	1.1		.08	.002	75													"
26	05-24	3290	1210	60	44	34	10	2	12.4	2.0		10.5	600	TR.	1.0		.085	TR.	75													DRIG 152 mm HOLE DISPLAYED
27	05-25	3308	1185	40	16	10	6	2	11.0	.05		10.0	150	TR.	.50		.045	.001	-	.50												HOLE TO A POLYMER SYSTEM
28	05-26	3334	1190	39	20	10	10	2	8.0	.05		10.0	150	TR.	.40		.06	.002	-	.75												DRIG. 152 mm HOLE.
29	05-27	3354	1190	37	20	10	10	2	8.0	.05		10.5	150	TR.	.45		.07	.003	-	1.1												" " "
30	05-28	3400	1185	37	20	10	10	2	8.0	.05		10.5	150	TR.	.45		.065	.003	-	1.2												DRIG. 152 mm HOLE

REMARKS: - 05-16 PRESSURE TEST 05-17/18 SET BRIDGE PLUG AT 3331 m SET UH. P. STOCK PACKER AT 3277 m LOGGED & RAN IN WITH MILL. AFTER MILLING WAS COMPLETED, DRILLED 152 mm HOLE TO 3290 m, AND THE HOLE WAS DISPLACED TO A LIQ. POLYMER SYSTEM. DENSITY - 1180 - 1200 kg/m³. THE YIELD PT. WAS RAISED TO 8-10 (Pa) USING IDVIS D + ASP-721. VIS - 35 - 40 s/L. PH - 10 - 10.5. FLUIDLOSS BELOW 15 ml.



International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED POLYMER SYSTEM.

WELL NAME COLUMBIA ET AL AREA GTANKEEF
 STOCK POINT ET ST JOHN Contractor KENTING #07
 ENGINEERS RICK REINHART

(4)

Day No.	DATE	DEPTH	MUD PROPERTIES																				OPERATION REMARKS		
			WEIGHT ppb				VISCOSITY			GEL		Filtrate Analysis					RETORT			OTHER					
			sec/L	A.V. cps	P.V. cps	Y.P. Pa	10	0	FLUID LOSS 30 Min cc's	CAKE mm	H.T.H.P. cc's	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m ³	POTASH kg/m ³	IO BOND kg/m ³	MLSS/MLL		SULPHITES	
31	05-29	3405	1180	38	20	10	10	3/4	9.0	.05	-	10.5	200	20	.5	TRC	.065	.001	10	-	.6	0	190	MAY-29 Run in w/ BIT #1 CLEAN 18 M. TO BOTTOM	
32	05-30	3414	1178	39	21	11	10.5	3/4	9.0	.05	-	10	200	20	.4	TRC	.065	.001	10	-	.5	0	190	DRILL TO 3414 M. RIG UP WIPE LINE.	
33	05-31	3420	1185	38	22	11	11	3/4	15	.15	-	10	200	20	.4	NO	.07	.001	10	-	.5	0	180	MAY-30 Run in WITH STEERING TOOL. Run SINGLE SHOT SURVEYS	
	05-31	3425	1180	38	22	12	10	2.5/3	9.6	.1	-	10.3	200	20	.6	NO	.068	.0015	8	-	.6	0	175	STEERING TOOL. Run SINGLE SHOT SURVEYS	
34	06-01	3435	1187	43	29	15	14	3/5	9.0	.1	-	10.3	200	20	.6	NO	.073	.001	9	-	.8	0	160	HOIST BIT FOR JARS. Run in BIT RR #2.	
36	06-03	3451	1195	41	26	15	11	2/3	9.5	.1	-	10.5	200	20	.9	NO	.075	.001	10	-	.7	0	180	MAY-31 Run in STEERING TOOL. TURN TOOL FACE	
37	06-04	3459	1190	41	28	15	11.5	2/3	14	.5	-	10	200	20	.7	NO	.072	.001	11	-	.6	1	150	DRILL AHEAD + COND. MUD. HOIST BIT RR #2	
38	06-05	3468	1180	41	26	15	11	2.5	10.5	.1	-	10.5	200	20	.8	NO	.068	.001	10	-	.5	-	135		

REMARKS: JUNE-01 Run in BIT #3 DRILL w/ STEERING TOOL. MIX GLASS DEADS TO REDUCE DRAG.
JUNE-02 Hoist BIT #3. Run in BIT #4. BEAM @ 3435-3440 M. Run WATER TO LOWER YIELD POINT.
JUNE-03 Hoist BIT #4. (SOME IRON IN HOLE) Run in BIT #5 w/ LUBRIC SUB. MIXED GRAPHITE TO REDUCE DRAG!
 BEAM FROM 3417 TO 3455 M. HARD REAMING @ 3417 TO 3426 M
JUNE-04 Hoist BIT #5 Run in BIT #6 (STRATA) MIXING 4 PTS-200 PRIOR TO TRIPS. DUE TO
 MUD GOING BAD ON BOTTOMS UP!



International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED POLYMER

(6)

WELL NAME COLUMBIA ETAL AREA KOTAWEE LEE

STOCK POINT FT. ST. JOHN Contractor KEATING #07

ENGINEERS RICK REINHART

Day No.	DATE	DEPTH	MUD PROPERTIES																		OPERATION REMARKS	
			WEIGHT ppm				VISCOSITY			GEL		Filtrate Analysis			RETORT		OTHERS					
			sec./L	A.V. cps	P.V. cps	Y.P. Pa	FLUID LOSS 30 Min cc/s	CAKE mm	H.T.H.P. cc/s	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m ³	POTASH kg/m ³	ID BOND kg/m ³	HTS-MGCL		SULPHITES
42	06-09	3559	1180	43.28	18	10	2.5	1.5	1.0	-	10.7	250	30	1.1	-	.07	.001	10	.7	0	170	JUNE-09 STOP ADDITION'S
43	06-10	3580	1190	42.26	17	9	1.5	2	1.6	-	10.7	300	30	1.0	-	.075	.0015	10	.7	0	150	OF ASP-721 AND DRISPAK
	06-10	3587	1195	42.27	18	9	1.5	2	15.5	1.0	10.7	300	40	1.0	-	.078	.0015	10	.7	0	150	UNTIL RHEOLOGY COMES
																						BACK INTO LINE. THE
																						PH IS UP TO 11.0 DUE
44	06-11	3598	1195	44.28	19	9	1.5	2	15.2	.5	10.5	300	60	.9	-	.075	.0015	10	.6	0	130	TO ADDITIONS OF PTS-
	06-11	3609	1190	42.24	17	9.5	1.5	2	16.5	1.0	10.5	300	50	.9	-	.075	.002	10	.6	0	130	200. DUE TO LOWER
																						BOTTOM HOLE TEMP.
45	06-12	3623	1185	43.26	18	8	1.5	2	16	.8	10.3	300	80	.8	-	.073	.002	10	.6	0	100	THAN EXPECTED. THERE
	06-12	3630	1195	44.27.5	19	8.5	1.5	2	15.8	.5	10.5	300	80	.85	-	.08	.002	10	.6	0	100	IS A GOOD CONCENTRATION
																						OF PTS-200 IN THE
																						MUD SYSTEM. WILL
																						INCREASE ADDITIONS
																						OF X-CIDE 207 TO

REMARKS: -PREVENT BACTERIA IN THE MUD. AS YOU CAN SMELL THE MUD ON BOTTOMS UP AFTER TRIPPING. AFTER THE TRIP, THERE WAS A LARGE AMOUNT OF GAS TO SURFACE RAISING MUD DENSITY TO 1190 KG/M³ FROM 1175 KG/M³. WILL START TO CONTROL THE FLUID LOSS + RHEOLOGY w/ DECL AS REQ'D.

JUNE-10 DRILL TO APP. 3592M. HOIST BIT # 8

JUNE-11 RUN IN BIT # 9. CONDITION MUD, YIELD POINT IS DOWN TO 7.5 PA. MUD IS IN GOOD CONDITION.

JUNE-12 KEEP MUD DENSITY = 1190 KG/M³ FLUID LOSS BELOW 16 CM³. YIELD POINT = 8-10 PA.

DRILL TO 3630 METERS MIX PTS-200 + X-CIDE. HOIST BIT # 9 AND PRESSURE TEST!



International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED POLYMER

WELL NAME COLUMBIA ETAL AREA KTANFELEF
 STOCK POINT FT. ST. JOHN Contractor KENTINE #02
 ENGINEERS RICK REINHART

①

Day No.	DATE	DEPTH M	MUD PROPERTIES																		OPERATION REMARKS				
			WEIGHT					VISCOSITY			GEL		Filtrate Analysis			RETORT		POLYMER							
			ppg	sec./l	A.V. cps	P.V. cps	Y.P. Pa	0	10	FLUID LOSS 30 Min cc's	CAKE mm	H.T.H.P. cc's	pH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m ³		POTASH SUPPLIES kg/m ³	ID BOND kg/m ³	TOTAL POLYMER kg/m ³	M/S/M/G/L
46	06-13	3636	1200	45	30	21	9	1.5	2	20	1.0	-	10.5	300	100	1.0	TTC	.083	.002	10	125	4.5	0	0	JUNE-13 PRESSURE TEST. RUN IN DIT #10
47	06-14	3654	1205	43	27	20	25	1.5	2	17	1.2	-	10.5	300	80	1.3	TTC	.085	.002	10	125	4.8	5	1.4	(SHOUL. HRS) ON DITMS. UP
	06-14	3565	1210	44	28	20	8	1.5	2	18	1.0	-	10.5	300	40	1.8	TTC	.09	.002	10	100	5.0	0	1.4	MIX 1.4 KG/M ³ S/D/L/D. FLUID LOSS WENT UP TO
48	06-15	3664	1215	44	29	21	8	1.5	2	18.5	1.2	-	10.5	300	50	1.6	TTC	.093	.002	10	120	5.0	0	1.4	70 CM ³ TREAT OUT 180
	06-15	3667	1215	43	28.5	22	25	1.5	2	22	1.0	-	10.5	300	60	1.5	TTC	.093	.002	10	130	5.0	0	1.4	M/G/L. (ALLIANCE W/ SODA ASH (PRE-MIX L.C.M. MUD IN PRE-MIX TANK.) VISCOSITY
49	06-16	3672	1200	43	27.5	20	25	1.5	2	26	1.0	-	10.5	350	40	1.5	TTC	.085	.002	12	130	4.5	0	1.2	0.50 SEC/L. W/ L.D. WIS-D
50	06-17	3681	1190	45	29	22	7	1.5	2	28	1.2	-	10.5	350	40	1.5	TTC	.075	.002	12	130	5.0	0	1.2	+ FWR-REG. ADD 15 M ³
	06-17	3685	1195	43	26	20	6	1.5	2	33	1.5	-	10.5	400	40	1.5	-	.08	.002	15	130	6.0	0	1.0	FROM ACTIVE SYSTEM TO LOWER MAIN TANK VOLUME.

REMARKS: - JUNE 14 RAISE MUD DENSITY IN PRE-MIX TANK TO 1210 KG/M³. HOIST DIT #10 @ 3664 METERS. LOST 3 CONES, RUN IN + MILL ON CONES, HOIST MILL.

JUNE-15 Run in DIT #11. CLEAR TO BTM. WORK TANK S/D. HOIST DIT #11 @ 3667 M. THE FLUID LOSS IS STILL CLADDING, LIKELY DUE TO ASP-721 USED UP. HIGH FLUID LOSS MAY BE NORMAL FOR THIS SYSTEM WHEN MIXING PDS-200 COATING POLYMERS. FILTER CAKE IS FIRM.

JUNE-16 Run in DIT #12 DRILL TO 3672 M. BEAM + WORK STABILIZER. HOIST DIT #12 Run in DIT #13

JUNE-17 CONDITION MUD. HOIST DIT @ 3681 M. Run in w/ BIT #14. BEAM 10 M TO BTM. MIXING ASP-721 TO LOWER FLUID LOSS.



International Drilling Fluids Corporation

Drilling Mud Properties Record

MUD SYSTEM WEIGHTED POLYMER

WELL NAME COLONIA ETAL AREA KOTANE FLEK

STOCK POINT FT. ST. JOHN Contractor KENTING #7

ENGINEERS RICIL REINHART / JIM WIELER

(8)

Day No.	DATE	DEPTH M	MUD PROPERTIES																		OPERATION REMARKS			
			VISCOSITY						GEL		Filtrate Analysis					RETORT								
			WEIGHT PPG	SEC./L	A.V. CPS	P.V. CPS	YP. Pa	IO	FLUID LOSS 30 Min cc/s	CAKE mm	H.T.H.P. cc/s	PH	Cl ppm	Ca ppm	PI	% OIL	% SOLIDS	% SAND	BENTONITE kg/m ³	POTASH kg/m ³		SOLPHITES	TD BOND kg/m ³	ETAL BY-PROD
51	06-18	369.3	1190	40	23.5	19	4.5	1.5	37	1.5	-	10.5	400	40	1.5	-	.078	.002	15	130	6	0	1.0	JUNE-18 DRILL TO 369.5
"		369.5	1195	41	24	19	5	1.5	35	1.5	SE	10.5	350	40	1.5	-	.08	.002	15	130	7	0	1.0	HOLST BIT #15. LOST
"		369.5	1193	43	25.5	20	5.5	1.5	20	.8	-	10.3	350	30	1.4	-	.08	.002	13	100	7.5	0	1.0	CONES ON BOTTOM.
52	06-19	370.5	1200	43	24	19	5	1.5	25	1.0	-	10.3	350	30	1.4	-	.085	.002	14	110	7.5	-	1.0	RUN IN W/ MAGNET
"	06-19	373.3	1195	43	26	20	6	1.5	15	.8	-	10.5	350	TR.	1.4	-	.085	.003	-	100	9.0	NEG.	-	WORK MAGNET + HOLST.
53	06-20	377.2	1210	43	26	20	6	1.2	19.4	.8	-	10.5	350	TR.	1.4	-	.09	.004	-	110	9.5	"	-	THE FLUID LOSS IS
54	06-21	379.0	1210	44	30	24	6	1.2	24.0	.8	-	10.5	350	TR.	1.3	-	.09	.004	-	115	9.5	"	-	STARTING TO COME
	06-21	380.2	1195	44	30	24	6	1.2	17.0	.8	-	11.0	350	TR.	1.5	-	.08	.003	-	120	9.5	"	-	DOWN AND FILTER CAKE
55	06-22	384.3	1195	46	28	22	6	1.2	7.6	.5	-	10.5	350	TR.	1.4	-	.08	.003	-	130	10	"	-	IS TIGHT DUE TO
56	06-23	385.0	1205	46	30	24	6	1.2	7.0	.5	-	10.5	350	TR.	1.4	-	.08	.004	-	120	9.5	"	-	ADDITIONS OF ASP-721
57	06-24	391.5	1205	44	26	20	6	1.2	6.6	.5	-	10.5	350	TR.	1.5	-	.08	.004	-	120	10.0	"	-	FLUID LOSS DROPPED FROM
58	06-25	391.5	1210	46	29	22	7	1.2	7.6	.5	-	11.0	350	TR.	1.8	-	.08	.002	-	120	10.0	"	-	24 m' TO BELOW E.M.I. AFF
59	06-27	391.5	1210	46	25	20	5	1.2	11.0	.8	-	11.0	350	TR.	1.8	-	.08	<	-	120	9.0	"	-	1.3 lb/BBL. FLOPLEX WAS ADDED TO SYSTEM.

REMARKS: - LOST APPROX. 8 m³ FLUID TO HOLE WHILE DRG. FROM 3784 - 3822 M. PRIOR TO TRIP OUT FOR B.I. #17, A 14 m² L.C.M. PILL WAS SPOTED IN ANNULUS NO FURTHER LOSSES WERE ENCOUNTERED. DRILLED 152 mm HOLE TO 3915 m (T.D.) & LOGGED. RAN 127 mm LINER TO 3915 m. LOST APPROX. 21 m³ MUD TO HOLE WHILE RUNNING LINER. PUMPED L.C.M. & BYPASSED SHAKER WHILE C.B. PRIOR TO CEMENTING.



International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 03/07/1991
 REPORT No. 1101
 SPUD DATE RE E. TR.

WELL NAME 101-10-20-21-10-15-16-17-18-19-20-21-22-23-24-25-26-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100 LOCATION VT U.S.
 OPERATOR AMERICAN GAS DEVELOPMENT CONTRACTOR KEATINGE #07
 REPORT FOR Mr. HAROLD B. ... REPORT FOR Mr. ...

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/4</u>	COND.	TANKS <u>25</u>	PUMP SIZE <u>114/40/6</u>	OPPOSITE D.P. <u>48</u>
DRILL PIPE <u>57</u> mm	SURFACE	HOLE <u>40</u>	m ³ /STK. <u>0.17</u>	OPPOSITE D.C.
DRILL COLLARS mm	INTER. <u>10.274</u>	TOTAL <u>95</u>	S.P.M. <u>50</u>	PUMP PRESS.
OTHER	OTHER	STANDBY	m ³ /min. <u>1.5</u>	CIRC. TIME <u>150</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>CEI 10-710</u>	FLOWLINE WT. kg/m ³	MUD WT. <u>1190</u> kg/m ³
HOLE COND.	UNDERFLOW WT. kg/m ³	VISCOSITY <u>45-50</u> s/L
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE cm ³ /30 min.
CURRENT OP. <u>CEI 10-710</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/> <u>SUCT</u>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>06:00</u>							
PRESENT DEPTH (m) <u>2545</u>		CEI <u>500</u>		<u>167</u>	<u>333</u>	<u>1670.00</u>	
FLOWLINE TEMPERATURE (°C)		RAVITE <u>5723</u>		<u>331</u>	<u>5051</u>	<u>2987.50</u>	
DENSITY (kg/m ³) <u>1.10</u>		CEI 10-710 <u>150</u>		<u>4</u>	<u>146</u>	<u>170.00</u>	
FUNNEL VISCOSITY (s/L) <u>49</u>		CEI 10-710 <u>40</u>		<u>1</u>	<u>29</u>	<u>30.00</u>	
APPARENT VISCOSITY (mPa.s) <u>24</u>							
PLASTIC VISCOSITY (mPa.s) <u>19</u>							
YIELD POINT (Pa) <u>5</u>							
GELS 0/10 min. (Pa) <u>214</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>115</u>							
FILTER CAKE (mm) <u>156000</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>31.25</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>36</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>350</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>		PREVIOUS COST <u>469.75</u>	STARTING VOLUME				
ELECTRICAL STABILITY (V) <u>-</u>		DAILY COST	VOL. BUILT <u>714.10</u>				
OIL/WATER RATIO <u>-</u>		CUM. COST	VOL. LOST on SURFACE				
CaCl ₂ w/w% <u>-</u>		CUM. ENG. COST <u>275.00</u>	VOL. LOST SUB SURFACE <u>1.00</u>				
"n"/"k" <u>100/300</u> <u>45.79</u>			END VOLUME				
			CUM. VOL. BUILT				

COMMENTS:
 1. MUD LOG # 45-50 SECT. 10-710-15-16-17-18-19-20-21-22-23-24-25-26-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100
 2. MUD LOG # 45-50 SECT. 10-710-15-16-17-18-19-20-21-22-23-24-25-26-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100
 3. MUD LOG # 45-50 SECT. 10-710-15-16-17-18-19-20-21-22-23-24-25-26-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100
 4. MUD LOG # 45-50 SECT. 10-710-15-16-17-18-19-20-21-22-23-24-25-26-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100
 5. MUD LOG # 45-50 SECT. 10-710-15-16-17-18-19-20-21-22-23-24-25-26-27-28-29-30-31-32-33-34-35-36-37-38-39-40-41-42-43-44-45-46-47-48-49-50-51-52-53-54-55-56-57-58-59-60-61-62-63-64-65-66-67-68-69-70-71-72-73-74-75-76-77-78-79-80-81-82-83-84-85-86-87-88-89-90-91-92-93-94-95-96-97-98-99-100

STOCK POINT ET ... I.D.F. ENGINEER ...
 * PHONE ... PHONE 766.0737 MOBILE # 10 10



International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 01/22/01
 REPORT No. 815
 SPUD DATE 01/19/01

WELL NAME W. 142nd St. at W. 155th St. LOCATION T-7-48

OPERATOR W. 142nd St. at W. 155th St. CONTRACTOR W. 142nd St. at W. 155th St.

REPORT FOR Mr. W. 142nd St. at W. 155th St. REPORT FOR Mr. W. 142nd St. at W. 155th St.

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/8"</u>	COND.	TANKS <u>45</u>	PUMP SIZE <u>114x446</u>	OPPOSITE D.P. <u>10</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>105</u>	m³/STK. <u>0.130</u>	OPPOSITE D.C.
DRILL COLLARS mm	INTER. <u>1.5-2-4</u>	TOTAL	S.P.M. <u>5</u>	PUMP PRESS. <u>4100</u>
OTHER	OTHER	STANDBY	m³/min. <u>10</u>	CIRC. TIME <u>150</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>CEL 1150</u>	FLOWLINE WT. kg/m³	MUD WT. <u>1150</u> kg/m³
HOLE COND. <u>1150</u>	UNDERFLOW WT. kg/m³	VISCOSITY <u>45</u> s/L
DEVIATION	OVERFLOW WT. kg/m³	FILTRATE cm³/30 min.
CURRENT OP. <u>1150</u>	UNDERFLOW RATE m³/min.	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>1150</u>	CEMENT	<u>551</u>		<u>443</u>	<u>4608</u>	<u>55000</u>
FLOWLINE TEMPERATURE (°C)	<u>45</u>	GEL	<u>337</u>	<u>38</u>	<u>395</u>	<u>38000</u>	
DENSITY (kg/m³)	<u>1150</u>	CEMENT	<u>146</u>	<u>4</u>	<u>145</u>	<u>17000</u>	
FUNNEL VISCOSITY (s/L)	<u>44</u>	CEMENT	<u>35</u>	<u>1</u>	<u>32</u>	<u>700</u>	
APPARENT VISCOSITY (mPa.s)	<u>745</u>						
PLASTIC VISCOSITY (mPa.s)	<u>7</u>						
YIELD POINT (Pa)	<u>45</u>						
GELS 0/10 min. (Pa)	<u>510</u>						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>140</u>						
FILTER CAKE (mm)	<u>20-25</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>210</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>50</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>800</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.0</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.0</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.0</u>	PREVIOUS COST	<u>41500</u>	STARTING VOLUME			
MBT (Kg/m³) <input type="checkbox"/> -1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>50</u>	DAILY COST	<u>10750</u>	VOL. BUILT <u>1150</u>			
ELECTRICAL STABILITY (V)	<u>-</u>	CUM. COST	<u>10750</u>	VOL. LOST ON SURFACE <u>-</u>			
OIL/WATER RATIO	<u>-</u>	CUM. ENG. COST	<u>75000</u>	VOL. LOST SUB SURFACE <u>-</u>			
CaCl₂ w/w%	<u>-</u>			END VOLUME <u>1150</u>			
"n"/"k" <u>100/1000</u>	<u>49/100</u>			CUM. VOL. BUILT <u>1150</u>			

COMMENTS:
 1. 1150 LBS OF GEL WAS ADDED TO THE MUD AT 10:00 AM ON 01/22/01.
 2. 100 LBS OF NaCl WAS ADDED TO THE MUD AT 10:00 AM ON 01/22/01.
 3. THE MUD DENSITY IS 1150 KG/M³ AND THE VISCOSITY IS 45 S/L.
 4. THE MUD IS BEING USED FOR DRILLING THE WELL TO A DEPTH OF 1150 METERS.
 5. THE MUD IS BEING USED FOR DRILLING THE WELL TO A DEPTH OF 1150 METERS.

STOCK POINT ST. NELSON I.D.F. ENGINEER RICHARD BROWN
 PHONE 500 800 0000 PHONE 500 800 0000 MOBILE 500 800 0000

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 02/01/1991
 REPORT No. 404
 SPUD DATE 11/29/91

WELL NAME W. NELSON LOCATION VT - T. 48
 OPERATOR W. NELSON CONTRACTOR W. NELSON
 REPORT FOR Mr. HAROLD ROSE REPORT FOR Mr. T. J. SIGNED

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE /# <u>149mm</u>	COND.	TANKS <u>55.0</u>	PUMP SIZE <u>114x41</u>	OPPOSITE D.P. <u>55</u>
DRILL PIPE <u>59</u> mm	SURFACE	HOLE <u>17.0</u>	m ³ /STK. <u>0.135</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>175 440</u>	TOTAL <u>115.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>11000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>1.5</u>	CIRC. TIME <u>150</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T. J. SIGNED</u>	FLOWLINE WT.	kg/m ³ MUD WT. <u>1150 1190</u> kg/m ³
HOLE COND. <u>11.5</u>	UNDERFLOW WT.	kg/m ³ VISCOSITY <u>40 5000</u> s/L
DEVIATION <u>T. J. SIGNED</u>	OVERFLOW WT.	kg/m ³ FILTRATE <u>1.1 1.0</u> cm ³ /30 min.
CURRENT OP. <u>T. J. SIGNED</u>	UNDERFLOW RATE	m ³ /min. pH <u>11.5 11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>7000</u>		CEL	215		11	25	100.00
FLOWLINE TEMPERATURE (°C) <u>25.0</u>		CELITE	128		5	126	40.00
DENSITY (kg/m ³) <u>1195</u>		CELITE	4291		179	4213	987.50
FUNNEL VISCOSITY (s/L) <u>6280</u>							
APPARENT VISCOSITY (mPa.s) <u>455</u>							
PLASTIC VISCOSITY (mPa.s) <u>30</u>							
YIELD POINT (Pa) <u>1250</u>							
GELS 0/10 min. (Pa) <u>714</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>11.5</u>							
FILTER CAKE (mm) <u>15 (100)</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>30</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L) <u>500</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>							
ELECTRICAL STABILITY (V)							
OIL/WATER RATIO <u>11.5/100</u>		PREVIOUS COST	15.000	STARTING VOLUME			
CaCl ₂ w/w% <u>6</u>		DAILY COST	114.775	VOL. BUILT	T. J. SIGNED		
"n"/"k" <u>1200</u>		CUM. COST	16.200	VOL. LOST on SURFACE			
		CUM. ENG. COST	1500.00	VOL. LOST SUB SURFACE			
				END VOLUME			
				CUM. VOL. BUILT			

COMMENTS: ALL TESTS WERE RUN AS FOLLOWS:
1. 500 cc of mud was taken for filtration at 10 min. at 100 psi.
2. Filtrate was 11.5 ml.
3. Filter cake was 15 mm (100).
4. Viscosity was 6280 s/L.

STOCK POINT VT NELSON I.D.F. ENGINEER T. J. SIGNED
 PHONE 508-238-1111 PHONE 508-238-1111 MOBILE # 508-238-1111

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 20.07.1991
 REPORT No. 405
 SPUD DATE 20.07.91

WELL NAME W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. LOCATION T. 49

OPERATOR W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. CONTRACTOR KENTING HO

REPORT FOR Mr. W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. REPORT FOR Mr. T. 49

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>140</u>	COND.	TANKS <u>5</u>	PUMP SIZE <u>111x40</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>59</u>	m ³ /STK. <u>135</u>	OPPOSITE D.C. <u>50</u>
DRILL COLLARS <u>100</u> mm	INTER. <u>100x443</u>	TOTAL <u>115</u>	S.P.M. <u>43</u>	PUMP PRESS. <u>12000</u>
OTHER	OTHER <u>100</u>	STANDBY	m ³ /min. <u>5004</u>	CIRC. TIME <u>190</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.</u>	FLOWLINE WT. kg/m ³	MUD WT. <u>1150</u> kg/m ³
HOLE COND. <u>W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.</u>	UNDERFLOW WT. kg/m ³	VISCOSITY <u>60</u> s/L
DEVIATION <u>W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.</u>	OVERFLOW WT. kg/m ³	FILTRATE <u>10</u> cm ³ /30 min.
CURRENT OP. <u>W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. PIT W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. MUD PROPERTIES: W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. MATERIALS INVENTORY & COST

TIME SAMPLE TAKEN	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>1000</u>	<u>W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.</u>			<u>47</u>		<u>575.00</u>
FLOWLINE TEMPERATURE (°C) <u>30.0</u>						
DENSITY (kg/m ³) <u>1.210</u>						
FUNNEL VISCOSITY (s/L) <u>15</u>						
APPARENT VISCOSITY (mPa.s) <u>34</u>						
PLASTIC VISCOSITY (mPa.s) <u>29</u>						
YIELD POINT (Pa) <u>5</u>						
GELS 0/10 min. (Pa) <u>315</u>						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>100</u>						
FILTER CAKE (mm) <u>1.5</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>30</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>300</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>						
MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>						
ELECTRICAL STABILITY (V)						
OIL/WATER RATIO <u>10/100</u>						
CaCl ₂ w/w% <u>5</u>						
"n"/"k" <u>100/200</u>						
PREVIOUS COST <u>11.200</u>						STARTING VOLUME
DAILY COST <u>5000</u>						VOL. BUILT <u>7.160113</u>
CUM. COST <u>12.900</u>						VOL. LOST ON SURFACE <u>4</u>
CUM. ENG. COST <u>15.750</u>						VOL. LOST SUB SURFACE <u>1.200</u>
						END VOLUME
						CUM. VOL. BUILT

COMMENTS: W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.

I AS SUPPLY OF YOUR STRENGTH CHEMICALS FOR WATER.
W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.

STOCK POINT W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. I.D.F. ENGINEER W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.

PHONE W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. PHONE W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100. MOBILE # W. 11. 12. 13. 14. 15. 16. 17. 18. 19. 20. 21. 22. 23. 24. 25. 26. 27. 28. 29. 30. 31. 32. 33. 34. 35. 36. 37. 38. 39. 40. 41. 42. 43. 44. 45. 46. 47. 48. 49. 50. 51. 52. 53. 54. 55. 56. 57. 58. 59. 60. 61. 62. 63. 64. 65. 66. 67. 68. 69. 70. 71. 72. 73. 74. 75. 76. 77. 78. 79. 80. 81. 82. 83. 84. 85. 86. 87. 88. 89. 90. 91. 92. 93. 94. 95. 96. 97. 98. 99. 100.

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 12/10/91
 REPORT No. 704
 SPUD DATE 12/20/91

WELL NAME W. 121.111.111.111 LOCATION W. 12. 45

OPERATOR INTERNATIONAL DRILLING FLUIDS CORPORATION CONTRACTOR VENTURA #007
 REPORT FOR Mr. HAROLD D. ... REPORT FOR Mr. T. ...

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>114.3</u>	COND.	TANKS <u>55.17</u>	PUMP SIZE <u>114.3</u>	OPPOSITE D.P. <u>4/4</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>60</u>	m ³ /STK. <u>0.158</u>	OPPOSITE D.C. <u>77</u>
DRILL COLLARS <u>1.75</u> mm	INTER. <u>100.443</u>	TOTAL <u>115.17</u>	S.P.M. <u>38</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>0.5744</u>	CIRC. TIME <u>7.30</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>7</u>	FLOWLINE WT. <u>1.195</u> kg/m ³	MUD WT. <u>1.195</u> kg/m ³
HOLE COND. <u>2515</u>	UNDERFLOW WT. kg/m ³	VISCOSITY <u>10.5</u> s/L
DEVIATION <u>PP-T-2515</u>	OVERFLOW WT. kg/m ³	FILTRATE <u>10</u> cm ³ /30 min.
CURRENT OP. <u>...</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2515</u>	<u>2515</u>		<u>661</u>	<u>717</u>				
FLOWLINE TEMPERATURE (°C)	<u>75.0</u>	<u>75.0</u>		<u>CRUDE</u>	<u>5147</u>		<u>188</u>	<u>5.50</u>	<u>1100.00</u>
DENSITY (kg/m ³)	<u>1.200</u>	<u>1.195</u>							
FUNNEL VISCOSITY (s/L)	<u>68</u>	<u>75</u>							
APPARENT VISCOSITY (mPa.s)	<u>775</u>								
PLASTIC VISCOSITY (mPa.s)	<u>77</u>								
YIELD POINT (Pa)	<u>3450</u>	<u>55</u>							
GELS 0/10 min. (Pa)	<u>714</u>								
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10</u>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>10</u>								
FILTER CAKE (mm)	<u>1.5</u>								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>81.9</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>40</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>85</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.07</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.75</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>9.75</u>			PREVIOUS COST	<u>16.00</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>75</u>			DAILY COST	<u>1100.00</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>-</u>			CUM. COST	<u>18.00</u>	VOL. LOST on SURFACE	<u>1.17</u>		
OIL/WATER RATIO	<u>0</u>			CUM. ENG. COST	<u>17.50</u>	VOL. LOST SUB SURFACE	<u>1.17</u>		
CaCl ₂ w/w%	<u>5</u>					END VOLUME			
"n"/"k"	<u>10/100</u>					CUM. VOL. BUILT			

COMMENTS: 1. 12/10/91 2. 12/10/91 3. 12/10/91

1. 12/10/91 2. 12/10/91 3. 12/10/91

1. 12/10/91 2. 12/10/91 3. 12/10/91

STOCK POINT FT. HENRY I.D.F. ENGINEER ...
 PHONE ... PHONE ... MOBILE ...

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 11/10/91
 REPORT No. 807
 SPUD DATE 08/26/91

WELL NAME WELL 1212 FT 01 KAZANDELE LOCATION WT 7-418

OPERATOR WELL 1212 GAS DEVELOPMENT CONTRACTOR KENTING #07

REPORT FOR Mr. _____ REPORT FOR Mr. T. J. SIGNED

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>63.0</u>	PUMP SIZE <u>114 x 4.1</u>	OPPOSITE D.P. <u>59</u>
DRILL PIPE <u>59</u> mm	SURFACE	HOLE <u>12.0</u>	m ³ /STK. <u>0.38</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>44.0</u>	TOTAL <u>173.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>11000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>19</u>	CIRC. TIME <u>180</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WATER BASE</u>	FLOWLINE WT. <u>1190</u> kg/m ³			MUD WT. <u>1190</u> kg/m ³	
HOLE COND. <u>0.1</u>	UNDERFLOW WT.			VISCOSITY <u>55.15</u> s/L	
DEVIATION <u>0.1</u>	OVERFLOW WT.			FILTRATE <u>10</u> cm ³ /30 min.	
CURRENT OP. <u>35.0</u>	UNDERFLOW RATE			pH <u>10.5</u>	

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2515</u>		<u>651</u>	<u>363</u>		<u>75</u>	<u>338</u>	<u>750.00</u>
FLOWLINE TEMPERATURE (°C)	<u>35.0</u>		<u>1.2116</u>	<u>196</u>		<u>7</u>	<u>194</u>	<u>20.00</u>
DENSITY (kg/m ³)	<u>1190</u>		<u>5.0000</u>	<u>788</u>		<u>30</u>	<u>318</u>	<u>98.00</u>
FUNNEL VISCOSITY (s/L)	<u>65</u>							
APPARENT VISCOSITY (mPa.s)	<u>315</u>							
PLASTIC VISCOSITY (mPa.s)	<u>75</u>							
YIELD POINT (Pa)	<u>65</u>							
GELS 0/10 min. (Pa)	<u>315</u>							
pH STRIP <input type="checkbox"/> -METER <input type="checkbox"/>	<u>10.5</u>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>10.5</u>							
FILTER CAKE (mm)	<u>1.5</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>40</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>200</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.5</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.7</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.5</u>		PREVIOUS COST	<u>15.000</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>70</u>		DAILY COST	<u>4.500</u>	VOL. BUILT			<u>7.12</u>
ELECTRICAL STABILITY (V)	<u>-</u>		CUM. COST	<u>15.450</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO	<u>1.0</u>		CUM. ENG. COST	<u>307.000</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w%	<u>4</u>				END VOLUME			<u>1.00</u>
"n"/"k"	<u>1.0/0.5</u>				CUM. VOL. BUILT			<u>7.12</u>

COMMENTS:
AS SAMPLED BY THE TESTER...
...

STOCK POINT FT ST TOWN I.D.F. ENGINEER ...
 PHONE ... PHONE ... MOBILE # ...

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 11/11/1991
 REPORT No. 419
 SPUD DATE 08/19/91

WELL NAME W. 121.2 ST. 167 AIR LIFT LOCATION ST. 115

OPERATOR W. 121.2 ST. 167 AIR LIFT CONTRACTOR KEITH'S HOD

REPORT FOR Mr. W. 121.2 ST. 167 AIR LIFT REPORT FOR Mr. W. 121.2 ST. 167 AIR LIFT

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>12.0</u>	PUMP SIZE <u>114 x 101</u>	OPPOSITE D.P. <u>45</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>10.0</u>	m ³ /STK. <u>0.125</u>	OPPOSITE D.C. <u>79</u>
DRILL COLLARS <u>70</u> mm	INTER. <u>100.000</u>	TOTAL <u>12.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>7000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>5000</u>	CIRC. TIME <u>700</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>W. 121.2 ST. 167 AIR LIFT</u>	FLOWLINE WT. <u>12.0</u> kg/m ³	MUD WT. <u>1190.000</u> kg/m ³
HOLE COND. <u>W. 121.2 ST. 167 AIR LIFT</u>	UNDERFLOW WT.	VISCOSITY <u>70.90</u> s/L
DEVIATION <u>W. 121.2 ST. 167 AIR LIFT</u>	OVERFLOW WT.	FILTRATE <u>10.0</u> cm ³ /30 min.
CURRENT OP. <u>W. 121.2 ST. 167 AIR LIFT</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>04:30</u>							
PRESENT DEPTH (m) <u>3540</u>							
FLOWLINE TEMPERATURE (°C) <u>37.0</u>							
DENSITY (kg/m ³) <u>1200</u>							
FUNNEL VISCOSITY (s/L) <u>90</u>							
APPARENT VISCOSITY (mPa.s) <u>45</u>							
PLASTIC VISCOSITY (mPa.s) <u>30</u>							
YIELD POINT (Pa) <u>10</u>							
GELS 0/10 min. (Pa) <u>10</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>10.0</u>							
FILTER CAKE (mm) <u>1.5</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)							
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>40</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>1000</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>							
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>							
ELECTRICAL STABILITY (V)							
OIL/WATER RATIO <u>10/100</u>							
CaCl ₂ w/w% <u>10/100</u>							
"n"/"k" <u>10/100</u>							
PREVIOUS COST	<u>19405</u>	STARTING VOLUME					
DAILY COST	<u>9000</u>	VOL. BUILT	<u>710.10</u>				
CUM. COST	<u>19305</u>	VOL. LOST ON SURFACE					
CUM. ENG. COST	<u>2750</u>	VOL. LOST SUB SURFACE					
		END VOLUME	<u>6400</u>				
		CUM. VOL. BUILT					

COMMENTS:

KEEP IN LINE & STAY FOR 10 MINUTES AT 3540
THE TO 10 MINUTES
KEEP THE MUD AT 1100 LBS PER CU YD
WHICH IS ABOUT 10 STPM & 4000 TO 10000 PSI

STOCK POINT ST 115 I.D.F. ENGINEER KEITH'S HOD
 PHONE 500 1000 PHONE 500 1000 MOBILE # 500 1000

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 04/12/91
REPORT No. 1109
SPUD DATE 04/12/91

WELL NAME ... LOCATION ... OPERATOR ... CONTRACTOR ... REPORT FOR Mr. ...

Table with 5 columns: ASSEMBLY, CASING, MUD Vol. (m³), PUMP OUTPUT, ANNULAR VEL. m./min. Includes rows for BIT SIZE, DRILL PIPE, DRILL COLLARS, OTHER.

Table with 3 columns: HOLE DATA, DESANDER/DESTILTER, DRILLING FLUID SPECIFICATIONS. Includes rows for MUD TYPE, HOLE COND., DEVIATION, CURRENT OP., FLOWLINE WT., UNDERFLOW WT., OVERFLOW WT., UNDERFLOW RATE, MUD WT., VISCOSITY, FILTRATE, pH.

EQUIPMENT: [] DEGASSER [] DESILTER [] DESANDER [] CENTRIFUGE [] DOUBLE DECK OR HIGH SPEED SHAKER

Table with 10 columns: TIME SAMPLE TAKEN, PRESENT DEPTH (m), FLOWLINE TEMPERATURE (°C), DENSITY (kg/m³), FUNNEL VISCOSITY (s/L), APPARENT VISCOSITY (mPa.s), PLASTIC VISCOSITY (mPa.s), YIELD POINT (Pa), GELS 0/10 min. (Pa), pH STRIP [] METER [], FILTRATE [] API [] HT HP (cm³), FILTER CAKE (mm), ALK [] (PF/MF) [] (PM/LIME), TOTAL HARDNESS [] Ca [] (mg/L), SAL [] NaCl [] Cl [] (mg/L), SAND CONTENT (%) [] (Ø) [], SOLIDS CONTENT (%) [] (Ø) [], OIL/WATER CONT. (%) [] (Ø) [], MBT (Kg/m³) [] /% [] OIL RET [], ELECTRICAL STABILITY (V), OIL/WATER RATIO (H-100), CaCl₂ w/w%, "n"/"k". Includes MATERIALS INVENTORY & COST sub-table.

COMMENTS: I KEPT A ... TO ...

STOCK POINT ... I.D.F. ENGINEER ... PHONE ... MOBILE-# ...



International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 02/17/1991
 REPORT No. 3110
 SPUD DATE 02/17/91

WELL NAME W. 114 N. 10 E. 10 S. 10 T. 42 R. 10 E. LOCATION W. 114 N. 10 E. 10 S. 10 T. 42 R. 10 E.

OPERATOR W. 114 N. 10 E. 10 S. 10 T. 42 R. 10 E. CONTRACTOR KENTING BOY
 REPORT FOR Mr. ALVIN D. BOY REPORT FOR Mr. TIM SIKNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE # <u>1 1/2 - 11.000</u>	COND.	TANKS <u>15.0</u>	PUMP SIZE <u>114x400</u>	OPPOSITE D.P. <u>49</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>15.0</u>	m ³ /STK. <u>0.75</u>	OPPOSITE D.C. <u>55</u>
DRILL COLLARS <u>17</u> mm	INTER. <u>5.000</u>	TOTAL <u>15.0</u>	S.P.M. <u>45</u>	PUMP PRESS. <u>9100</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>0.75</u>	CIRC. TIME

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>7 CE 11.000</u>	FLOWLINE WT. <u>100.00</u> kg/m ³	MUD WT. <u>1150</u> kg/m ³
HOLE COND. <u>1.000</u>	UNDERFLOW WT. <u>100.00</u> kg/m ³	VISCOSITY <u>75</u> s/L
DEVIATION <u>1.000</u>	OVERFLOW WT. <u>100.00</u> kg/m ³	FILTRATE <u>10.00</u> cm ³ /30 min.
CURRENT OP. <u>1.000</u>	UNDERFLOW RATE <u>100.00</u> m ³ /min.	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. PIT CHANGE! MUD PROPERTIES 1.000 MATERIALS INVENTORY & COST

TIME SAMPLE TAKEN	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>2500</u>	<u>100.00</u>	<u>4500</u>	<u>22</u>	<u>4079</u>	<u>4175</u>	<u>50</u>
FLOWLINE TEMPERATURE (°C) <u>30.0</u>						
DENSITY (kg/m ³) <u>1215</u>						
FUNNEL VISCOSITY (s/L) <u>125</u>						
APPARENT VISCOSITY (mPa.s) <u>575</u>						
PLASTIC VISCOSITY (mPa.s) <u>38</u>						
YIELD POINT (Pa) <u>145</u>						
GELS 0/10 min. (Pa) <u>216</u>						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>15.0</u>						
FILTER CAKE (mm) <u>18.000</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>111.0</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>40</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>800</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>						
MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>						
ELECTRICAL STABILITY (V) <u>-</u>						
OIL/WATER RATIO <u>0</u>						
CaCl ₂ w/w% <u>4</u>						
"n"/"k" <u>100/100</u>						

COMMENTS:

I KEEP A CLOSE WATCH ON THE MUD TO USE FOR A GOOD QUALITY OF MUDS?
FOR THE 10.5 - 11.0 LBS PER GALLON MUDS TO BE USED.

THANKS

STOCK POINT ET - T. 42 N. I.D.F. ENGINEER ALVIN D. BOY
 PHONE 503-251-1111 PHONE 503-251-1111 MOBILE # 503-251-1111

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE MAY 14 1991
 REPORT No. 417
 SPUD DATE 000 30 91

WELL NAME 1011212121212121212121 LOCATION WT. T. 48
 OPERATOR 1011212121212121212121 CONTRACTOR KENTING #07
 REPORT FOR Mr. HAROLD BURG REPORT FOR Mr. T. J. SIGNED

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>10 7/8</u>	COND.	TANKS <u>7000</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>6000</u>	m ³ /STK. <u>0178</u>	OPPOSITE D.C. <u>20</u>
DRILL COLLARS <u>150</u> mm	INTER. <u>105-3800</u>	TOTAL <u>10000</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>8000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>5904</u>	CIRC. TIME <u>300</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>7000</u>	FLOWLINE WT. <u>1190</u> kg/m ³	MUD WT. <u>1190-1200</u> kg/m ³
HOLE COND. <u>1.00</u>	UNDERFLOW WT. <u>100</u> kg/m ³	VISCOSITY <u>55</u> s/L
DEVIATION <u>1.00</u>	OVERFLOW WT. <u>100</u> kg/m ³	FILTRATE <u>10-15</u> cm ³ /30 min.
CURRENT OP.	UNDERFLOW RATE	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. PIT SURFACE MUD PROPERTIES SAVED MATERIALS INVENTORY & COST

TIME SAMPLE TAKEN	PRESENT DEPTH (m)	FLOWLINE TEMPERATURE (°C)	DENSITY (kg/m ³)	FUNNEL VISCOSITY (s/L)	APPARENT VISCOSITY (mPa.s)	PLASTIC VISCOSITY (mPa.s)	YIELD POINT (Pa)	GELS 0/10 min. (Pa)	pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	FILTER CAKE (mm)	ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	ELECTRICAL STABILITY (V)	OIL/WATER RATIO	CaCl ₂ w/w%	"n"/"k"	PREVIOUS COST	DAILY COST	CUM. COST	CUM. ENG. COST	STARTING VOLUME	VOL. BUILT	VOL. LOST on SURFACE	VOL. LOST SUB SURFACE	END VOLUME	CUM. VOL. BUILT	
<u>09:00</u>	<u>2740</u>	<u>42.00</u>	<u>1190</u>	<u>55</u>	<u>30</u>	<u>35</u>	<u>5</u>	<u>110</u>	<u>11.0</u>	<u>11.0</u>	<u>1.86000</u>	<u>1.5-11.3</u>	<u>30</u>	<u>800</u>	<u>100</u>	<u>10</u>	<u>10</u>	<u>50</u>	<u>-</u>	<u>-</u>	<u>1.5-11.3</u>	<u>5</u>	<u>10/200</u>	<u>10/200</u>	<u>3000</u>	<u>3000</u>	<u>7000</u>	<u>4800</u>	<u>3000</u>	<u>3000</u>	<u>3000</u>	<u>3000</u>	<u>3000</u>

COMMENTS:
I NEED A FINE LATER FOR A LAYER OF PIT GR...
IF WE CAN GET DOWN TO 50 SEED ...
IF WE CAN GET ...

T. H. SIGNED

STOCK POINT WT. T. TOWN I.D.F. ENGINEER Bill Pfeiffer
 PHONE 500 300 1111 PHONE 500 300 1111 MOBILE # 500 300 1111

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 01/15/91
 REPORT No. 4173
 SPUD DATE 001/29/91

WELL NAME CONCRETE VITRIFIED LOCATION VT - T - 418
 OPERATOR CONCRETE GAS DEVELOPMENT CONTRACTOR KEATING CO
 REPORT FOR Mr. ALBERT BURG - P.O. Box 100 REPORT FOR Mr. ALBERT BURG - P.O. Box 100

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>5 1/2</u>	COND.	TANKS <u>24</u>	PUMP SIZE <u>114X116</u>	OPPOSITE D.P. <u>55</u>
DRILL PIPE <u>50</u> mm	SURFACE	HOLE <u>57</u>	m³/STK. <u>0.128</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>120</u> mm	INTER. <u>2200</u>	TOTAL <u>1-9.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>-</u>
OTHER	OTHER	STANDBY	m³/min. <u>1.0</u>	CIRC. TIME <u>150-180</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT 1150+</u>	FLOWLINE WT. <u>1.150</u> kg/m³	MUD WT. <u>1150+</u> kg/m³
HOLE COND. <u>2200</u>	UNDERFLOW WT. <u>1.150</u> kg/m³	VISCOSITY <u>55</u> s/L
DEVIATION <u>2200</u>	OVERFLOW WT. <u>1.150</u> kg/m³	FILTRATE <u>10.17</u> cm³/30 min.
CURRENT OP. <u>2200</u>	UNDERFLOW RATE <u>1.150</u> m³/min.	pH <u>9.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2300</u>	<u>PACITE 4978</u>			<u>25</u>	<u>4943</u>	<u>4375.50</u>
FLOWLINE TEMPERATURE (°C)	<u>47.0</u>	<u>PLIANT 10</u>			<u>5</u>	<u>55</u>	<u>300.00</u>
DENSITY (kg/m³)	<u>1150</u>						
FUNNEL VISCOSITY (s/L)	<u>58</u>						
APPARENT VISCOSITY (mPa.s)	<u>78</u>						
PLASTIC VISCOSITY (mPa.s)	<u>70</u>						
YIELD POINT (Pa)	<u>5</u>						
GELS 0/10 min. (Pa)	<u>216</u>						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>140</u>						
FILTER CAKE (mm)	<u>2.0</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.3/2.1</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>7</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>500</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>100</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.5</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>95</u>						
MBT (Kg/m³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>50</u>						
ELECTRICAL STABILITY (V)	<u>-</u>						
OIL/WATER RATIO	<u>1</u>						
CaCl₂ w/w%	<u>7</u>						
"n"/"k"	<u>600/200</u>						
		PREVIOUS COST	<u>2000</u>	STARTING VOLUME			
		DAILY COST	<u>1375</u>	VOL. BUILT	<u>4.5</u>		
		CUM. COST	<u>3375</u>	VOL. LOST ON SURFACE			
		CUM. ENG. COST	<u>5750</u>	VOL. LOST SUB SURFACE			
				END VOLUME			
				CUM. VOL. BUILT			

COMMENTS: To drill vertical hole with 5 1/2 inch diameter. Mud weight 1150 kg/m³. Filtrate 10.17 cm³/30 min. pH 9.5. Viscosity 55 s/L. Yield point 5 Pa. Gels 0/10 min 216 Pa. Sand content 100%. Solids content 0.5%. Oil/water ratio 1.0. MBT 50 kg/m³. Electrical stability - V. CaCl₂ w/w% 7. "n"/"k" 600/200.

STOCK POINT ST. JOHNS I.D.F. ENGINEER ALBERT BURG
 PHONE 877-2700 PHONE 802-251-1000 MOBILE # 877-2700

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE NOV 11 1991
 REPORT No. 414
 SPUD DATE SEP 29 91

WELL NAME WELL 1015 FT 01 KITAUFELER LOCATION YR-T 48
 OPERATOR INTERNATIONAL DRILLING FLUIDS CORP CONTRACTOR WELTUNG 807
 REPORT FOR Mr. WOLFGANG RUCKENBERGER REPORT FOR Mr. WOLFGANG RUCKENBERGER

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/4</u>	COND.	TANKS <u>82.0</u>	PUMP SIZE <u>140x400</u>	OPPOSITE D.P. <u>53</u>
DRILL PIPE <u>80</u> mm	SURFACE	HOLE <u>52.0</u>	m³/STK. <u>0.179</u>	OPPOSITE D.C. <u>91</u>
DRILL COLLARS <u>150</u> mm	INTER. <u>5.0</u>	TOTAL <u>134.0</u>	S.P.M. <u>45</u>	PUMP PRESS. <u>17000</u>
OTHER	OTHER	STANDBY	m³/min. <u>6.71</u>	CIRC. TIME <u>715</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T 6511 170</u>	FLOWLINE WT. <u>40.0</u> kg/m³	MUD WT. <u>1150</u> kg/m³
HOLE COND. <u>R</u>	UNDERFLOW WT. <u>15.0</u> kg/m³	VISCOSITY <u>50.5</u> s/L
DEVIATION <u>1.0</u>	OVERFLOW WT. <u>0</u> kg/m³	FILTRATE <u>10.17</u> cm³/30 min.
CURRENT OP. <u>1.0</u>	UNDERFLOW RATE <u>0</u> m³/min.	pH <u>9.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2300</u>		<u>SARITE 4943</u>			<u>56.4573</u>		<u>875.00</u>
FLOWLINE TEMPERATURE (°C)	<u>25.0</u>	<u>42.0</u>						
DENSITY (kg/m³)	<u>1190</u>	<u>1190</u>						
FUNNEL VISCOSITY (s/L)	<u>56</u>	<u>90</u>						
APPARENT VISCOSITY (mPa.s)	<u>35</u>							
PLASTIC VISCOSITY (mPa.s)	<u>30</u>							
YIELD POINT (Pa)	<u>5</u>							
GELS 0/10 min. (Pa)	<u>711</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>11.5</u>	<u>10.5</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>175</u>							
FILTER CAKE (mm)	<u>700000</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>14121</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>700</u>							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>500</u>							
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.5</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>1.5</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>0.5</u>		PREVIOUS COST <u>170</u>			STARTING VOLUME		
MBT (Kg/m³) <input type="checkbox"/> 7% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>50</u>		DAILY COST <u>375.00</u>			VOL. BUILT		
ELECTRICAL STABILITY (V)	<u>-</u>		CUM. COST <u>7150.00</u>			VOL. LOST ON SURFACE		
OIL/WATER RATIO	<u>0</u>		CUM. ENG. COST <u>5675</u>			VOL. LOST SUB SURFACE		
CaCl₂ w/w%	<u>0.2</u>					END VOLUME		
"n"/"k" <u>600/300</u>	<u>50/200</u>					CUM. VOL. BUILT		

COMMENTS:
REFER TO I.D.F.C. REPORT # 17 FOR DETAILS OF MUD SYSTEM
1 FIGHTER BARRIER SYSTEM
THANKS

STOCK POINT RT 37 TONNA I.D.F. ENGINEER WOLFGANG RUCKENBERGER
 PHONE 500 000 000 PHONE 500 000 000 MOBILE 115 311



International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 91-05-17
 REPORT No. 15
 SPUD DATE 91-04-29

WELL NAME COLUMBIA #1 KATANFELEE LOCATION V-T-T-40

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING #7

REPORT FOR Mr. HAROLD ROSS / JOB TOOLS REPORT FOR Mr. PHILIP S. SMITH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1-1/2</u>	COND.	TANKS	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>45</u>
DRILL PIPE <u>69 mm</u>	SURFACE	HOLE	m ³ /STK. <u>0.118</u>	OPPOSITE D.C. <u>78</u>
DRILL COLLARS <u>120 mm</u>	INTER. <u>1775 / 2300</u>	TOTAL	S.P.M. <u>45</u>	PUMP PRESS.
OTHER	OTHER	STANDBY	m ³ /min. <u>5.0</u>	CIRC. TIME <u>330</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>GEL CAUSTIC</u>	FLOWLINE WT.	MUD WT. <u>1190</u> kg/m ³
HOLE COND.	UNDERFLOW WT.	VISCOSITY <u>55-55</u> s/L
DEVIATION	OVERFLOW WT.	FILTRATE <u>10-12</u> cm ³ /30 min.
CURRENT OP.	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>33:00</u>						
FLOWLINE TEMPERATURE (°C)	<u>-</u>						
DENSITY (kg/m ³)	<u>1185</u>						
FUNNEL VISCOSITY (s/L)	<u>48</u>						
APPARENT VISCOSITY (mPa.s)	<u>21</u>						
PLASTIC VISCOSITY (mPa.s)	<u>22</u>						
YIELD POINT (Pa)	<u>4</u>						
GELS 0/10 min. (Pa)	<u>112</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>104</u>						
FILTER CAKE (mm)	<u>2.0</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.4/3.2</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>12</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>750</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>18</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>27</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>23</u>	PREVIOUS COST	<u>21,554</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>65</u>	DAILY COST		VOL. BUILT			
ELECTRICAL STABILITY (V)		CUM. COST		VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>1:2.5</u>	<u>AKG.</u>	CUM. ENG. COST	<u>6000</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w%				END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS:

CONTROL WATER BY RT 1000 kg/m³ 11/4KITE.

MAINTAIN PH AT 10.5 USING CAUSTIC.

KEEP DO LOSS 4.0 FOR PH.

KEEP VS. AT 50-55 SL USING GEL.

STOCK POINT FT ST. JAMES I.D.F. ENGINEER JIM WHEELER

PHONE 765-4332 PHONE AT LOCATION MOBILE #



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-18
 REPORT No. 16
 SPUD DATE 91-04-29

WELL NAME <u>COLUMBIA 01 of KOTANEELEE</u>			LOCATION <u>Y-T-I-48</u>		
OPERATOR <u>COLUMBIA GAS DEVEL.</u>			CONTRACTOR <u>KENTING #7</u>		
REPORT FOR Mr. <u>POP. TOOLE</u>			REPORT FOR Mr. <u>PHIL JOSEPH WIRTH</u>		
ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.	
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>14 x 406</u>	OPPOSITE D.P.	
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>52</u>	m ³ /STK. <u>.018</u>	OPPOSITE D.C.	
DRILL COLLARS <u>120 mm</u>	INTER <u>177.8</u>	TOTAL <u>120</u>	S.P.M. <u>37</u>	PUMP PRESS.	
OTHER	OTHER	STANDBY	m ³ /min. <u>.436</u>	CIRC. TIME <u>200</u>	
HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>GEL CAUSTIC</u>	FLOWLINE WT.	kg/m ³	MUD WT. <u>1190</u>	kg/m ³	
HOLE COND. <u>OK.</u>	UNDERFLOW WT.	kg/m ³	VISCOSITY <u>50-55</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m ³	FILTRATE <u>12</u>	cm ³ /30 min.	
CURRENT OP. <u>P.R.</u>	UNDERFLOW RATE	m ³ /min.	pH <u>10.5</u>		
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input checked="" type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER					
SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>		MUD PROPERTIES		MATERIALS INVENTORY & COST	
TIME SAMPLE TAKEN <u>15:00</u>			MATERIALS	INITIAL	RECEIVED
PRESENT DEPTH (m) <u>3274</u>			<u>BARITE</u>		<u>35</u>
FLOWLINE TEMPERATURE (°C) <u>30</u>					<u>438</u>
DENSITY (kg/m ³) <u>1190</u>					
FUNNEL VISCOSITY (s/L) <u>62</u>					
APPARENT VISCOSITY (mPa.s) <u>36</u>					
PLASTIC VISCOSITY (mPa.s) <u>28</u>					
YIELD POINT (Pa) <u>8</u>					
GELS 0/10 min. (Pa) <u>3/3</u>					
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>				
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>12.6</u>				
FILTER CAKE (mm) <u>2.0</u>					
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.4/2.3</u>				
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>				
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	<u>750</u>				
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>TR.</u>				
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>27</u>				
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.93</u>		PREVIOUS COST <u>21,554</u>	STARTING VOLUME	
MBT (Kg/m ³) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>70</u>		DAILY COST <u>438</u>	VOL. BUILT	
ELECTRICAL STABILITY (V)	<u>-</u>		CUM. COST <u>21,992</u>	VOL. LOST ON SURFACE	
OIL/WATER RATIO <u>H₂O</u>	<u>NEG.</u>		CUM. ENG. COST <u>6375</u>	VOL. LOST SUB SURFACE	
CaCl ₂ w/w%				END VOLUME	
"n"/"k"				CUM. VOL. BUILT	
COMMENTS: <u>SET BRIDGE PLUG AT 3331 m</u>					
<u>SET WHIPSTOCK BACKLOG - 3277 m</u>					
<u>LOGGED - PAN IN TO PULL!</u>					
<u>HOLD DENSITY AT 1190 kg/m³ WITH BARITE.</u>					
<u>PH AT 10.5 WITH CAUSTIC.</u>					
<u>KEEP V.S. AT 50-55 SL USING GEL.</u>					
<u>RUN TO 1750S H₂O PER MIN.</u>					
STOCK POINT <u>FT. ST. JOHN</u>	I.D.F. ENGINEER <u>JIM WIELER</u>				
PHONE <u>785-4222</u>	PHONEM/ LOCATION		MOBILE #		

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-19
 REPORT No. 17
 SPUD DATE 71-04-27

WELL NAME COLUMBIA #1 KATANEELER LOCATION Y-J-E-48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING #7
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. PHIL ROSAMBERTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND.	TANKS <u>75</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52</u>	m ³ /STK. <u>0.118</u>	OPPOSITE D.C.
DRILL COLLARS <u>122</u> mm	INTER <u>177.81</u>	TOTAL <u>127</u>	S.P.M. <u>5</u>	PUMP PRESS <u>8715</u> psi
OTHER	OTHER	STANDBY	m ³ /min. <u>59</u>	CIRC. TIME <u>215 ±</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>GEL CAUSTIC</u>	FLOWLINE WT.	kg/m ³	MUD WT. <u>1190</u>	kg/m ³	
HOLE COND. <u>AGED</u>	UNDERFLOW WT.	kg/m ³	VISCOSITY <u>50-60</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m ³	FILTRATE <u>12</u>	cm ³ /30 min.	
CURRENT OP. <u>M.L.L.</u>	UNDERFLOW RATE	m ³ /min.	pH <u>11.0</u>		

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST				
TIME SAMPLE TAKEN	<u>05:00</u>	<u>23:30</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3274</u>	<u>3274</u>	<u>BARITE</u>			<u>70</u>		<u>875</u>
FLOWLINE TEMPERATURE (°C)	<u>35</u>	<u>37</u>						
DENSITY (kg/m ³)	<u>1195</u>	<u>1190</u>						
FUNNEL VISCOSITY (s/L)	<u>62</u>	<u>53</u>						
APPARENT VISCOSITY (mPa.s)	<u>39</u>	<u>35</u>						
PLASTIC VISCOSITY (mPa.s)	<u>30</u>	<u>28</u>						
YIELD POINT (Pa)	<u>9</u>	<u>7</u>						
GELS 0/10 min. (Pa)	<u>212</u>	<u>113</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>	<u>11.0</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>12.6</u>	<u>12.0</u>						
FILTER CAKE (mm)	<u>2.0</u>	<u>2.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.3/2.3</u>	<u>1.3/2.4</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>	<u>TR.</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>750</u>	<u>750</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>TR.</u>	<u>TR.</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>07</u>	<u>07</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>93</u>	<u>93</u>	PREVIOUS COST	<u>21,973</u>	STARTING VOLUME			
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>70</u>	<u>70</u>	DAILY COST	<u>875</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)	<u>-</u>	<u>-</u>	CUM. COST	<u>22,867</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>H₂O</u>	<u>NEG.</u>	<u>NEG.</u>	CUM. ENG. COST	<u>6750</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w%					END VOLUME			
"n"/"k"					CUM. VOL. BUILT			

COMMENTS: MILLING WINDDL
CONTROL DENSITY AT 1190 kg/m³ USING BARITE.
KEEP PH AT 11.0 WITH CAUSTIC.
HOLD VIS. AT 50-55 cP W/ GEL.
NOTE: IF VIS CLOUDS RUN WATER.

STOCK POINT FT. ST. TOWN I.D.F. ENGINEER TIM WILCOX
 PHONE 785-4222 PHONEDN LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-20
 REPORT No. 18
 SPUD DATE 91-05-29

WELL NAME COLUMBIA of KOTANEELEE LOCATION Y-J-5-4B
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING #7
 REPORT FOR Mr. BOB TROLE REPORT FOR Mr. PHIL BASCOMBORTH

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>87</u> mm	SURFACE	HOLE <u>52</u>	m³/STK. <u>.0118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120</u> mm	INTER. <u>171.8/3274</u>	TOTAL <u>122</u>	S.P.M. <u>40</u>	PUMP PRESS.
OTHER	OTHER	STANDBY	m³/min. <u>.473</u>	CIRC. TIME

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. GEL/CAUSTIC</u>	FLOWLINE WT.	MUD WT. <u>1190</u> kg/m³
HOLE COND. <u>CASED</u>	UNDERFLOW WT.	VISCOSITY <u>50-55</u> s/L
DEVIATION	OVERFLOW WT.	FILTRATE <u>12</u> cm³/30 min.
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>03:30</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3276</u>							
FLOWLINE TEMPERATURE (°C) <u>38</u>							
DENSITY (kg/m³) <u>1190</u>							
FUNNEL VISCOSITY (s/L) <u>53</u>							
APPARENT VISCOSITY (mPa.s) <u>35</u>							
PLASTIC VISCOSITY (mPa.s) <u>28</u>							
YIELD POINT (Pa) <u>7</u>							
GELS 0/10 min. (Pa) <u>113</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>11.0</u>							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³) <u>13.0</u>							
FILTER CAKE (mm) <u>2.0</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>1.3/2.4</u>							
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L) <u>750</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.001</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.07</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.93</u>		PREVIOUS COST	<u>22,867</u>	STARTING VOLUME			
MBT (Kg/m³) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>70</u>		DAILY COST	<u>-</u>	VOL. BUILT			
ELECTRICAL STABILITY (V)		CUM. COST	<u>22,867</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>H₂O</u> <u>NEG.</u>		CUM. ENG. COST	<u>7125</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w%				END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: MILLING

1 CONTROL DENSITY AT 1190 kg/m³ WITH BARITE.

2 PH AT 11.0 USING CAUSTIC.

3 HOLD VIS AT 50-55 s/L WIGEL.

NOTE: IF VIS. CLUMPS RUN H₂O

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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I.D.F.C.-015 (3)



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-21
 REPORT No. 19
 SPUD DATE 91-04-29

WELL NAME COLUMBIA #1 of KOTANELEE LOCATION Y-J-I-48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. BOB TADLE REPORT FOR Mr. PHIL ROSENBLUTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>52</u>	m ³ /STK. <u>.018</u>	OPPOSITE D.C.
DRILL COLLARS <u>120 mm</u>	INTER. <u>170/13274</u>	TOTAL <u>122</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>575.0 = 110</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.472</u>	CIRC. TIME <u>260</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. GEL/CAUSTIC</u>	FLOWLINE WT. kg/m ³	MUD WT. <u>1190</u> kg/m ³
HOLE COND.	UNDERFLOW WT. kg/m ³	VISCOSITY <u>50-55</u> s/L
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>12</u> cm ³ /30 min.
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>02:30</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>32.77</u>		<u>BARITE</u>			<u>35</u>		<u>438</u>
FLOWLINE TEMPERATURE (°C) <u>37</u>							
DENSITY (kg/m ³) <u>1190</u>							
FUNNEL VISCOSITY (s/L) <u>53</u>							
APPARENT VISCOSITY (mPa.s) <u>35</u>							
PLASTIC VISCOSITY (mPa.s) <u>28</u>							
YIELD POINT (Pa) <u>7</u>							
GELS 0/10 min. (Pa) <u>112</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>11.0</u>							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>13.0</u>							
FILTER CAKE (mm) <u>2.0</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>1.3/2.3</u>							
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>TR.</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CaCl ₂ (mg/L) <u>750</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.001</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.37</u>							
OIL WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/> <u>.93</u>		PREVIOUS COST <u>22.867</u>	STARTING VOLUME				
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>70</u>		DAILY COST <u>438</u>	VOL. BUILT				
ELECTRICAL STABILITY (V) <u>-</u>		CUM. COST <u>23305</u>	VOL. LOST ON SURFACE				
OIL/WATER RATIO <u>H₂O</u> <u>NEG.</u>		CUM. ENG. COST <u>7500</u>	VOL. LOST SUB SURFACE				
CaCl ₂ w/w%			END VOLUME				
"n"/"k"			CUM. VOL. BUILT				

COMMENTS: MILLING.

CONTROL DENSITY AT 1190 kg/m³ USING BARITE.

KEEP PH AT 11.0 WITH CAUSTIC.

HOLD VIS. AT 50-60 SL USING GEL.

IF VIS. CLIMBS OVER 60 SL RUN H₂O

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER
 PHONE 785-4222 PHONEAN LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-22
 REPORT No. 20
 SPUD DATE 91-04-29

WELL NAME <u>COLUMBIA #1 KATANSLEE</u>		LOCATION <u>Y J I - 48</u>		
OPERATOR <u>COLUMBIA GAS DEVEL.</u>		CONTRACTOR <u>KENTING HI-TOWER #7</u>		
REPORT FOR Mr. <u>BOB TOOLE</u>		REPORT FOR Mr. <u>PHIL BOSOMWORTH</u>		
ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>43</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>52</u>	m ³ /STK. <u>0118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120 mm</u>	INTER <u>178/3274</u>	TOTAL <u>122</u>	S.P.M. <u>43</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>1.507</u>	CIRC. TIME <u>240</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. B.L. CAUSTIC</u>	FLOWLINE WT.	kg/m ³	MUD WT. <u>1190</u>	kg/m ³	
HOLE COND. <u>CRSD</u>	UNDERFLOW WT.	kg/m ³	VISCOSITY <u>50-55</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m ³	FILTRATE <u>12</u>	cm ³ /30 min.	
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE	m ³ /min.	pH <u>10.5-11.0</u>		

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>09:30</u>				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3277</u>				<u>BARITE</u>			<u>70</u>		<u>875</u>
FLOWLINE TEMPERATURE (°C) <u>37</u>									
DENSITY (kg/m ³) <u>1195</u>									
FUNNEL VISCOSITY (s/L) <u>53</u>									
APPARENT VISCOSITY (mPa.s) <u>35</u>									
PLASTIC VISCOSITY (mPa.s) <u>28</u>									
YIELD POINT (Pa) <u>7</u>									
GELS 0/10 min. (Pa) <u>113</u>									
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>10.5</u>									
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>12.8</u>									
FILTER CAKE (mm) <u>2.0</u>									
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>1.0/2.0</u>									
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>									
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L) <u>700</u>									
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> <u>0.01</u>									
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> <u>0.75</u>									
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input type="checkbox"/> <u>925</u>				PREVIOUS COST <u>23,305</u>	STARTING VOLUME				
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>70</u>				DAILY COST <u>875</u>	VOL. BUILT				
ELECTRICAL STABILITY (V) <u>-</u>				CUM. COST <u>24,180</u>	VOL. LOST ON SURFACE				
OIL/WATER RATIO <u>H₂O</u> <u>NEG.</u>				CUM. ENG. COST <u>7875</u>	VOL. LOST SUB SURFACE				
CaCl ₂ w/w% <u>-</u>					END VOLUME				
"n"/"k" <u>-</u>					CUM. VOL. BUILT				

COMMENTS: MILLING Runs. UP 100 MIN.

HOLD DENSITY AT 1190 Kg/m³ WITH BARITE.

KEEP PH AT 10.5-11.0 USING CAUSTIC.

CONTROL VISC. AT 50-55 SLU W/ GEL.

NOTE: IF VISC. COMBS OVER 60 SLU RUN H₂O.

STOCK POINT PT. ST. JOHN I.D.F. ENGINEER TIM WIELER

PHONE 785-4225 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-23
 REPORT No. 21
 SPUD DATE 91-04-29

WELL NAME COLUMBIA of ROTANGETEE LOCATION VJI-48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING HI-TOWER #7
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. PHIL BOSOMWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1</u>	COND. <u>OK</u>	TANKS <u>75</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>44</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>53</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C.
DRILL COLLARS <u>120</u> mm	INTER <u>170/13274</u>	TOTAL <u>137</u>	S.P.M. <u>45</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.531</u>	CIRC. TIME <u>240</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. GEL CAUSTIC</u>	FLOWLINE WT. <u>1190</u> kg/m ³	MUD WT. <u>1190</u> kg/m ³
HOLE COND. <u>OK</u>	UNDERFLOW WT. <u>50-55</u> s/L	VISCOSITY <u>50-55</u> s/L
DEVIATION	OVERFLOW WT. <u>12</u> cm ³ /30 min.	FILTRATE <u>12</u> cm ³ /30 min.
CURRENT OP. <u>MILLING</u>	UNDERFLOW RATE <u>10.5-11.0</u> pH	pH <u>10.5-11.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>07:00</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3279</u>		<u>BARITE</u>			<u>70</u>		<u>875</u>
FLOWLINE TEMPERATURE (°C) <u>38</u>		<u>GEL</u>			<u>25</u>		<u>250</u>
DENSITY (kg/m ³) <u>1205</u>		<u>CAUSTIC</u>			<u>1</u>		<u>30</u>
FUNNEL VISCOSITY (s/L) <u>57</u>							
APPARENT VISCOSITY (mPa.s) <u>41</u>							
PLASTIC VISCOSITY (mPa.s) <u>32</u>							
YIELD POINT (Pa) <u>9</u>							
GELS 0/10 min. (Pa) <u>2/3</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>12.0</u>						
FILTER CAKE (mm) <u>2.0</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.1/2.2</u>						
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>650</u>						
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.000</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.08</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.92</u>	PREVIOUS COST	<u>24,180</u>	STARTING VOLUME			
MBT (Kg/m ³) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>75</u>	DAILY COST	<u>1155</u>	VOL. BUILT			
ELECTRICAL STABILITY (V) <u>-</u>		CUM. COST	<u>25,335</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>H:1</u>	<u>NEG.</u>	CUM. ENG. COST	<u>6,250</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w%				END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: MILLING. STIMS. UP - 100 MIN.

1) CONTROL DENSITY AT 1190 kg/m³ USING BARITE.

2) KEEP PH AT 10.5-11.0 WITH CAUSTIC.

3) HOLD VIS. AT 50-55 s/L w/GEL.

4) RUN 15 LITRES H₂O PER MIN. IF VIS. OVER 60 s/L.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 9-05-24
 REPORT No. 23
 SPUD DATE 01-04-29

WELL NAME COLUMBIA 01 of KOTANDELES LOCATION N.T. 1-42
 OPERATOR COLUMBIA GAS FIELD CONTRACTOR KENTING - HT #7
 REPORT FOR Mr. Tom Todd REPORT FOR Mr. Tom M. Smith

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/8 / 152</u>	COND.	TANKS	PUMP SIZE <u>110 x 406</u>	OPPOSITE D.P.
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE	m ³ /STK. <u>0.18</u>	OPPOSITE D.C.
DRILL COLLARS <u>130 mm</u>	INTER. <u>178/374</u>	TOTAL	S.P.M.	PUMP PRESS.
OTHER	OTHER	STANDBY	m ³ /min.	CIRC. TIME

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. GEL/CAUSTIC</u>	FLOWLINE WT. kg/m ³	MUD WT. <u>1190</u> kg/m ³
HOLE COND.	UNDERFLOW WT. kg/m ³	VISCOSITY <u>45-50</u> s/L
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u><10</u> cm ³ /30 min.
CURRENT OP. <u>PLC</u>	UNDERFLOW RATE m ³ /min.	pH <u>10</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES <u>(04:25)</u>		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	16:20	10:10 04:30	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	3290	3290	KARITE			25		300
FLOWLINE TEMPERATURE (°C)	37	—	GEL			10		100
DENSITY (kg/m ³)	1310	1010						
FUNNEL VISCOSITY (s/L)	60	42						
APPARENT VISCOSITY (mPa.s)	114	74						
PLASTIC VISCOSITY (mPa.s)	30	2						
YIELD POINT (Pa)	10	6						
GELS 0/10 min. (Pa)	212	112						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	10.5	10.0						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	12.4	10.0						
FILTER CAKE (mm)	3.0	.05						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	1.0/2.1	.55/1.85						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	98	—						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	600	300						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	TR.	—						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	.086	—						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	.715	—	PREVIOUS COST	25.230	STARTING VOLUME			
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	.75	—	DAILY COST	400	VOL. BUILT			
ELECTRICAL STABILITY (V)	1	—	CUM. COST	25.75	VOL. LOST on SURFACE			
OIL/WATER RATIO <u>H.C</u>	14.6	—	CUM. ENG. COST	8125	VOL. LOST SUB SURFACE			
CaCl ₂ w/w%					END VOLUME			
"n"/"k"					CUM. VOL. BUILT			

COMMENTS: DRILLED 153 m HOLE TO 3290 m.
SAW LEAK OFF TEST DUMPED TANKS TO MIX PUMPED SYSTEM.

ADD 2 SL. SPM WITH + MIX TANKS AT 15 MIN. SO TO OBTAIN 11.5
45-50 S/L
ADD 3 TANKS TOTAL AT 30 MIN. TOTAL.
MIX PARTS TO RAISE DENSITY TO 1300 kg/m³ 15 MIN.

STOCK POINT ST. JOHN I.D.F. ENGINEER Tom M. Smith
 PHONE 785-4222 PHONE at location MOBILE #



International Drilling Fluids Corporation

DRILLING FLUID REPORT

DATE 91-05-25
 REPORT No. 23
 SPUD DATE 91-04-29

WELL NAME COLUMBIA AT 1 PARALLEL

LOCATION V.T. I-42

OPERATOR COLUMBIA GAS SVCS.

CONTRACTOR KENTON H.T. #7

REPORT FOR Mr. Bob Taylor

REPORT FOR Mr. PHILIP M. BERTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/8 / 153</u>	COND. <u>174/2574</u>	TANKS <u>50</u>	PUMP SIZE <u>110 x 406</u>	OPPOSITE D.P. <u>49</u>
DRILL PIPE <u>89 mm</u>	SURFACE <u>174/2574</u>	HOLE <u>45</u>	m ³ /STK. <u>0.112</u>	OPPOSITE D.C. <u>110 x 110</u>
DRILL COLLARS <u>120 mm</u>	INTER.	TOTAL <u>95</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>59</u>	CIRC. TIME <u>165"</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>POLYMER</u>	FLOWLINE WT. kg/m ³	MUD WT. <u>1190-1200</u> kg/m ³
HOLE COND.	UNDERFLOW WT. kg/m ³	VISCOSITY <u>45-50</u> s/L
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>410-</u> cm ³ /30 min.
CURRENT OP. <u>DRILL</u>	UNDERFLOW RATE m ³ /min.	pH <u>10-10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> DPIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN	PRESENT DEPTH (m)	FLOWLINE TEMPERATURE (°C)	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
	<u>23:00</u>	<u>3300</u>	<u>22</u>	<u>BARITE</u>	<u>4500</u>		<u>200</u>	<u>3060</u>	<u>8750</u>
			<u>1185</u>	<u>GEL</u>	<u>305</u>			<u>305</u>	
			<u>40</u>	<u>CAUSTIC</u>	<u>100</u>		<u>3</u>	<u>187</u>	<u>90</u>
			<u>16</u>	<u>RICAR</u>	<u>50</u>			<u>55</u>	
			<u>10</u>	<u>FLUOR</u>	<u>260</u>		<u>10</u>	<u>250</u>	<u>49</u>
			<u>6</u>	<u>SILIC</u>	<u>26</u>			<u>96</u>	
			<u>212</u>	<u>SP-721</u>	<u>30</u>		<u>2</u>	<u>36</u>	<u>78</u>
			<u>10.0</u>	<u>FLR</u>	<u>40</u>		<u>2</u>	<u>40</u>	<u>380</u>
			<u>11.0</u>	<u>SP-721</u>	<u>80</u>		<u>8</u>	<u>70</u>	<u>800</u>
			<u>05</u>	<u>SP-721</u>	<u>30</u>			<u>30</u>	
			<u>50/80</u>	<u>FLR</u>	<u>80</u>		<u>4</u>	<u>76</u>	<u>128</u>
			<u>10.</u>	<u>EDS</u>	<u>80</u>		<u>13</u>	<u>67</u>	<u>5400</u>
			<u>150</u>						
			<u>0.01</u>						
			<u>0.45</u>						
			<u>985</u>						
			<u>—</u>	PREVIOUS COST	<u>25,735</u>	STARTING VOLUME			
				DAILY COST	<u>19,435</u>	VOL. BUILT			
				CUM. COST	<u>41,370</u>	VOL. LOST ON SURFACE			
				CUM. ENG. COST	<u>2,000</u>	VOL. LOST SUB SURFACE			
						END VOLUME			
						CUM. VOL. BUILT			

COMMENTS: DRILL 152" HOLE DISPLACED HOLE TO POLYMER SYSTEM
AT 3000 m
CONTROL VISCOSITY AT 1180 kg/m³ USING BARITE (2-3 ml/sk)
KEEP PH AT 10-10.5 WITH CAUSTIC (2-3 ml/sk)
HOLD VISC. AT 40-45 SL. USE FLUOR INJ. P, RSP-721 + FLR.
IF VISC. DROPS BELOW 40 SL. ADD 5 SL. INJ. P
ADD 2-3 GALL. RSP-721 EVERY 10 HR.
CONTROL FLUID LOSS USING FLR 4 SL/CIR.
RUN 10-15 LITRES H. 150 MIN.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER TIM WELER
 PHONE 705-432-9400 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-26
 REPORT No. 24
 SPUD DATE 91-04-29

WELL NAME COLUMBIA of KOTANEELER LOCATION V.T. I-48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. # 7
 REPORT FOR Mr. EAR TOOLE REPORT FOR Mr. PHIL BASHMORTH

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>64</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>49</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>46</u>	m³/STK. <u>.0118</u>	OPPOSITE D.P. <u>BTMS VP=75</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>12A/3213</u>	TOTAL <u>110</u>	S.P.M.	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m³/min. <u>.59</u>	CIRC. TIME <u>180±</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>POLYMER</u>	FLOWLINE WT.	MUD WT. <u>1150 - 1180</u> kg/m³
HOLE COND. <u>OK.</u>	UNDERFLOW WT.	VISCOSITY <u>36 - 45</u> s/L
DEVIATION	OVERFLOW WT.	FILTRATE <u>< 12</u> cm³/30 min.
CURRENT OP. <u>DRG.</u>	UNDERFLOW RATE	pH <u>10 - 10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>14:30</u>	PRESENT DEPTH (m) <u>3390</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
FLOWLINE TEMPERATURE (°C) <u>44</u>	DENSITY (kg/m³) <u>1190</u>	<u>BARITE</u>	<u>3868</u>		<u>205</u>	<u>3663</u>	<u>2562</u>
FUNNEL VISCOSITY (s/L) <u>39</u>	APPARENT VISCOSITY (mPa.s) <u>20</u>	<u>GEL</u>	<u>325</u>			<u>305</u>	
PLASTIC VISCOSITY (mPa.s) <u>10</u>	YIELD POINT (Pa) <u>10</u>	<u>CAUSTIC</u>	<u>147</u>			<u>187</u>	
GELS 0/10 min. (Pa) <u>2/3</u>	pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>10.0</u>	<u>DUST</u>	<u>350</u>			<u>250</u>	
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³) <u>8.0</u>	FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm³) <u>8.0</u>	<u>ASP-721</u>	<u>72</u>		<u>3</u>	<u>69</u>	<u>300</u>
FILTER CAKE (mm) <u>.05</u>	ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>40/70</u>	<u>X.C.D.E</u>	<u>40</u>			<u>40</u>	
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>	SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>150</u>	<u>FLR</u>	<u>76</u>		<u>4</u>	<u>72</u>	
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> <u>.002</u>	SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> <u>.06</u>	<u>EDV'S D</u>	<u>67</u>		<u>11</u>	<u>56</u>	<u>4620</u>
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> <u>.94</u>	MBT (Kg/m³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>SOD. SULF.</u>	<u>30</u>		<u>2</u>	<u>28</u>	<u>100</u>
ELECTRICAL STABILITY (V) <u>H₂S</u> <u>NEG.</u>	ASPH/WATER RATIO <u>POLYMER</u> <u>.75</u>	<u>DEFORMER</u>	<u>20</u>		<u>2</u>	<u>18</u>	<u>213</u>
CaCl ₂ w/w% <u>-</u>	"n"/"k" <u>-</u>	<u>PTS-200</u>	<u>64</u>		<u>1</u>	<u>63</u>	<u>260</u>
PREVIOUS COST <u>41,370</u>	DAILY COST <u>8115</u>	CUM. COST <u>49,485</u>	CUM. ENG. COST <u>4375</u>	STARTING VOLUME	VOL. BUILT	VOL. LOST ON SURFACE	VOL. LOST SUB SURFACE
				END VOLUME	CUM. VOL BUILT		

COMMENTS: DRG. 152 mm HOLE.
ALLOW DENSITY TO DROP BACK TO 1150 kg/m³.
KEEP PH AT 10-10.5 USING CAUSTIC. 2 SX. 1 CR.
CONTROL V.S. AT 36-42 S/L WITH ADJUS + ASP-721. ADD 2 PALS ASP-721 EVERY 12 HRS. WHILE DRG. ADD SLOWLY.
RUN 10-15 LITRES H₂O PER MIN.
MIX 2 SX. SOD. SULFITE DAILY. ADD TO H₂O IN CHEM. BDL * TOP W DIESEL.
 STOCK POINT FT. ST. JOHN I.D.F. ENGINEER TIM WIELER
 PHONE 785-4330 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-27
 REPORT No. 25
 SPUD DATE 91-04-29

WELL NAME COLUMBIA of al KOTAMELEE LOCATION Y.T. I-48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. PAUL TOBLE REPORT FOR Mr. PHIL CASOM WORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>152</u>	COND.	TANKS <u>70</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE <u>47B/3273</u>	HOLE <u>47</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>BTM. # 75</u>
DRILL COLLARS <u>120 mm</u>	INTER.	TOTAL <u>117</u>	S.P.M. <u>53</u>	PUMP PRESS. <u>11,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.62</u>	CIRC. TIME <u>195</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>POLYMER</u>	FLOWLINE WT.	kg/m ³ MUD WT. <u>1180</u> kg/m ³
HOLE COND. <u>OK.</u>	UNDERFLOW WT.	kg/m ³ VISCOSITY <u>35.40</u> s/L
DEVIATION	OVERFLOW WT.	kg/m ³ FILTRATE <u>12</u> cm ³ /30 min.
CURRENT OP. <u>DRILG.</u>	UNDERFLOW RATE	m ³ /min. pH <u>10-10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>23:30</u>		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3354</u>		BARITE	<u>3663</u>			<u>3663</u>	
FLOWLINE TEMPERATURE (°C) <u>44</u>		CAUSTIC	<u>187</u>		<u>2</u>	<u>185</u>	<u>60</u>
DENSITY (kg/m ³) <u>1190</u>		ASP 721	<u>69</u>		<u>1</u>	<u>68</u>	<u>100</u>
FUNNEL VISCOSITY (s/L) <u>37</u>		SOD. SUL.	<u>28</u>		<u>2</u>	<u>26</u>	<u>100</u>
APPARENT VISCOSITY (mPa.s) <u>20</u>							
PLASTIC VISCOSITY (mPa.s) <u>10</u>							
YIELD POINT (Pa) <u>10</u>							
GELS 0/10 min. (Pa) <u>213</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> <u>10.5</u>							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>8.0</u>							
FILTER CAKE (mm) <u>.25</u>							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>.45/1.95</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L) <u>TR.</u>							
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L) <u>150</u>							
SAND CONTENT (%) <input type="checkbox"/> (20) <u>.003</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (20) <u>.07</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (20) <u>.93</u>		PREVIOUS COST	<u>49,485</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>		DAILY COST	<u>260</u>	VOL. BUILT			
ELECTRICAL STABILITY (V) <u>H₂O</u> <u>NEG.</u>		CUM. COST	<u>49,745</u>	VOL. LOST on SURFACE			
OIL/WATER RATIO <u>—</u>		CUM. ENG. COST	<u>9750</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w% <u>ASP POLYMER</u> <u>1.1</u>				END VOLUME			
"n"/"k"				CUM. VOL BUILT			

COMMENTS: DRILG. 152 MM HOLE.
CONTROL DENSITY AT 1180 Kg/m³.
KEEP PH AT 10-10.5 USING CAUSTIC. 2 SX / CIR.
MAINTAIN VISC. AT 35-40 s/L WITH IDVIS + ASP-721. ADD 2 PAILS ASP-721 EVERY 12 HRC.
ADD 1 SX. SOD. SULFIDE DAILY. ADD TO H₂O IN CHEM. PAL # 704 W/RESER.
RIN 5-6 LITRES H₂O PER MIN.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WHEELER
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-05-28
 REPORT No. 26
 SPUD DATE 91-04-29

WELL NAME COLUMBA et al KOTANEELEE LOCATION Y.T. - I - 48
 OPERATOR COLUMBA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. Bob TOOLE REPORT FOR Mr. PHIL BOSMORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # 152	COND.	TANKS 72	PUMP SIZE 114 x 406	OPPOSITE D.P. 51
DRILL PIPE 69 mm	SURFACE	HOLE 48	m ³ /STK. 0.118	OPPOSITE D. 671 # = 80
DRILL COLLARS 152 mm	INTER 498/3273	TOTAL 120	S.P.M. 53	PUMP PRESS. 12.100
OTHER	OTHER	STANDBY	m ³ /min. .63	CIRC. TIME 195 F

HOLE DATA	DESANDER/DESTILER	DRILLING FLUID SPECIFICATIONS
MUD TYPE WT POLYMER	FLOWLINE WT.	MUD WT. 1180 kg/m ³
HOLE COND. OK.	UNDERFLOW WT.	VISCOSITY 35-40 s/L
DEVIATION	OVERFLOW WT.	FILTRATE 12 cm ³ /30 min.
CURRENT OP. DRUG.	UNDERFLOW RATE	pH 10-10.5

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN 23:30		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) 3400		ASP-721	68		3	65	300
FLOWLINE TEMPERATURE (°C) 45		SOD. SUL.	26		1	25	50
DENSITY (kg/m ³) 1185		XCIDR	40		1	39	140
FUNNEL VISCOSITY (s/L) 31		PTC-200	63		2	61	320
APPARENT VISCOSITY (mPa.s) 20							
PLASTIC VISCOSITY (mPa.s) 10							
YIELD POINT (Pa) 10							
GELS 0/10 min. (Pa) 2/3							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/> 10.5							
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) 8.0							
FILTER CAKE (mm) .05							
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) 45/1.1							
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L) TR.							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CaCl ₂ (mg/L) 150							
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> .003							
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> .065							
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/> .935		PREVIOUS COST	47,745	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>		DAILY COST	10.10	VOL. BUILT			
ELECTRICAL STABILITY (V) H ₂ S NEG.		CUM. COST	50,755	VOL. LOST ON SURFACE			
OIL/WATER RATIO ASP-721 1.2		CUM. ENG. COST	10,125	VOL. LOST SUB SURFACE			
CaCl ₂ w/w% 600/300 40/30				END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: DRUG. 152 mm HOLE.

1) HOLD DENSITY IN THE 1180 kg/m³ RANGE.

2) KEEP PH AT 10-10.5 USING CAUSTIC. 2.5x/CIR.

3) MAINTAIN V.S. AT 35-40 s/L WITH IDV15 + ASP-721. ADD 1-2 ASP-721 EVERY 12 HRS.

4) ADD 1.5x. SOD. SULFITE + 1 GAL XCIDR DRUG.

5) RUN 5.6 LITRES H₂O PER MIN.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WHEELER
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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DRILLING FLUID REPORT

DATE MAY 29 91
 REPORT No. # 37
 SPUD DATE APR. 29 91

INTERNATIONAL DRILLING FLUIDS

WELL NAME COLUMBIA FTAL KOTANEFIFE LOCATION VT. J-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07
 REPORT FOR Mr. POP TOLE REPORT FOR Mr. TIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>2 1/8</u>	COND.	TANKS <u>73 m³</u>	PUMP SIZE <u>177x406</u>	OPPOSITE D.P. <u>56</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57 m³</u>	m ³ /STK. <u>.0167</u>	OPPOSITE D.C. <u>98</u>
DRILL COLLARS <u>170</u> mm	INTER <u>15803273</u>	TOTAL <u>125 m³</u>	S.P.M. <u>40</u>	PUMP PRESS <u>12,000</u>
OTHER <u>THS 3024</u>	OTHER	STANDBY	m ³ /min. <u>.668</u>	CIRC. TIME <u>190</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>ANNUAL 29 m³</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³
HOLE COND. <u>CLEAN 18 m.</u>	UNDERFLOW WT. <u>7.0</u> kg/m ³	VISCOSITY <u>35-40</u> s/L
DEVIATION <u>To L.T.M.</u>	OVERFLOW WT. kg/m ³	FILTRATE <u>CFLOW 10</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input checked="" type="checkbox"/> <u>Suction</u>		MUD PROPERTIES <u>SHAKER</u>		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2405</u>	<u>15:00</u>	<u>15:00</u>	CARITE	<u>2663</u>		<u>25</u>	<u>2638</u>	<u>312.50</u>
FLOWLINE TEMPERATURE (°C)	<u>24.0</u>		<u>25.0</u>	ASP-731	<u>65</u>		<u>1</u>	<u>64</u>	<u>100.00</u>
DENSITY (kg/m ³)	<u>1180</u>		<u>1185</u>	X-CIDE	<u>39</u>		<u>1</u>	<u>38</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>38</u>		<u>41</u>	SULFITE	<u>25</u>		<u>1</u>	<u>24</u>	<u>49.70</u>
APPARENT VISCOSITY (mPa.s)	<u>20</u>								
PLASTIC VISCOSITY (mPa.s)	<u>10</u>								
YIELD POINT (Pa)	<u>10</u>								
GELS 07/10 min. (Pa)	<u>214</u>								
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>9.0</u>								
FILTER CAKE (mm)	<u>.05 SOFT.</u>								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.51.8</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>30</u>								
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>								
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.001</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.065</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.975</u>								
MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>								
ELECTRICAL STABILITY (V) <u>H.S.</u>	<u>0</u>								
OIL/WATER RATIO <u>ASP-731</u>	<u>.6 KG/m³</u>								
CaCl ₂ w/w% <u>SULFITES</u>	<u>190</u>								
"n"/"k" <u>40/30</u>	<u>40/30</u>								
PREVIOUS COST	<u>50.755</u>								
DAILY COST	<u>60.279</u>								
CUM. COST	<u>5125.2</u>								
CUM. ENG. COST	<u>10,500</u>								
STARTING VOLUME									
VOL. BUILT									
VOL. LOST ON SURFACE									<u>9.115</u>
VOL. LOST SUB SURFACE									
END VOLUME									
CUM. VOL. BUILT									

COMMENTS: MAINTAIN SYSTEM AS FOLLOWS:
1. DENSITY = 1180 KG/M³ NOT BELOW 1170 KG/M³
2. VISCOSITY = 35-40 SEC/CL. NOT BELOW 35 SEC/CL. IF VEG. MIX 2 BAGS 12 OZS - 1 = 100 ML. VEG.
3. PH = 10.0. 1 CAUSTIC SOLA = 2 BAGS A CIRC. WHEN REQD.
4. SLOWLY ADD 1-2 PAILS ASP-731 EVERY 12 HRS. WHEN DRUG SHALL
5. MIX 1 TUB X-CIDE DAILY + EVERY 2 PAILS MIX 1 SLOW SODIUM
6. ADD WATER = 5-6 LITRES/MIN WHEN CIRCULATING
 STOCK POINT FT. ST JOHN I.D.F. ENGINEER ALICK REINHART
 PHONE 785-4222 PHONE FAR FROM OFFICE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 01/20/1991
 REPORT No. 75
 SPUD DATE 01/19/91

WELL NAME COLOMBIA FT AL KUTANEE FLE

LOCATION YT-T 48

OPERATOR COLOMBIA GAS DEVELOPMENT

CONTRACTOR KEATING H.T. MOE

REPORT FOR Mr. BOB TOOLE

REPORT FOR Mr. JIM SINGER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE # <u>7 1/2</u> mm	COND.	TANKS <u>77</u>	PUMP SIZE <u>175 x 40</u>	OPPOSITE D.P. <u>56</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>53.17</u>	m ³ /STK. <u>.0167</u>	OPPOSITE D.C. <u>98</u>
DRILL COLLARS <u>130</u> mm	INTER <u>18.25</u>	TOTAL <u>125</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>13000</u>
OTHER <u>THD 2024</u>	OTHER	STANDBY	m ³ /min. <u>6.68</u>	CIRC. TIME <u>190</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>LT. POLYMER</u>	FLOWLINE WT. <u>AM. Vol. 29.17</u> kg/m ³	MUD WT. <u>1190</u> kg/m ³			
HOLE COND. <u>6001</u>	UNDERFLOW WT. <u>60.11</u> kg/m ³	VISCOSITY <u>35-40</u> s/L			
DEVIATION <u>14° 22' 29" N</u>	OVERFLOW WT.	FILTRATE <u>1100</u> cm ³ /30 min.			
CURRENT OP. <u>HIST. TAGS</u>	UNDERFLOW RATE	pH <u>10.0</u>			

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> SHAKER		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>11:00</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2414</u>			<u>PARITE</u>	<u>2638</u>		<u>25</u>	<u>2613</u>	<u>312.50</u>
FLOWLINE TEMPERATURE (°C)	<u>35.0</u>			<u>PTS-200</u>	<u>61</u>		<u>3</u>	<u>58</u>	<u>780.00</u>
DENSITY (kg/m ³)	<u>1178</u>			<u>EFFORM</u>	<u>18</u>		<u>1</u>	<u>17</u>	<u>136.50</u>
FUNNEL VISCOSITY (s/L)	<u>39</u>								
APPARENT VISCOSITY (mPa.s)	<u>71.5</u>								
PLASTIC VISCOSITY (mPa.s)	<u>11</u>								
YIELD POINT (Pa)	<u>10.5</u>								
GELS 0/10 min. (Pa)	<u>314</u>								
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.0</u>								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>9.0</u>								
FILTER CAKE (mm)	<u>.05 SOFT</u>								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.41.6</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>70</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>700</u>								
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.001</u>	<u>BEADINGS</u>		<u>look-42</u>	<u>2001-37</u>	<u>2001-37</u>			
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.065</u>			<u>look-19</u>	<u>60-4</u>	<u>30-3</u>			
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.925</u>			PREVIOUS COST	<u>51.357</u>	STARTING VOLUME			
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>			DAILY COST	<u>1229.0</u>	VOL BUILT	<u>14.419</u>		
ELECTRICAL STABILITY (V) <u>HES</u>	<u>0</u>			CUM. COST	<u>53.586</u>	VOL LOST ON SURFACE	<u>2</u>		
OIL/WATER RATIO <u>A.P. 221</u>	<u>.5</u>			CUM. ENG. COST	<u>10.825</u>	VOL LOST SUB SURFACE	<u>1</u>		
CaCl ₂ w/w% <u>SULPHATES</u>	<u>190</u>					END VOLUME			
"n"/"k"						CUM. VOL BUILT			

COMMENTS: 1. MUD DENSITY = 1170 - 1180 KG/M³ NOT BELOW 1170 KG/M³
 2. VISCOSITY = 35-40 SEC/30 MIN. NOT BELOW 35 SEC/30 MIN.
 3. PH = 10.0 WITH CAUSTIC SOLID = 2 BAGS A. (100.0 A.P. 221).
 4. SLOWLY RUN IN 1 BAG OF ASP. 7.21 EFFORM 9 HOURS.
 5. MIX 1 BAG OF X-CIDE IN CHELL. L.F.L. CUFF 190 MIN. DAILY.
 6. EVERY TWO DAYS MIX 1 BAG OF SOLVING SULPHATE.
 7. PUMP WATER - 5.0 LITRES/HR. IN HES (CIRCULATING).
 8. PRIOR TO TRIPPING ISOLATE SECTION TANK, MIX IN
 9. 2 BAGS OF PTS-200. PUMP THIS DOWN THE HOLE AND
 10. REPLACE IT WITH MUD FOR 15 MINUTES, THEN
 11. PUMP PULL

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER ALICE REINHART
 PHONE 285.4333 PHONE FAR Road OUTMOBILE# 21.

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE MAY 21 1996
 REPORT No. # 79
 SPUD DATE APR. 29-91

WELL NAME COLUMBIA ET AL KOTANEE LEE LOCATION VT. I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING #07

REPORT FOR Mr. POP TOOLE REPORT FOR Mr.

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>VAR. 150mm</u>	COND.	TANKS <u>72m³</u>	PUMP SIZE <u>175x406</u>	OPPOSITE D.P. <u>57</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52m³</u>	m ³ /STK. <u>.0167</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>8.25m³</u>	TOTAL <u>124m³</u>	S.P.M. <u>41</u>	PUMP PRESS. <u>14,500</u>
OTHER <u>NA. 191m³</u>	OTHER	STANDBY	m ³ /min. <u>.6847</u>	CIRC. TIME <u>180</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>29m³</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³
HOLE COND.	UNDERFLOW WT. <u>60m³</u> kg/m ³	VISCOSITY <u>35-40</u> s/L
DEVIATION <u>NA. OF TOOL FACE</u>	OVERFLOW WT.	FILTRATE <u>210</u> cm ³ /30 min.
CURRENT OP. <u>DRILL AHEAD</u>	UNDERFLOW RATE	pH <u>10.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u>		MUD PROPERTIES		INVENTORY MATERIALS INVENTORY & COST <u>16:00 HRS</u>					
TIME SAMPLE TAKEN	<u>10:00</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2470</u>			GEL	<u>665</u>		<u>255</u>	<u>710</u>	<u>2550.00</u>
FLOWLINE TEMPERATURE (°C)	<u>42°C</u>			CARBITE	<u>6196</u>		<u>2582</u>	<u>3612</u>	<u>27,282.50</u>
DENSITY (kg/m ³)	<u>1185</u>			CAUSTIC	<u>710</u>	<u>(7)</u>	<u>29</u>	<u>181</u>	<u>970.00</u>
FUNNEL VISCOSITY (s/L)	<u>38</u>			SOAP ASH	<u>40</u>		<u>5</u>	<u>25</u>	<u>100.00</u>
APPARENT VISCOSITY (mPa.s)	<u>77</u>			SOLLAN	<u>100</u>		<u>4</u>	<u>96</u>	<u>840.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>11</u>			DI-CARB	<u>60</u>		<u>5</u>	<u>55</u>	<u>500.00</u>
YIELD POINT (Pa)	<u>11</u>			FIR-LO	<u>80</u>	<u>(3)</u>	<u>7</u>	<u>73</u>	<u>1170.00</u>
GELS 0/10 min. (Pa)	<u>2/4</u>			ASP-721	<u>80</u>		<u>15</u>	<u>65</u>	<u>1500.00</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10</u>			IRONS-D	<u>80</u>		<u>28</u>	<u>52</u>	<u>11,760.00</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>15</u>			PTS-200	<u>64</u>		<u>8</u>	<u>56</u>	<u>2080.00</u>
FILTER CAKE (mm)	<u>.15 GOOD</u>			X-CIDE	<u>47</u>	<u>(1)</u>	<u>25</u>	<u>7</u>	<u>980.00</u>
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>41.6</u>			NA-SOFT	<u>20</u>		<u>6</u>	<u>24</u>	<u>298.25</u>
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>20</u>			DEFOAM	<u>20</u>		<u>3</u>	<u>17</u>	<u>409.50</u>
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>700</u>			SA-MINT	<u>288</u>	<u>(12)</u>	<u>50</u>	<u>238</u>	<u>245.00</u>
SAND CONTENT (%) <input checked="" type="checkbox"/> (0) <input type="checkbox"/>	<u>.001</u>			600R= <u>44</u> 300R= <u>23</u> 200R= <u>28</u>					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.07</u>			100R= <u>20</u> AR= <u>4</u> ER= <u>3</u>					
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.92</u>			PREVIOUS COST	<u>52,586.00</u>	STARTING VOLUME			
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>			DAILY COST	<u>2654.00</u>	VOL. BUILT			
ELECTRICAL STABILITY (V) <u>10</u>	<u>0</u>			CUM. COST	<u>56,240.00</u>	VOL. LOST ON SURFACE <u>7 HA 11 S</u>			
OIL/WATER RATIO <u>180</u>	<u>180</u>			CUM. ENG. COST	<u>11,250.00</u>	VOL. LOST SUB SURFACE <u>2</u>			
CaCl ₂ w/w% <u>ASP-721</u>	<u>.5 KG/L³</u>			END VOLUME					
"n"/"k"				CUM. VOL. BUILT					

COMMENTS:

1 MIX 4 BAGS OF FLUR X-10 @ 45 MILLS / BAG.
= FLUR 10 W/ CAUSTIC SOAP AS REQD.
= Slowly Pumped 1 BAG OF ASP-721 FLUR @ 8 HOURS.

STOCK POINT FT. ST. JOHN
 PHONE 885.4222

I.D.F. ENGINEER ALICIA BELLINART
 PHONE FAR ROOM 0 MOBILE 7, 1E 21

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE MAY 31 1996
 REPORT NO. # 79A
 SPUD DATE APR 79 91

WELL NAME COLUMBIA FT ALKUTANEE LEE LOCATION VT. I-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING #107
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 7/8" 1 5/8"</u>	COND.	TANKS <u>70 m³</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>59</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>57 m³</u>	m ³ /STK. <u>.0115</u>	OPPOSITE D.C. <u>107</u>
DRILL COLLARS <u>170 mm</u>	INTER <u>58-377</u>	TOTAL <u>177 m³</u>	S.P.M. <u>60</u>	PUMP PRESS <u>17.400</u>
OTHER <u>THA-196</u>	OTHER	STANDBY	m ³ /min. <u>.708</u>	CIRC. TIME <u>175-180</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>7 POLYMER</u>	FLOWLINE WT. <u>1180</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³
HOLE COND. <u>HT HT HT HT HT</u>	UNDERFLOW WT. <u>55</u> kg/m ³	UNDERFLOW WT. <u>55</u> kg/m ³	UNDERFLOW WT. <u>55</u> kg/m ³	UNDERFLOW WT. <u>55</u> kg/m ³	UNDERFLOW WT. <u>55</u> kg/m ³
DEVIATION <u>MIX LEADS</u>	OVERFLOW WT. <u>10.0</u> kg/m ³	OVERFLOW WT. <u>10.0</u> kg/m ³	OVERFLOW WT. <u>10.0</u> kg/m ³	OVERFLOW WT. <u>10.0</u> kg/m ³	OVERFLOW WT. <u>10.0</u> kg/m ³
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>10.0</u> m ³ /min.	UNDERFLOW RATE <u>10.0</u> m ³ /min.	UNDERFLOW RATE <u>10.0</u> m ³ /min.	UNDERFLOW RATE <u>10.0</u> m ³ /min.	UNDERFLOW RATE <u>10.0</u> m ³ /min.

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u>		MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>19:30</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3425</u>			PARITE	<u>2648</u>		<u>25</u>	<u>2613</u>	<u>427.50</u>
FLOWLINE TEMPERATURE (°C)	<u>4300</u>			CAUSTIC	<u>184</u>		<u>2</u>	<u>182</u>	<u>60.00</u>
DENSITY (kg/m ³)	<u>1180</u>			ASP-221	<u>65</u>		<u>3</u>	<u>62</u>	<u>300.00</u>
FUNNEL VISCOSITY (s/L)	<u>38</u>			SOFAASH	<u>36</u>		<u>1</u>	<u>35</u>	<u>30.00</u>
APPARENT VISCOSITY (mPa.s)	<u>77</u>			L.D.OIS-D	<u>56</u>		<u>4</u>	<u>52</u>	<u>1680.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>13</u>			PTS-200	<u>58</u>		<u>7</u>	<u>51</u>	<u>570.00</u>
YIELD POINT (Pa)	<u>10</u>			X-CIDE	<u>38</u>		<u>3</u>	<u>35</u>	<u>470.00</u>
GELS 0/10 min. (Pa)	<u>2513</u>			FIR-LO	<u>72</u>		<u>3</u>	<u>69</u>	<u>480.00</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.3</u>			DISP-LO	<u>80</u>		<u>1</u>	<u>79</u>	<u>162.40</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>9.6</u>			SAL-DUST	<u>260</u>		<u>27</u>	<u>238</u>	<u>107.80</u>
FILTER CAKE (mm)	<u>1 FAIR!</u>								
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>61.9</u>			LEADS #	<u>90.00</u>				
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>30</u>			CAWHITE #	<u>90.00</u>				
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	<u>700</u>								
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.0015</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.068</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.932</u>								
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>8</u>			PREVIOUS COST	<u>52874</u>				
ELECTRICAL STABILITY (V) <u>H-5</u>	<u>0</u>			DAILY COST	<u>4187</u>				
OIL/WATER RATIO <u>ASP-221</u>	<u>.6</u>			CUM. COST	<u>57017</u>				
CaCl ₂ w/w% <u>SULPHITES</u>	<u>175</u>			CUM. ENG. COST	<u>11750</u>				
"n"/"k"									

COMMENTS: AS SOON AS THE GLASS LEADS GET HERE! MIX 10 BAGS AT 18 MINUTES A BAG. ALSO MIX 2 BAGS OF DISPAC-LO @ 90 MIN/BAG. AND MIX 2 BAGS L.D.OIS-D @ 90 MIN/BAG. -MIX 2 PAILS OF ASP-221 @ 4 HOURS A PAIL. THEN 1 PAIL EVERY 2 HRS. -PH @ 10 W/ 1 BAG CAUSTIC SHA OVER 1 CIRC. OR AS REQ'D. -MIX 1 JUG X-CIDE ONCE A DAY! -MIX 1 BAG SOLID SULPHITE EVERY TWO DAYS -PUSH TO TRIPPINGS ISOLATE SECTION TANK. MIX 2 PAILS OF PTS-200 @ 5 MIN/PAIL & PUMP DOWN THE HOLE AND DISPLACE W/ MUD FOR 15 MINUTES. -WHEN MIXING PILL IN PILL TANK: ADD 1/2 - 1/3 PAIL OF DEFORMER. PUSH TO MIXING TANK. -MUD DENSITY @ 1180 KG/M³: MAKE GUNS AROUND ALL THE TIME!

STOCK POINT FT ST. JOHN I.D.F. ENGINEER KICIK KEINHART
 PHONE 785-4222 PHONE EAR Room MOBILE SIDE.

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 01 1991
 REPORT No. 1170
 SPUD DATE APR. 29.91

WELL NAME COLUMBIA FT AL KOTANEELEE LOCATION VT. T-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #007
 REPORT FOR Mr. POP TOOLE REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>3.157 in</u>	COND.	TANKS <u>69.0</u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>45</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52.5</u>	m³/STK. <u>.0118</u>	OPPOSITE D.C. <u>72</u>
DRILL COLLARS <u>130</u> mm	INTER <u>5-2353</u>	TOTAL <u>171.5</u>	S.P.M. <u>45</u>	PUMP PRESS. <u>10,000</u>
OTHER <u>THA-195</u>	OTHER	STANDBY	m³/min. <u>.531</u>	CIRC. TIME <u>720</u>

HOLE DATA	DESANDER/DESILTTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT.	kg/m³- MUD WT. <u>1180-1185</u> kg/m³
HOLE COND.	UNDERFLOW WT.	kg/m³ VISCOSITY <u>38.40</u> s/L
DEVIATION <u>W/STEAD</u>	OVERFLOW WT.	kg/m³ FILTRATE <u>1.10</u> cm³/30 min.
CURRENT OP. <u>TOOL</u>	UNDERFLOW RATE	m³/min. pH <u>10.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3425</u>		GEI	<u>210</u>		<u>1</u>	<u>309</u>	<u>10.00</u>
FLOWLINE TEMPERATURE (°C) <u>40.00</u>		BARITE	<u>2612</u>		<u>25</u>	<u>2588</u>	<u>312.50</u>
DENSITY (kg/m³) <u>1187</u>		CAUSTIC	<u>182</u>		<u>1</u>	<u>181</u>	<u>30.00</u>
FUNNEL VISCOSITY (s/L) <u>43</u>		ASP-721	<u>67</u>		<u>2</u>	<u>59</u>	<u>300.00</u>
APPARENT VISCOSITY (mPa.s) <u>29</u>		X-CIDE	<u>25</u>		<u>1</u>	<u>34</u>	<u>140.00</u>
PLASTIC VISCOSITY (mPa.s) <u>15</u>		DISPAC	<u>79</u>		<u>2</u>	<u>77</u>	<u>374.80</u>
YIELD POINT (Pa) <u>14</u>		IL-015-D	<u>57</u>		<u>2</u>	<u>50</u>	<u>840.00</u>
GELS 0/10 min. (Pa) <u>315</u>		DEFOS	<u>17</u>		<u>1</u>	<u>16</u>	<u>126.50</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.3</u>	PTS-200	<u>56</u>		<u>2</u>	<u>57</u>	<u>780.00</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm³)	<u>9.0</u>	PEARS			<u>10</u>		<u>800.00</u>
FILTER CAKE (mm)	<u>.1 GOOD!</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>61.9</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>20</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>750</u>						
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.001</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.072</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.937</u>	PREVIOUS COST	<u>57012</u>	STARTING VOLUME			
MBT (Kg/m³) <input checked="" type="checkbox"/> 7% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>9</u>	DAILY COST	<u>3672.8</u>	VOL. BUILT	<u>7 HOURS</u>		
ELECTRICAL STABILITY (V) <u>25</u>	<u>0</u>	CUM. COST	<u>10684</u>	VOL. COST ON SURFACE			
OIL/WATER RATIO <u>ASP-721</u>	<u>.8</u>	CUM. ENG. COST	<u>12,375</u>	VOL. LOST SUB SURFACE			
CaCl₂ w/w% <u>SOLPHITE</u>	<u>160</u>			END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: DENSITY = 1180-1190 KCL/PP. HOWE HILL 600'S (EXCEPT SHAKER)
 2 ROLL COATED 5 S LITERS / MIN. FOR 1 CIRC. FOR 12 HOURS.
 2 VISCOSITY = 38.40 SEC/11.
 4 PM-10 W/1 CAUSTIC SOLA. OUFFE 1 FULL CIRC. WHEN BEG'D
 2 SLOWLY FOR 1/2 HAIL OF ASP-721 FLEAD 2 HOURS.
 1 MIX 1 JOG OF X-CIDE. ONCE A DAY!
 2 MIX 1 BAG OF SWISSOL SULPHITE EVERY TWO DAYS.
 3 PRIOR TO TRIPPING ISOLATE SURTICAL TANK, MIX 2 BAILS
 OF PTS-200 & 5 MIN. HAIL 2 PUMP DOWN HOLE + DISPLACE
 W/ W/ FOR 15 MINUTES.
 4 WHEN MIXING ALL W. PILL TANK. ADD 1/2 TO 1/2 HAIL OF
 DEFOS. PRIOR TO MIXING BARITE.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART
 PHONE 785-4772 PHONE FOR ACCIDENT OR MOBILE #1

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DRILLING FLUID REPORT

DATE JUNE 07 1991
 REPORT No. #31
 SPUD DATE APR. 29.91

INTERNATIONAL DRILLING FLUIDS

WELL NAME COLUMPIA FT ALKOTANEELEE LOCATION VT-L-48
 OPERATOR COLUMPIA GAS DEVELOPMENT CONTRACTOR KENITING H.T. #07
 REPORT FOR Mr. POP TOOLE REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>4.152 IN</u>	COND.	TANKS <u>69 M³</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57 M³</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>130</u> mm	INTER <u>78.2373</u>	TOTAL <u>127 M³</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9.000</u>
OTHER <u>CHA-195</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>210</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>40</u> kg/m ³	MUD WT. <u>1180-1185</u> kg/m ³
HOLE COND.	UNDERFLOW WT. <u>68 MI</u> kg/m ³	VISCOSITY <u>38-40</u> s/L
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>210</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.0</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

TIME SAMPLE TAKEN	MUD PROPERTIES			MATERIALS INVENTORY & COST					
	04:00	06:00	30:00	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	2451	2454	2444	PARITE	2588		30	2558	275.00
FLOWLINE TEMPERATURE (°C)	43.00		39.00	PTS-200	53		3	50	780.00
DENSITY (kg/m ³)	1195	1195	1195	SAPPHIRE	74		1	73	49.70
FUNNEL VISCOSITY (s/L)	41	41	42	PEFOAM	16		1	15	126.50
APPARENT VISCOSITY (mPa.s)	26.5	26	(28)	GLASS BEADS	65		10	45	800.00
PLASTIC VISCOSITY (mPa.s)	15	15	15						
YIELD POINT (Pa)	11.5	11	13.5						
GELS 0/10 min. (Pa)	25/25	2/3	3/4						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5								
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	9.5								
FILTER CAKE (mm)	1.600								
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	9/1.4								
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	30								
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	250								
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.001								
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.075								
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.925								
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	10								
ELECTRICAL STABILITY (V) <u>H2S</u>	0								
OIL/WATER RATIO (SP. 221)	.7								
CaCl ₂ w/w% <u>PHOSPHATES</u>	180								
"n"/"k"									

COMMENTS: DENSITY: 1180-1190 KG/M³; MUD NOT GOOD EXCEPT SHAKER TANK!
 2 BBL WATER @ 5 LITRES/MIN FOR 1 CIRC. EVERY 13 HOURS
 VISCOSITY: 38 TO 40 SEC/L
 PH = 10.0 CAUSTIC SOLA OVER 1 FULL CIRC. WHEN REQ'D.
 2 CIRC. RUN TO 1 PAIL OF ASP. 221 EVERY 13 HOURS.
 1 MIX 1 JOB OF X-CIDE. ONCE A DAY
 2 PAIL TO TROUBLESHOOTING: ISOLATE SECTION TANK, MIX 3 PAILS
 OF PTS-200 @ 5 MIN PAIL PUMP LOAD HOLE & DISPLACE
 1 CIRC FOR 15 MINUTES.
 2 WHEN MIXING PAIL IN PAIL TANK, ADD 1/2 PAIL OF
 PEFOAM FROM MIXING PARITE.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART
 PHONE 785-4333 PHONE BAR ROOM QUINCY ILL 618-245-1111

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 04 1991
 REPORT No. # 22
 SPUD DATE APR 29 91

WELL NAME <u>COLOMPIA FTAL KOTANEE LEE</u>		LOCATION <u>YT-I-48</u>		
OPERATOR <u>COLOMPIA GAS DEVELOPMENT</u>		CONTRACTOR <u>KENTING H.T. 07</u>		
REPORT FOR Mr. <u>BOB TOOLE</u>		REPORT FOR Mr. <u>JIM SIGNER</u>		
ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>5.15 7/8" (127)</u>	COND.	TANKS <u>75 MP</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>54.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>53 MP</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>120</u> mm	INTER <u>120 2 272</u>	TOTAL <u>178 MP</u>	S.P.M. <u>55</u>	PUMP PRESS. <u>8500</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.649</u>	CIRC. TIME <u>300</u>
HOLE DATA		DESANDER/DESTILER		DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>40 MP</u>	kg/m ³	MUD WT. <u>1180-1190</u>	kg/m ³
HOLE COND. <u>HARD KEEPING</u>	UNDERFLOW WT. <u>62</u>	kg/m ³	VISCOSITY <u>38-40</u>	s/L
DEVIATION <u>2417-2476 m</u>	OVERFLOW WT.	kg/m ³	FILTRATE <u>110</u>	cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE	m ³ /min.	pH <u>10.0-10.5</u>	
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER				
SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>				
TIME SAMPLE TAKEN <u>02:30</u>		MATERIALS INVENTORY & COST		
PRESENT DEPTH (m) <u>2459</u>	MATERIALS	INITIAL	RECEIVED	USED
FLOWLINE TEMPERATURE (°C) <u>420C</u>	<u>LARITE 3588</u>		<u>20</u>	<u>3588</u>
DENSITY (kg/m ³) <u>1190</u>	<u>PTS-200 50</u>		<u>3</u>	<u>47</u>
FUNNEL VISCOSITY (s/L) <u>41</u>	<u>X-CIDE 34</u>		<u>1</u>	<u>33</u>
APPARENT VISCOSITY (mPa.s) <u>26.5</u>	<u>DEFOAM 15</u>		<u>1</u>	<u>14</u>
PLASTIC VISCOSITY (mPa.s) <u>15</u>				
YIELD POINT (Pa) <u>11.5</u>				
GELS 0/10 min. (Pa) <u>213</u>				
pH STRIP 2-METER <input type="checkbox"/>				
FILTRATE 3-API <input type="checkbox"/> HT HP (cm ³) <u>14.0</u>				
FILTER CAKE (mm) <u>.5 FAIR</u>				
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>.7/9</u>				
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L) <u>20</u>				
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L) <u>250</u>				
SAND CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/> <u>.001</u>				
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input type="checkbox"/> <u>.077</u>				
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input type="checkbox"/> <u>.978</u>				
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/> <u>11</u>				
ELECTRICAL STABILITY (V) <u>H=2 (MCL) and 2 hrs. up!</u>				
OIL/WATER RATIO <u>FOR 201</u> <u>.6</u>				
CaCl ₂ w/w% <u>SOLPHITE</u> <u>150</u>				
"n"/"k"				
COMMENTS: <u>DENSITY = 1180-1190 KG/M³. HAVE GELS EXCEPT SHAKER TANK</u>				
<u>20 LITRE (5.5 GAL) 0-TIL VISCOSITY = 12 SEC @ 40</u>				
<u>20 VISCOSITY = 27-29 SEC @ 10.5</u>				
<u>1 BAG 10.5 LIT CAUSTIC SOLA + 1 BAG A CIRC. WHEN REQ'D.</u>				
<u>5 BAGS 10.5 LIT PAIR OF ASP 201 FOR 12 HOURS.</u>				
<u>1 MIX 1 JUG OF X-CIDE, ONCE A DAY.</u>				
<u>2 PAIL TO MIXING PULL 1 PAIL TANK, MIX 1/2 PAIL + OF LFCARIES</u>				
<u>2 PAIL TO THIPPING & ISOLATE LAST TWO TANKS, MIX 2 PAIL</u>				
<u>OF PTS-200 + S MUD/PAIL 12 EACH TANK, (4 PAIL TOTAL)</u>				
<u>POUR POUND HOLE FOR 30 MIN. + 1 SPACER WITHIN FOR 10 MIN.</u>				
<u>AS SOON AS YOU GET BACK ON BOTTOM W/ LIT # 6.</u>				
<u>1 ROLL WATER = 20 LITRE, MIX 2 BAGS OF LINSPEC-LO</u>				
<u>ES MUD 1 BAG, MIX 1 BAG OF SOLIUM SOLPHITE!</u>				
STOCK POINT <u>ET. ST. JOHN</u>	I.D.F. ENGINEER <u>KICK BEINHARDT</u>			
PHONE <u>785-4372</u>	PHONE <u>FAR ROOM</u> OR MOBILE # <u>1</u>			

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 05 91
 REPORT No. # 33
 SPUD DATE APR 29 91

WELL NAME COLUMBIA ET AL KOTANEELEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07

REPORT FOR Mr. POP TOOLE REPORT FOR Mr. JUL SIGNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>#6.152mm</u>	COND.	TANKS <u>75 m³</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>54.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>52 m³</u>	m ³ /STK. <u>0.188</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>120</u> mm	INTER <u>58-2772</u>	TOTAL <u>178 m³</u>	S.P.M. <u>55</u>	PUMP PRESS. <u>13,500</u>
OTHER <u>THA 193</u>	OTHER	STANDBY	m ³ /min. <u>649</u>	CIRC. TIME <u>700</u>

HOLE DATA	DESANDER/DESILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T. POLYMER</u>	FLOWLINE WT <u>400</u> kg/m ³	MUD WT. <u>1180</u> kg/m ³
HOLE COND. <u>(BY I.S.F. TESTS)</u>	UNDERFLOW WT <u>67</u> kg/m ³	VISCOSITY <u>38.40</u> s/L
DEVIATION	OVERFLOW WT <u>1040 (45.1)</u> kg/m ³	FILTRATE <u>L10</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>2810 (2.4)</u> m ³ /min.	pH <u>10-10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>04:00</u>							
PRESENT DEPTH (m) <u>3468</u>		BARITE <u>3528</u>		<u>30</u>	<u>2498</u>	<u>275.00</u>	
FLOWLINE TEMPERATURE (°C) <u>42°</u>		FTS-200 <u>47</u>		<u>4</u>	<u>43</u>	<u>1040.00</u>	
DENSITY (kg/m ³) <u>1180</u>		X-CIDE <u>33</u>		<u>1</u>	<u>32</u>	<u>140.00</u>	
FUNNEL VISCOSITY (s/L) <u>41</u>		(PLASTIC) <u>181</u>		<u>1</u>	<u>180</u>	<u>30.00</u>	
APPARENT VISCOSITY (mPa.s) <u>76</u>		LEFOR <u>14</u>		<u>1</u>	<u>13</u>	<u>126.50</u>	
PLASTIC VISCOSITY (mPa.s) <u>15</u>							
YIELD POINT (Pa) <u>11</u>							
GELS 0/10 min. (Pa) <u>7/25</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>10.5</u>						
FILTER CAKE (mm)	<u>1.0 GOOD!</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>8/1.1</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>750</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.001</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.068</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.932</u>	PREVIOUS COST <u>4,259.14</u>		STARTING VOLUME			
MBT (Kg/m ³) <input checked="" type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	DAILY COST <u>172.50</u>		VOL BUILT	<u>THANKS</u>		
ELECTRICAL STABILITY (V) <u>H2S</u>	<u>0</u>	CUM. COST <u>45,980.68</u>		VOL LOST ON SURFACE			
OIL/WATER RATIO <u>P.P. 221</u>	<u>.5</u>	CUM. ENG. COST <u>13,500.00</u>		VOL LOST SUB SURFACE			
CaCl ₂ w/w% <u>SULPHITES</u>	<u>135</u>			END VOLUME			
"n"/"k"				CUM. VOL BUILT			

COMMENTS: LENGTH 1180 KCLD. MAKE 10L GEL EXCEPT 1. SHAKE TANK
2 DISCONT. 38.40 SEC. BE. V. AFTER AT 5 LITRES 1 MIN.
3 PH. 10.5 (1 PLASTIC SUP. 1 LAG. 1 CIRC. 1 WHEN REG. 1
4 TANKS. RE. 1.1 PAIR OF ASP. 21 EVERY 12 HOURS.
5 MIX 1 TUB OF X-CIDE. CONC. A LAY!
6 PUMP TO MIXING PILL. PILL TANK. MIX 2 PART OF LEFORNER.
7 PUMP TO TRIPPING. ISOLATE LAST TWO TANKS. MIX 2 PART
OF FTS-200 25 M. 1 PART IN EACH TANK. (4 PARTS TOTAL)
8 PUMP DOWN HOLE FOR 30 MIN. 14 DISPLACE WITH H2O FOR
10 MINUTES.

STOCK POINT ET ST JOHN I.D.F. ENGINEER RICK REINHART
 PHONE 785-4222 PHONE FOR POOL MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 05 91
 REPORT No. # 24
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FTAL KOTANEELEE LOCATION VT-I-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #107
 REPORT FOR Mr. POP TOOLE-NEIL FUSSELL-JOHN A. REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/4 157mm</u>	COND.	TANKS <u>25.5</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>54.5</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>52.5</u>	m ³ /STK. <u>0.188</u>	OPPOSITE D.C. <u>100</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>17802773</u>	TOTAL <u>179 m³</u>	S.P.M. <u>55</u>	PUMP PRESS. <u>11,000</u>
OTHER <u>THA 197m</u>	OTHER	STANDBY	m ³ /min. <u>649</u>	CIRC. TIME <u>300</u>

HOLE DATA	DESANDER/DESTILER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>ANIL. VOL. 40.5 m³ kg/m³</u>	MUD WT. <u>1175-1180 kg/m³</u>
HOLE COND. <u>(2x15.8 SETS)</u>	UNDERFLOW WT. <u>TOP. UP 65 m³ kg/m³</u>	VISCOSITY <u>38-40 s/L</u>
DEVIATION <u>10° 34' 00" 2474</u>	OVERFLOW WT. kg/m ³	FILTRATE <u>110 cm³/30 min.</u>
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>23:30</u>	<u>15:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3492</u>	<u>3481</u>	DISPAC 10	<u>27</u>		<u>7</u>	<u>70</u>	<u>1176.80</u>
FLOWLINE TEMPERATURE (°C)	<u>46°C</u>	<u>42°C</u>	SULPHITE	<u>23</u>		<u>1</u>	<u>22</u>	<u>49.70</u>
DENSITY (kg/m ³)	<u>1175</u>	<u>1175</u>	ASP. 721	<u>59</u>		<u>3</u>	<u>56</u>	<u>300.00</u>
FUNNEL VISCOSITY (s/L)	<u>41</u>	<u>41</u>	X-CIDE	<u>23</u>		<u>1</u>	<u>21</u>	<u>140.00</u>
APPARENT VISCOSITY (mPa.s)	<u>25</u>	<u>26</u>						
PLASTIC VISCOSITY (mPa.s)	<u>15</u>	<u>15</u>						
YIELD POINT (Pa)	<u>10</u>	<u>11</u>						
GELS 0/10 min. (Pa)	<u>212.5</u>	<u>212.5</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>10.5</u>	<u>17.0</u>						
FILTER CAKE (mm)	<u>1.0</u>	<u>1.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>9/11.2</u>	<u>8.5/11.2</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>70</u>	<u>70</u>						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>250</u>	<u>250</u>	PR = 2	AR = 2	100 AR = 20			
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.001</u>	<u>.001</u>	2000R = 30	300R = 35	ACOR = 50			
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.065</u>	<u>.065</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.935</u>	<u>.935</u>	PREVIOUS COST <u>65,980.45</u>	STARTING VOLUME				
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST <u>1626.55</u>	VOL BUILT	<u>THANIS</u>			
ELECTRICAL STABILITY (V) <u>H:5</u>	<u>0</u>	<u>0</u>	CUM. COST <u>67,607.00</u>	VOL LOST ON SURFACE				
OIL/WATER RATIO <u>ASP. 721</u>	<u>.6</u>	<u>.5</u>	CUM. ENG. COST <u>13,500.00</u>	VOL LOST SUB SURFACE				
CaCl ₂ w/w% <u>SULPHITES</u>	<u>120</u>	<u>120</u>		END VOLUME				
"n"/"k"				CUM. VOL BUILT				

COMMENTS: 1. DENSITY @ 1180 KG/L. MUD GUMS EXCEPT IN SHAKER TANK!
 - VISCOSITY @ 38-40 SEC/100 RPM WATER @ 5 L/MIN. 10 MIN. EVERY 15 MIN.
 - pH @ 10.5 w/ CAUSTIC SOLAR 1 BAG A CIRC. WHEN REQ.
 - 4 Slowly Pour 1 1/2 PAIL OF ASP. 721 EVERY 12 HOURS.
 - MIX 1 JUG OF X-CIDE ONCE A DAY!
 - PITCH TO MIXING PULL IN PULL TANK: MIX 1/2 PAIL + DEFORMER!
 - PITCH TO TRIPPING ISOLATE LAST TWO TANKS: MIX 2 PAILS
 OF PTS-200 @ 5 L/MIN. 1 PAIL IN EACH TANK. (4 PAILS TOTAL)
 PUMP DOWN HOLE FOR 30 MIN. AND DISPLACE w/ MUD
 FOR 10 MINUTES.
 - IF MUD DENSITY DROPS LEAVE 1170 KG/L. MIX 50 SXS CAUSTIC
 AT 4 MINUTES / BAG.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART
 PHONE 785-4777 PHONE FAR ROOM 0 MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 06 1991
 REPORT No. # 35
 SPUD DATE APR 29 91

WELL NAME COLUMBIA FTAL KOTAN FEELE LOCATION YT-I-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07
 REPORT FOR Mr. NEIL BLISS REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1.57mm</u>	COND.	TANKS <u>77 m³</u>	PUMP SIZE / <u>14x406</u>	OPPOSITE D.P. <u>55</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>54 m³</u>	m ³ /STK. <u>0118</u>	OPPOSITE D.C. <u>95</u>
DRILL COLLARS <u>170</u> mm	INTER / <u>ES-3773</u>	TOTAL <u>131 m³</u>	S.P.M. <u>55</u>	PUMP PRESS. <u>12,500</u>
OTHER <u>CHD-194</u>	OTHER	STANDBY	m ³ /min. <u>.649</u>	CIRC. TIME <u>300</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>1125-1180</u> kg/m ³	MUD WT. <u>1125-1180</u> kg/m ³
HOLE COND.	UNDERFLOW WT. <u>11.5</u> kg/m ³	VISCOSITY <u>38-40</u> s/L
DEVIATION	OVERFLOW WT.	FILTRATE <u>1.0</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>16:30</u>	<u>11:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3495</u>	<u>3494</u>	DATE	<u>3498</u>		<u>38</u>	<u>3468</u>	<u>462.50</u>
FLOWLINE TEMPERATURE (°C)	<u>45°C</u>	<u>45°C</u>	ASP-721	<u>56</u>		<u>1</u>	<u>55</u>	<u>100.00</u>
DENSITY (kg/m ³)	<u>1180</u>	<u>1180</u>	X-CHE	<u>31</u>		<u>1</u>	<u>30</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>42</u>	<u>42</u>	SULFATE	<u>22</u>		<u>1</u>	<u>21</u>	<u>49.70</u>
APPARENT VISCOSITY (mPa.s)	<u>27</u>	<u>26</u>	PTS-200	<u>42</u>		<u>4</u>	<u>39</u>	<u>1040.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>16</u>	<u>15</u>	DISPAC-10	<u>70</u>		<u>4</u>	<u>65</u>	<u>649.60</u>
YIELD POINT (Pa)	<u>11</u>	<u>11</u>	GRAPHITE	<u>-</u>		<u>2</u>	<u>-</u>	
GELS 0/10 min. (Pa)	<u>212.5</u>	<u>212</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>11.5</u>	<u>17.0</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.85/1.2</u>	<u>.85/1.2</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>30</u>	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	<u>750</u>	<u>700</u>	PR=2	LR=4	100R=31			
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.002</u>	<u>.001</u>	200R=31	300R=35	600R=54			
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.068</u>	<u>.068</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.932</u>	<u>.932</u>	PREVIOUS COST	<u>67,607.18</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> % OIL RET <input type="checkbox"/>	<u>11</u>	<u>11</u>	DAILY COST	<u>3441.80</u>	VOL. BUILT			<u>TH 2.171</u>
ELECTRICAL STABILITY (V) <u>12.5</u>	<u>0</u>	<u>0</u>	CUM. COST	<u>70,048.98</u>	VOL. LOST ON SURFACE			<u>✓</u>
OIL/WATER RATIO <u>ASP-721</u>	<u>.75</u>	<u>.7</u>	CUM. ENG. COST	<u>13,875.58</u>	VOL. LOST SUB SURFACE			<u>✓</u>
CaCl ₂ w/w% <u>CL WHITE</u>	<u>150</u>	<u>170</u>			END VOLUME			
"n"/"k" TOTAL POLYMER <u>3.5 KG/L</u>					CUM. VOL. BUILT			

COMMENTS: DENSITY = 1125-1180 KG/L. MOVE MUD GUMS EXCEPT 100 SHAKER TANK, IF DENSITY GOES BELOW 1170 KG/L. MIX 50 SXS OF DATE = 4 MINUTES A PAG.
 VISCOSITY = 38-40 SECUL. RUN WATER + SULFATE. 1 LITRE EVERY 12 HRS.
 PH = 10.5 ON CALSTIC SOLAG / LAG A CIRC. WHEN RECD.
 4 RUN 100 PAIL OF ASP-721 EVERY 12 HOURS.
 5 MIX 1 TUB OF X-CHE, ONCE A DAY.
 1 PAIL TO MIXING PAIL IN PAIL TANK. MIX 1/2 PAIL + DEGASSER.
 2 PAIL TO TRIPPING. ISOLATE LAST TWO TANKS. MIX 2 PAIL OF PTS-200 IN EACH TANK - 5 MIN PAIL. (4 PAIL TOTAL) PUMP DOWN HOLE FOR 20 MIN. PAIL. 10 MINUTE W/ HOLE FOR 10 MINUTES.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART
 PHONE 785-4777 PHONE ROOM ROOM MOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 07 91
 REPORT No. #36
 SPUD DATE APR 29 91

WELL NAME COLUMPIA ETAL KOTANEE LEE LOCATION VT. J-48

OPERATOR COLUMPIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07

REPORT FOR Mr. NEIL PLISS REPORT FOR Mr. JIM SIGNED

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>7 1/2</u>	COND.	TANKS <u>77 m³</u>	PUMP SIZE <u>20x40</u>	OPPOSITE D.P. <u>56</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>54 m³</u>	m ³ /STK. <u>.0167</u>	OPPOSITE D.C. <u>98</u>
DRILL COLLARS <u>120</u> mm	INTER <u>5-2202</u>	TOTAL <u>131 m³</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>11,500</u>
OTHER <u>THE 194 m</u>	OTHER	STANDBY	m ³ /min. <u>.668</u>	CIRC. TIME <u>700</u>

HOLE DATA	DESANDER/DESTILER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>41 m³</u> kg/m ³	MUD WT. <u>1175-1180</u> kg/m ³
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>67 m³</u> kg/m ³	VISCOSITY <u>38-40</u> s/L
DEVIATION	OVERFLOW WT <u>BOTTOM OF HOLE</u> kg/m ³	FILTRATE <u>10-12</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>215 m³/min.</u>	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. PIT MUD PROPERTIES MATERIALS INVENTORY & COST

TIME SAMPLE TAKEN	19:00	11:00	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	2574	2510	X-CIDE	30		1	29	140.00
FLOWLINE TEMPERATURE (°C)	43.00	43.00	SULPHITE	21		1	20	49.70
DENSITY (kg/m ³)	1175	1180	DFCL	20		12	18	2126.00
FUNNEL VISCOSITY (s/L)	43	43	DISPAC 66			3	63	487.20
APPARENT VISCOSITY (mPa.s)	29	29.5	GLASS					
PLASTIC VISCOSITY (mPa.s)	18	18	DEALS	45		5	40	400.00
YIELD POINT (Pa)	11	11.5						
GELS 0/10 min. (Pa)	212	212						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5	10.5						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	12.0	12						
FILTER CAKE (mm)	1.0 ^{TIGHT}	1.5						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	.85/1.2	1.0/1.4						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	20	20						
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	250	250						
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.0015	.007						
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.066	.068						
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	.934	.927						
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	10	10						
ELECTRICAL STABILITY (V) <u>11.5</u>	0	0						
OIL/WATER RATIO <u>2.81</u>	.8	.8						
CaCl ₂ w/w% <u>SULPHITES</u>	150	150						
"n"/"k" <u>TOTAL POLYMER</u>	3.0	3.0						

COMMENTS: DE DENSITY 1175-1180 KCL. MUD OF HOLE GOOD EXCEPT IN SHAKEL TANK IF DENSITY GOES TO 1150 KCL. 1.5 MIN 50 XS SULPHITE AT 4 MINUTES A BAG.
2 DISCONTINUED 38-40 SECIL. 10 LITERS WATER 5 LITERS LIME.
3 PH 10.5 W/ CAUSTIC SODA 1 BAG A CIRC. WHEN REQ'D.
4 STOP ADDITIONS OF DISP. 771!
5 MIX 1 JUG X-CIDE, 1 BAG NAT. SULPHITE ONCE A DAY!
6 PRIOR TO MIXING PULL 1/2 PAIL TANK. MIX 1/2 PAIL DFCL/DMER!
7 HULL TO THIPPING 2 L'CLATE LAST TWO TANKS. MIX 2 PAILS OF FTS. 200 L/ EACH TANK 5 MIN. 1 PAIL PUMP DOWN HOLE FOR 40 MINUTES. ALL THE PUMP FILL!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK REINHART
 PHONE 785-4772 PHONE FAR ROOM MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 08 1991
 REPORT No. #37
 SPUD DATE APR 29 91

WELL NAME COLOMBIA FT ALKUTANEELEE LOCATION VT - I - 48
 OPERATOR COLOMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07
 REPORT FOR Mr. NEIL PLISS REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>7.157mm</u>	COND.	TANKS <u>85.17</u>	PUMP SIZE / <u>175x406</u>	OPPOSITE D.P. <u>50.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>55.17</u>	m ³ /STK. <u>.0167</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>170</u> mm	INTER / <u>8.7373</u>	TOTAL <u>140.17</u>	S.P.M. <u>36</u>	PUMP PRESS. <u>12,000</u>
OTHER <u>PHB-194M</u>	OTHER	STANDBY	m ³ /min. <u>.6013</u>	CIRC. TIME <u>230</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>ST. POLYMER</u>	FLOWLINE WT. <u>106.45</u> kg/m ³	MUD WT. <u>1175-1180</u> kg/m ³
HOLE COND.	UNDERFLOW WT. <u>76</u> kg/m ³	VISCOSITY <u>40 SEC/100</u> s/L
DEVIATION <u>10 1/4°</u>	OVERFLOW WT. <u>ETAL HOLE TEMP</u> kg/m ³	FILTRATE <u>10-12</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>215</u> m ³ /min.	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>11:00</u>							
PRESENT DEPTH (m) <u>3544</u>		PAPITE <u>7461</u>			<u>25</u>	<u>2476</u>	<u>427.50</u>
FLOWLINE TEMPERATURE (°C) <u>42.0</u>		X-CIDE <u>29</u>			<u>1</u>	<u>78</u>	<u>140.00</u>
DENSITY (kg/m ³) <u>1175</u>		DEFORM <u>13</u>			<u>1</u>	<u>12</u>	<u>126.50</u>
FUNNEL VISCOSITY (s/L) <u>47</u>		SUBHITE <u>30</u>			<u>1</u>	<u>19</u>	<u>49.50</u>
APPARENT VISCOSITY (mPa.s) <u>27</u>		PTS-200 <u>29</u>			<u>4</u>	<u>35</u>	<u>1040.00</u>
PLASTIC VISCOSITY (mPa.s) <u>17</u>							
YIELD POINT (Pa) <u>10</u>							
GELS 0/10 min. (Pa) <u>2/7.5</u>							
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>12.5</u>						
FILTER CAKE (mm)	<u>.5 TIGHT!</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>.85/1.1</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>250</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.001</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.066</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.934</u>						
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>						
ELECTRICAL STABILITY (V) <u>0</u>		PREVIOUS COST <u>23,241.70</u>			STARTING VOLUME		
OIL/WATER RATIO <u>ASP. 721</u>	<u>27</u>	DAILY COST <u>1802.70</u>			VOL. BUILT		<u>THANKS</u>
CaCl ₂ w/w% <u>LI PHITES</u>	<u>130</u>	CUM. COST <u>75,065.70</u>			VOL. LOST ON SURFACE		
"n"/"K" <u>ETAL POWDER</u>	<u>3.5 K/LM</u>	CUM. ENG. COST <u>14,675.70</u>			VOL. LOST SUB SURFACE		
					END VOLUME		
					CUM. VOL. BUILT		

COMMENTS:
A. SOON AS YOU GET BACK ON BOTTOM W/ BIT #8!
1. RUN WATER @ 20 LITRES / MIN. FOR 1 CIRCULATION, THEN
SLOW THE WATER DOWN TO 5 LITRES / MIN. NOTE.
2. MIX 1 JUG OF X-CIDE AND THEN 1 BAG OF SODIUM SULPHITE.
3. AFTER 1 FULL CIRCULATION, MIX 3 BAGS OF DRISPAK
LOW AT 30 MINUTES A BAG!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICIE REINHART
 PHONE 785-4722 PHONE EAR ROOM MOBILE # 1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 09 1991
 REPORT No. # 38
 SPUD DATE APR 29 91

WELL NAME <u>COLOMBIA FTAL KOTANEELEE</u>			LOCATION <u>VT-I-48</u>					
OPERATOR <u>COLOMBIA GAS DEVELOPMENT</u>			CONTRACTOR <u>KENTING H.T. #07</u>					
REPORT FOR Mr. <u>NEIL PLISS</u>			REPORT FOR Mr. <u>JIM SIGNED</u>					
ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.				
BIT SIZE <u>8.125</u>	COND.	TANKS <u>80 m³</u>	PUMP SIZE <u>177x406</u>	OPPOSITE D.P. <u>60</u>				
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>55 m³</u>	m ³ /STK. <u>0.167</u>	OPPOSITE D.C. <u>105</u>				
DRILL COLLARS <u>130</u> mm	INTER <u>178.3333</u>	TOTAL <u>135 m³</u>	S.P.M. <u>40</u>	PUMP PRESS. <u>10,000</u>				
OTHER <u>THA</u>	OTHER	STANDBY	m ³ /min. <u>0.7181</u>	CIRC. TIME <u>190</u>				
HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS				
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WTA <u>45 m³</u>	kg/m ³	MUD WT. <u>1190</u>	kg/m ³				
HOLE COND.	UNDERFLOW WT <u>65 m³</u>	kg/m ³	VISCOSITY <u>40 SEC/LL</u>	s/L				
DEVIATION	OVERFLOW WT <u>15 m³</u>	kg/m ³	FILTRATE <u>10-17</u>	cm ³ /30 min.				
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE <u>2150 F</u>	m ³ /min.	pH <u>10.5</u>					
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER								
SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>								
MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>70:00</u>	<u>13:00</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2559</u>	<u>2557</u>	BARITE	<u>247</u>		<u>100</u>	<u>237</u>	<u>1750.00</u>
FLOWLINE TEMPERATURE (°C)	<u>44°</u>	<u>47°</u>	SULPHITE	<u>19</u>		<u>1</u>	<u>18</u>	<u>49.70</u>
DENSITY (kg/m ³)	<u>1180</u>	<u>1170</u>	DFCL	<u>18</u>		<u>6</u>	<u>17</u>	<u>1068.00</u>
FUNNEL VISCOSITY (s/L)	<u>43</u>	<u>45</u>	DRISPAC	<u>13</u>		<u>7</u>	<u>60</u>	<u>487.70</u>
APPARENT VISCOSITY (mPa.s)	<u>28</u>	<u>30</u>						
PLASTIC VISCOSITY (mPa.s)	<u>18</u>	<u>19</u>						
YIELD POINT (Pa)	<u>10</u>	<u>11</u>						
GELS 0/10 min. (Pa)	<u>212.5</u>	<u>213</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.7</u>	<u>11.0</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ²)	<u>15</u>	<u>13.0</u>						
FILTER CAKE (mm)	<u>1.0 FIRM.</u>	<u>1.0</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.1/1.4</u>	<u>1.3/2.1</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L)	<u>30</u>	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>250</u>	<u>300</u>	BR=3	LR=4	100R=70			
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.001</u>	<u>.001</u>	200R=30	300R=28	400R=56			
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.07</u>	<u>.065</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.93</u>	<u>.925</u>	PREVIOUS COST	<u>25,065</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>11</u>	DAILY COST	<u>2854.9</u>	VOL. BUILT <u>THA</u> ml/s			
ELECTRICAL STABILITY (V)	<u>0</u>	<u>0</u>	CUM. COST	<u>27970</u>	VOL. LOST ON SURFACE <u>1</u>			
OIL/WATER RATIO	<u>.7</u>	<u>.7</u>	CUM. ENG. COST	<u>15,000</u>	VOL. LOST SUB SURFACE <u>1</u>			
CaCl ₂ w/w% <u>170</u>	<u>170</u>	<u>175</u>			END VOLUME <u>1</u>			
"n"/"K" <u>4</u>	<u>4</u>	<u>4</u>			CUM. VOL BUILT <u>1</u>			
COMMENTS: DENSITY 1190 KG/L? MORE W/TE GELS EXCEPT W/SHAKER TANK. IF DENSITY GOES BELOW 1185 KG/L, MIX 50% XS BARITE AT 4 MINUTES A BAG! - VISCOSITY 40 SEC/LL, ADD WATER - 5 LITRES L/LL. - PH 10.5, DO NOT ADD ANY MORE CAUSTIC FOR NOW! - 4 STAG ADDITIONS OF ASP 271 BUT DRISPAC 10. - 2 STAG ADDITIONS OF FTS 300 FOR NOW! - MIX 1 JUG OF X-CIDE A DAY - ALSO ALL 1 JUG OF X-CIDE - CHECK TO TRIPPING! - CHECK TO MIXING FILL IN FILL TANK, MIX 1/2 BAG OF - DEFAMER!								
STOCK POINT <u>FT. ST JOHN</u>			I.D.F. ENGINEER					
PHONE <u>888 4337</u>			PHONE					
			MOBILE #					

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-10-1991
 REPORT No. # 39
 SPUD DATE APR-29-91

WELL NAME COLUMBIA FT AL KOTANEELEE LOCATION VT-I-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07
 REPORT FOR Mr. NEIL PLISS REPORT FOR Mr. TIM SINGER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>8.1576 in</u>	COND.	TANKS <u>85 m³</u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>55.5</u>	m ³ /STK. <u>.0119</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>28-3200</u>	TOTAL <u>140.5</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>7500</u>
OTHER <u>HAC 196 L.</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>230</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>UCL 45.5 kg/m³</u>	MUD WT. <u>1190-1195 kg/m³</u>
HOLE COND.	UNDERFLOW WT. <u>UCL 80 ml/kg m³</u>	VISCOSITY <u>40-42 s/L</u>
DEVIATION <u>7/4° 3561</u>	OVERFLOW WT. <u>UCL HOLE TEMP 80 m³</u>	FILTRATE <u>API CAKE cm³/30 min.</u>
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE <u>275°F-107°C m³/min.</u>	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>16:00</u>	<u>09:30</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>3587</u>	<u>3580</u>	<u>PARITE 2326</u>			<u>85</u>	<u>2741</u>	<u>1067.50</u>
FLOWLINE TEMPERATURE (°C)	<u>45.0</u>	<u>44.0</u>	<u>DFLC 17</u>			<u>7</u>	<u>5</u>	<u>1746.00</u>
DENSITY (kg/m ³)	<u>1195</u>	<u>1190</u>	<u>X-CIDE 28</u>			<u>1</u>	<u>27</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>47</u>	<u>47</u>	<u>DISP-10 60</u>			<u>3</u>	<u>57</u>	<u>487.50</u>
APPARENT VISCOSITY (mPa.s)	<u>77</u>	<u>26</u>						
PLASTIC VISCOSITY (mPa.s)	<u>18</u>	<u>17</u>						
YIELD POINT (Pa)	<u>9</u>	<u>9</u>						
GELS 0/10 min. (Pa)	<u>1512</u>	<u>1512</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.7</u>	<u>10.7</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>15.5</u>	<u>16</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.0</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.0/1.2</u>	<u>1.0/1.2</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>	<u>300</u>	<u>28=2 LR=2 1000=19</u>					
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.0015</u>	<u>.0015</u>	<u>2000=28 2000=36 2000=54</u>					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.078</u>	<u>.075</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.922</u>	<u>.925</u>	PREVIOUS COST <u>77.970</u>	STARTING VOLUME				
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST <u>7925.2</u>	VOL. BUILT <u>1 HA. M³</u>				
ELECTRICAL STABILITY (V) <u>H2S</u>	<u>0</u>	<u>0</u>	CUM. COST <u>80,856.18</u>	VOL. LOST ON SURFACE <u>1</u>				
OIL/WATER RATIO <u>ASP 771</u>	<u>.7</u>	<u>.7</u>	CUM. ENG. COST <u>15,375.88</u>	VOL. LOST SUB SURFACE <u>1</u>				
CaCl ₂ w/w% <u>SUBPHITES</u>	<u>150</u>	<u>150</u>		END VOLUME <u>1</u>				
"n"/"k" <u>TOTAL POLYMER</u>	<u>4.0 KG/L³</u>	<u>4.0</u>		CUM. VOL. BUILT				

COMMENTS: 1. MUD DENSITY @ 1190-1195 KG/M³: IF DENSITY GOES BELOW 1185 KG/M³ MIX 50 GALS PARITE @ 4 MIN. / BAG. & RAISE DENSITY TO 1270 KG/M³ PRIOR TO 2650 M. (CHECK W/ ENG.)
 2. VISCOSITY @ 40-42 SEC/100 ml WATER @ 5 LITRES / MIN.
 3. PH @ 10.5, DO NOT ADD CAUSTIC FOR NOW!
 4. STOP ADDITION OF ASP 771!
 5. SINCE A NEW MIX 1 JUG OF X-CIDE - ALSO 1 X-CIDE PRIOR TO TRIP!
 6. CONTROL FLUID LOSS @ 15-17 CM @ 12 DISPAC-10 @ 75 MIN / BAG!
 7. PRIOR TO MIXING PULLING PILL TANK, MIX 1/2 PAIL DEFOAMER.
 8. HURRY TO TRIP! IF YOU ARE GOING TO PRESSURE TEST!
 MIX 4 PAILS OF PTS-200, ISOLATE LAST TWO TANKS, MIX 2 PAILS IN EACH TANK! PUMP FOR 40 MINUTES, THEN PUMP PILL!
 STOCK POINT FT. ST. JOHN I.D.F. ENGINEER RICK KEIN, SHART
 PHONE 785-4727 PHONE FAR ROOM MOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 11 1991
 REPORT No. # 40
 SPUD DATE APR 29 91

WELL NAME COLUMBIA ET AL KOTANEE LEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #07

REPORT FOR Mr. _____ REPORT FOR Mr. JIM SIGNER

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 9/16 IN</u>	COND.	TANKS <u>85.1</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>56.1</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>150</u> mm	INTER <u>178-220</u>	TOTAL <u>141.1</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9500</u>
OTHER <u>THA 196.1</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>230</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T. POLYMER</u>	FLOWLINE WT <u>46.1</u> kg/m ³	MUD WT. <u>1190-1195</u> kg/m ³
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>80.1</u> kg/m ³	VISCOSITY <u>40-45</u> s/L
DEVIATION <u>JETS 3X10.3</u>	OVERFLOW WT <u>70.1</u> kg/m ³	FILTRATE <u>15-17</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>7.5</u> m ³ /min.	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2609</u>	<u>2598</u>	SULPHITE	<u>18</u>		<u>1</u>	<u>17</u>	<u>49.70</u>
FLOWLINE TEMPERATURE (°C)	<u>44.0</u>	<u>40.0</u>	X-CIDE	<u>27</u>		<u>1</u>	<u>76</u>	<u>140.00</u>
DENSITY (kg/m ³)	<u>1190</u>	<u>1195</u>						
FUNNEL VISCOSITY (s/L)	<u>47</u>	<u>44</u>						
APPARENT VISCOSITY (mPa.s)	<u>74.5</u>	<u>78</u>						
PLASTIC VISCOSITY (mPa.s)	<u>17</u>	<u>19</u>						
YIELD POINT (Pa)	<u>7.5</u>	<u>9</u>						
GELS 0/10 min. (Pa)	<u>1.512</u>	<u>1.512</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>16.5</u>	<u>15.7</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>.5</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>9/1.3</u>	<u>9/1.3</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>50</u>	<u>60</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>300</u>	<u>300</u>	TR = 1 LR = 3 LOSR = 16					
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.007</u>	<u>.0015</u>	TCOR = 25 FCOR = 27 LOR = 49					
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.075 TRACE</u>	<u>.075</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.925 (OIL)</u>	<u>.925</u>	PREVIOUS COST <u>80.856</u>					
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST <u>189.70</u>					
ELECTRICAL STABILITY (V) H ₂ S	<u>0</u>	<u>0</u>	CUM. COST <u>81045.86</u>					
OIL/WATER RATIO <u>ASP. 721</u>	<u>.6</u>	<u>.6</u>	CUM. ENG. COST <u>15.250</u>					
CaCl ₂ w/w% <u>SULPHITES</u>	<u>130</u>	<u>130</u>						
"n" <u>KRTAL POLYMER</u>	<u>4.0</u>	<u>4.0</u>						

COMMENTS: 1. MUD DENSITY 1190-1195 KG/M³ IF DENSITY GOES BELOW 1185 KG/M³ MIX 50 SXS BARITE 4 MIN/1 BAG.
 2. VISCOSITY 47-45 SEC/CL. K/WATER = 5 LITRES/1 MIN.
 3. PH = 10.5: DO NOT ADD CAUSTIC FOR NOW!
 4. STOP ADDITIONS OF ASP. 721
 5. MIX 1 JOG OF X-CIDE ONCE A DAY!
 6. CONTINUED FLUID LOSS - 15-17 CM³/L = DISPLACE LO OVER 1 CIRC.
 7. PRIOR TO MIXING PILL IN PILL TANKS MIX 1/2 PAIL DEFORMER.
 8. PRIOR TO TRIPS IF YOU ARE GOING TO PRESSURE TEST, MIX 4 PAILS OF PTS-200 + 1 JOG X-CIDE ISOLATE LAST TWO TANKS. MIX 2 PAILS PTS 200 IN EACH TANK. MIX 1/2 JOG X-CIDE IN EACH TANK. PUMP FOR 40 MIN. THEN PUMP PILL!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KICK KENNHART
 PHONE 785-4777 PHONE FAR ROOM MOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-17-1991
 REPORT No. # 41
 SPUD DATE APR-29-91

WELL NAME COLUMBIA ET AL KUTANEE LEE LOCATION YT-I-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. PORTER-NEIL RUSS REPORT FOR Mr. PHIL ROSEWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>9.157mm</u>	COND.	TANKS <u>84.17</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>56.17</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>170</u> mm	INTER <u>178-3777</u>	TOTAL <u>140.17</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9.000</u>
OTHER <u>PHI-196m</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>730</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>1190-1195</u> kg/m ³	MUD WT. <u>1190-1195</u> kg/m ³			
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>PT. 1.00</u> kg/m ³	VISCOSITY <u>45 SEC 1L</u> s/L			
DEVIATION <u>8° @ 2610m</u>	OVERFLOW WT. <u>EST. C.H.T.F.</u> kg/m ³	FILTRATE <u>15.17</u> cm ³ /30 min.			
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE <u>275 F</u> m ³ /min.	pH <u>10.5</u>			

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>14:00</u> <u>3630</u>	<u>08:00</u> <u>3673</u>				<u>90</u>	<u>351</u>	<u>1125.00</u>
FLOWLINE TEMPERATURE (°C)	<u>42°</u>	<u>41°</u>	<u>BARITE</u>	<u>3241</u>		<u>8</u>	<u>49</u>	<u>1799.20</u>
DENSITY (kg/m ³)	<u>1195</u>	<u>1185</u>	<u>DISPAC</u>	<u>57</u>		<u>4</u>	<u>31</u>	<u>1040.00</u>
FUNNEL VISCOSITY (s/L)	<u>44</u>	<u>43</u>	<u>PT-300</u>	<u>35</u>		<u>2</u>	<u>74</u>	<u>780.00</u>
APPARENT VISCOSITY (mPa.s)	<u>27.5</u>	<u>26</u>	<u>X-CIDE</u>	<u>26</u>				
PLASTIC VISCOSITY (mPa.s)	<u>19</u>	<u>18</u>						
YIELD POINT (Pa)	<u>8.5</u>	<u>8</u>						
GELS 0/10 min. (Pa)	<u>1.5/7</u>	<u>1.5/7</u>						
pH STRIP <input type="checkbox"/> METER <input type="checkbox"/>	<u>10.</u>	<u>10.3</u>						
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>15.8</u>	<u>16.0</u>						
FILTER CAKE (mm)	<u>.5</u>	<u>.8</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>85/11.2</u>	<u>8/11.3</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>80</u>	<u>80</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>	<u>300</u>	<u>PRE-1</u>	<u>AR-7</u>	<u>100R-17</u>			
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.007</u>	<u>.007</u>	<u>300R-27</u>	<u>300R-36</u>	<u>600R-55</u>			
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.08</u>	<u>.077</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.97</u>	<u>.977</u>	PREVIOUS COST	<u>81,045.89</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> 7% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>	<u>10</u>	DAILY COST	<u>3744.20</u>	VOL. BUILT	<u>7 HANKS</u>		
ELECTRICAL STABILITY (V) <u>H.S</u>	<u>0</u>	<u>0</u>	CUM. COST	<u>84,790.09</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>OSP-731</u>	<u>.6</u>	<u>.6</u>	CUM. ENG. COST	<u>16,125.09</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w% <u>SULPHITES</u>	<u>100</u>	<u>100</u>			END VOLUME			
"n"/"k" <u>TOTAL POLYMER</u>	<u>4.2</u>	<u>4.2</u>			CUM. VOL. BUILT			

COMMENTS:

AS SOON AS YOU GET BACK ON POTTIUM W/ BIT #10

1 ROW WATER = 10 LITRES / MINUTE FOR 1 CIRCULATION?

3 ROWS = 1 BAG OF SODIUM SULPHITE OVER 1 CIRCULATION?

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER ALICE REINHART
 PHONE 785-4777 PHONE FAR ROOM OVERSIDE #1

THE INFORMATION IN THIS REPORT IS BASED ON OUR EXPERIENCE. REPRESENTS OUR BEST JUDGEMENT IN THE MATTER AND IS INTENDED TO BE HELPFUL. BUT WE CANNOT ASSUME RESPONSIBILITY FOR ANY LOSS OR ACCIDENT THAT MAY RESULT FROM ITS USE. FURTHERMORE, NOTHING CONTAINED HEREIN SHALL BE CONSTRUED AS A RECOMMENDATION TO USE ANY PRODUCT IN CONFLICT WITH EXISTING PATENTS COVERING ANY MATERIALS OR USE.



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUN 13 1991
 REPORT No. # 43
 SPUD DATE APR 29 91

WELL NAME COLEAS FT. ST. JOHN FIELD LOCATION VT - J - 48
 OPERATOR COLEAS GAS DEVELOPMENT CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. BOB TOOLE - NEW PLISS REPORT FOR Mr. PAUL COOK - WORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>10.1575</u>	COND.	TANKS <u>70 M³</u>	PUMP SIZE <u>4 1/4 x 4 1/2</u>	OPPOSITE D.P. <u>53.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>56 M³</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>93</u>
DRILL COLLARS <u>170</u> mm	INTER. <u>55 x 27.7</u>	TOTAL <u>176 M³</u>	S.P.M. <u>54</u>	PUMP PRESS. <u>11,000</u>
OTHER <u>SHA - 300 M.</u>	OTHER	STANDBY	m ³ /min. <u>6.272</u>	CIRC. TIME <u>200</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>T. Polymer</u>	FLOWLINE WT. <u>46 M³</u> kg/m ³	MUD WT. <u>1195 - 1200</u> kg/m ³
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>70 M³</u> kg/m ³	VISCOSITY <u>45 SECIL</u> s/L
DEVIATION	OVERFLOW WT.	FILTRATE <u>15.17</u> cm ³ /30 min.
CURRENT OP. <u>DRILLING</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

TIME SAMPLE TAKEN	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	DATE	TIME	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
JUN 14	05:00	19:30	F.L.R.	79		4	75	640.00
	2654	2636	LLUIS	50		3	47	1760.00
	41°C	38°C	SUPHITE	17		1	16	49.70
	1305	1300	SWASH	75		1	34	20.00
	47	45						
	27.5	30						
	20	21						
	7.5	9						
	1.512	1.512						
	10.5	10.5						
	17	20						
	1.7	1.0						
	1.2/1.7	1.0/1.7						
	80	100						
	300	300						
	.002	.002						
	.085	.083						
	.915	.917	PREVIOUS COST	84.790	STARTING VOLUME			
	10	10	DAILY COST	1969.70	VOL. BUILT			THANIS
			CUM. COST	86,759.70	VOL. LOST ON SURFACE			
			CUM. ENG. COST	16,500.00	VOL. LOST SUB SURFACE			
	1.75	1.75			END VOLUME			
	4.8	4.5			CUM. VOL. BUILT			

COMMENTS: 1) DENSITY 1190-1195 KG/L - KEEP MIXING AND GUM!
IF DENSITY COEF. BELOW 1190 KG/L, MIX 50 LBS DAPITE @ 4 MIN/ BAG!
2) VISCOSITY @ 45 SECIL. RUN WATER @ 5 LITERS/MIN. WHEN (1)C.
3) MIX 1 TUB OF X-CIDE ONCE A DAY. MIX 1 SUPHITE A DAY.
4) HAVE PRE-MIX TANK 3/4 FULL. RAISE DENSITY TO 1270 KG/L
MIX 200 TO 250 SX DAPITE @ 1/2 MINUTE A BAG!

5) MAIN SYSTEMS MIX TONIGHT 10 PAILS OF SOLIDAN @ 30 MIN
PAIL, 3 BAGS SOLIDASH + 3 BAGS OF AMISAC-LO.

6) KEEP VISCOSITY @ 45 SECIL. PRE-MIX @ 55 SECIL @ 1 BAG F.L.R.
ONLY IF REGIL. DO NOT ADD ANY WATER TO PRE-MIX.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KICK REINHART
 PHONE 785-4777 PHONE FAR. FROM OUTMOBILE #1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 14 1991
 REPORT No. # 43
 SPUD DATE APR 29 91

WELL NAME COIGAS ETAL KOTANEE LEE LOCATION VT. I-48
 OPERATOR COLOMBIA GAS DEVELOPMENT CONTRACTOR KENTING HT. 7
 REPORT FOR Mr. POD TOLE-NEIL BLISS REPORT FOR Mr. PHIL COSCILLWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>10-1/8 IN</u>	COND.	TANKS <u>70 LIT</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57 IN</u>	m ³ /STK. <u>0.118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120</u> mm	INTER <u>2223</u>	TOTAL <u>177 M³</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>10,000</u>
OTHER <u>PHA-300</u>	OTHER	STANDBY	m ³ /min. <u>59</u>	CIRC. TIME <u>215</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>1205-1310</u> kg/m ³	MUD WT. <u>1205-1310</u> kg/m ³	MUD WT. <u>1205-1310</u> kg/m ³	MUD WT. <u>1205-1310</u> kg/m ³	MUD WT. <u>1205-1310</u> kg/m ³
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>78 MIN</u> kg/m ³	UNDERFLOW WT <u>78 MIN</u> kg/m ³	VISCOSITY <u>45</u> s/L	VISCOSITY <u>45</u> s/L	VISCOSITY <u>45</u> s/L
DEVIATION	OVERFLOW WT <u>HOLE DRAG</u> kg/m ³	OVERFLOW WT <u>HOLE DRAG</u> kg/m ³	FILTRATE <u>15-18</u> cm ³ /30 min.	FILTRATE <u>15-18</u> cm ³ /30 min.	FILTRATE <u>15-18</u> cm ³ /30 min.
CURRENT OP <u>HOIST LIT #10</u>	UNDERFLOW RATE <u>11,000</u> m ³ /min.	UNDERFLOW RATE <u>11,000</u> m ³ /min.	pH <u>10.5</u>	pH <u>10.5</u>	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> <u>SHAKER</u>	MUD PROPERTIES <u>PRE-MIX</u>		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN	<u>13:30</u>	<u>13:30</u>	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>2664</u>		<u>BARITE</u>	<u>2151</u>		<u>435</u>	<u>7716</u>	<u>5477.50</u>
FLOWLINE TEMPERATURE (°C)	<u>38.00</u>		<u>FLR</u>	<u>65</u>		<u>3</u>	<u>67</u>	<u>480.00</u>
DENSITY (kg/m ³)	<u>1310</u>	<u>1210</u>	<u>DISPAC</u>	<u>49</u>		<u>7</u>	<u>47</u>	<u>1136.80</u>
FUNNEL VISCOSITY (s/L)	<u>44</u>	<u>51</u>	<u>SODASH</u>	<u>24</u>		<u>6</u>	<u>28</u>	<u>120.00</u>
APPARENT VISCOSITY (mPa.s)	<u>78</u>	<u>34</u>	<u>SULPHAN</u>	<u>96</u>		<u>10</u>	<u>86</u>	<u>2100.00</u>
PLASTIC VISCOSITY (mPa.s)	<u>30</u>	<u>70</u>						
YIELD POINT (Pa)	<u>8</u>	<u>14.5</u>						
GELS 0/10 min. (Pa)	<u>1.5/2</u>	<u>2/4</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>18</u>	<u>8.5</u>						
FILTER CAKE (mm)	<u>1.0 TIGHT</u>	<u>1.0</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.8/2.3</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>300</u>							
SAND CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.007</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.09</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (2) <input checked="" type="checkbox"/>	<u>.91</u>							
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>							
ELECTRICAL STABILITY (V) <u>H2S</u>	<u>0</u>							
OIL/WATER RATIO <u>SULPHAN</u>	<u>1.4 KG/M³</u>							
CaCl ₂ w/w% <u>SULPHITE</u>	<u>100 AGIL</u>							
"n"/"k" <u>TOTAL POLYMER</u>	<u>5 KG/L</u>							
PREVIOUS COST	<u>86,259.50</u>							
DAILY COST	<u>9774.00</u>							
CUM. COST	<u>96,034.50</u>							
CUM. ENG. COST	<u>16,875.80</u>							
STARTING VOLUME	<u>7,100 L</u>							
VOL. BUILT	<u>1</u>							
VOL. LOST ON SURFACE	<u>1/2</u>							
VOL. LOST SUB SURFACE	<u>1/2</u>							
END VOLUME								
CUM. VOL. BUILT								

COMMENTS: 1 ADD DENSITY TO 1205 KG/M³. KEEP MUD GUNS RUNNING!
IF DENSITY GOES BELOW 1200 KG/M³: MIX 50 BARITE + 4 LITERS/ BAG
AS SOON AS YOU GET BACK ON BOTTOM W/ LIT #11!
1 RUN WATER TO 10 LITERS/ MIN. FOR 1 CIRCULATION.
2 RUN IN 1X-LINE OVER 1 FULL CIRC. THEN RUN 1 SULPHITE.
3 AFTER BOTTOMS UP MIX 4 BAGS DISPAC TO 55 MIN/ BAG.
4 KEEP VISCOSITY IN PRE-MIX TO 55 SEC/L. MIX 1/2 BAG OF FLR-REG. AS REQD.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KICK REINHART
 PHONE 785-4772 PHONE FAR ROOM OUT MOBILE # #1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE-15-1991
 REPORT No. # 44
 SPUD DATE APR-29-91

WELL NAME COLGAS ETAL KOTANELEE LOCATION V7-I-48
 OPERATOR COLGAS ETAL GAS DEVELOPMENT CONTRACTOR KENTING HI-TOWER
 REPORT FOR Mr. POP TOOLE-NEIL BLISS REPORT FOR Mr. PAUL ROSONI/COLITH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/8" MILL</u>	COND.	TANKS <u>73</u>	PUMP SIZE <u>114X406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120</u> mm	INTER <u>58-3372</u>	TOTAL <u>130 m³</u>	S.P.M. <u>50</u>	PUMP PRESS <u>10.000</u>
OTHER <u>THAN 700</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>215</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>ST. POLYMER</u>	FLOWLINE WT <u>APPROX. 001 = 46 m³</u> kg/m ³	MUD WT. <u>1205-1210</u> kg/m ³
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>ETA. U = 78 m³</u> kg/m ³	VISCOSITY <u>45</u> s/L
DEVIATION	OVERFLOW WT <u>PRE-MIX = 55 m³</u> kg/m ³	FILTRATE <u>15-17</u> cm ³ /30 min.
CURRENT OP <u>MILL AND CONES</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN	<u>01:30</u>						
PRESENT DEPTH (m)	<u>3664</u>						
FLOWLINE TEMPERATURE (°C)	<u>27.0</u>						
DENSITY (kg/m ³)	<u>1215</u>						
FUNNEL VISCOSITY (s/L)	<u>44</u>						
APPARENT VISCOSITY (mPa.s)	<u>29</u>						
PLASTIC VISCOSITY (mPa.s)	<u>21</u>						
YIELD POINT (Pa)	<u>8</u>						
GELS 0/10 min. (Pa)	<u>1.517</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>18.5</u>						
FILTER CAKE (mm)	<u>1.2 FIRM.</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.6/2.0</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>50</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>200</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.002</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.093</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.907</u>						
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>						
ELECTRICAL STABILITY (V) H ₂ S	<u>0</u>						
OIL/WATER RATIO <u>SULFATES</u>	<u>1.4 KG/L</u>						
CaCl ₂ w/w%	<u>120</u>						
"n" / "K" TOTAL POLYMER	<u>5 KG/L</u>						
PREVIOUS COST	<u>96,034.95</u>	STARTING VOLUME					
DAILY COST		VOL. BUILT			<u>THAN 115</u>		
CUM. COST		VOL. LOST ON SURFACE					
CUM. ENG. COST	<u>17,250.00</u>	VOL. LOST SUB SURFACE					
		END VOLUME					
		CUM. VOL. BUILT					

COMMENTS:
 AS SOON AS YOU GET BACK ON BOTTOM W/ BIT #11
 I RUN WATER @ 10 LITRES/MIN. FOR 1 CIRCULATION
 2 RUN 1/2 BAG OF SOLIDIFY SUFFINITE OVER 1 FULL CIRCULATION
 3 AFTER BOTTOMS UP? MIX 4 BAGS OF ENIS PAC - LOW
 @ 55 MINUTES TAG!
 4 KEEP VISCOSITY IN PRE-MIX @ 55 SEC. MIX 1/2 BAG
 OF F.L.R. REGUMAN IF REQ'D.

STOCK POINT ET. ST. JOHN I.D.F. ENGINEER KILIK REUSHAIT
 PHONE 785-4222 PHONE FAR ROOM MOBILE # 1

THE INFORMATION IN THIS REPORT IS BASED ON OUR EXPERIENCE. REPRESENTS OUR BEST JUDGEMENT IN THE MATTER AND IS INTENDED TO BE HELPFUL BUT WE CANNOT ASSUME RESPONSIBILITY FOR ANY LOSS OR ACCIDENT THAT MAY RESULT FROM ITS USE. FURTHERMORE, NOTHING CONTAINED HEREIN SHALL BE CONSTRUED AS A RECOMMENDATION TO USE ANY PRODUCT IN CONFLICT WITH EXISTING PATENTS COVERING ANY MATERIALS OR USE



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 15 1991
 REPORT No. #44A
 SPUD DATE APR 29 91

WELL NAME COIGAS FTAL KUTANEE LEE LOCATION YT-I-48

OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING HI TOWER 7

REPORT FOR Mr. FOR TOOLE-NEIL PLISS REPORT FOR Mr. PHIL COSEWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / #11- <u>1 1/2 in</u>	COND.	TANKS <u>72 m³</u>	PUMP SIZE <u>14x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57 m³</u>	m ³ /STK. <u>.0018</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>130</u> mm	INTER <u>78-3372</u>	TOTAL <u>130 m³</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9200</u>
OTHER <u>THA-</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>215</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT <u>ANN. VOL. 46 m³</u>	kg/m ³	MUD WT <u>1305-1310 KG</u>	kg/m ³	
HOLE COND. <u>GOOD</u>	UNDERFLOW WT <u>ETA. U¹ 78 m³</u>	kg/m ³	VISCOSITY <u>45</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m ³	FILTRATE <u>15-17</u>	cm ³ /30 min.	
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE	m ³ /min.	pH <u>10.5</u>		

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST				
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE
TIME SAMPLE TAKEN <u>19:00</u>						
PRESENT DEPTH (m) <u>2667</u>		<u>BARITE 2716</u>		<u>70</u>	<u>2646</u>	<u>875.00</u>
FLOWLINE TEMPERATURE (°C) <u>36.0</u>		<u>X-CIDE 24</u>		<u>2</u>	<u>22</u>	<u>280.00</u>
DENSITY (kg/m ³) <u>1215</u>		<u>SIPHITE 16</u>		<u>2</u>	<u>14</u>	<u>99.40</u>
FUNNEL VISCOSITY (s/L) <u>42</u>		<u>MUSPAC 42</u>		<u>3</u>	<u>39</u>	<u>487.20</u>
APPARENT VISCOSITY (mPa.s) <u>29.5</u>		<u>FIR-REG 62</u>		<u>1</u>	<u>61</u>	<u>160.00</u>
PLASTIC VISCOSITY (mPa.s) <u>27</u>						
YIELD POINT (Pa) <u>7.5</u>						
GELS 0/10 min. (Pa) <u>1.5/2</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>					
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>27</u>					
FILTER CAKE (mm)	<u>1.0 THICK!</u>					
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.5/1.9</u>					
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	<u>60</u>					
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl (mg/L)	<u>300</u>					
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.002</u>					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.092</u>					
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.907</u>					
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>10</u>					
ELECTRICAL STABILITY (V) <u>115</u>	<u>0</u>					
OIL/WATER RATIO <u>WATER 1.4 KG/L</u>						
CaCl ₂ w/w% <u>SIPHITES 120</u>						
"n"/"k" <u>TOTAL POLYMER 5 KG/M³</u>						
PREVIOUS COST <u>96,034.</u>						
DAILY COST <u>1901.60</u>						
CUM. COST <u>97,935.</u>						
CUM. ENG. COST <u>17,750</u>						
STARTING VOLUME						
VOL. BUILT <u>THICKS</u>						
VOL. LOST ON SURFACE <u>1</u>						
VOL. LOST SUB SURFACE <u>1</u>						
END VOLUME						
CUM. VOL. BUILT						

COMMENTS:
AS SOON AS YOU GET ON BOTTOM W/ BIT #12!
1 Run THE CENTRIFUGE FOR 1 FULL CIRCULATION!
MIX 5 BAGS MUSPAC-10 AT 45 MINUTES A BAG!
MIX 1 JUG OF X-CIDE OVER 1 FULL CIRCULATION!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER MICHAEL REINHART
 PHONE 785-4372 PHONE AR Room 0115 MOBILE # 81

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 16 1991
 REPORT No. # 45
 SPUD DATE APR 79 91

WELL NAME COI GAS FT AL KOTANEE LEE LOCATION VT-I-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING HITOWER
 REPORT FOR Mr. POE TOOLE NEIL BLISS REPORT FOR Mr. PHIL BROWN

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 7/8 150mm</u>	COND.	TANKS <u>72m³</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>51.5</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>57m³</u>	m ³ /STK. <u>.0018</u>	OPPOSITE D.C. <u>90</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>19.2772</u>	TOTAL <u>130m³</u>	S.P.M. <u>53</u>	PUMP PRESS. <u>9200</u>
OTHER <u>114 200m³</u>	OTHER	STANDBY	m ³ /min. <u>.6136</u>	CIRC. TIME <u>210</u>

HOLE DATA		CENTRIFUGAL DESANDER/DESILT		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>1215 to 1200</u> kg/m ³	MUD WT. <u>1200</u> kg/m ³			
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>2720</u> kg/m ³	UNDERFLOW RATE <u>20 L/min.</u> m ³ /min.	VISCOSITY <u>45</u> s/L		
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>270</u> cm ³ /30 min.			
CURRENT OP <u>DRILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>			

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/> SHAKER	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>10.00</u>	<u>3672</u>	LAPITE	<u>246</u>		<u>25</u>	<u>2611</u>	<u>427.50</u>
FLOWLINE TEMPERATURE (°C)	<u>2700</u>		DRISPOC	<u>29</u>		<u>5</u>	<u>34</u>	<u>817.00</u>
DENSITY (kg/m ³)	<u>1200</u>		X-CIDE	<u>27</u>		<u>1</u>	<u>21</u>	<u>140.00</u>
FUNNEL VISCOSITY (s/L)	<u>42</u>		ATS-200	<u>21</u>		<u>4</u>		<u>1040.00</u>
APPARENT VISCOSITY (mPa.s)	27.5	<u>27.5</u>						
PLASTIC VISCOSITY (mPa.s)	20	<u>20</u>						
YIELD POINT (Pa)	7.5	<u>7.5</u>						
GELS 0/10 min. (Pa)	<u>1.5/2</u>							
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>							
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>36</u>							
FILTER CAKE (mm)	<u>1.0 FIRM.</u>							
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.5/1.9</u>							
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>40</u>							
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>250</u>							
SAND CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.002</u>		<u>PRE-1 67=2 1000=15</u>					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>.085</u>		<u>SCOPE=25 2000=25 6000=55</u>					
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input type="checkbox"/>	<u>915</u>		PREVIOUS COST	<u>97,925.60</u>	STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>17</u>		DAILY COST	<u>3429.50</u>	VOL. BUILT			<u>THIA-VS</u>
ELECTRICAL STABILITY (V) <input type="checkbox"/>	<u>0</u>		CUM. COST	<u>100,355.10</u>	VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>1.2 KOLM</u>			CUM. ENG. COST	<u>17,675.50</u>	VOL. LOST SUB SURFACE			
CaCl ₂ w/w% <u>SUBSTITUTES</u>	<u>130</u>				END VOLUME			
"n"/"k" <u>TOTAL LAYERS</u>	<u>4.5</u>				CUM. VOL. BUILT			

COMMENTS:
AS SOON AS YOU GET ON BOTTOM W/ BIT #12!
1 RUN WATER @ 5 LITRES/MIN. FOR 1 CIRCULATION!
MIX 5 BAGS DISPA-10 AT 45 MINUTES A BAG!
MIX 1 PAIL OF ASP-721 OVER 1 FULL CIRCULATION!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER PHIL BROWN
 PHONE 255-4222 PHONE FAR FROM OFFICE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 17-91
 REPORT No. # 46
 SPUD DATE APR - 29-91

WELL NAME COIGAS FT AL KOTANEELE LOCATION VT-7-48
 OPERATOR COIGAS GAS DEVELOPMENT CONTRACTOR KENTING HI-TOUR #7
 REPORT FOR Mr. BOB TOOLE-NEIL PLISS REPORT FOR Mr. PHIL ESCOBAR

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>12.154 mm</u>	COND.	TANKS <u>23M</u>	PUMP SIZE <u>1/4x406</u>	OPPOSITE D.P. <u>50</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>57M</u>	m ³ /STK. <u>0.118</u>	OPPOSITE D.C. <u>86</u>
DRILL COLLARS <u>120 mm</u>	INTER <u>155-3222</u>	TOTAL <u>120.0</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9500</u>
OTHER <u>THA 300L</u>	OTHER	STANDBY	m ³ /min. <u>.59</u>	CIRC. TIME <u>715</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>L.T. PULVER</u>	FLOWLINE WT.	kg/m ³	MUD WT. <u>1200</u>	kg/m ³	
HOLE COND. <u>GOOD</u>	UNDERFLOW WT.	kg/m ³	VISCOSITY <u>45</u>	s/L	
DEVIATION	OVERFLOW WT.	kg/m ³	FILTRATE <u>270</u>	cm ³ /30 min.	
CURRENT OP <u>HOLE BIT #12</u>	UNDERFLOW RATE	m ³ /min.	pH <u>10.5</u>		

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> SHAKER	MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>04:00</u>			MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>2681</u>			<u>INVENTORY JUNE 16 91 20:00 HRS.</u>					
FLOWLINE TEMPERATURE (°C) <u>35.0</u>			SODA ASH <u>28</u>			4	24	80.00
DENSITY (kg/m ³) <u>1190</u>			ASP-771 <u>55</u>			1	54	100.00
FUNNEL VISCOSITY (s/L) <u>45</u>			FT-200 <u>27</u>			2	25	570.00
APPARENT VISCOSITY (mPa.s) <u>29</u>			X-CILE <u>21</u>			1	20	140.00
PLASTIC VISCOSITY (mPa.s) <u>22</u>			SULPHITE <u>14</u>			1	13	49.70
YIELD POINT (Pa) <u>7</u>			DEFORM <u>13</u>			3	9	409.50
GELS 0/10 min. (Pa) <u>1.512</u>			DISPAC <u>34</u>			2	32	324.80
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>		FLU <u>5</u>			2	3	356.00
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³) <u>28</u>			SAL-257 <u>225</u>			28	200	186.20
FILTER CAKE (mm) <u>1.2 F/100L</u>			LINE <u>20</u>			4	16	24.40
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME) <u>1.5/1.9</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca. <input checked="" type="checkbox"/> (mg/L) <u>40</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L) <u>250</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>0.07</u>							
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>0.75</u>							
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>975</u>							
MBT (Kg/m ³) <input checked="" type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>17</u>							
ELECTRICAL STABILITY (V) <u>H:5</u>	<u>0</u>							
OIL/WATER RATIO <u>SULPHAN</u>	<u>1.2</u>							
CaCl ₂ w/w% <u>SULPHITE</u>	<u>120</u>							
"n"/"K" <u>TOTAL RUNNER</u>	<u>5.0 KG/M³</u>							

COMMENTS:
AS SOON AS YOU GET TO BOTTOM OF PIT #14!
1 BBL WATER = 10 LITRES/110L FOR 1 CIRCULATION!
MIX 4 BAGS OF DISPAC 10 @ 55 MIN/EA!
MIX 1 @ 1 BAG OF ASP-771 OVER 1 FULL CIRCULATION!

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER ALIC REINHART
 PHONE 785-4222 PHONE FAL ROCK ON MOBILE #1

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 17 1991
 REPORT No. #46A
 SPUD DATE APRIL 29 91

WELL NAME COLOMBIA GAS DEVELOPMENT LOCATION VT - I - 48

OPERATOR COLOMBIA GAS DEVELOPMENT CONTRACTOR KENTING HITOWER 7

REPORT FOR Mr. FOR TOOLE NEIL ELISS REPORT FOR Mr. PHIL ROSOMWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE <u>1 1/4 - 1 1/2 IN</u>	COND.	TANKS <u>69.5</u>	PUMP SIZE <u>114x406</u>	OPPOSITE D.P. <u>51.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>57.5</u>	m ³ /STK. <u>0.118</u>	OPPOSITE D.C. <u>90</u>
DRILL COLLARS <u>120</u> mm	INTER <u>158-2773</u>	TOTAL <u>177.17</u>	S.P.M. <u>57</u>	PUMP PRESS. <u>9500</u>
OTHER <u>THAC 500M.</u>	OTHER	STANDBY	m ³ /min. <u>6.136</u>	CIRC. TIME <u>710</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT POLYMER</u>	FLOWLINE WT. <u>46.5</u> kg/m ³	MUD WT. <u>1190-1200</u> kg/m ³			
HOLE COND. <u>GOOD</u>	UNDERFLOW WT. <u>76</u> kg/m ³	VISCOSITY <u>45</u> s/L			
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE cm ³ /30 min.			
CURRENT OF <u>DRILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>			

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. PIT June EMUD PROPERTIES

TIME SAMPLE TAKEN	EMUD PROPERTIES			MATERIALS INVENTORY & COST					
	04:00	01:00	30:00	MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	2695	2697	2685	BARITE	2611		35	2576	427.50
FLOWLINE TEMPERATURE (°C)	40°C	40°C	39°C	Y-CIDE	30		3	17	470.00
DENSITY (kg/m ³)	1195	1190	1195	DRISPAC	33		8	74	1799.70
FUNNEL VISCOSITY (s/L)	41	40	43	ASP-721	54		3	51	300.00
APPARENT VISCOSITY (mPa.s)	74	73.5	76	F.L.R	61		1	60	160.00
PLASTIC VISCOSITY (mPa.s)	19	19	20						
YIELD POINT (Pa)	5	4.5	6						
GELS 0/10 min. (Pa)	111.5	111.5	151.7						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	10.5	10.5	10.5						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	35	37	33						
FILTER CAKE (mm)	1.5/1.8	1.5	1.5						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	1.5/2.0	1.5/2.0	1.5/2.1						
TOTAL HARDNESS <input type="checkbox"/> Ca <input checked="" type="checkbox"/> (mg/L)	40	40	40						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	350	400	400	300 = 1 600 = 1 1000 = 12					
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	.007	.007	.007	2000 = 21 3000 = 39 6000 = 48					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	.08	.078	.08						
OIL/WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	.92	.922	.93	PREVIOUS COST <u>102,855.7</u>	STARTING VOLUME				
MBT (Kg/m ³) <input checked="" type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	15	15	15	DAILY COST <u>3616.70</u>	VOL. BUILT <u>THANKS</u>				
ELECTRICAL STABILITY (V) <u>H2S</u>	0	0	0	CUM. COST <u>105,472.40</u>	VOL. LOST ON SURFACE				
OIL/WATER RATIO <u>SULFAN</u>	1.0	1.0	1.0	CUM. ENG. COST <u>18,000.28</u>	VOL. LOST SUB SURFACE				
CaCl ₂ w/w% <u>SULFITE</u>	130	130	130		END VOLUME <u>✓</u>				
"n" <u>TOTAL POLYMER</u> <u>7 KG/M</u> <u>76.5</u> <u>6 KG/M</u>					CUM. VOL. BUILT				

COMMENTS:

AS SOON AS YOU GET BACK ON BOTTOM w/ BIT #15!

FINISH RUNNING IN THE ASP-721 IN CHEM. EEL OVER 70 MIN.

RUN IN THE LAST BAG OF F.L.R. REG. OVER 70 MIN.

RUN IN WATER AT 5 LITRES/MINUTE.

1 RUN IN 3 BAGS OF ASP-721 IN 70 MIN. 1 BAG?

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER KEVIN REINHART

PHONE 785-4777 PHONE FAR DOON MOBILE # 1



INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE JUNE 19, 1991

REPORT No. # 48

SPUD DATE APR. 29, 91

WELL NAME COLGAS ETAL KUTANEELEE

LOCATION YT. I. 48

OPERATOR COLUMBIA GAS DEVELOPMENT

CONTRACTOR KENTING HI TOWER 7

REPORT FOR Mr. Bob Toole - Neil Pluss

REPORT FOR Mr. Will Roseworth

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>4.5-1.5 IN</u>	COND.	TANKS <u>72</u>	PUMP SIZE <u>414 x 406</u>	OPPOSITE D.P. <u>51.5</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>58</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>90</u>
DRILL COLLARS <u>170</u> mm	INTEREST <u>3773</u>	TOTAL <u>130</u>	S.P.M. <u>53</u>	PUMP PRESS.
OTHER <u>LHA-200</u>	OTHER	STANDBY	m ³ /min. <u>.6136</u>	CIRC. TIME <u>210</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. Polymer</u>	FLOWLINE WT. <u>46.5</u> kg/m ³	MUD WT. <u>1190-1200</u> kg/m ³			
HOLE COND. <u>Good</u>	UNDERFLOW WT. <u>76</u> kg/m ³	VISCOSITY <u>45</u> s/L			
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>L15</u> cm ³ /30 min.			
CURRENT OF <u>FILLING</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>			

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH-SPEED SHAKER

SAMPLE FROM FL. PIT

MUD PROPERTIES		MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>08:00</u> <u>3705</u>						
FLOWLINE TEMPERATURE (°C)	<u>36.0</u>						
DENSITY (kg/m ³)	<u>1200</u>						
FUNNEL VISCOSITY (s/L)	<u>43</u>						
APPARENT VISCOSITY (mPa.s)	<u>24</u>						
PLASTIC VISCOSITY (mPa.s)	<u>19</u>						
YIELD POINT (Pa)	<u>5</u>						
GELS <u>0</u> 10 min. (Pa)	<u>111.5</u>						
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.3</u>						
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>25</u>						
FILTER CAKE (mm)	<u>1.0 FIRM.</u>						
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.4/2.0</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>30</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>350</u>						
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.007</u>						
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.085</u>						
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.915</u>						
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>14</u>						
ELECTRICAL STABILITY (V) <u>112</u>	<u>0</u> <u>M61L</u>						
OIL/WATER RATIO <u>5/100</u>	<u>1.0</u> <u>K61M</u>						
CaCl ₂ w/w% <u>SLIPWITE</u>	<u>110</u> <u>M61L</u>						
"n" <u>"K" TOTAL POLYMER</u>	<u>7.5</u> <u>K61M</u>						

COMMENTS:

1. Pump WATER = 5 LITRE / MIN.
 2. AFTER MIXING THE NEXT 3 ASP. 20% IF THE VISCOSITY IS 45 SEC/L OR LESS, MIX 3 MORE PAILS.
 3. PRIOR TO NEXT TRIP: ISOLATE LAST TWO TANKS MIX 4 PAILS OF PTS-200, 2 PAILS IN EACH TANK. LIP PLAC FOR 40 MINUTES AND PUMP FILL.

STOCK POINT FT. ST. JOHN
 PHONE 854 777

I.D.F. ENGINEER RICK BELMONT
 PHONE 800 601 6011 MOBILE 81

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-19
 REPORT No. 49
 SPUD DATE 91-04-29

WELL NAME Colcas et al KOTAVELEF LOCATION YT - I - 48
 OPERATOR COLUMBIA GAS DEVELOP. CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. BOB TADLE / NEIL BLISS REPORT FOR Mr. PHIL BOSOMWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>15 / 152</u>	COND.	TANKS <u>72</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>58</u>	m ³ /STK. <u>0118</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER. <u>178/3273</u>	TOTAL <u>130</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.6</u>	CIRC. TIME <u>215 ±</u>

HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>BTTMS UP = 80</u> kg/m ³	MUD WT. <u>1190-1200</u> kg/m ³			
HOLE COND. <u>OK.</u>	UNDERFLOW WT. kg/m ³	VISCOSITY <u>40-45</u> s/L			
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>15</u> cm ³ /30 min.			
CURRENT OP. <u>CIR</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>			

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES			MATERIALS INVENTORY & COST					
TIME SAMPLE TAKEN <u>22:30</u>				MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m) <u>3733</u>				BARITE			35		438
FLOWLINE TEMPERATURE (°C) <u>40</u>				ASP-721			10		1200
DENSITY (kg/m ³) <u>1195</u>				SOD. SUL.			1		50
FUNNEL VISCOSITY (s/L) <u>43</u>				X-CIDE			3		280
APPARENT VISCOSITY (mPa.s) <u>26</u>				FLR			6		960
PLASTIC VISCOSITY (mPa.s) <u>20</u>				PTS-200			4		1040
YIELD POINT (Pa) <u>6</u>				EDVIS			2		840
GELS 0/10 min. (Pa) <u>1/1.5</u>				K. SEAL (PREV)			10		238
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>								
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>15.0</u>								
FILTER CAKE (mm) <u>.8</u>									
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.4/5.0</u>								
TOTAL HARDNESS <input type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>TR.</u>								
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CaCl ₂ (mg/L)	<u>350</u>								
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.003</u>								
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.085</u>								
OIL/WATER CONT. (%) <input type="checkbox"/> (Ø) <input type="checkbox"/>	<u>.915</u>								
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u>								
ELECTRICAL STABILITY (V) H ₂ S <u>N+G.</u>									
OIL/WATER RATIO <u>SULFITE 100</u>									
CaCl ₂ w/w% <u>TOTAL POLYMER 9 Kg/m³</u>									
"n"/"k"									

(600/300 52/32)
 (200/100 23/14)
 6/3 1.5/1

COMMENTS: DRILLED TO 3733 m + TRIP FOR BIT.

- CONTROL DENSITY AT 1195. 1200 kg/m³. RUN 5 LITRES H₂O PER MIN.
- KEEP PH AT 10.5 USING CAUSTIC.
- MAINTAIN VIS. AT 40-45 s/L USING ASP-721 + FLR. ADD 3 ASP-721 EVERY 12 HRS.
- ADD 1 X-CIDE + 1 SK. SOD. SUL. DAILY.

STOCK POINT FT ST JOHN D.F. ENGINEER JIM WHEELER
 PHONE 785-4323 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-21
 REPORT No. 51
 SPUD DATE 91-04-29

WELL NAME COLGAS of a KOTANELEGE LOCATION VT F-48
 OPERATOR COLUMBIA GAS DEVELOPMENT CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. BOB TOOLE / NEIL RUSSELL REPORT FOR Mr. PHIL BOSOMWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>17 / 1</u>	COND.	TANKS <u>74</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>60</u>	m ³ /STK. <u>0118</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER. <u>178/3273</u>	TOTAL <u>134</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9700</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.6</u>	CIRC. TIME <u>225±</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT.	kg/m ³ MUD WT. <u>1190-1200</u> kg/m ³
HOLE COND.	UNDERFLOW WT.	kg/m ³ VISCOSITY <u>40-45</u> s/L
DEVIATION <u>7°14' @ 3767 m 11 1/4"</u>	OVERFLOW WT.	kg/m ³ FILTRATE <u>2.15</u> cm ³ /30 min.
CURRENT OP. <u>DRUG.</u>	UNDERFLOW RATE	m ³ /min. pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST				
		INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN	<u>22:00</u> / <u>02:00</u>					
PRESENT DEPTH (m)	<u>3190</u> / <u>3802</u>	ASP-721		<u>2</u>		<u>200</u>
FLOWLINE TEMPERATURE (°C)	<u>40</u> / <u>41</u>	FLR		<u>5</u>		<u>800</u>
DENSITY (kg/m ³)	<u>1210</u> / <u>1195</u>	PTS-200		<u>3</u>		<u>780</u>
FUNNEL VISCOSITY (s/L)	<u>44</u> / <u>44</u>	PARITE		<u>35</u>		<u>438</u>
APPARENT VISCOSITY (mPa.s)	<u>30</u> / <u>30</u>	CAUSTIC		<u>2</u>		<u>60</u>
PLASTIC VISCOSITY (mPa.s)	<u>24</u> / <u>24</u>					
YIELD POINT (Pa)	<u>6</u> / <u>6</u>					
GELS 0/10 min. (Pa)	<u>112</u> / <u>112</u>					
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u> / <u>11.0</u>					
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>24</u> / <u>17.0</u>					
FILTER CAKE (mm)	<u>.8</u> / <u>.8</u>					
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.3/5.0</u> / <u>1.5/5.5</u>					
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u> / <u>TR.</u>					
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input checked="" type="checkbox"/> (mg/L)	<u>350</u> / <u>350</u>					
SAND CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.004</u> / <u>.003</u>					
SOLIDS CONTENT (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.09</u> / <u>.08</u>					
WATER CONT. (%) <input type="checkbox"/> (0) <input checked="" type="checkbox"/>	<u>.91</u> / <u>.92</u>	PREVIOUS COST	<u>115,692</u>	STARTING VOLUME		
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u> / <u>-</u>	DAILY COST	<u>2278</u>	VOL. BUILT		
ELECTRICAL STABILITY (V) <u>H₂S</u>	<u>NEG.</u> / <u>NEG.</u>	CUM. COST	<u>117,970</u>	VOL. LOST ON SURFACE		
OIL/WATER RATIO <u>SULFATE</u>	<u>115</u> / <u>120</u>	CUM. ENG. COST	<u>19,875</u>	VOL. LOST SUB SURFACE		
CaCl ₂ w/w% <u>POLYMER (K₂CO₃)</u>	<u>9.5</u> / <u>9.5</u>			END VOLUME		
"n"/"k"				CUM. VOL. BUILT		

COMMENTS: DRUG. 152 mm HOLE RAN CENTRIFUGE FOR 1 HR.
MAINTAIN VISC. AT 40-45 S/L USING ASP-721 + FLR.
HOLD DENSITY AT 1190-1200 Kg/m³. RUN 5 LITRES H₂O PER MIN.
ADD 1 L ACIDE + 1 L SOL. SULFATE DAILY.
ADD 2 ASP-721 EVERY 12 HRS.
KEEP PH AT 10.5 USING CAUSTIC.

STOCK POINT FT. ST. JOHN G.H.E.D.F. ENGINEER TIM WHEELER
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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DRILLING FLUID REPORT

DATE 91-06-22
 REPORT No. 52
 SPUD DATE 91-04-29

INTERNATIONAL DRILLING FLUIDS

WELL NAME Colgas of Kotanefelle LOCATION YT I 48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. #7
 REPORT FOR Mr. Bob Toole / Neil Bliss REPORT FOR Mr. Phil Basomworth

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>17 / 152</u>	COND.	TANKS <u>72</u>	PUMP SIZE <u>114 x 406</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89</u> mm	SURFACE	HOLE <u>61</u>	m ³ /STK. <u>.0118</u>	OPPOSITE D.C. <u>68</u>
DRILL COLLARS <u>120</u> mm	INTER <u>178 / 323</u>	TOTAL <u>133</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>9600</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.6</u>	CIRC. TIME <u>200 ±</u>

HOLE DATA	DESANDER/DESILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>BAMS UP = 85 MIN</u> kg/m ³	MUD WT. <u>1190 - 1200</u> kg/m ³
HOLE COND. <u>OK.</u>	UNDERFLOW WT. kg/m ³	VISCOSITY <u>40-45</u> s/L
DEVIATION	OVERFLOW WT. kg/m ³	FILTRATE <u>< 15</u> cm ³ /30 min.
CURRENT OP. <u>CIR.</u>	UNDERFLOW RATE m ³ /min.	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST					
	TIME SAMPLE TAKEN		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
PRESENT DEPTH (m)	<u>09:00</u> <u>3820</u>	<u>19:00</u> <u>3843</u>	<u>BARITE</u>	<u>2468</u>		<u>35</u>	<u>2433</u>	<u>438</u>
FLOWLINE TEMPERATURE (°C)	<u>42</u>	<u>43</u>	<u>FLO PLEX</u>	<u>56</u>		<u>22</u>	<u>34</u>	<u>2750</u>
DENSITY (kg/m ³)	<u>1195</u>	<u>1195</u>	<u>FLR</u>	<u>49</u>		<u>6</u>	<u>38</u>	<u>960</u>
FUNNEL VISCOSITY (s/L)	<u>46</u>	<u>46</u>	<u>XCIDE</u>	<u>13</u>		<u>1</u>	<u>14</u>	<u>140</u>
APPARENT VISCOSITY (mPa.s)	<u>28</u>	<u>28</u>	<u>ASP-721</u>	<u>32</u>		<u>7</u>	<u>25</u>	<u>700</u>
PLASTIC VISCOSITY (mPa.s)	<u>22</u>	<u>22</u>	<u>SOD. SULF.</u>	<u>11</u>		<u>1</u>	<u>10</u>	<u>50</u>
YIELD POINT (Pa)	<u>6</u>	<u>6</u>	<u>SAWDUST</u>	<u>200</u>		<u>70</u>	<u>130</u>	<u>343</u>
GELS 0/10 min. (Pa)	<u>112</u>	<u>112</u>	<u>PTS-200</u>	<u>18</u>			<u>18</u>	
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>	<u>10.5</u>	<u>CAUSTIC</u>	<u>178</u>			<u>178</u>	
FILTRATE <input type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>8.0</u>	<u>7.6</u>						
FILTER CAKE (mm)	<u>45</u>	<u>5</u>						
ALK <input type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>14 / 5.2</u>	<u>14 / 5.4</u>						
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>	<u>TR.</u>						
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>350</u>	<u>350</u>	<u>600/300</u>	<u>56/34</u>				
SAND CONTENT (%) <input type="checkbox"/> (0/1)	<u>.003</u>	<u>.003</u>	<u>200/100</u>	<u>26/14</u>				
SOLIDS CONTENT (%) <input type="checkbox"/> (0/1)	<u>.08</u>	<u>.08</u>	<u>613</u>	<u>312</u>				
WATER CONT. (%) <input type="checkbox"/> (0/1)	<u>.92</u>	<u>.92</u>	PREVIOUS COST	<u>115.692</u>			STARTING VOLUME	
MBT (Kg/m ³) <input type="checkbox"/> % <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u>	<u>-</u>	DAILY COST	<u>5381</u>			VOL. BUILT	
ELECTRICAL STABILITY (V) <u>H₂S</u>	<u>NEG.</u>	<u>NEG</u>	CUM. COST	<u>121,072</u>			VOL. LOST ON SURFACE	
OIL/WATER RATIO <u>SULFITE</u>	<u>130</u>	<u>130</u>	CUM. ENG. COST	<u>19,875</u>			VOL. LOST SUB SURFACE	
CaCl ₂ w/w% <u>POLYMER</u>	<u>10</u>	<u>10</u>					END VOLUME	
"n"/"k"							CUM. VOL BUILT	

COMMENTS: CIR. PRIOR TO TRIP FOR BIT #17 LOST 8 m³ FROM 3822-3784 m
PUMPED 14 m³ W.C.M. FILL PRIOR TO TRIP
CONTROL DENSITY AT 1190-1200 kg/m³. RUN 5 LITRES H₂O PER MIN.
MAINTAIN PH AT 10.5 WITH CAUSTIC.
HOLD VISC. AT 40-45 S/L USING ASP-721. ADD 3 PAILS EVERY 12 HRS
ADD 1 SA. SOD. SULFITE + 1 XCIDE PAIL.
PRIOR TO TRIP OUT TO LOG, MIX 7 PAILS PTS-200 + 2 XCIDE.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WIELER
 PHONE 785-4222 PHONE AT LOCATION MOBILE #

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DRILLING FLUID REPORT

DATE 91-06-24
 REPORT No. 54
 SPUD DATE 91-04-29

INTERNATIONAL DRILLING FLUIDS

WELL NAME <u>COLGAS 2 of KOTANELEE</u>			LOCATION <u>YT - I 48</u>		
OPERATOR <u>COLUMBIA GAS DEVEL.</u>			CONTRACTOR <u>KENTON H.T. # 7</u>		
REPORT FOR Mr. <u>BOB TADDE / NEIL RICE</u>			REPORT FOR Mr. <u>PHIL RASOMI, NORTH</u>		
ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT		ANNULAR VEL. m./min.
BIT SIZE / # <u>18 / 152</u>	COND.	TANKS <u>75</u>	PUMP SIZE <u>114 x 406</u>		OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>69 mm</u>	SURFACE	HOLE <u>62</u>	m ³ /STK. <u>1018</u>		OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER. <u>178 / 373</u>	TOTAL <u>137</u>	S.P.M. <u>50</u>		PUMP PRESS. <u>9100</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>6</u>		CIRC. TIME <u>230±</u>
HOLE DATA		DESANDER/DESTILTER		DRILLING FLUID SPECIFICATIONS	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>600/200 52/32</u>	kg/m ³	MUD WT. <u>1190-1200</u>	kg/m ³	
HOLE COND. <u>OK</u>	UNDERFLOW WT. <u>200/100 24/14</u>	kg/m ³	VISCOSITY <u>40-45</u>	s/L	
DEVIATION <u>8° 2388 N34° E</u>	OVERFLOW WT. <u>613 3/2</u>	kg/m ³	FILTRATE <u>< 15</u>	cm ³ /30 min.	
CURRENT OP. <u>CIR.</u>	UNDERFLOW RATE	m ³ /min.	pH <u>10.5</u>		
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input checked="" type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER					
SAMPLE FROM FL. <input checked="" type="checkbox"/> PIT <input type="checkbox"/> <u>OK</u>		MUD PROPERTIES		MATERIALS INVENTORY & COST	
TIME SAMPLE TAKEN	<u>15:30</u>				
PRESENT DEPTH (m)	<u>3915</u>		MATERIALS	INITIAL	RECEIVED
FLOWLINE TEMPERATURE (°C)	<u>44</u>		<u>PARTE</u>	<u>2888</u>	<u>35</u>
DENSITY (kg/m ³)	<u>1205</u>		<u>FLR</u>	<u>25</u>	<u>35</u>
FUNNEL VISCOSITY (s/L)	<u>44</u>		<u>X-CIDE</u>	<u>13</u>	<u>12</u>
APPARENT VISCOSITY (mPa.s)	<u>26</u>		<u>ASP-721</u>	<u>25</u>	<u>5</u>
PLASTIC VISCOSITY (mPa.s)	<u>20</u>		<u>SD-SUL</u>	<u>9</u>	<u>9</u>
YIELD POINT (Pa)	<u>6</u>		<u>SAWDUST</u>	<u>130</u>	<u>130</u>
GELS 0/10 min. (Pa)	<u>1/2</u>		<u>HTS-200</u>	<u>18</u>	<u>8</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>10.5</u>		<u>CAUSTIC</u>	<u>173</u>	<u>6</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>6.6</u>		<u>TDMS D</u>	<u>45</u>	<u>5</u>
FILTER CAKE (mm)	<u>5</u>		<u>SUREAN</u>	<u>82</u>	<u>82</u>
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.5/5.5</u>		<u>SWA TICH</u>	<u>18</u>	<u>18</u>
TOTAL HARDNESS <input type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>		<u>LIME</u>	<u>16</u>	<u>5</u>
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input type="checkbox"/> (mg/L)	<u>350</u>		<u>CRISPAC</u>	<u>27</u>	<u>8</u>
SAND CONTENT (%) <input type="checkbox"/> (0.1) <input type="checkbox"/> (0.2) <input type="checkbox"/> (0.3)	<u>.004</u>		<u>DEFAMER</u>	<u>6</u>	<u>6</u>
SOLIDS CONTENT (%) <input type="checkbox"/> (0.1) <input type="checkbox"/> (0.2) <input type="checkbox"/> (0.3)	<u>.08</u>		<u>CSL</u>	<u>310</u>	<u>310</u>
OIL/WATER CONT. (%) <input type="checkbox"/> (0.1) <input type="checkbox"/> (0.2) <input type="checkbox"/> (0.3)	<u>.92</u>		<u>POLYMER</u>	<u>50</u>	<u>5</u>
MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>-</u>		PREVIOUS COST	<u>123,809</u>	STARTING VOLUME
ELECTRICAL STABILITY (VH ₂ S) <u>N.G.</u>	<u>N.G.</u>		DAILY COST	<u>6781</u>	VOL. BUILT
OIL/WATER RATIO <u>SULFITE</u>	<u>120 mg/L</u>		CUM. COST	<u>130,590</u>	VOL. LOST ON SURFACE
CaCl ₂ w/w% <u>POLYMER</u>	<u>10 kg/m³</u>		CUM. ENG. COST	<u>20,625</u>	VOL. LOST SUB SURFACE
"n"/"k"					END VOLUME
COMMENTS: <u>T.D. 3915 m CIR. PRIOR TO TRIP OUT TO LOG.</u>					CUM. VOL. BUILT
<u>MAINTAIN PH AT 10.5 USING CAUSTIC.</u>					
<u>CONTROL DENSITY AT 1190-1200 kg/m³. RUN 5 LINES H₂O WHEN CIR.</u>					
<u>Vis 40-45 s/L.</u>					
<u>NOTE: PRIOR TO TRIP OUT TO RUN LNER ADD 8 PAILS HTS-200 + 1 GAL X-CIDE.</u>					
STOCK POINT <u>R. ST. TOWN</u>			I.D.F. ENGINEER <u>TIM WIELER</u>		
PHONE <u>785-4222</u>			PHONE ON LOCATION		
			MOBILE #		

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-25
 REPORT No. 55
 SPUD DATE 91-04-29

WELL NAME COLGAS of 1 KOTANEE LEE LOCATION VT I-48
 OPERATOR COLUMBIA GAS DEVEL. CONTRACTOR KENTING H.T. # 7
 REPORT FOR Mr. BOB TOOLE REPORT FOR Mr. PHIL PASCOWORTH

ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT	ANNULAR VEL. m./min.
BIT SIZE / # <u>1 1/2</u>	COND.	TANKS <u>74</u>	PUMP SIZE <u>114 x 4 1/2</u>	OPPOSITE D.P. <u>51</u>
DRILL PIPE <u>89 mm</u>	SURFACE	HOLE <u>63</u>	m ³ /STK. <u>0.118 (0.067)</u>	OPPOSITE D.C. <u>88</u>
DRILL COLLARS <u>120 mm</u>	INTER. <u>178/2273</u>	TOTAL <u>136</u>	S.P.M. <u>50</u>	PUMP PRESS. <u>10,000</u>
OTHER	OTHER	STANDBY	m ³ /min. <u>.6 .6</u>	CIRC. TIME <u>230</u>

HOLE DATA	DESANDER/DESTILTER	DRILLING FLUID SPECIFICATIONS
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT. <u>600/300 58/36</u> kg/m ³	MUD WT. <u>1190-1200</u> kg/m ³
HOLE COND. <u>OK.</u>	UNDERFLOW WT. <u>200/100 27/16</u> kg/m ³	VISCOSITY <u>40-45</u> s/L
DEVIATION	OVERFLOW WT. <u>613 312</u> kg/m ³	FILTRATE <u>415</u> cm ³ /30 min.
CURRENT OP. <u>CIR.</u>	UNDERFLOW RATE	pH <u>10.5</u>

EQUIPMENT: DEGASSER DESILTER DESANDER CENTRIFUGE DOUBLE DECK OR HIGH SPEED SHAKER

SAMPLE FROM FL <input checked="" type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES	MATERIALS INVENTORY & COST					
		MATERIALS	INITIAL	RECEIVED	USED	BALANCE	COST
TIME SAMPLE TAKEN <u>20:00</u>							
PRESENT DEPTH (m) <u>3915</u>		BARITE <u>2353</u>			35	2318	438
FLOWLINE TEMPERATURE (°C) <u>41</u>		FLR <u>35</u>				35	
DENSITY (kg/m ³) <u>1210</u>		XCIDE <u>12</u>		2	10	280	
FUNNEL VISCOSITY (s/L) <u>46</u>		ASP-201 <u>20</u>			20		
APPARENT VISCOSITY (mPa.s) <u>29</u>		SND. SUL. <u>9</u>			9		
PLASTIC VISCOSITY (mPa.s) <u>22</u>		SAWDUST <u>130</u>			130		
YIELD POINT (Pa) <u>7</u>		PTS-200 <u>102</u>		8	96	2080	
GELS 0/10 min. (Pa) <u>112</u>		CRUSTIC <u>167</u>		1	166	30	
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>	TDUS D <u>40</u>			40		
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>7.6</u>	SULBAN <u>82</u>			82		
FILTER CAKE (mm) <u>.5</u>		SODALASH <u>18</u>			18		
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>48/6.0</u>	LIME <u>11</u>			11		
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca. <input type="checkbox"/> (mg/L)	<u>78.</u>	DRISPAK <u>19</u>			19		
SAL. <input type="checkbox"/> NaCl <input type="checkbox"/> CL <input checked="" type="checkbox"/> (mg/L)	<u>350</u>	DEFAMER <u>6</u>			6		
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.002</u>	CEL <u>310</u>			310		
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.05</u>	POLYTRAMP <u>.50</u>			.50		
OH ₂ /WATER CONT. (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.92</u>	PREVIOUS COST <u>127,290</u>		STARTING VOLUME			
MBT (Kg/m ³) <input type="checkbox"/> 1% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>—</u>	DAILY COST <u>2828</u>		VOL. BUILT			
ELECTRICAL STABILITY (VH ₂₅) <u>N.G.</u>		CUM. COST <u>132,118</u>		VOL. LOST ON SURFACE			
OIL/WATER RATIO <u>SULFITE</u>	<u>120</u>	CUM. ENG. COST <u>21,000</u>		VOL. LOST SUB SURFACE			
CaCl ₂ w/w% <u>POLYMER</u>	<u>10</u>			END VOLUME			
"n"/"k"				CUM. VOL. BUILT			

COMMENTS: T.D. 3915 m LOGGED. RAN CLEAN OUT TRIP TO RUN LINER.

STOCK POINT FT. ST. JOHN I.D.F. ENGINEER JIM WYLER
 PHONE 785-4222 PHONE ON LOCATION MOBILE #

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INTERNATIONAL DRILLING FLUIDS

DRILLING FLUID REPORT

DATE 91-06-26/27
 REPORT No. 56
 SPUD DATE 91-04-29

WELL NAME <u>COLGAS #1 of KOTANEFIELD</u>		LOCATION <u>VT I-48</u>	
OPERATOR <u>COLUMBIA GAS DEVELOPMENT</u>		CONTRACTOR <u>KENTING H.T. #7</u>	
REPORT FOR Mr. <u>BOE TADLE</u>		REPORT FOR Mr. <u>PHIL RAMMERTH</u>	
ASSEMBLY	CASING	MUD Vol. (m ³)	PUMP OUTPUT
BIT SIZE / # /	COND.	TANKS	ANNULAR VEL. m./min.
DRILL PIPE mm	SURFACE	HOLE	OPPOSITE D.P.
DRILL COLLARS mm	INTER <u>172/3273</u>	TOTAL	OPPOSITE D.C.
OTHER	OTHER <u>127/3915</u>	STANDBY	PUMP PRESS.
HOLE DATA		DESANDER/DESTILTER	
MUD TYPE <u>WT. POLYMER</u>	FLOWLINE WT.	kg/m ³	DRILLING FLUID SPECIFICATIONS
HOLE COND. <u>OK.</u>	UNDERFLOW WT.	kg/m ³	MUD WT. kg/m ³
DEVIATION	OVERFLOW WT.	kg/m ³	VISCOSITY s/L
CURRENT OP. <u>C.R.</u>	UNDERFLOW RATE	m ³ /min.	FILTRATE cm ³ /30 min.
EQUIPMENT: <input type="checkbox"/> DEGASSER <input type="checkbox"/> DESILTER <input type="checkbox"/> DESANDER <input type="checkbox"/> CENTRIFUGE <input type="checkbox"/> DOUBLE DECK OR HIGH SPEED SHAKER			
SAMPLE FROM FL. <input type="checkbox"/> PIT <input type="checkbox"/>	MUD PROPERTIES		MATERIALS INVENTORY & COST
TIME SAMPLE TAKEN <u>09:30</u>		MATERIALS	INITIAL RECEIVED USED BALANCE COST
PRESENT DEPTH (m) <u>3915</u>		<u>BARITE</u>	<u>23.8</u> <u>10</u> <u>2308</u> <u>125</u>
FLOWLINE TEMPERATURE (°C) <u>40</u>		<u>FLR</u>	<u>35</u> <u>35</u>
DENSITY (kg/m ³) <u>1210</u>		<u>XCLIDE</u>	<u>10</u> <u>3</u> <u>7</u> <u>420</u>
FUNNEL VISCOSITY (s/L) <u>46</u>		<u>ASP-721</u>	<u>21</u> <u>21</u>
APPARENT VISCOSITY (mPa.s) <u>25</u>		<u>SOD. SUL.</u>	<u>9</u> <u>9</u>
PLASTIC VISCOSITY (mPa.s) <u>20</u>		<u>SAWDUST</u>	<u>130</u> <u>30</u> <u>100</u> <u>147</u>
YIELD POINT (Pa) <u>5</u>		<u>PTS-200</u>	<u>96</u> <u>5</u> <u>91</u> <u>1300</u>
GELS 0/10 min. (Pa) <u>112</u>		<u>CAUSTIC</u>	<u>166</u> <u>166</u>
pH STRIP <input checked="" type="checkbox"/> METER <input type="checkbox"/>	<u>11.0</u>	<u>IDV D</u>	<u>40</u> <u>40</u>
FILTRATE <input checked="" type="checkbox"/> API <input type="checkbox"/> HT HP (cm ³)	<u>11.0</u>	<u>SULFAN</u>	<u>82</u> <u>82</u>
FILTER CAKE (mm) <u>.8</u>		<u>SOD. ASH</u>	<u>18</u> <u>18</u>
ALK <input checked="" type="checkbox"/> (PF/MF) <input type="checkbox"/> (PM/LIME)	<u>1.8/6.4</u>	<u>LIME</u>	<u>11</u> <u>11</u>
TOTAL HARDNESS <input checked="" type="checkbox"/> Ca <input type="checkbox"/> (mg/L)	<u>TR.</u>	<u>DR. STAC</u>	<u>19</u> <u>19</u>
SAL <input type="checkbox"/> NaCl <input type="checkbox"/> Cl <input type="checkbox"/> (mg/L)	<u>350</u>	<u>DESANDER</u>	<u>6</u> <u>1</u> <u>5</u> <u>136</u>
SAND CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>---</u>	<u>GEL</u>	<u>310</u> <u>10</u> <u>300</u> <u>100</u>
SOLIDS CONTENT (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.08</u>	<u>POLYTEMP</u>	<u>50</u> <u>50</u>
Oil/WATER CONT. (%) <input type="checkbox"/> (Ø) <input checked="" type="checkbox"/>	<u>.92</u>	PREVIOUS COST	<u>132118</u> STARTING VOLUME
MBT (Kg/m ³) <input type="checkbox"/> /% <input type="checkbox"/> OIL RET <input type="checkbox"/>	<u>---</u>	DAILY COST	<u>3172</u> VOL. BUILT
ELECTRICAL STABILITY (V) <u>H₂S</u>	<u>NEG.</u>	CUM. COST	<u>135290</u> VOL. LOST on SURFACE
OIL/WATER RATIO <u>SULFITE</u>	<u>120</u>	CUM. ENG. COST	<u>21,750</u> VOL. LOST SUB SURFACE
CaCl ₂ w/w% <u>POLYMER</u>	<u>9.0</u>		END VOLUME
"n"/"k"			CUM. VOL. BUILT
COMMENTS: <u>RAN LINER (127 mm)</u>		<u>BICARB</u>	<u>55</u> <u>55</u>
<u>LOST APPROX. 21 m³ MUD TO HOLE</u>		<u>RESIN</u>	<u>#</u> <u>---</u>
<u>WHILE RUNNING LINER PUMPED</u>		<u>DFCL</u>	<u>3</u> <u>3</u>
<u>L.C.M. & BYPASSED SHAKER WHILE</u>		<u>BEADS</u>	<u>32</u> <u>32</u>
<u>CIR. DRIP TO CEMENTING.</u>		<u>FCL</u>	<u>60</u> <u>60</u>
		<u>POLYTEMP</u>	<u>50</u> <u>50</u>
		<u>K. SEAL</u>	<u>100</u> <u>11</u> <u>89</u> <u>262</u>
		<u>IDRGE</u>	<u>4</u> <u>4</u>
		<u>VISPLEX</u>	<u>10</u> <u>2</u> <u>8</u> <u>500</u>
		<u>CaCO₃</u>	<u>102</u> <u>102</u>
		<u>CELLULOSE</u>	<u>20</u> <u>8</u> <u>12</u> <u>185</u>
		<u>WALNUT</u>	<u>20</u> <u>20</u>
		<u>FLOPER</u>	<u>34</u> <u>34</u>
STOCK POINT <u>FT. ST. JOHN</u>	I.D.F. ENGINEER <u>JIM WHEELER</u>		
PHONE <u>785-4222</u>	PHONE ON LOCATION	MOBILE #	

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Kotanelee I-48

**THIN SECTION STUDY
NAHANNI FORMATION
KOTANEELEE AREA**

*Report in Liard M-25
file*

**Ian G. Hunter, Ph.D., P. Geol.
Ian Hunter Consulting Ltd.**

January, 2001