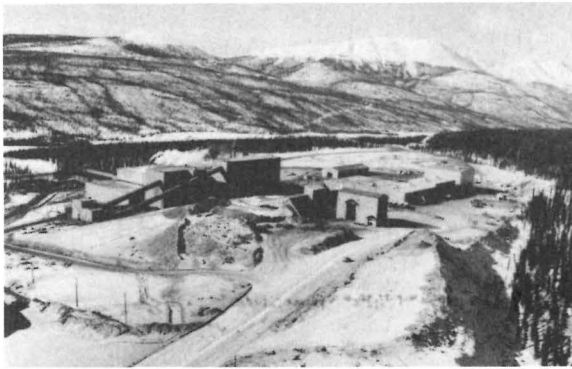
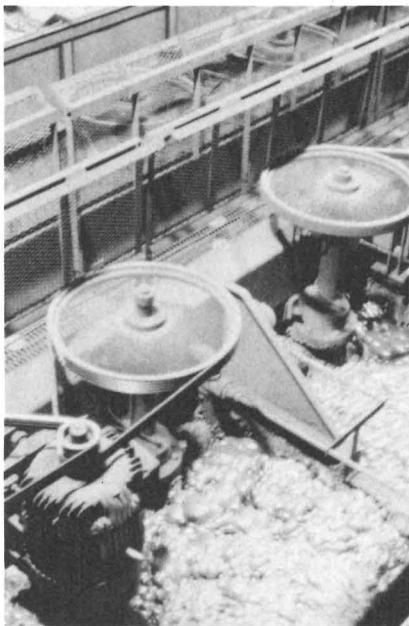


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The Development of Vangorda Plateau Ore Deposits



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RE AHO 2 JOHN BRUK



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1.
PROGRAM

THE DEVELOPMENT OF THE VANGORDA PLATEAU ORE DEPOSITS

A continuing objective of Cyprus Anvil Mining Corporation is to increase the mineable ore reserves in the Anvil District to extend the life of the Faro Operation. To this end, an agreement was consummated between Cyprus Anvil Mining Corporation and Kerr Addison Mines Limited and Canadian Natural Resources Limited on May 15th, 1979, whereby Cyprus Anvil acquired all of the mineral properties of the respective companies in the Anvil District. These properties cover approximately 31 square kilometres and include the Grum and Vangorda deposits, located on the Vangorda Plateau. These two lead, zinc and silver orebodies contain significant amounts of ore mineable by open pit methods. This development program includes only the proven open pit portions of the Vangorda Plateau deposits.

Subsequent to the acquisition, studies were conducted to determine the most financially attractive schedule for the development of the Vangorda Plateau deposits. The recommended program is based upon the sequential development of the Vangorda and Grum open pit reserves and the concurrent milling of these ores with mill feed from the Faro pit, which otherwise would have been exhausted in 1989. In the economic analysis of this development, the present

mining plan is used as the base case and identified as Case 1.

The program, identified as Case 4B-V provides for modifications to the existing concentrator to be completed by January 1st, 1982 and the subsequent construction of ancillary facilities to treat Vangorda Plateau ores. Pre-production stripping of the Vangorda deposit will commence in 1984 to permit ore production prior to the end of that year. Vangorda and Faro ores will be milled in equal proportions at the current capacity of 3.4 million tonnes per year until 1988, at which time the Vangorda reserves will be exhausted. To ensure continuity of ore supply, the pre-production stripping of Grum will commence in 1985 to permit the phased development of Vangorda ore with that from Grum in 1988.

The Vangorda deposit is structurally simple and well understood based on the results of recent intensive drilling. The early development of this deposit will extend the life of the Faro pit providing both increased flexibility and reliability in ore supply and will allow the time necessary to develop an efficient mining plan for the geologically more complex Grum deposit. Since less pre-production stripping is required, the Vangorda deposit can be developed sooner than the Grum, thereby facilitating the early inclusion of the Vangorda Plateau ore to economic advantage into

the overall mining plan. The ore from the Vangorda Plateau will be transported approximately 14 kilometres to the mill by one of three haulage systems. Currently under study are off-highway trucks, railway and a cable belt conveyor. Supplemental power generating facilities and new tailings impoundment ponds are provided for in the program.

The total capital cost of this development program during the next nine years will be \$155.9 million in January 1980 dollars. Escalated for inflation, the capital budget is estimated to be \$239.3 million.

The appreciable reduction in the cost per pound of marketable metal produced realized through the implementation of the 4B-V program reflects the significant increase in metal production, particularly that of gold and silver.

The project will be financed by internal cash flow generation and borrowing through available lines of credit. When compared to the cash flow generated by milling only the Faro deposits, the program will yield a return on investment based on discounted cash flows (DCF/ROI) of 36.6%. This DCF/ROI results from the increased production of lead, zinc and precious metals, improved metallurgical performance and the extension from 1989 to 1997 of the open

pit mining operations. Using an after tax discount rate of 12 percent the comparative net present value per share on currently issued shares of the cash flows available for distribution at equilibrium prices are; Case 1 \$27.28, Case 4B-V \$39.75 for an increase of 45.5 percent. Discounting at 15 percent the development case increased the net present value per share from \$24.05 to \$32.83 or 36.5 percent.

FIGURE I-1 VANGORDA PLATEAU DEVELOPMENT
PAYABLE METAL PRODUCTION

FARO ALONE
CASE 4B-V

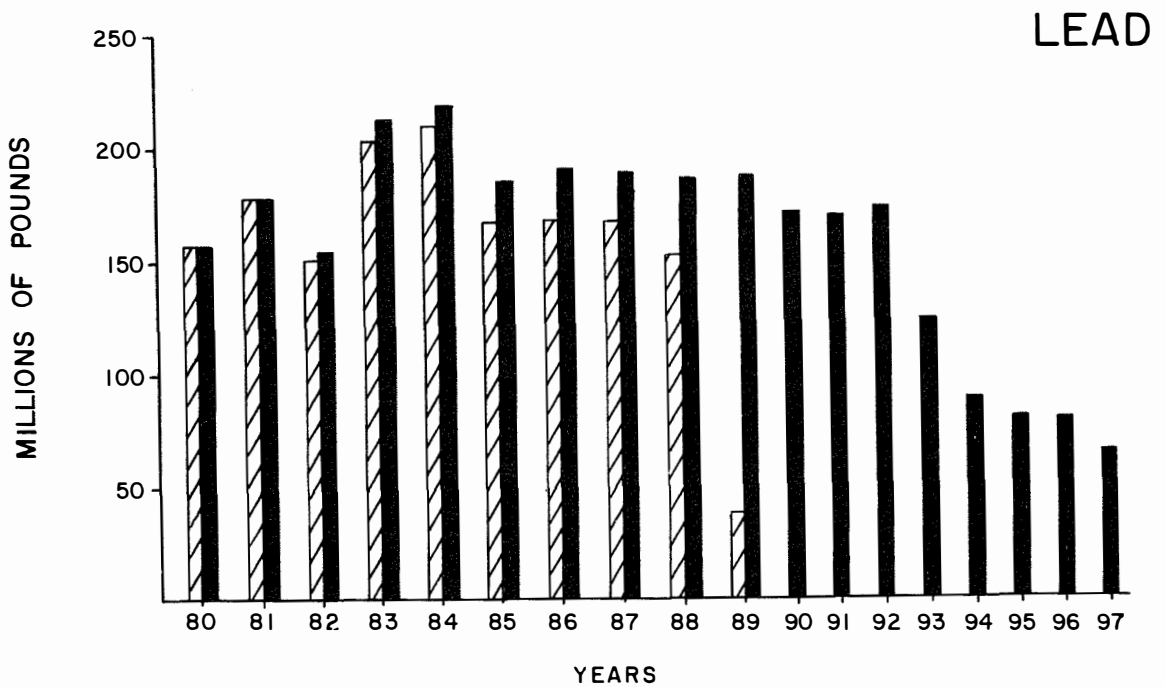
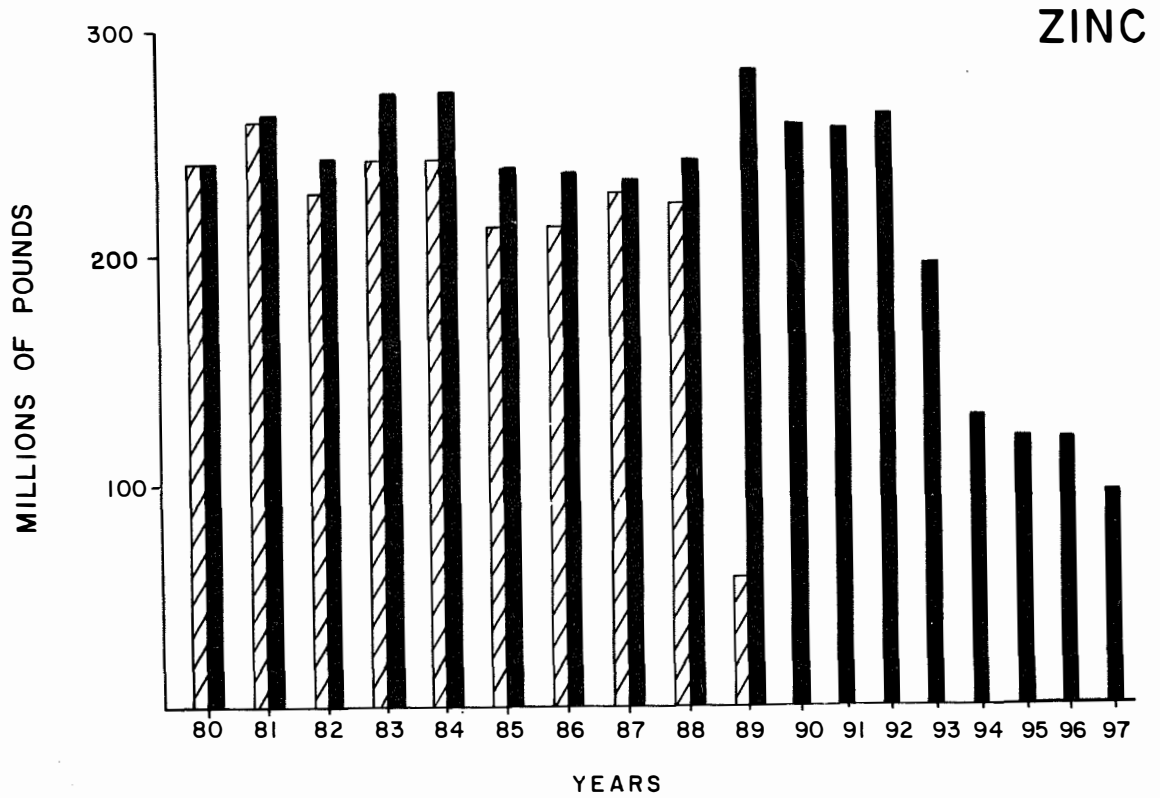


FIGURE 1-2 VANGORDA PLATEAU DEVELOPMENT
PAYABLE METAL PRODUCTION

FARO ALONE
CASE 48 - V

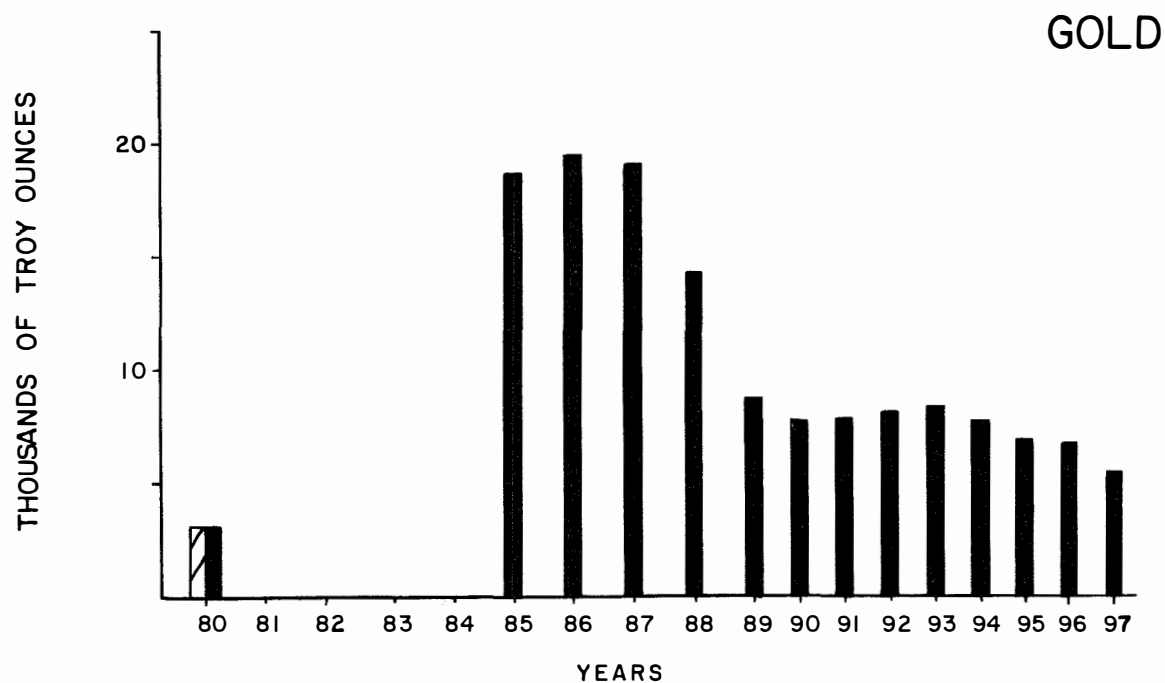
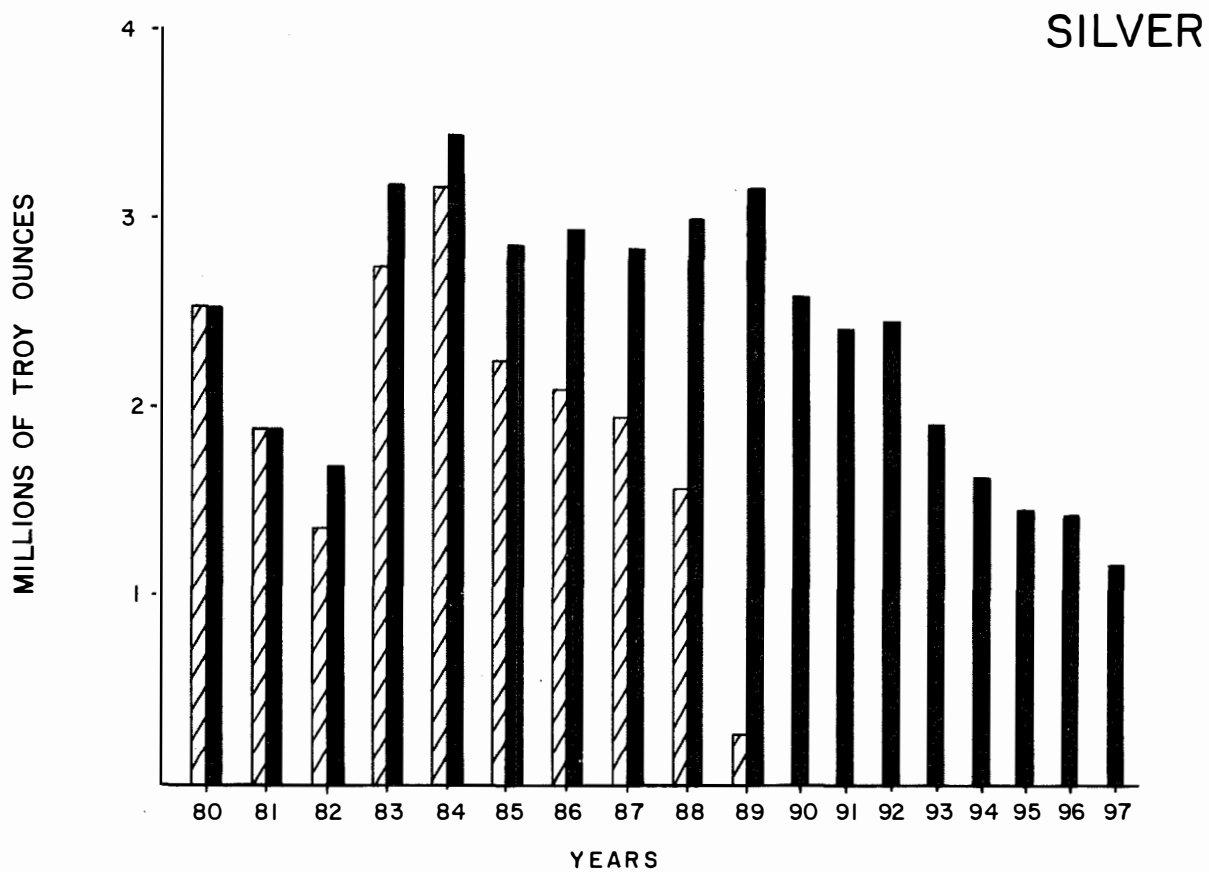
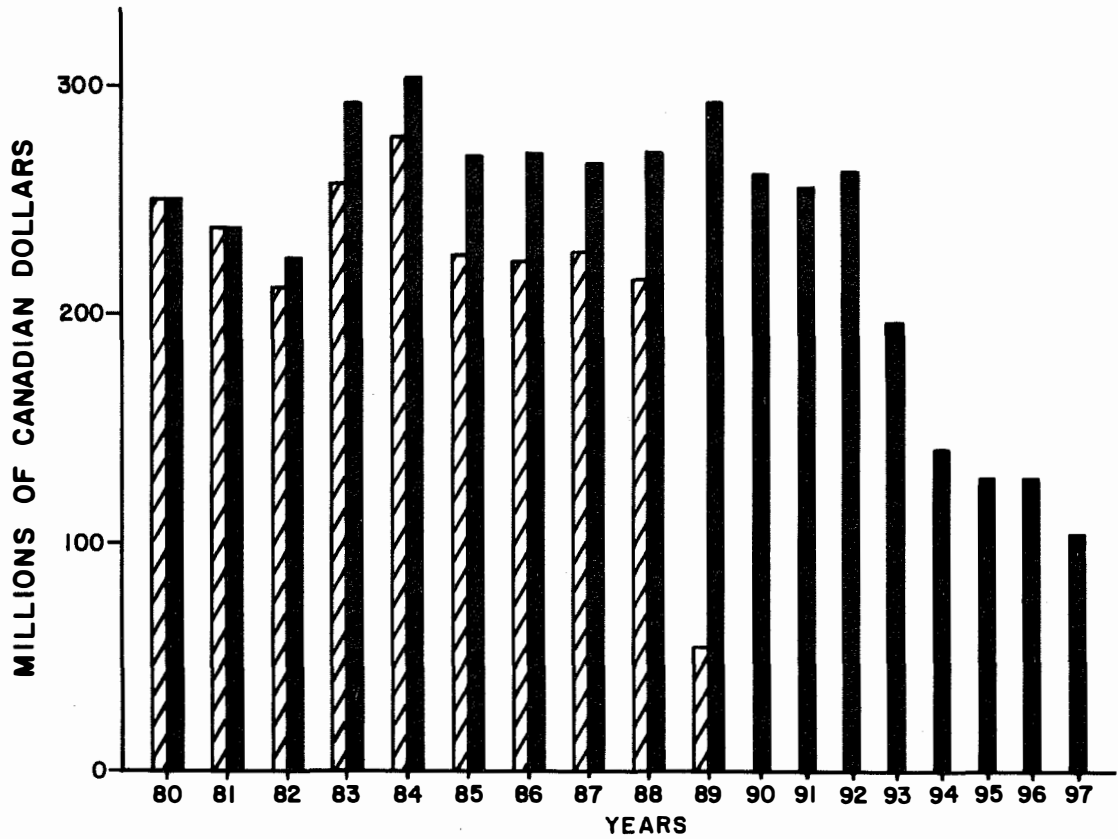


FIGURE 1-3 VANGORDA PLATEAU DEVELOPMENT

FARO ALONE 
CASE 4B-V 

GROSS SALES



NET PROFIT AFTER TAX

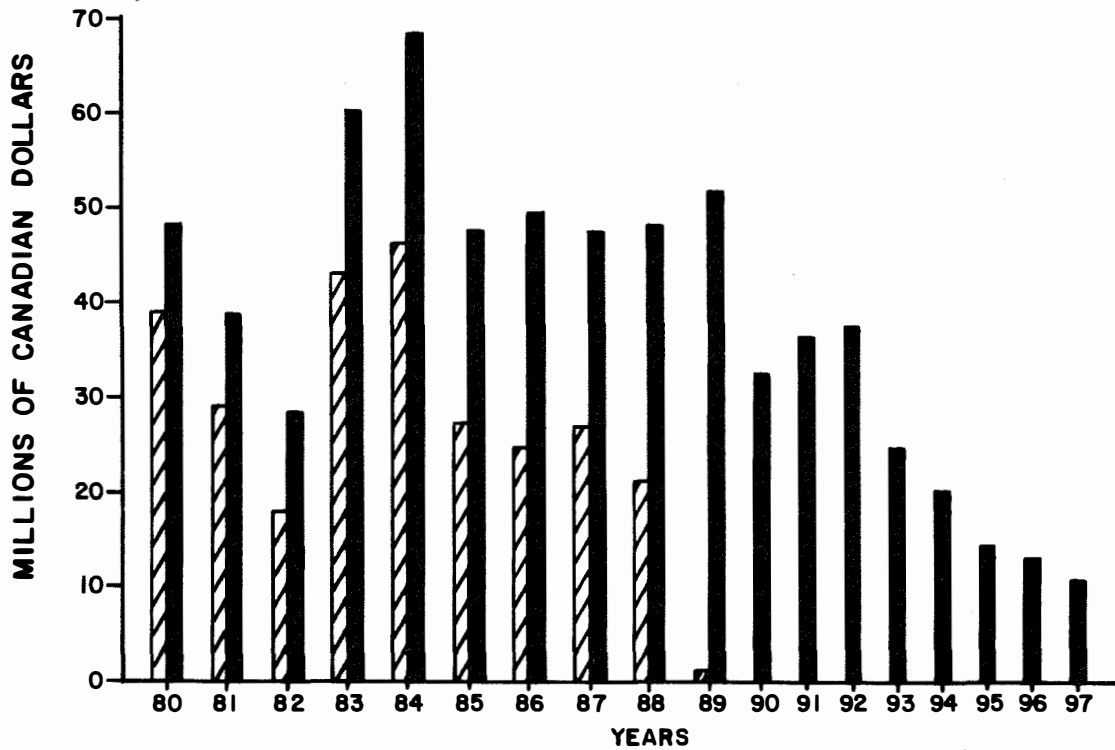
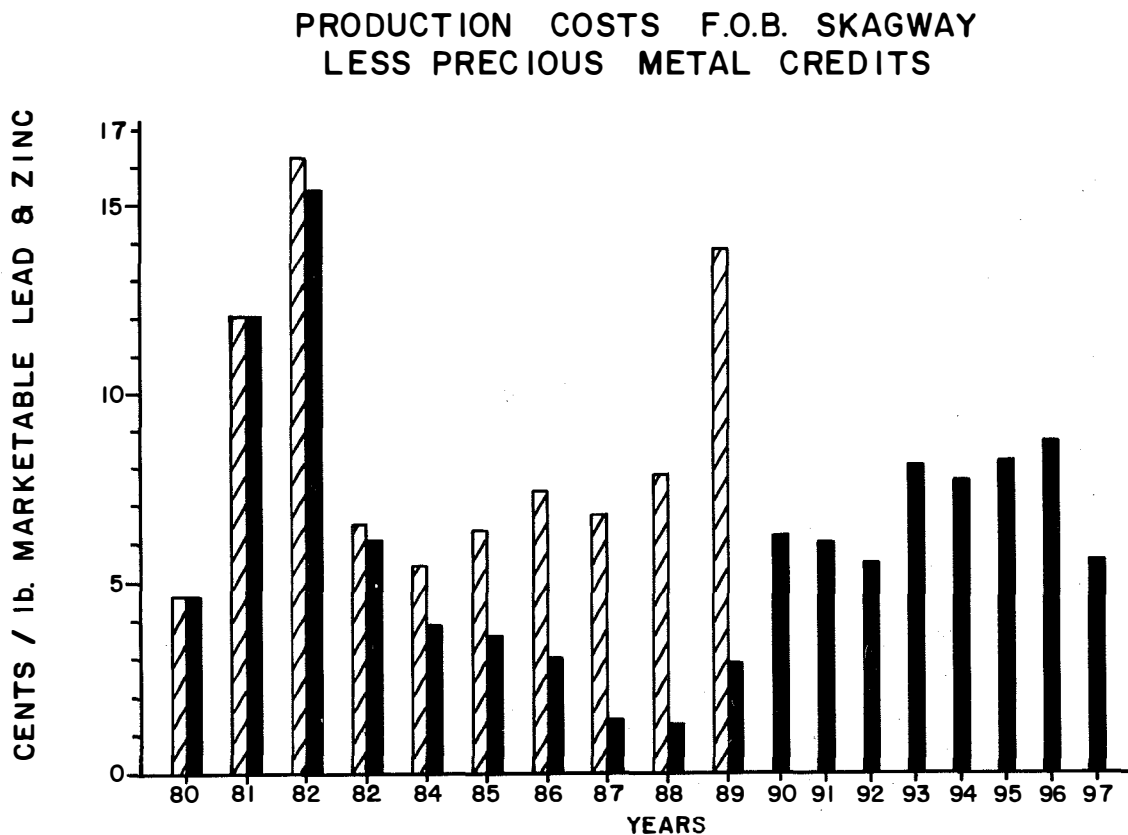
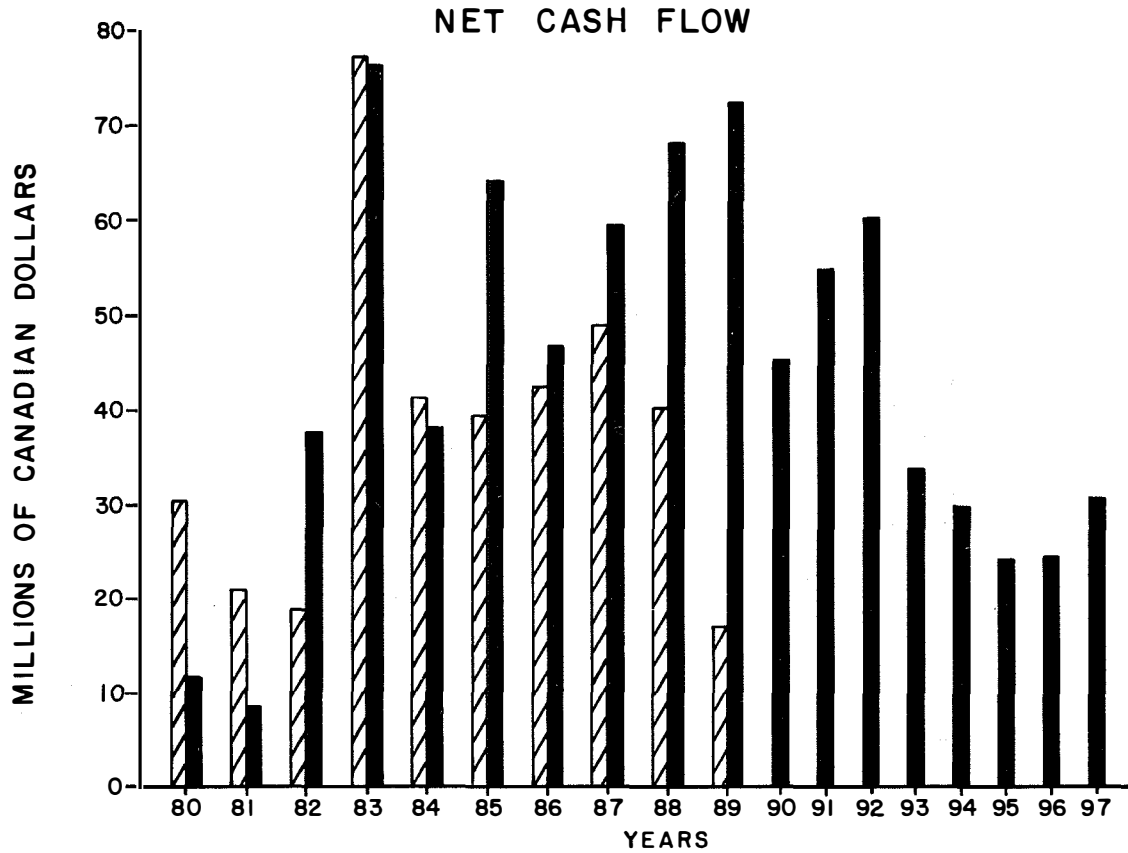
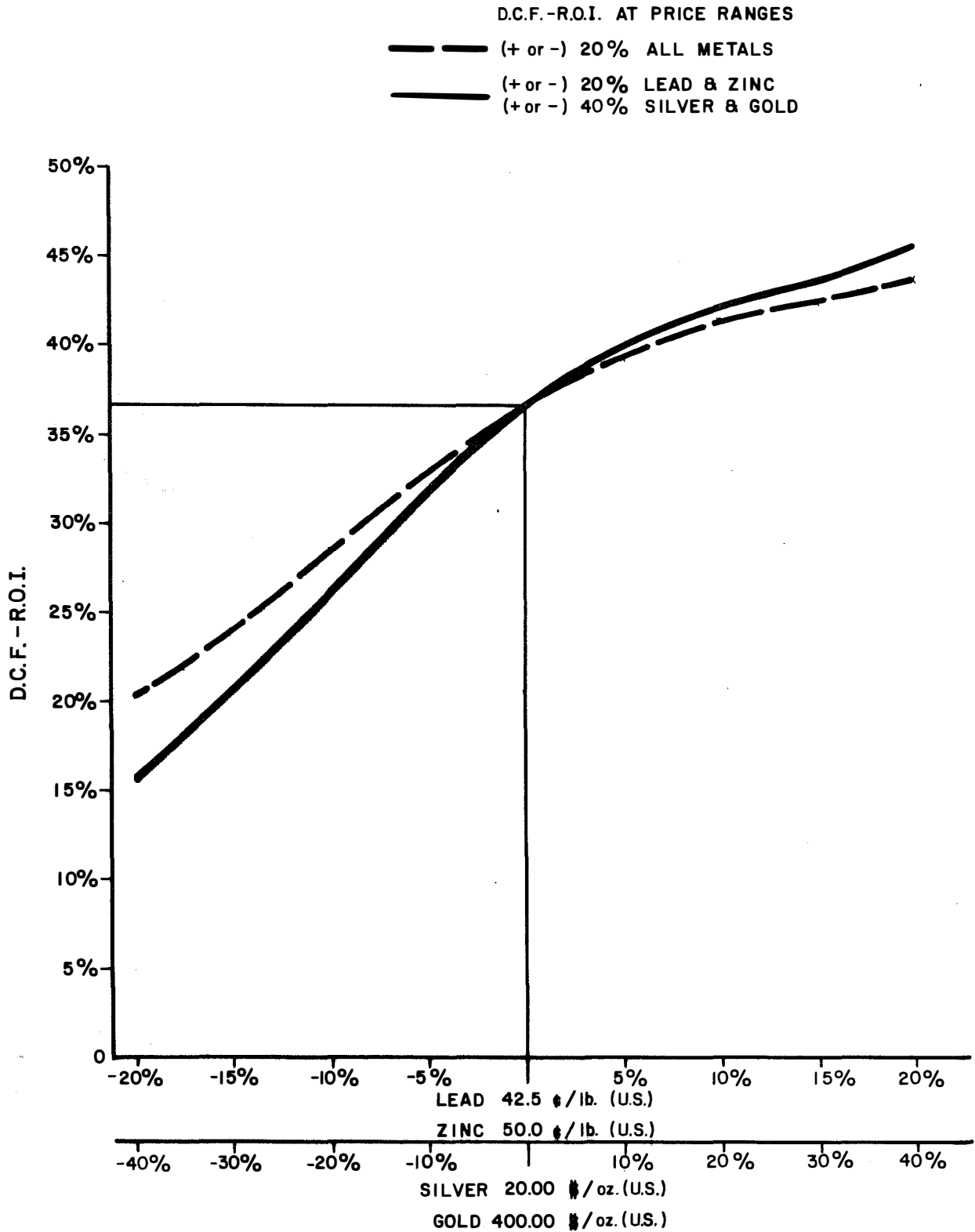


FIGURE I-4 VANGORDA PLATEAU DEVELOPMENT

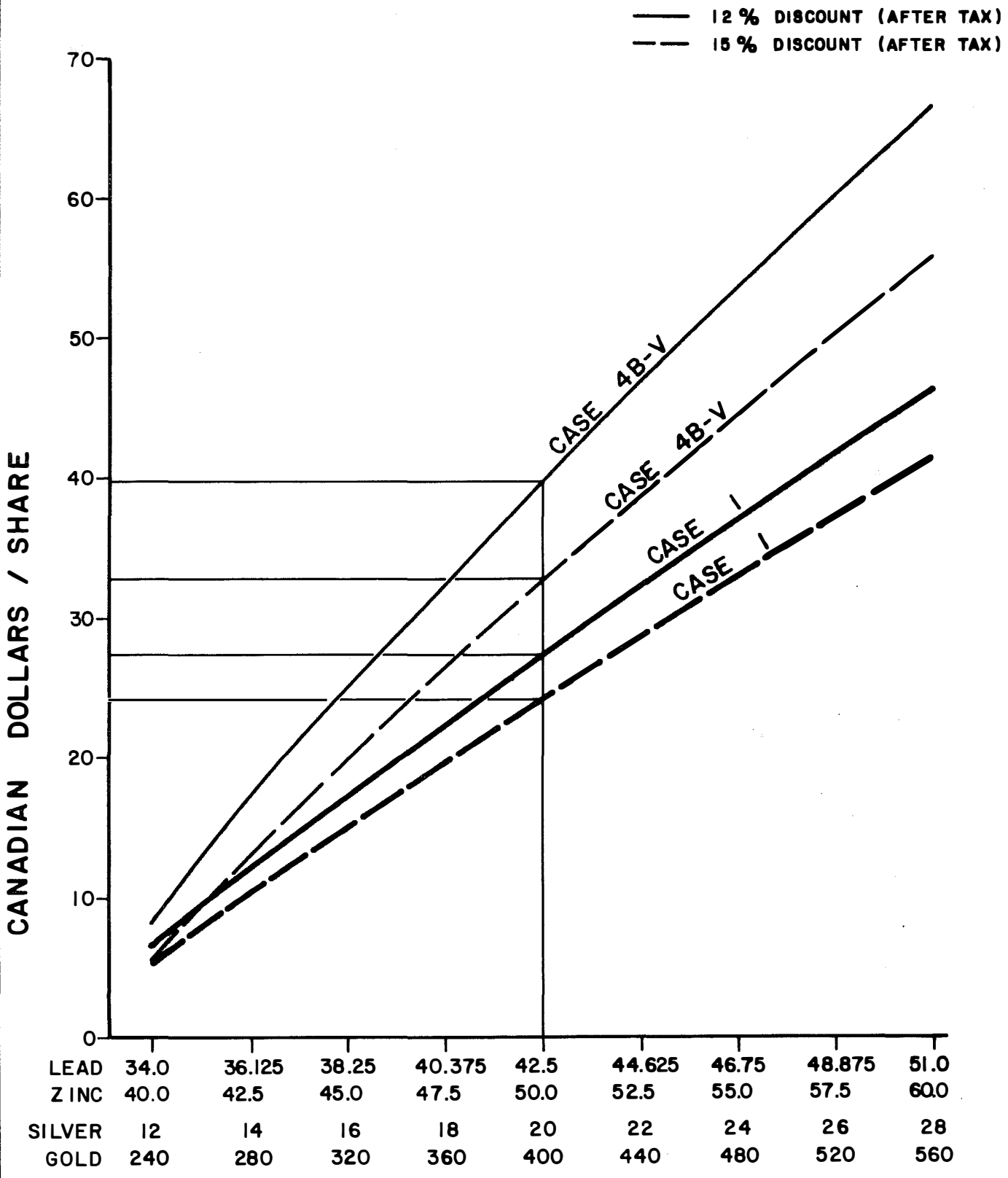
FARO ALONE 
 CASE 48-V 



**FIGURE 1-5 VANGORDA PLATEAU DEVELOPMENT
SENSITIVITY ANALYSIS**



**FIGURE I-6 VANGORDA PLATEAU DEVELOPMENT
NET PRESENT VALUE PER SHARE
OF FUTURE CASH FLOW**



NOTE: LEAD and ZINC in U.S. CENTS / POUND
 SILVER and GOLD in U.S. DOLLARS / TROY OUNCE

FIGURE 1-7
 VANGORDA PLATEAU DEVELOPMENT
 CAPITAL EXPENDITURES
 CDN. \$ MILLION

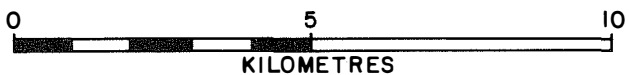
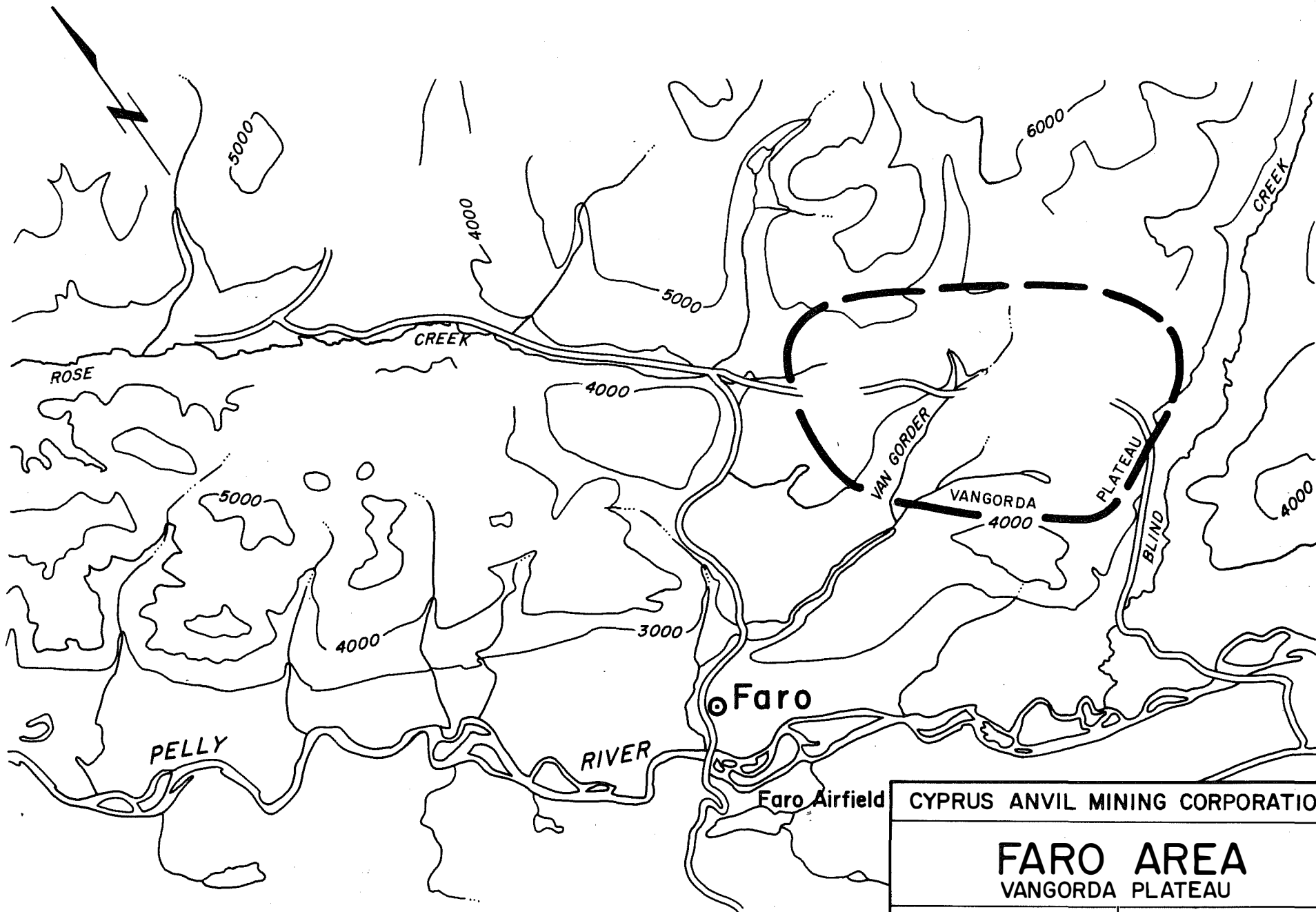
	1980	1981	1982	1983	1984	1985	1986	1987	1988	TOTAL
<u>CAPITAL EXPENDITURES</u> <u>JANUARY 1980 DOLLARS</u>										
Mill Modifications	18.970	14.411	-	-	-	-	-	-	-	33.381
Power Plant	4.610	6.390	-	-	1.000	-	-	-	-	12.000
Tailings Dam	4.420	7.580	-	-	-	-	-	-	-	12.000
Ore Haulage	-	-	-	17.150	17.150	-	-	-	-	34.300
Mine Equipment	-	-	-	-	10.585	5.120	-	-	-	15.705
Mine Facilities	-	-	-	-	6.515	-	-	-	-	6.515
Townsite	-	5.000	-	-	2.000	-	-	-	-	7.000
Pre-Production Stripping	-	-	-	-	4.000	2.520	7.111	12.050	7.500	33.181
Other	1.861	-	-	-	-	-	-	-	-	1.861
<u>TOTALS</u>										
Annual	29.861	33.381	-	17.150	41.250	7.641	7.111	12.050	7.500	155.943
Cumulative	29.861	63.242	63.242	80.392	121.642	129.283	136.394	148.444	155.944	
<u>ESCALATION FACTOR</u>										
Annual	7.5	15.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	
Cumulative		1.236	1.36	1.496	1.645	1.81	1.99	2.19	2.41	
<u>CAPITAL EXPENDITURES</u> <u>ESCALATED FOR INFLATION</u>										
Annual	32.100	41.267	-	25.656	67.856	13.830	14.151	26.390	18.075	
Cumulative	32.100	73.367	73.367	99.023	166.879	180.709	194.860	221.250	239.325	

2.
SUMMARY

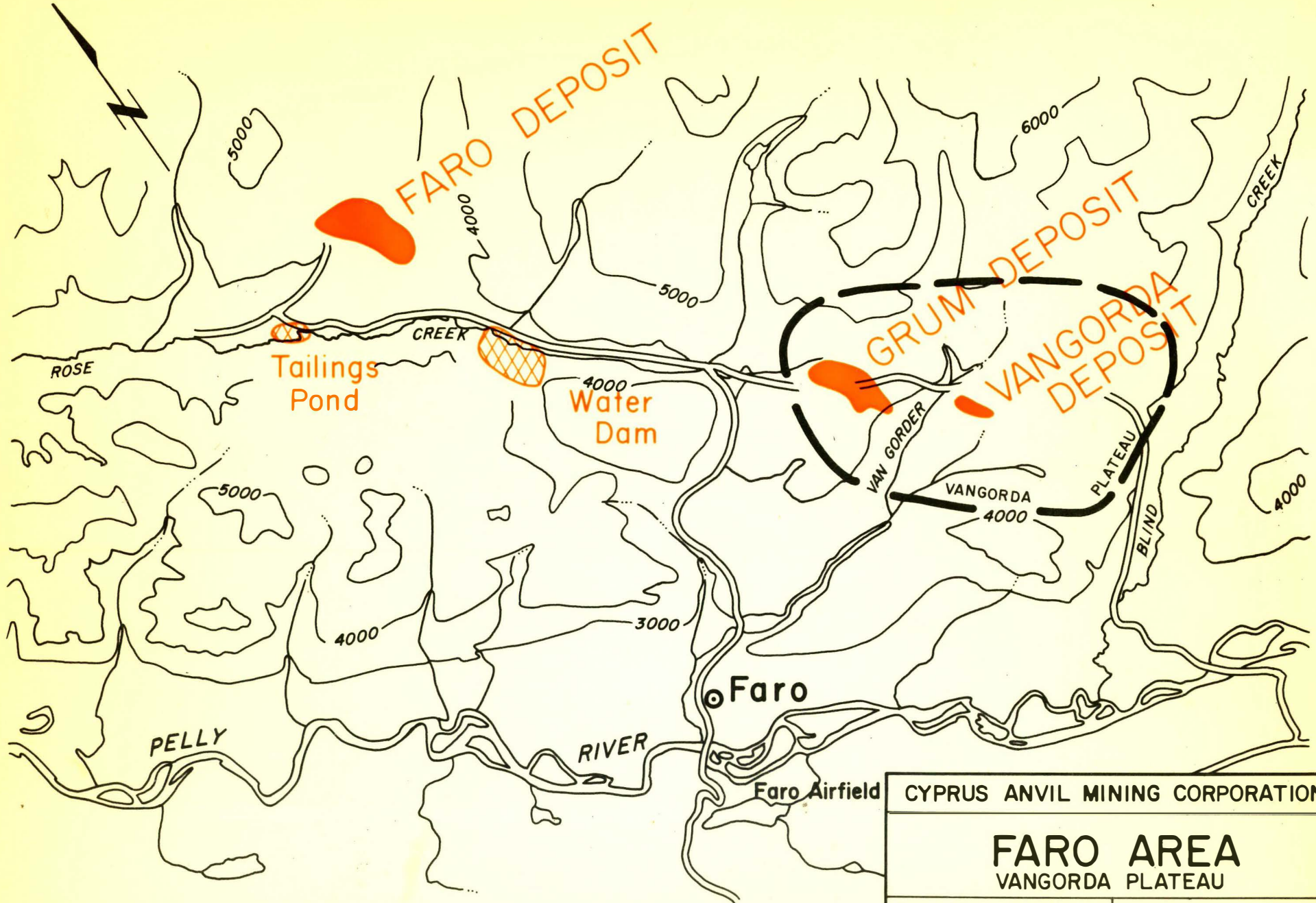
2.1 INTRODUCTION

An agreement was consummated on May 15th, 1979 between Cyprus Anvil Mining Corporation and Kerr Addison Mines Ltd. and Canadian Natural Resources Ltd., whereby Cyprus Anvil acquired all of the mineral property interests of the respective companies in the Anvil District which include those of the Kerr Addison subsidiary, Vangorda Mines Ltd. The principal properties involved cover approximately 31 square kilometers in the heart of the known mineralized section of the District and include the Grum and Vangorda deposits, (Figure 2-1) both of which contain significant amounts of ore mineable by conventional open pit methods.

Engineering studies have been conducted to establish the most financially attractive sequential development program by which ores may be mined from the Faro, Grum and Vangorda deposits to feed the modified mineral processing facilities. These investigations were conducted using the mineable reserves shown below, all of which are economically available by surface mining.



CYPRUS ANVIL MINING CORPORATION	
FARO AREA VANGORDA PLATEAU	
N.T.S. 105 K TAY RIVER SCALE: 1 : 125,000 DRAWN BY: C. L. C.	DATE: FEB. 28, 1980 FIGURE 2-1

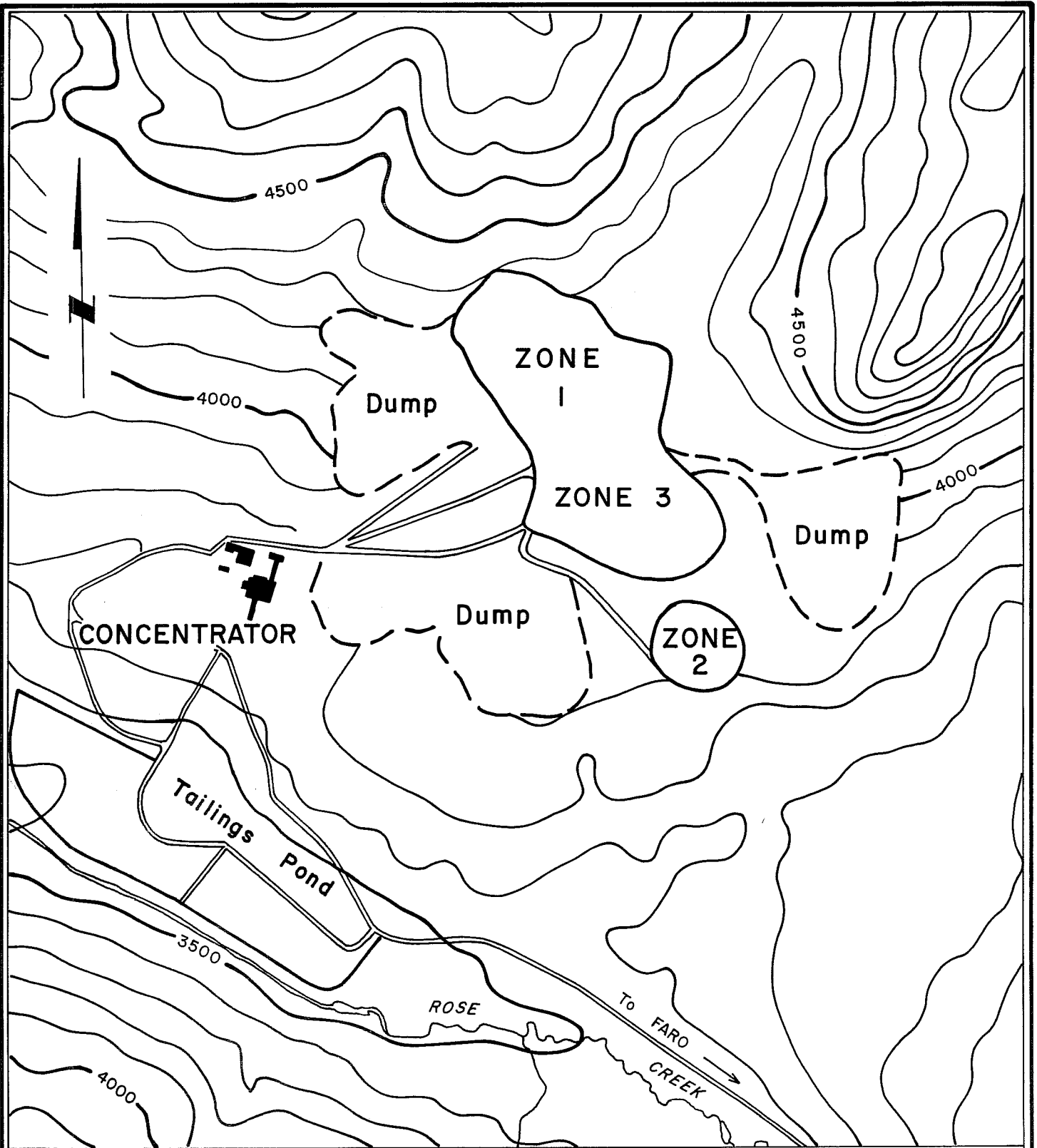


CYPRUS ANVIL MINING CORPORATION	
FARO AREA VANGORDA PLATEAU	
N.T.S. 105 K TAY RIVER SCALE: 1:125,000 DRAWN BY: C. L. C.	DATE: FEB. 28, 1980 FIGURE 2-1

FIGURE 2-2
FARO, GRUM & VANGORDA DEPOSITS
MINEABLE OPEN PIT ORE RESERVES
JANUARY 1st, 1980

DEPOSIT	MINEABLE RESERVES (tonnes)	LEAD Pb %	ORE GRADE	
			ZINC Zn %	SILVER Ag g/tonne
Faro - Zone I & III	26,385,000	2.9	4.6	34.8
- Zone II	3,724,000	2.7	4.3	42.5
Grum	15,583,000	3.1	5.0	47.0
Vangorda	6,134,000	3.5	4.6	50.2
Total	51,826,000	3.0	4.7	40.8

The above data is adjusted for waste dilution.



CYPRUS ANVIL MINING CORPORATION

FARO DEPOSIT

YUKON TERRITORY

FARO MINESITE

1000 0 1000 2000
 SCALE 1" = 2000'

NTS 105 K-6
 SURVEY BY:
 DRAWN BY: C. L. C.

DATE: MARCH 10, 1980
 FIG. 2 - 3

2.2 THE FARO DEPOSIT

The Faro deposit consists of three discrete zones (Figure 2-3). Zone I has been the source of ore since the commencement of operations in late 1969. Since this ore is virtually exhausted, the 1980 ore supply will be taken almost exclusively from the Zone II which exists as a small, physically detached deposit. Thereafter ore will be mined from Zone III until the presently defined mineable reserves are exhausted in 1989, based on the present mining schedule which does not provide for the Vangorda Plateau ores.

FIGURE 2-4
FARO DEPOSITS - ANNUAL PRODUCTION SCHEDULE

YEAR	1980	1981	1982	1983	1984	1985	1986	1987	1988	1989	TOTAL
Waste (000'm ³)	9342	10872	10022	8268	7560	2678	1828	1530	382	-	52,482
Ore (000's tonnes)	3317	3404	3404	3404	3404	3404	3404	3404	3404	912	31,461
Lead (% Pb)	2.8	3.0	2.6	3.4	3.5	2.8	2.8	2.8	2.7	2.0	2.9
Zinc (% Zn)	4.4	5.2	4.7	4.8	4.8	4.2	4.2	4.5	4.4	3.9	4.6
Silver (Ag g/tonne)	41.6	31.3	28.7	40.0	44.3	39.1	36.8	34.2	28.5	22.0	35.6
Gold (Au g/tonne)											N/A

N/A: Not available at this time.

Gold assays performed on representative samples of ore from Zone III indicated that gold distribution was erratic. For this purpose it was assumed that no payable gold would be produced when milling only Zone III ore.

In addition to these in-situ ore reserves, there are approximately 1.5 million tonnes of oxidized ore assaying 2.8% lead and 4.8% Zn

that are stockpiled of which 1.3 million tonnes will be milled in 1982.

The Zones I and III ore reserves quoted in Figure 2-2 are based upon a 4.0% combined lead plus zinc cut-off grade, while a 4.5% cut-off has been applied to Zone II to compensate to some degree for the generally inferior metallurgical response exhibited by this material. Ore grades and tonnages predicted using the computerized model have been adjusted to compensate for waste dilution. The "cut-off grade", for this purpose is defined as the sum of the average contained lead and zinc values below which ore will not be mined.

2.3 THE GRUM DEPOSIT.

The Grum discovery hole was drilled in the Fall of 1973. Thereafter exploration programs were conducted that included a total of 41,000 metres of surface diamond drilling, 15,000 metres of underground diamond drilling and 2,900 metres of underground development. The information obtained from these extensive programs was interpreted to develop an understanding of the complex structural geology of the Grum deposit.

The original drill hole log data was compiled and stored on magnetic tape by Noranda Mines Ltd. This information was transformed by Cyprus Anvil to a format compatible with the computerized geologic model programs currently in use and applied to calculate approximate geological reserves. The application of associated programs and basic operating principles established the phase development of the open pit, generating volumes of material to be moved and ore grades by year as shown in Figure 2-5.

FIGURE 2-5
GRUM DEPOSIT - ANNUAL PRODUCTION SCHEDULE

YEAR	1	2	3	4	5	6	7	8	9	10	TOTAL
Waste (000's m ³)	4010	4010	4010	4010	4010	4010	4010	4010	2001	0	34,081
Ore (000's tonnes)	1701	1701	1701	1701	1701	1701	1701	1701	1701	274	15,583
Lead (% Pb)	3.9	2.9	2.9	3.1	3.3	3.2	2.8	2.7	2.8	2.9	3.1
Zinc (% Zn)	6.4	4.9	4.8	5.0	5.4	5.0	4.5	4.4	4.5	4.7	5.0
Silver (Ag g/tonne)	58.5	45.3	44.8	46.5	50.4	48.5	42.6	42.1	44.1	46.3	47.0
Gold (Au g/tonne)											N/A

N/A: Not available at this time.

Since gold determinations were not performed initially on samples of the Grum core, gold values were not integrated into the preliminary computer model. Pilot plant and laboratory flotation test results indicated probable gold contents of 3.5 grams per tonne in the lead concentrate.

This schedule was based on a 4.0% cut-off grade and assumes an average mine ore production rate of 4,660 tonnes per calendar day. The ore grades and tonnages shown were adjusted to compensate for waste dilution.

2.4 THE VANGORDA DEPOSIT

Mineralized showings in the Anvil District were first located in a small outcrop on Vangorda Creek which were subsequently proven to be the surface manifestation of the Vangorda deposit.

Extensive drilling carried out by Prospectors Airways, a subsidiary of Kerr Addison Mines Ltd. in the mid 1950's, clearly established a significant mineralized tonnage but failed to produce precise information relating to ore reserves and grades due to difficulties encountered in achieving satisfactory core recoveries. Accordingly in 1979, an extensive diamond drilling program was implemented to better define the tonnage, grade and morphology of the deposit between section lines 2 West and 12 East.

Using only data generated by the 1979 diamond drill program, total approximate geological reserves were calculated for this portion of the deposit using the same basic techniques that were applied in the calculations of the Grum reserves. Mine development and production plans were then produced to yield the values shown below (Figure 2-6).

FIGURE 2-6
VANGORDA DEPOSIT - ANNUAL PRODUCTION SCHEDULE

YEAR	1	2	3	4	TOTAL
Waste (000's m ³)	2920	2920	659	-	6,499
Ore (000's tonnes)	1701	1701	1701	1031	6,134
Lead (% Pb)	3.5	3.6	3.6	3.2	3.5
Zinc (% Zn)	4.9	4.8	4.7	3.6	4.6
Silver (Ag g/tonne)	47.3	52.6	53.0	46.6	50.2
Gold (Au g/tonne)					N/A

N/A: Not available at this time.

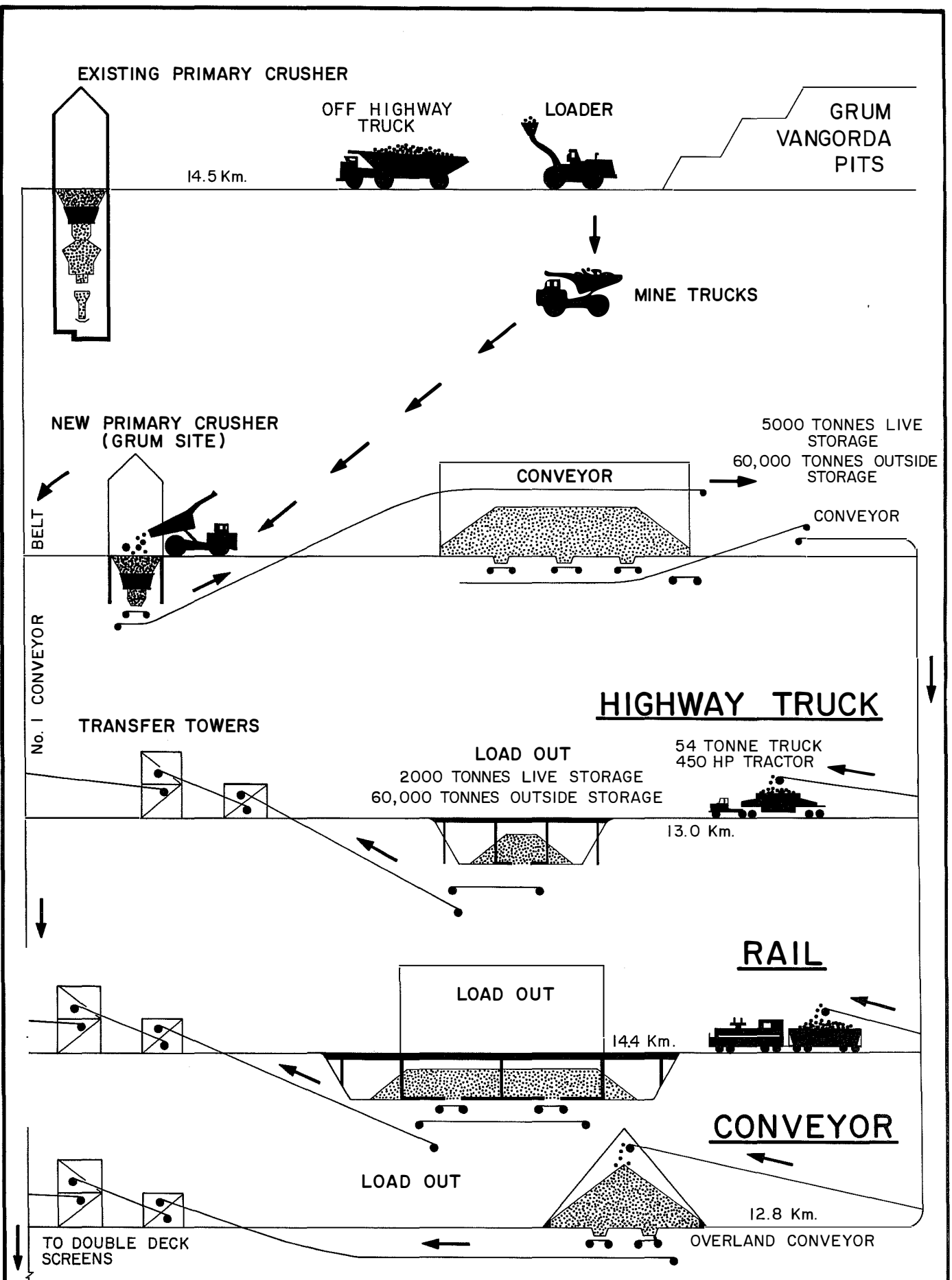
While gold determinations were carried out on the majority of sulphide core samples, the gold distribution data is incomplete at the time of writing this report. Gold contents of lead concentrate were predicted to be 6.5 grams/tonne based upon the results of laboratory testwork.

The schedule was based upon a 4.0% cut-off grade and an average mine ore production rate of 4,660 tonnes per calendar day. Appropriate factors were applied to compensate for dilution.

2.5 HAULAGE SYSTEMS

A number of systems were considered to haul ore from the Vangorda Plateau to the concentrator, including the use of off-highway trucks, highway trucks, conveyor systems and railroad. The rail, conveyor and highway truck alternatives included crushing and ore stockpiling facilities at the Vangorda Plateau. The off-highway system assumed that the haulage units would be loaded at the mine face and subsequently travel directly to the existing primary crusher at the mill site as shown in Figure 2-7.

Based upon these preliminary studies, approximate capital and operating costs were developed for each haulage system. The direct operating costs shown in Figure 2-8, do not include amortization or interest on capital but are based upon the total anticipated operating costs expressed in 1980 dollars divided by the total tonnage of ore to be transported.



ORE HAULAGE ALTERNATIVES

FIGURE 2-8
RELATIVE COSTS OF THE HAULAGE SYSTEMS

SYSTEM	*INITIAL CAPITAL COST \$ million	*AVERAGE OPERATING COST \$/tonne	NUMBER OF EMPLOYEES REQUIRED
Off-Highway Trucks	32.5	1.37	37
Highway Trucks	42.4	2.12	68
Rail	38.6	1.39	33
Conventional Conveyor	44.1	1.34	30
Cable Belt Conveyor	38.1	1.65	30

* includes \$100,000 per employee capital housing provision and \$5,575/employee for housing maintenance per year.

Operating and Capital Costs cover transportation of ore from the pit face to the existing crushing plant.

The conventional conveyor belt alternative was rejected since the overall system design was not conducive to efficient operation in cold weather. The best highway trucking alternative utilized 450 HP tractor/bottom dump-trailer units capable of hauling a 54 tonne payload. This labour intensive approach was rejected due to the high operating costs.

Extensive detailed engineering studies are now in progress to thoroughly evaluate the rail, conveyor and off-highway trucking alternatives. In view of the above, and for reasons given later, operating and capital costs have been applied that will provide sufficient funds for any one of the rail, conveyor or the off-highway transportation alternatives. The final selection of the transportation system to be used will be made later this year based upon the results of these studies now in progress.

2.6 CONCENTRATOR MODIFICATIONS

2.61 METALLURGY

a) Grum Ore:

Extensive metallurgical testwork was conducted on samples of Grum ores over recent years, under the direction of the Noranda Milling Committee. Results from laboratory and pilot plant testwork clearly demonstrated that optimum metallurgical performance could only be achieved by fine grinding this material to maximize the liberation of the finely disseminated minerals. These findings were confirmed by the results of detailed microscopic analyses of the various ore types within the Grum deposit.

Although the Grum metallurgical forecast used in this report depends heavily on the results from these programs, the metallurgical data inferred by Noranda were adjusted downward in this analysis to reflect the effect of mill feed grades lower than those experienced during the pilot plant work. Thus the results shown below are based on the average diluted feed grade for the Grum deposit.

FIGURE 2-9
 PREDICTED PLANT METALLURGICAL PERFORMANCE - GRUM ORE

CONCENTRATE	LEAD Pb %	ZINC Zn %	ASSAYS				MERCURY Hg g/tonne	DISTRIBUTION		
			GOLD Au g/tonne	SILVER Ag g/tonne	ARSENIC As %	LEAD Pb %		ZINC Zn %	GOLD Au %	SILVER Ag %
Lead	60	11	3.5	750	0.10	90	80	*	33	65
Zinc	2.5	55	*	*	0.05	650	*	83	*	*

b) Vangorda Ore:

The earlier lack of reproducibility in metallurgical test results generated by a number of competent authorities since the discovery of the Vangorda deposit, reflects the difficulties that were experienced in acquiring adequate quantities of representative ore samples.

The 1979 Vangorda diamond drill program was based upon a closely spaced drill pattern using larger diameter drill bits to generate sufficient quantities of representative ore samples for metallurgical testwork. A program was implemented in 1979 to develop metallurgical response profiles for each of the known principal ore species within the Vangorda deposit. The forecast plant metallurgical performance was based upon the results of this testwork and weighted to compensate for the relative occurrence of these ore types within the Vangorda orebody. The metallurgical parameters shown below are predicated upon the average feed grade for the deposit.

FIGURE 2-10
 PREDICTED PLANT METALLURGICAL PERFORMANCE - VANGORDA ORE

CONCENTRATE	ASSAYS						DISTRIBUTION			
	LEAD Pb %	ZINC Zn %	GOLD Au g/tonne	SILVER Ag g/tonne	ARSENIC As %	MERCURY Hg g/tonne	LEAD Pb %	ZINC Zn %	GOLD Au %	SILVER Ag %
Lead	50	*	6.5	575	0.25	60	80	*	35	55
Zinc	*	52.8	*	*	0.10	300	*	77	*	*

During the course of this comprehensive metallurgical investigation, it became evident that the best metallurgical performance could only be achieved by finely grinding the ores prior to the flotation process.

c) Faro Ore:

Testwork has been conducted to evaluate the effects of finer grinding Faro ores. The acquisition of the Vangorda Plateau deposits stimulated the implementation of comprehensive test programs to study the metallurgical responses of various species of Faro ore types at pre-determined levels of grind. Technical investigations were conducted by Cyprus Anvil, Kamloops Research & Assay Laboratory, Sachtleben Bergbau and the Mitsui Mining & Smelting Company Limited. Results from each of these independently conducted studies confirmed that the improved mineral liberation achieved through finer grinding significantly enhanced metallurgical performance.

The Figure 2-11 indicates the optimum grind levels as determined from laboratory scale flotation tests. The unit "P₈₀" represents the size (microns) of a hypothetical screen mesh through which 80% of the material would pass.

FIGURE 2-11

PRIMARY GRIND LEVEL FOR OPTIMUM METALLURGY - FARO ORE

DATA SOURCE	TYPE OF TESTS	APPROXIMATE NO. OF TESTS	OPTIMUM GRIND P ₈₀
Cyprus Anvil Test Laboratory	Rougher & Cleaner Tests	100	40-45
Kamloops Research Laboratory	Rougher & Cleaner Tests	120	45-50
Sachtleben	Cleaning Testing	30	52
Mitsui Mining & Smelting	Rougher & Cleaner Tests	50	37-70

Pilot plant testwork conducted in 1979 on two samples of Faro ores, were carried out at selected levels of grind to generate results that could be used to determine the economic optimum metallurgical flow-sheets. In this case it was determined that the flowsheet which produced the best metallurgical performance also generated the most favourable return on investment.

The results of the pilot plant testwork obtained when

treating the sample considered most typical of Zone III ores, were adjusted to compensate for atypical levels of sample oxidation. This data was then used as a basis to predict plant metallurgical performance.

FIGURE 2-12
 PREDICTED PLANT METALLURGICAL PERFORMANCE - FARO ORE

ORE SOURCE	CONC.	ASSAYS						DISTRIBUTION			
		LEAD Pb %	ZINC Zn %	GOLD Au g/tonne	SILVER Ag g/tonne	ARSENIC As g/tonne	MERCURY Hg %	LEAD Pb %	ZINC Zn %	GOLD Au %	SILVER Ag %
Faro Zone III	Lead	67	*	0.6	600	0.03	40	87.5	*	33	65
	Zinc	*	53.5	*	*	0.01	300	*	88.5	*	*

The present concentrator design is predicated upon the production of three concentrates; namely selective lead, selective zinc and a bulk concentrate. The modified plant flowsheet makes no such provision for the production of bulk concentrate, initially intended to provide an economic outlet for those flotation middlings that were incapable of producing acceptable selective concentrate grades without finer grinding. It is clear from results of recent work that the higher degree of mineral liberation achieved through finer grinding obviates the need to produce bulk concentrate, which is a less profitable product.

d) Ore Type Compatibility:

Testwork has been carried out by Lakefield Research to investigate the metallurgical compatibility of the subject ores. It has been determined that the flowsheet selected provides the optimum flotation environment for all the ores under investigation. Further it is noted that while each ore type within its respective deposit exhibits differing metallurgical response, concurrent milling of two discrete ore species produces no adverse effect on either of the two constituent metallurgical results.

2.62 MODIFIED CONCENTRATOR DESIGN

The forecast metallurgical performance of each ore will only be achieved by grinding finer and providing a controlled flotation environment which depends upon longer flotation times and lower pulp densities than those currently in use.

The finer grind will be achieved by incorporating an additional grinding circuit into the modified mill design. The required flotation residence times and pulp densities will be attained within the confines of the existing flotation section by replacing existing flotation machines with larger and more

efficient units. The elimination of bulk concentrate production will permit the re-allocation of thickener capacities to accommodate the finer concentrates produced. Existing disc filters will be replaced with larger units to provide the additional filtering capacity required to effectively dewater the finer concentrates. The filter performance will be further enhanced by the application of heat to the filter feed pulps.

The Anvil district ores are metallurgically complex, consisting of multiple finely disseminated minerals contained in generally massive sulphide matrices. It is known that each deposit consists of several readily identifiable ore types that exhibit differing metallurgical characteristics. To maximize plant metallurgical efficiencies certain sophisticated, well-proven instrumentation systems will be installed that will monitor, and in some cases control critical operating parameters. Though basic initially, this instrumentation will be capable of organized development in accordance with long term process control strategies.

Figure 2-13 schematically represents the modified plant flow-sheet and Figure 2-14 provides an appreciation of the new physical layout of the Anvil concentrator.

The capital cost of the modifications to the concentrator will be \$33.4 million. The operating costs were increased to reflect the higher consumptions of power, grinding liners and media.

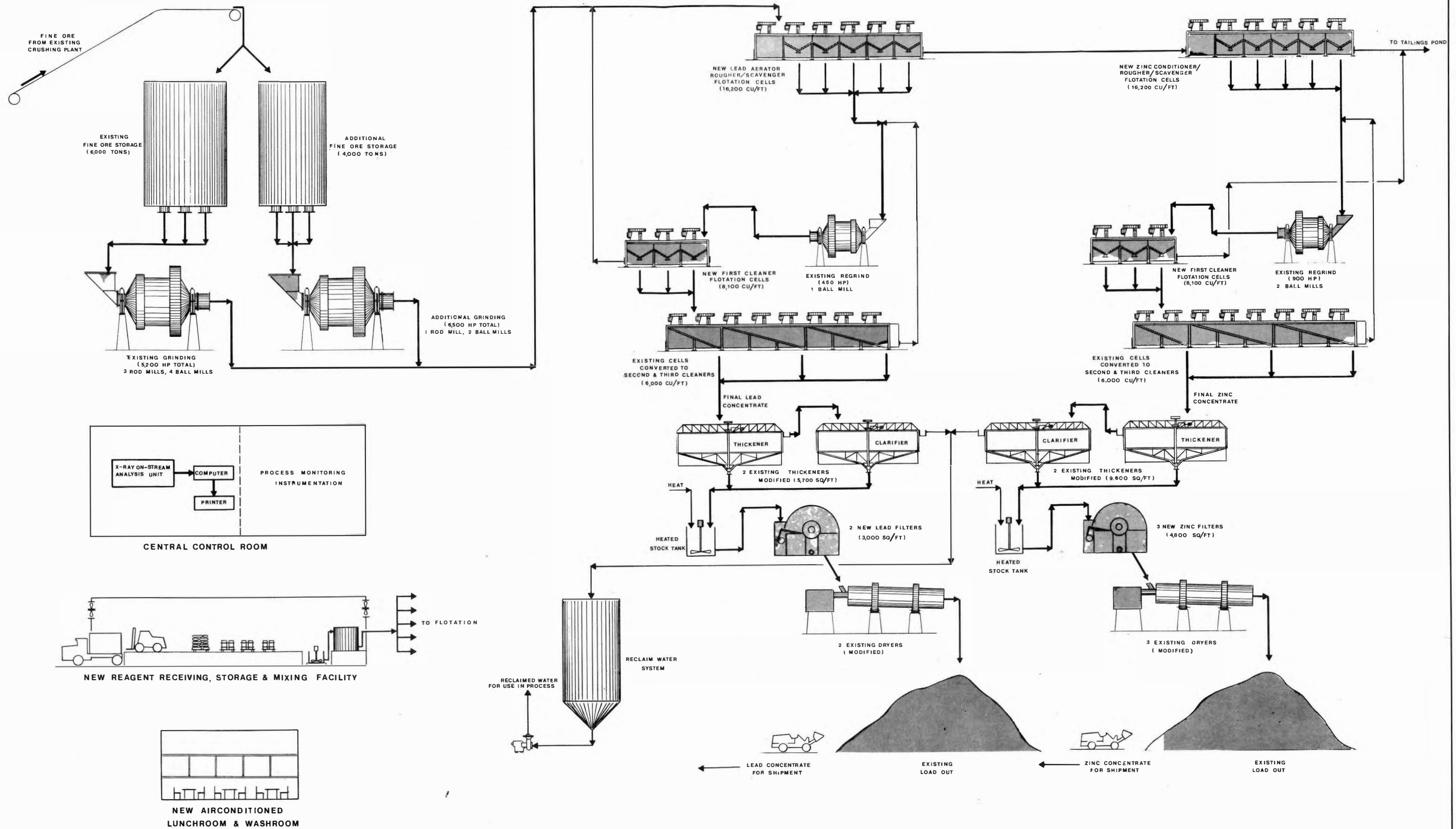


FIG 2-13

TITLE
MODIFIED MILL
SCHEMATIC FLOWSHEET

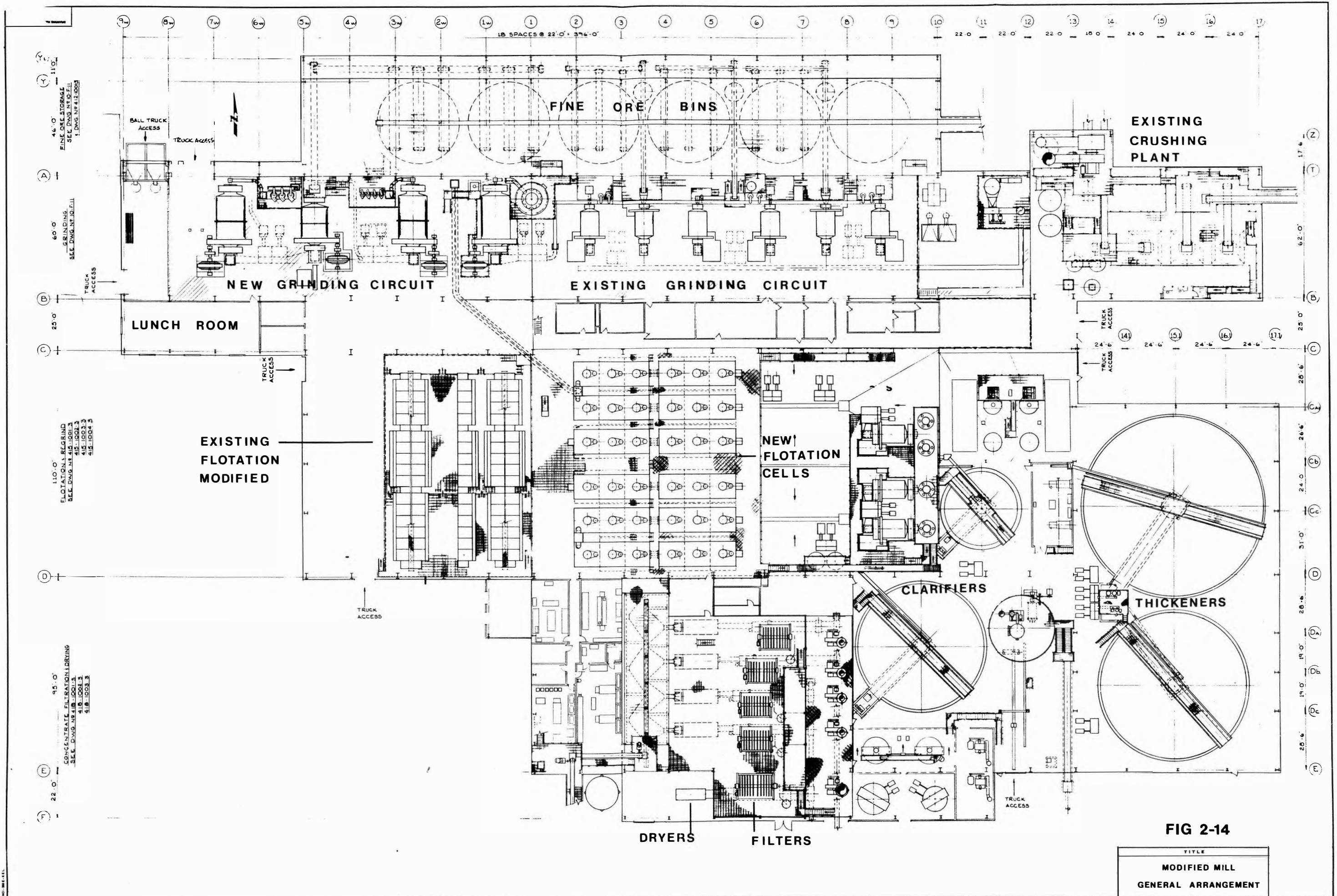


FIG 2-14

TITLE
**MODIFIED MILL
 GENERAL ARRANGEMENT**

2.7 POWER SUPPLY

The Northern Canada Power Commission (N.C.P.C.) presently supplies hydroelectric and diesel generated power to service the minesite and the town of Faro by means of its operating facilities at Whitehorse and Aishihik. The power is transmitted to Faro via a 138 kV overhead line.

The current minesite electrical load, has a maximum demand of 16 megawatts (MW) and an annual energy consumption of approximately 100 million kilowatt hours (100 KW hrs).

The development of the Vangorda deposits and attendant mill modifications will impose an additional maximum 9 MW load on the system, most of which is scheduled to be on line by January 1st, 1982.

FIGURE 2-15

MINESITE POWER STATISTICS

	TOTAL CONNECTED HP	MAXIMUM DEMAND (MW)	ENERGY CONSUMPTION (GW hr/year)
Proposed	46,470	25	155
Present	30,006	16	100
Increase	16,464	9	55

While N.C.P.C. will provide some of this additional energy, it will

be necessary to install supplementary electric generating facilities interconnected with the utility grid to ensure the maintenance of adequate system reserve capacity. Failure to provide such a plant would increase the risk of power shortages to Cyprus Anvil thereby jeopardizing the continuity of production at planned levels.

For this purpose, it was assumed that one generating unit would be located in close proximity to the concentrator to provide normal system reserve and long term emergency power supply. It was further assumed that two generating units would be installed adjacent to the existing N.C.P.C. power plant in Faro. The total cost of these facilities, the transmission line and transformers will be \$12.0 million.

The N.C.P.C. propose to install an additional hydroelectric turbine in the Whitehorse plant to be on line by mid 1983. Further the Commission has initiated studies to evaluate potential sites for small hydroelectric developments in the Yukon, some of which are within a 150 kilometre radius of Faro. As these studies proceed and system load forecasts are refined, the required power generating capabilities will be constantly reviewed to examine the possibility of reducing the size of the proposed plant at Faro and the premium to be paid for diesel electric energy.

2.8 ENVIRONMENTAL CONSIDERATIONS

New tailings impoundment facilities will be required to accommodate the increased total tonnages of finer tailings, and to provide additional time for water clarification. Dykes, creek diversion canals and related structures will be designed to ensure compliance with all regulatory requirements. Capital cost of the new facilities will be \$12.0 million.

The modified mill flowsheet depends upon the internal recirculation of certain process waters to maintain fresh water consumption at current levels while operating the flotation circuit at lower pulp densities. The use of this recycled water represents one of the first steps in a long term strategy designed to minimize the use of fresh water.

Base line studies have commenced to monitor the indigenous flora, fauna, fish populations and water qualities in those areas most likely to be affected by future mine developments. Programs will be established to reduce to an absolute minimum any detrimental impact future mining activities may impart to the natural environment.

Building design, mechanical layouts and equipment selections were conducted with a view to improving the working environment within

the modified mill by reducing spillage and minimizing air and noise pollution. By so doing, the Company has the opportunity to demonstrate its sincere interest in the health and welfare of its employees which will be reflected in improved morale.

2.9 OUTLOOK FOR LEAD AND ZINC

2.91 LEAD

After four consecutive years of declining statistical balances for lead metal, recent statistics indicate the world lead market will move into a small surplus position in 1980. The primary explanation for this lies in the major decline to date of the North American automobile market which affects the demand for storage batteries, the most important end-use of lead metal. Prices in 1979 were dramatically improved but mine production increased only slightly since long lead times are required before production can actually respond to improved market conditions.

In 1980 the first major lead mine in ten years has come on stream - the Aggeneys Mine in South Africa producing about 90,000 tonnes of lead in concentrate annually. The ability of the lead smelting industry in Europe to cover its concentrate needs over the next six months has been somewhat relieved by the arrival of these concentrates some four or five months ahead of the original schedule. Production and milling problems continue to restrict mine output at Aznacollar (Spain) and Woodlawn (Australia). However, a concern over long term lead supply arises from the fact that less than one third of all

lead is mined from lead ores while projected developments indicate a continued preponderance of zinc in combined orebodies.

Secondary recovery is more important in lead than for any other metal, contributing about 38% of feed to refineries. However, secondary smelters in industrialized nations face strict environmental regulations which raise the break-even prices needed to sustain production; moreover, the supply of scrap lead is quite unpredictable. The current scrap shortage in Europe illustrates how quickly inventories in one region can be depleted by high prices, how quickly scrap metal can flow to the shortage area, (in this case from the U.S.), and how at the same time weakening battery demand can create conditions for further market imbalance.

Forecasts of lead consumption vary but even a conservative growth trend rate of 2.0% from 1979 levels with adjustments for the slowdown in 1980 maintain the supply/demand balance in a reasonably balanced state. Major mine additions as occur in 1980 and 1983 are quickly absorbed. The long run supply curve for lead can be expected to parallel the costs of bringing new production on stream given:

- a) Declining grades in existing orebodies.

- b) The decreasing ratio of lead to zinc in anticipated combined orebodies, which are likely to be developed in the future.

- c) The costs of complying with strict environmental regulations affecting both primary and secondary producers of metal.

2.92 ZINC

In the last two years some major adjustments have occurred in the zinc industry which, barring a severe and prolonged recession in 1980, should provide the foundations for a more profitable future for producers of both concentrates and metal.

1978: Mine production declined by 2.0% from the historical high of 1977; metal production remained virtually constant. Since consumption rose dramatically by about 7.7% from the previous year, an extremely large adjustment to metal inventories took place, close to a 400,000 tonnes decline.

1979: Mine production declined slightly while metal production jumped by 10.3%. Consumption of metal still

managed a 2.4% increase over 1978. Accordingly, there occurred a substantial drawdown on zinc metal in concentrate inventories of about 330,000 tonnes.

Not surprisingly, a zinc concentrate shortage has emerged early in 1980. Production of both metal and concentrates so far this year is lower than many industry observers had originally estimated. Demand for metal should remain sluggish as the United States moves into recession.

The full impact of the concentrate shortage will begin to be widely felt in 1981 as the western economies begin to recover and the demand for zinc assumes a 2.0% growth trend. As smelters try to increase capacity utilization by increasing production they will be severely constrained by the shortage of zinc concentrates. The price of zinc will have to rise in response to these forces and such movement will be encouraged by the cost of energy and currency exchange pressures experienced by existing smelters in Japan and Europe.

Rising concentrate and metal prices, security of concentrate supplies and relatively lower energy costs will benefit integrated Canadian zinc producers over the next five years.

2.10 FINANCIAL ANALYSIS

The financial analyses are based on a comparison of cash flows generated by processing the reserves outlined in the current operating plan with those realized by milling the Vangorda Plateau ores concurrently with those from the Faro pit. These cash flows exclude dividends, exploration expenditures and interest other than 1980 commitments and continuing interest on housing mortgages. The cash flows do provide for those capital costs required for the existing mining programs and the cost of routine equipment replacements.

A number of development cases were examined, varying the time and sequence of pit operations (Section 5). The most attractive case, identified as 4B-V requires that the mill modifications be completed by 1982. Vangorda ore would be supplied to the mill from 1985 to late 1988 with ore from the Faro pit in equal proportions. When exhausted the Vangorda ore, would be replaced by material from the Grum in 1988.

The basic assumptions used in the construction of these cases are:

- a) Open pit reserves of the Vangorda Plateau deposits are as shown in Figure 2-2.

- b) The capital expenditures shown in Figure 2-18 are based on January 1980 dollars.
- c) Ores from all sources are compatible for milling in any given ratio without adverse effects on the metallurgical performance.
- d) Mining costs are based on experience with the Faro operation. Contract pre-production stripping costs for the Vangorda deposit are based on the results of an independent study. Pre-production stripping unit costs for the Grum deposit are based upon experience.
- e) Milling costs will increase by about ten percent due principally to increased steel consumption. Power costs have been increased to reflect the high price of diesel generated power.
- f) Transportation to tidewater and terminal costs are at present levels.
- g) Ocean freight costs will be as follows:

FIGURE 2-16

OCEAN FREIGHT RATES U.S. \$/tonne

	1980	1981	1982 AND ONWARD
To Japan	20.50	22.00	22.00
To Europe	39.50	40.00	40.00

h) All concentrate will be sold at treatment charges at current levels under Japanese and European concentrate sales contracts.

i) The price and exchange assumptions shown below are expressed in 1980 dollars.

FIGURE 2-17

METAL PRICE AND EXCHANGE RATE ASSUMPTIONS

	1980	1981	1982 AND ONWARD
Zinc U.S. ¢/lb	39.23	44.0	50.0
Lead U.S. ¢/lb	43.0	42.5	42.5
Silver U.S. \$/oz	24.00	20.00	20.00
Gold U.S. \$/oz	456.00	400.00	400.00
U.S. 1\$ = CDN. \$	1.124	1.050	1.025

j) No residual values for either plant or equipment have been included in these calculations.

- k) In the opinion of the company's tax counsel, each of the Grum and Vangorda deposits will constitute a "new mine" and all expenditures being considered, with the possible exception of the tailings dam, will be subject to the fast write-off provisions for new mines (100%).

With the exception of railway track and related property, and possibly the tailings dam, all expenditures will also qualify for earned depletion (33.3%). The company is seeking an advance tax ruling from the Department of National Revenue confirming the opinion of counsel.

As in any analysis of this nature the most subjective area and also the area of greatest impact is that of metal prices. Sensitivities have been calculated and the results tabulated in section 10 of this report and illustrated graphically in the Program section. These indicate that should equilibrium prices be 20% lower for lead and zinc and 40% lower for silver and gold than those expected, the DCF/ROI is 15.5% as opposed to 36.6% DCF/ROI in the base price comparison. If prices are 20% and 40% respectively, higher than those expected the DCF/ROI is 45.6%.

Other sensitivities were run using equilibrium prices as follows:

Feed grades + 10% - DCF/ROI 40.4%

- 10% - DCF/ROI 31.0%

Operating costs + 10% - 32.7%

Capital costs + 10% - 33.2%

FINANCIAL COMPARISONS

(Values Reported as \$MM)

	<u>CASE 1</u>	<u>CASE 4B-V</u>	<u>DIFFERENCE</u>
DCF/ROI	-	36.6	-
N.P.V. at 12 percent	209.4	305.1	95.7
at 15 percent	184.6	252.0	67.4
Value per Share			
12 percent	27.28	39.75	12.47
15 percent	24.05	32.83	8.78

The 10 year cash flow included in section 10 indicates that assuming dividends and exploration are continued at current levels, the only year in which annual cash generation is less than expenditure is 1981. This deficiency is covered by cash on hand at the end of 1980. Under the same assumption, should metal prices for lead and zinc be 10% lower than expected and silver and gold 20% lower than expected, maximum year end debt (1981) would be in the order of \$35,000,000, well within the company's borrowing potential.

FIGURE 2-18

CAPITAL EXPENDITURES

VANGORDA PLATEAU DEVELOPMENT: CASE 48-V

(IN CONSTANT JANUARY 1980 \$000's)

	1980	1981	1982	1983	1984	1985	1986	1987	1988	1989	1990	1991	1992	1993	1994	1995	TOTAL
<u>VANGORDA PLATEAU DEVELOPMENT</u>																	
Mill Modifications	18.970	14.411	-	-	-	-	-	-	-	-	-	-	-	-	-	-	33.381
Power Plant	4.610	6.390	-	-	1.000	-	-	-	-	-	-	-	-	-	-	-	12.000
Tailings Dam	4.420	7.580	-	-	-	-	-	-	-	-	-	-	-	-	-	-	12.000
Ore Haulage	-	-	-	17.150	17.150	-	-	-	-	-	-	-	-	-	-	-	34.300
Mine Equipment	-	-	-	-	10.585	5.120	-	-	-	-	-	-	-	-	-	-	15.705
Mine Facilities	-	-	-	-	6.515	-	-	-	-	-	-	-	-	-	-	-	6.515
Townsite	-	5.000	-	-	2.000	-	-	-	-	-	-	-	-	-	-	-	7.000
Pre-Production Stripping	-	-	-	-	4.000	2.520	7.111	12.050	7.500	-	-	-	-	-	-	-	33.181
Other	1.861	-	-	-	-	-	-	-	-	-	-	-	-	-	-	-	1.861
ANNUAL TOTALS	29.861	33.381	-	17.150	41.250	7.641	7.111	12.050	7.500	-	-	-	-	-	-	-	155.943
CUMULATIVE TOTALS	29.861	63.242	63.242	80.392	121.642	129.283	136.394	248.444	155.944	-	-	-	-	-	-	-	-
<u>CAPITAL BUDGET ESCALATED FOR INFLATION</u>																	
Annual	32.100	41.267	-	25.656	67.856	13.830	14.151	26.390	18.075	-	-	-	-	-	-	-	-
Cumulative	32.100	73.367	73.367	99.023	166.879	180.709	194.860	221.250	239.325	-	-	-	-	-	-	-	-
<u>ESCALATION FACTOR</u>																	
Annual	7.5	15.0	10.0	10.0	10.0	10.0	10.0	10.0	10.0	-	-	-	-	-	-	-	-
Cumulative	-	1.236	1.36	1.496	1.645	1.81	1.99	2.19	2.41	-	-	-	-	-	-	-	-
<u>CONTINUING CAPITAL</u>																	
Present Mining Plan	17.265	6.475	2.100	2.000	2.000	2.000	2.000	1.000	-	-	-	-	-	-	-	-	34.840
Development Plan	-	-	-	1.000	1.000	1.000	1.000	2.000	3.000	3.000	3.000	3.000	2.000	1.000	1.000	1.000	23.000

FIGURE 2-19
VANGORDA PLATEAU DEVELOPMENT
CASE 4B-V PRODUCTION STATISTICS

YEAR	TOTAL MINE WASTE (M ³ 000)	PRODUCTION ORE (000 tonnes)	FEED LEAD %	GRADE ZINC %	LEAD CONC. GRADE % Pb	LEAD RECOVERY %	ZINC CONC. GRADE % Zn	ZINC RECOVERY %	CONCENTRATE LEAD (DMT)	PRODUCTION ZINC (DMT)	LEAD (000/lbs)	PAYABLE ZINC (000/lbs)	SILVER (000/oz)	GOLD (oz.)
1980	9,102	3,322	2.83	4.41	58.23	77.70	50.53	80.39	114,713	213,968	157,155	239,693	2,546	3,044
1981	10,872	3,404	3.00	5.18	61.00	84.00	50.40	80.00	130,296	260,440	178,566	260,060	1,907	-
1982	10,022	3,404	2.60	4.65	61.64	83.39	51.60	81.89	119,733	251,202	154,572	241,457	1,700	-
1983	8,268	3,404	3.40	4.80	67.00	87.50	53.50	88.50	151,148	270,284	212,095	270,971	3,030	-
1984	7,560	3,404	3.50	4.80	67.00	87.50	53.50	88.50	155,593	270,284	218,333	270,971	3,459	-
1985	4,400	3,402	3.13	4.56	56.77	83.36	53.14	82.30	156,096	240,226	185,426	239,086	2,862	18,685
1986	4,300	3,402	3.22	4.48	56.57	83.27	53.15	82.40	160,995	236,009	190,526	234,921	2,948	19,539
1987	1,333	3,402	3.18	4.43	56.66	83.31	53.15	82.46	158,818	233,529	188,259	232,471	2,835	19,160
1988	2,400	3,402	3.14	4.46	59.39	83.35	53.75	84.11	149,752	237,416	186,250	239,115	3,067	14,303
1989	4,800	3,402	3.16	5.15	63.07	85.32	54.31	85.40	142,034	275,505	187,602	280,390	3,169	8,756
1990	4,700	3,402	2.87	4.69	63.38	83.66	54.25	85.64	128,653	251,889	170,787	256,050	2,591	7,699
1991	4,383	3,402	2.85	4.65	63.29	83.56	54.26	85.60	127,792	249,332	169,380	254,394	2,406	7,830
1992	4,000	3,402	2.92	4.78	63.20	83.47	54.28	85.53	131,194	256,263	173,655	260,637	2,485	8,099
1993	4,000	2,613	2.77	4.72	61.74	81.89	54.54	84.59	95,943	191,292	124,057	195,501	1,916	8,276
1994	4,000	1,701	3.15	4.84	60.00	80.00	55.00	83.00	71,442	124,241	89,776	128,049	1,636	7,741
1995	2,500	1,701	2.81	4.51	60.00	80.00	55.00	83.00	63,731	115,770	80,086	119,318	1,459	6,906
1996	2,500	1,701	2.78	4.50	60.00	80.00	55.00	83.00	63,050	115,513	79,231	119,054	1,444	6,832
1997	581	1,306	2.75	4.50	60.00	80.00	55.00	83.00	47,887	88,689	64,228	96,095	1,170	5,447

N.B. Bulk production will be 34,724 DMT and 35,000 DMT in 1980 & 1981 respectively. Thereafter no bulk concentrate will be produced.

3.
THE GRUM DEPOSIT

3.1 REVIEW OF EXPLORATION AND DEVELOPMENT 1973-1976.

The Grum deposit was discovered in 1973 by the late Dr. Aaro Aho of the A.E.X. Syndicate while drilling a broad area of high Turam response and a coincident gravity anomaly in the general area of the Champ Deposit.

A.E.X. Syndicate drilled 16 holes totalling 4,000 metres to July 1974 when Kerr Addison Mines Limited assumed control of the project and drilled a further 13,000 metres of surface diamond drill holes spaced 60 metres apart on section lines 120 metres apart. This work indicated a deposit 1,680 metres long and 366 metres wide between sections 62W and 88W.

Upon completion of this initial drilling phase, an extensive underground development program was initiated. The deposit was explored by means of an 800 metre decline on a 16 percent grade. Two ramps, 120 metres apart, were driven along the plunge of the mineralization with connecting cross cuts at 120 metre intervals. Ring drilling in the plane of the geologic sections was conducted from the ramps at 60 metre intervals. The program included 2,900 metres of openings and 15,000 metres of diamond drilling.

Concurrent with the underground development, a further 24,000

metres of surface diamond drilling was carried out to complete the grid at 60 metre spacing on lines 60 metres apart from section 60W to 88W. Fill-in holes at 30 metre spacing were also drilled on sections 64W and 68W (Figure 3-7).

3.2 GEOLOGY

Both the Grum and Vangorda deposits occupy similar positions within the regional stratigraphy of the Anvil Range. The section is generally dominated by calcareous chlorite and chlorite-sericite phyllites in the hanging wall, and non-calcareous biotite-sericite phyllites and biotite-garnet-staurolite schists in the footwall. It appears that the amphibolite facies footwall sequence is separated from the hanging wall green schist facies by a low angle thrust fault at the base of the sulphide horizon. The sulphide horizons are closely associated with graphitic phyllite.

The sulphide horizons and enclosing rock units have been subjected to at least four periods of plastic deformation. The main structure controlling the distribution of rock type is a North-Westerly plunging series of more or less concentric "S" shaped recumbent folds. This folding was accompanied by a pervasive axial plane foliation which in turn has been kink folded and gently warped into broad synforms and antiforms. The deposit has been further complicated by North East striking high angle faults which cut all structures except the footwall thrust fault.

Though the sulphide horizon stratigraphy is complicated by overturned folds, two basic horizons generally predominate. The

upper horizon consists of massive pyritic sulphides, variably base metal bearing and variably baritic. The lower horizon consists of pyritic quartzites, banded or foliated and generally deficient in base metals.

3.3 THE DEVELOPMENT OF GEOLOGICAL RESERVES

3.31 THE CONSTRUCTION OF GEOLOGICAL SECTIONS

Geological sections and plans were constructed on a 1:500 scale by plotting data obtained from the underground development and the diamond drilling results. Since the deposit is both strataform and stratabound it was possible to treat the mineralized zones as rock types when constructing geological sections. Geological plans were constructed from the sections at 9 metre intervals corresponding to the mine levels. Simplified geological longitudinal and cross sections are shown in Figures 3-1 and 3-2 respectively. Equivalent sections of the Faro deposit are shown in Figure 3-3 and 3-4 to demonstrate the relative structural complexity of the Grum deposit.

3.32 THE DEVELOPMENT OF THE KERR ADDISON TONNAGE AND GRADE MODEL

Cyprus Anvil has begun to re-log the original diamond drill core and extend the assay and lithological data to allow the construction of an independent tonnage and grade model. In view of the time required to complete this project however, the Kerr Addison model was used as a basis for this evaluation.

short term manpower peaks and the attendant problems encountered in accommodating employees. The stripping contractor will provide camp accommodation for his workers.

The costs of this overburden stripping were estimated by Wright Engineers Limited, December 1979. Mining equipment selection was based upon the production criteria as shown and was chosen when practicable to duplicate equipment that is presently providing satisfactory service at the Faro pit.

FIGURE 3-8
EQUIPMENT PERFORMANCE CRITERIA

ITEM	PERFORMANCE
Shovel P & H 2100 or equivalent	3,000,000 m ³ /year
Drill Electric M4 or equivalent	10,000 m ³ /shift
Loader L800 in ore or equivalent in waste	148 m ³ /hour 281 m ³ /hour

Haulage of the ore and waste will be accomplished using electric wheel trucks similar to those currently in service.

Suitable waste dump sites were selected following deep hole drilling and some geotechnical evaluations of the potential sites.

The local mine infrastructure was predicated upon the number of

employees and types of equipment scheduled to work at the Vangorda Plateau open pit minesites. The capital provides for the shops, offices, warehouse and ancillary facilities deemed necessary to support an efficient mining operation, while reflecting the availability of existing support services at the Faro minesite.

Operating costs in general were based upon current experience in the Faro pit.

The study assumed that adequate supplies of fresh water could only be supplied by pumping from a well located near Vangorda Creek. Power will be supplied by a "branch" high tension line taken off the main transmission line servicing the existing facilities. A sub-station will be located at the Grum minesite.

4.1 HISTORICAL REVIEW

The Vangorda deposit, discovered in 1953 by the late Mr. Al Kulan, was the first mineral deposit discovered in the Anvil District. The property was subsequently optioned by Prospector's Airways Co. Ltd., a subsidiary of Kerr Addison Mines Ltd. During 1954 and 1955 the deposit was diamond drilled on a 60 metre center grid pattern with fill-in holes at 30 metre spacing along alternate cross sections.

A preliminary mining and cost study was conducted by General Engineering Company Ltd. in 1964. The results of this study indicated a probable mineable ore reserve of 5.6 million tonnes with grades of 3.0% lead, 4.9% zinc, 50.9 gms/tonne silver, and 0.75 gms/tonne gold. This data was based upon a 10 percent mining dilution factor.

4.2 THE 1979 EXPLORATION & DEVELOPMENT PROGRAM

Analysis of the earlier Vangorda diamond drill data indicated serious deficiencies in the identification of those geologic units now recognized as critical to the understanding of deposits in the Anvil District. Poor core recoveries, inadequate logging techniques, assaying inconsistencies and sample deterioration further complicated the task.

Accordingly a re-drilling program was initiated along sections 2E, 6E, 10E, 18E and 26E (Figure 4-4) to assess the reliability of original assay values, evaluate original geological interpretation and provide samples of various ore types for metallurgical bench testwork.

The results of this re-drilling program, when compared with original data clearly indicated the need to extend the re-drilling program to obtain dependable information to construct a geologically based grade and tonnage model.

The extended program provided for the systematic drilling of all section 2W to 12E inclusive at 30 metre centres along sections 60 metres apart. Fifty three holes were drilled in an area approximately 800 metres long (NW-SE) by 200 metres wide (NE-SW).

All holes were logged for structure and lithology, and the sulphide bearing lithologies were routinely sampled at 1.0 to 2.0 metre long assay intervals selected to correspond with lithologic breaks where possible. Units less than one metre thick were combined with other units above or below and the samples assayed for lead, zinc, silver and copper. Gold, barium, mercury, manganese, pyrite, pyrrhotite, and specific gravity determinations were added for intervals of potential mining width grading more than 3% combined lead-zinc.

The data generated by the 1979 diamond drill program was used as the basis for the development of the tonnage and grade model, and the preliminary mine operating plans. Work performed by others determined that mineralized zones between sections 14E and 30E offered a relatively small economic tonnage potential. In 1979 some test drilling in this area yielded poor core recoveries when using conventional equipment. This zone containing sulphide sub-outcrops will be further examined in 1980.

4.3 GEOLOGY

The Vangorda deposit lies within the Anvil Range which is located along the southwestern margin of the Selwyn Fold Basin, immediately northeast of the Tintina Trench. Regionally stratabound between lower Paleozoic units, the deposit is spatially related to a graphitic phyllite that occurs at a facies change between calcareous phyllites of the Vangorda formation above and non-calcareous phyllites of the Mt. Mye formation below. Meta volcanic rocks are rare in the immediate vicinity of the deposit but are regionally common throughout the Vangorda formation. The deposit has been deformed to produce large scale "Z" symmetry folds. The principal foliation as observed in outcrop and core is axial and planar to these folds.

The sulphide horizon consists of the following principal lithologies from top to bottom:

- a) Sulphide bearing graphitic quartzite, generally pyrite rich and locally base metal bearing.
- b) Barite and massive pyritic sulphides, which are base metal bearing.

4.4 THE DEVELOPMENT OF GEOLOGICAL RESERVES

4.41 THE CONSTRUCTION OF GEOLOGICAL SECTIONS.

Geological cross-sections, oriented at 050° azimuth from true North and looking toward the North West were constructed at 1:500 scale (Figure 4-1). Drill holes were computer plotted in their deviated position onto the plan of the section. Structural data was plotted with reference to an average S2 strike of 130° azimuth with dips to the South West.

Using the strataform and stratabound nature of the deposit as a guide, a generalized outline of the horizon was interpreted on each section. At the margins of the deposit, the sulphide limit was extrapolated by one-half the drill hole spacing.

4.42 DEVELOPMENT OF THE TONNAGE AND GRADE MODEL

A three dimensional block model, parallel to the section grid, was developed for the Vangorda deposit. The unit block dimensions used were 6.3 metres bench height by 19.0 metres width on Easting by 61.0 metres width on Northing.

The sulphide horizon outline on the geological sections was converted into block data. Blocks were designated as "sulphide" when fifty percent or more of the block was located within the sulphide horizon. All other blocks were coded "waste".

The following values were assigned to each unit block:

1. Lead content (%)
2. Zinc content (%)
3. Copper content (%)
4. Silver content (gms/tonne)
5. Combined lead and zinc content
6. Rock Code
7. Proportion of unit block beneath topography (%)
8. Unit block weight (tonnes)

Composite lead, zinc, copper and silver values over a bench height were calculated from each drill hole. For all external contacts, and for internal contacts where the waste thickness was greater than one-half the bench height, "not assayed" intervals were excluded from the composite calculation. In

these cases, a dip projection method was simulated by calculating bench height composites up or down from the contact. When this failed to give a composite length greater than 3.2 metres, no value was calculated for that bench.

The composite values were used to interpolate grades into the blocks. Interpolation was achieved by level, and then by section using a search distance along a section of 30 metres. Where two or more composites were used, an inverse squared weighting was applied to the values.

Tonnage for "sulphide" blocks was calculated at 4.2 tonnes per cubic metre, based solely on a geological estimate of rock type distribution and past experience.

The topographic surface used in the model was interpolated and extrapolated from drill hole collar elevations

4.43 GEOLOGICAL RESERVES

The following geological reserves were calculated at varying combined lead-zinc cut-off grades:

FIGURE 4-2
VANGORDA GEOLOGICAL RESERVES

CUT-OFF GRADE (Pb + Zn)	3.5%	4.0%	4.5%	5.0%
Tonnage (tonnes 000's)	7,090	6,751	6,473	6,134
Lead (% Pb)	3.4	3.5	3.6	3.7
Zinc (% Zn)	4.5	4.6	4.7	4.8
Silver (Ag g/tonne)	49.6	50.7	51.7	52.8

4.5 THE PLANNING OF THE VANGORDA PIT

The program used to develop the Vangorda "ultimate economic pit" was the same as that used for the Grum pit analysis. The metallurgical performance, operating costs and pit slope angle criteria were adjusted to reflect the differing operating and geotechnical parameters between the two deposits.

4.51 ANNUAL PRODUCTION SCHEDULES

Using the phase inventories by bench, a production rate of 4660 tonnes per day, and 934,000 cubic meters of pre-production alluvial stripping, ore delivery schedules were determined and annual feed grades were calculated. Since the model block grades do not include any dilution at geological ore-waste contacts, these grades were subsequently adjusted downward to allow for mining dilution.

Using historical data from the Faro Deposit as a guide, a review of the waste/ore contacts to be mined yielded the following grade dilution schedule for the Vangorda Deposit.

FIGURE 4-3
VANGORDA PIT DILUTION FACTORS

YEAR	1	2	3	4
Lead	-5%	-3%	-2%	-2%
Zinc	-3%	-3%	-2%	-2%
Silver	-5%	-3%	-2%	-2%

FIGURE 4-4
VANGORDA ANNUAL PRODUCTION SCHEDULE

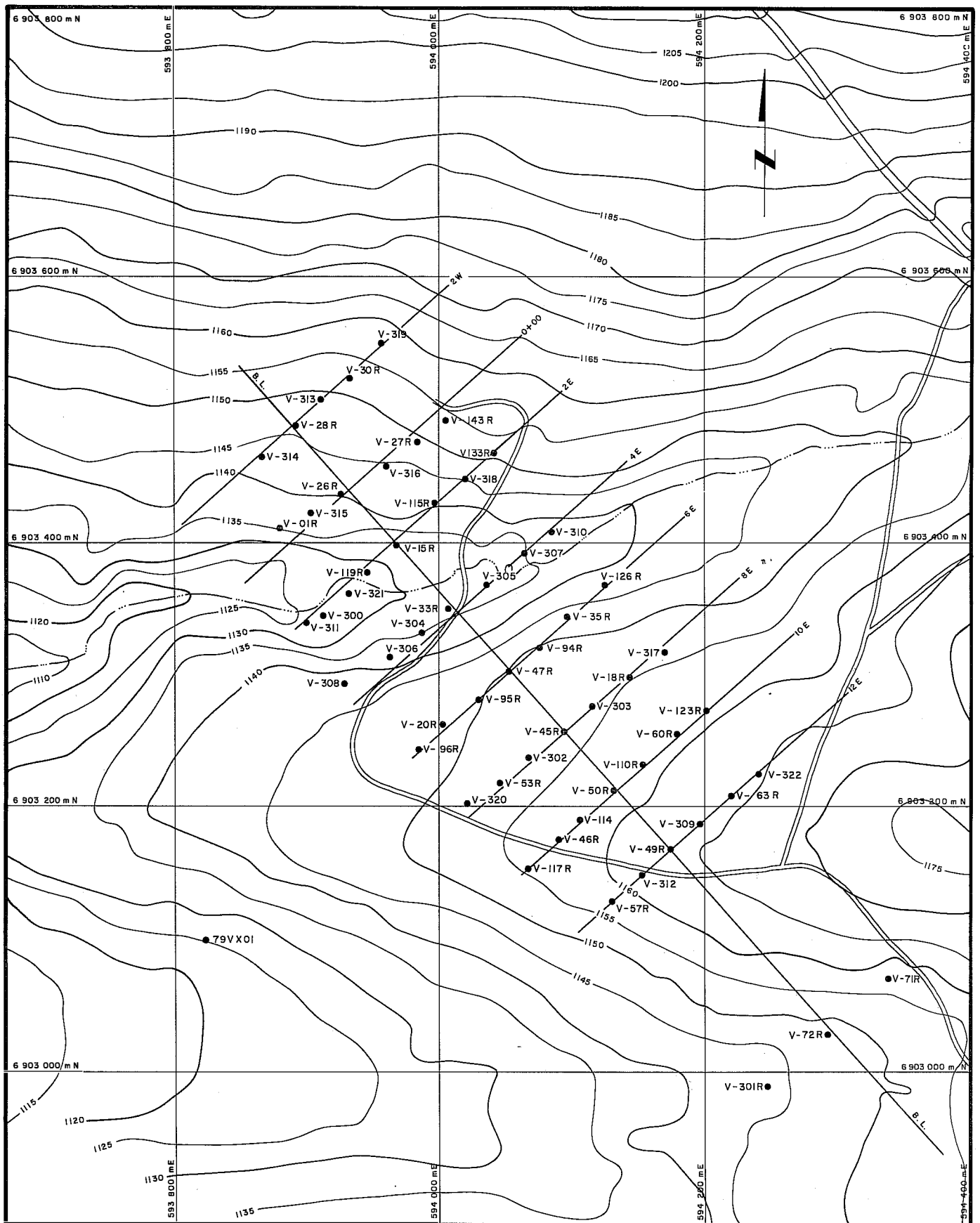
A. Cut-off grade = 4.0%

YEAR	1	2	3	4	TOTAL
Waste (000's m ³)	2920	2920	659	0	6499
Ore (000's tonnes)	1701	1701	1701	1031	6134
Lead (% Pb)	3.5	3.6	3.6	3.2	3.5
Zinc (% Zn)	4.9	4.8	4.7	3.6	4.6
Silver (Ag g/tonne)	47.3	52.6	53.0	46.6	50.2
Gold (Au g/tonne)					N/A

N/A: Not available at this time.

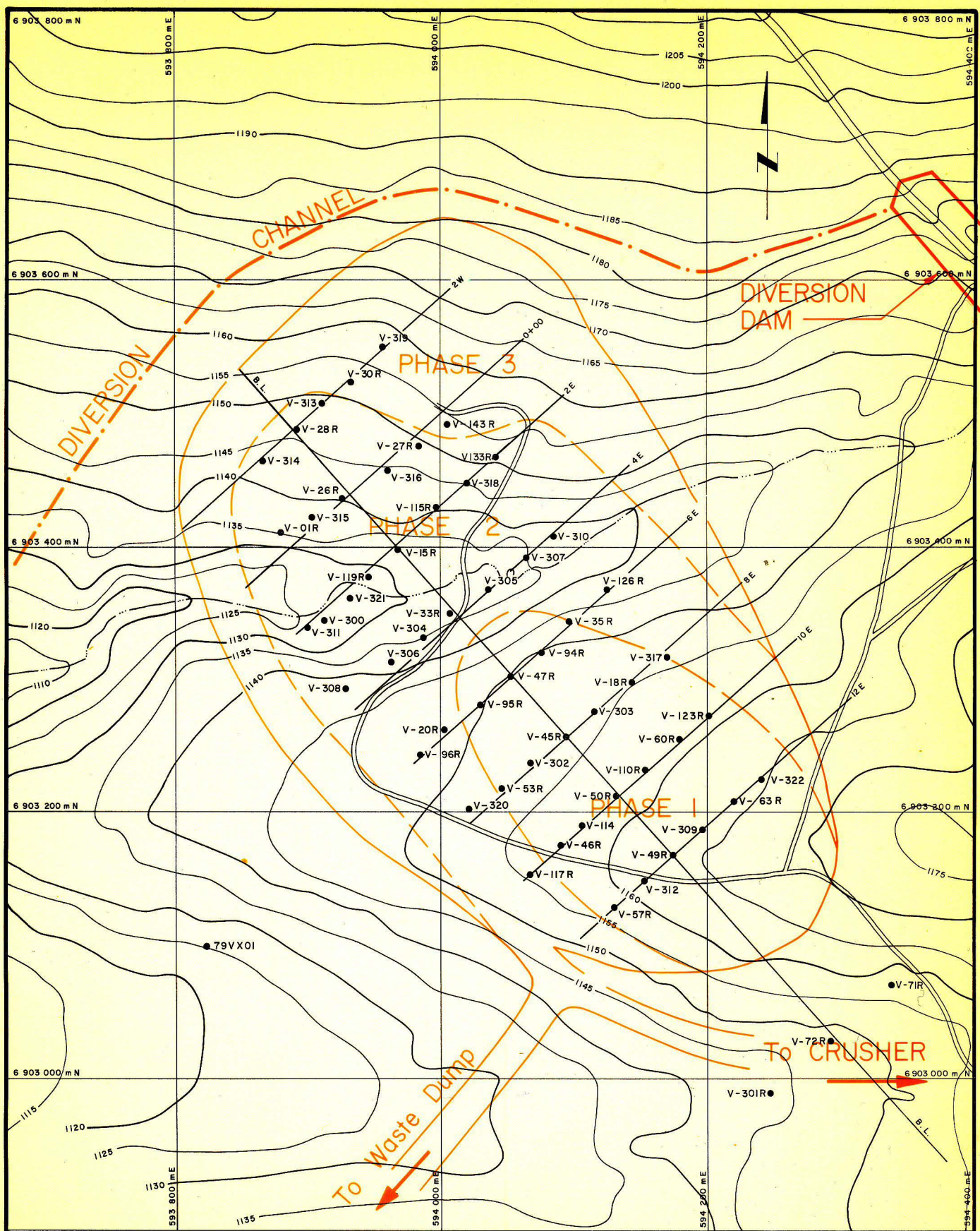
B. Cut-off grade = 4.5%

YEAR	1	2	3	4	TOTAL
Waste (000's m ³)	2920	2920	696	0	6536
Ore (000's tonnes)	1701	1701	1701	877	5980
Lead (% Pb)	3.5	3.6	3.6	3.2	3.5
Zinc (% Zn)	5.0	4.8	4.7	3.7	4.6
Silver (Ag g/tonne)	47.5	52.7	53.9	47.0	50.7

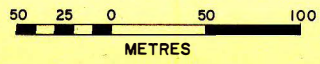


VANGORDA DEPOSIT
D.D.H. PLAN





March 1980 P.T. / c.i.c.



VANGORDA DEPOSIT
D.D.H. PLAN
OPEN PIT OUTLINE

FIGURE 4-5

4.6 THE OPERATION OF THE VANGORDA PIT

The preliminary mine plan formed the basis for predicting operating criteria, capital expenditures and operating costs. Though detailed studies of this deposit commenced in the Spring of 1979, the high quality of the data generated by the closely spaced drilling program provided a sound basis for this analysis - and for the necessary continuing detailed engineering studies. As shown in Figure 4-5 the Westerly portion of the deposit to be mined is situated in the Vangorda Creek Valley and directly beneath the creek. Preliminary engineering studies were conducted in 1979 to design an environmentally acceptable diversion ditch to direct the creek flow to the west of the ultimate pit wall. A suitable routing was located by which the flow will be returned to the original water course to the South of the open pit.

All mine production equipment will be similar to units presently in service. Waste will be mined primarily by an electric shovel, supplemented as required by a loader. A suitable waste dump site was located and tested by deep hole drilling immediately to the south of the proposed open pit. Ore will be mined with a front end loader and transported to the Grum crushing plant by large electric wheel trucks. The complete cycle time for an ore truck to be loaded at the bottom of the ultimate pit, to deliver ore to the crusher and

to return to the ore face was predicted to be approximately 40 minutes, assuming a maximum ramp grade of 8 percent. Blast hole drilling will be carried out by one electric drill.

The mechanical shops, offices, warehouse facilities and other services will be located adjacent to the Grum open pit in deference to the larger size of the Grum deposit.

Power to the pit will be supplied by a 4160 volt overhead line from the main substation located at the Grum minesite.

5.1 INTRODUCTION

In order to maximize the benefits derived from the acquisition of the Grum and Vangorda deposits a number of mine development plans were evaluated to select the one which offered the best security of ore supply and the most attractive return on investment.

The financial benefits attributed to each development plan were calculated by comparing the cash flow generated by the particular plan with that which would result from the implementation of the present mining schedule, which excludes Vangorda Plateau ores.

Any development program to integrate the ore reserves in the Vangorda Plateau orebodies into the Faro operation and treat these ores in the existing mill would consist of the following activities:

- A modification of the existing mill in order to provide additional grinding and flotation capacity to treat the Vangorda Plateau ores. Although mineralogically similar to the Faro ore, these ores are structurally different and require a finer grind in order to achieve satisfactory metallurgical recoveries. No increase in total throughput is envisaged at this time.

- Additional tailings disposal capacity.

- The provision of additional electric power required by the increased mill horsepower requirements.
- Construction of additional married housing accommodation in the Town of Faro to improve the ratio of married to single employees in order to promote long term stability of the work force.
- Provision of an ore haulage system to transport the ore from the Vangorda Plateau orebodies to the existing mill, a distance of approximately 14 kilometers.
- Pre-production stripping of the orebodies.
- Construction of ancillary facilities such as a shop, change house, warehouse, and offices.
- Construction of required housing facilities in the Town of Faro for any additional personnel required.

These modifications, made for the purpose of milling the Vangorda Plateau ores, will enhance the metallurgical performance of Faro

ores, thus offering a wide variety of development options.

Having identified those cases which offered the most favourable returns on investment, practical considerations were integrated into the final analysis to select the recommended mine development plan.

5.2 MINE DEVELOPMENT CASES

Eight mine development cases were examined and are schematically depicted in Figure 5-1. These cases were divided into four series and are briefly described below.

SERIES 1:

This series considered only Faro pit ores and made no provision for the mining of the recently acquired Vangorda Plateau orebodies. Accordingly mining operations cease in 1990.

CASE 1:

This case is the present Faro mining plan and represents the base case against which all development plans are compared. The case provides for no major capital expenditures during the rest of the life of the Faro pit, and the metallurgical performance equal to that achieved in 1978 and 1979.

CASE 1A:

This case differs from case 1 in that \$11 million would be spent in 1980 and 1981 to upgrade the existing flotation circuit and install basic instrumentation systems to improve metallurgical control. Metallurgical performance was improved to reflect the changes in the flotation circuit.

CASE 1B:

This case was based on the implementation of the recommended mill modifications to be complete by year end 1981. The modifications, which included the additional grinding circuit, expanded flotation and dewatering sections and the supplemental power generating facility would cost approximately \$44 million. The plant metallurgical performance was adjusted to recognize the benefits derived from finer grinding.

In addition to the mill modifications, the new tailings impoundment facilities costing \$12 million were required to provide adequate capacity and settling times for the finer tailings.

SERIES 2:

These cases assume that Vangorda Plateau ores would be mined upon the exhaustion of the Faro pit ore reserves in 1989.

CASE 2A-G:

This case is identical to case 1A through 1988. Thereafter only Grum and Vangorda ores would be milled in turn at the rate of 4,660 tonnes per day until the exhaustion of these deposits in

2001. The finer grind necessary for the effective selective flotation of these minerals would be obtained by treating the reduced throughput in the existing grinding circuit.

CASE 2B-G:

This case is identical to case 1B through 1988. Thereafter, 6,525 tonnes of ore per day would be mined from the Grum and Vangorda deposits concurrently in the proportion of 4660 tonnes and 1825 tonnes respectively until the exhaustion of the Vangorda Plateau ores in 1998.

SERIES 3:

These cases assumed that Vangorda Plateau ore would be mined concurrently with that from the Faro pit in equal proportions commencing in 1983 to provide a total daily mill feed tonnage of 9,320 tonnes.

CASE 3B-G:

This case is identical to case 1B through 1982. Grum ore deliveries would commence in 1983 at the rate of 4,660 tonnes per day and continue until the exhaustion of the Grum reserves in 1992. Grum ore would be replaced with that from Vangorda until the exhaustion of this deposit in 1995.

CASE 3B-V:

Case 3B-V assumes that ore from the Vangorda pit is mined in 1983 followed by Grum ore in 1986. Otherwise this case is the same as 3B-G.

SERIES 4:

This series assume that the Vangorda Plateau ore would be mined concurrently with that from the Faro pit and in equal proportions commencing in 1985 to sustain a mill throughput rate of 9,320 tonnes per day.

CASE 4B-G:

This case is identical to case 1B through 1985. Grum ore deliveries would commence in 1985 at the rate of 4,660 tonnes per day and continue until the exhaustion of these reserves in 1993. Grum ore would be replaced with that from the Vangorda until the exhaustion of this deposit in 1995.

CASE 4B-V:

Case 4B-V assumes that ore from the Vangorda pit is mined in 1985 followed by Grum ore in 1988. Otherwise this case is the same as 4B-G.

5.3 THE ANALYSIS OF THE MINE DEVELOPMENT CASES

In a preliminary financial analysis, Cases 1A and 2A-G were immediately precluded from further consideration because of the very poor relative economic performance. For practical reasons, in that Grum mining plans could not be developed and implemented in the time schedule, Case 3B-G was rejected.

Complete financial analyses were carried out for each of the five remaining development cases. Of these five, the most attractive return on investment was exhibited by case 4B-V. In addition to being the most financially attractive, this case also is desirable from a practical standpoint. Adequate time is available to develop the necessary planning and construction of an ore haulage system as well as to develop the necessary mine planning to commence ore production from the Vangorda Deposit in 1985 and from the Grum Deposit in 1988.

Case 2B-G demonstrated the next best DCF/ROI of the five cases. This case is not recommended because of the fact that after 1988, the full capacity of the mill is not utilized, thereby reducing concentrate output and sales. This under-utilization results from the fact that in the present planning the Grum Deposit is limited to an annual production rate of 1.7 million tonnes due to the

complexity of the orebody, and the Vangorda Deposit reserves are not sufficient to sustain full mill capacity throughout the life of the Grum Deposit. Further, this case depends both upon an earlier total supply of ore from the Vangorda Plateau and attendant dependency upon the ore haulage system.

Case 4B-G shows no advantage, either financial or practical, over Case 4B-V. The same applies to Cases 1B and 3B-V. Case 1B is not truly a development case, because it does not include any ore development from the Vangorda Plateau. Case 3B-V has a practical limitation in that the time allowed for planning and construction of the ore haulage system is limited.

Based on both financial and physical considerations, Case 4B-V is the recommended development case.

6
ORE HAULAGE

6.1 INTRODUCTION

Various ore haulage systems were examined to determine the most dependable and cost efficient means of transporting 1.7 million tonnes of ore per year from the Vangorda Plateau to the existing mill site; a distance of approximately 14 kilometres. In consideration of possible mill expansions, and the requirement to produce the entire mill ore supply from the Vangorda Plateau in the future, each of the systems investigated would be capable of providing increased haulage rates to meet projected requirements.

A preliminary engineering study was commenced in the fall of 1979 to evaluate a number of potentially feasible ore haulage systems which included:

- a) Trucking utilizing off-highway equipment
- b) Rail transportation
- c) Conveyor by means of a conventional belt system
- d) Trucking using smaller highway trucks
- e) Conveying ore on a cable belt

The capital expenditures, operating costs and manpower requirements shown in Figure 6-1 were derived from preliminary data generated during the feasibility study of the haulage alternatives conducted by Swan Wooster Engineering Co. Ltd., February 1980.

FIGURE 6-1
ORE HAULAGE SYSTEMS - PRELIMINARY COST DATA

ITEM	OFF-HIGHWAY TRUCKS	RAIL	CABLE BELT CONVEYOR	HIGHWAY TRUCKS	CONVENTIONAL BELT CONVEYOR
Initial Capital Cost (\$million)	32.5	38.6	38.1	42.4	44.1
Average Direct Operating Costs (\$/tonne)	1.37	1.39	1.65	2.12	1.34
Total Number of Employees	37	33	30	68	30

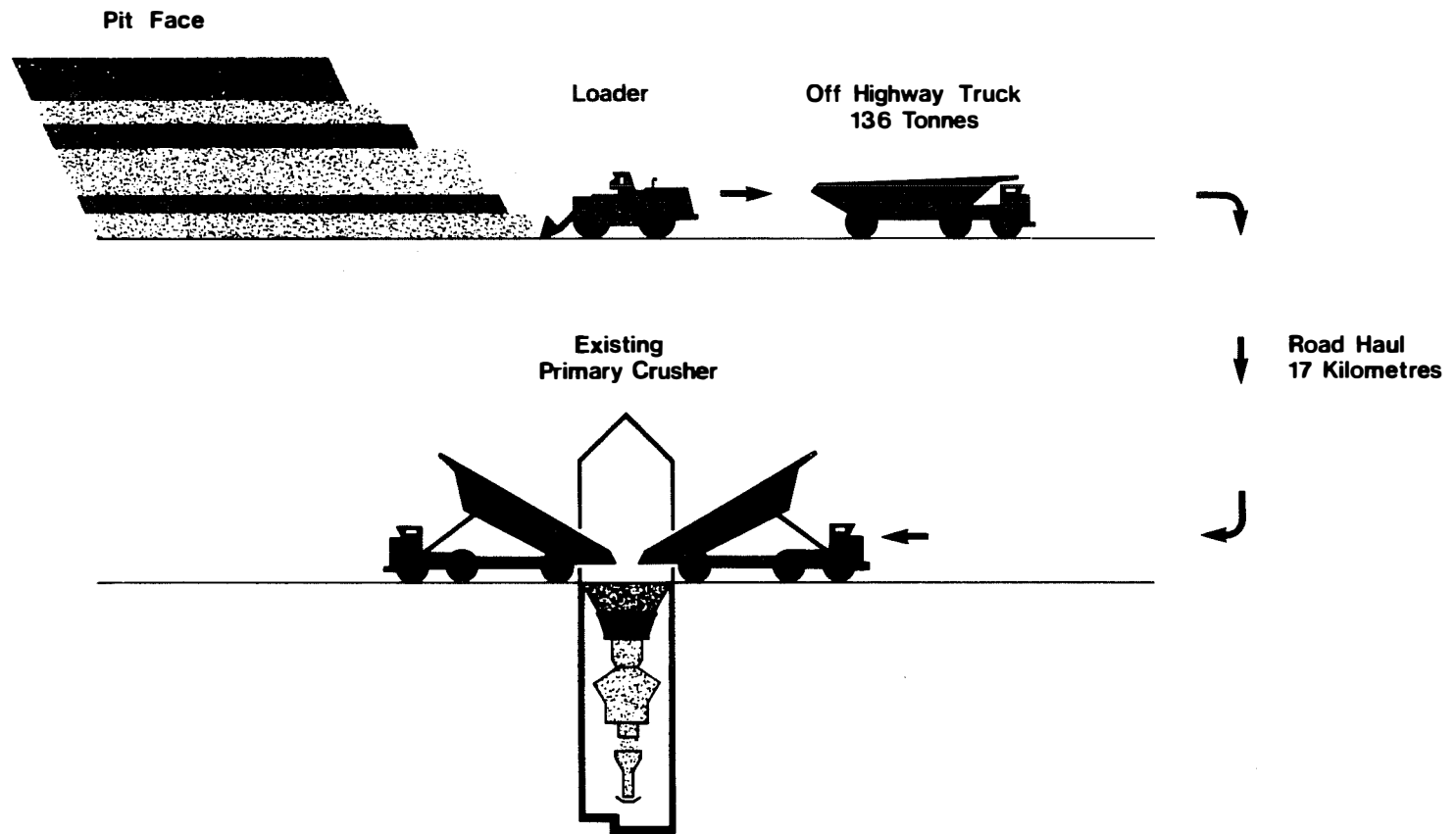
The capital and operating expenses include the cost of housing, and provide for the transportation of ore from the pit face to the existing crusher.

6.2 TRANSPORTATION ALTERNATIVES

6.21 OFF-HIGHWAY TRUCKING

Off-highway trucking utilizes equipment which, by virtue of size and weight of the individual units, may not travel upon conventional highways. Conceptually this alternative required that off-highway trucks and or trailers be loaded at the respective ore face by a front end loader. The truck would then proceed directly to the existing primary crusher at the millsite, over a 30.5 metre wide haulage road to be built between the Vangorda Plateau and the millsite. Figure 6-2.

The 136 tonne Caterpillar tractor/rear dump trailer was found to be the most cost efficient off-highway unit, when compared to various rear dump, side dump and train configurations. This unit which is currently successfully used by Pine Point Mines Ltd. in the Northwest Territories offered the most attractive net payload/gross weight ratio and was demonstrably more fuel efficient than the other units considered. An analysis of the cycle times between the Grum deposit and the mill based on a maximum speed of 48 km/hr indicated that 7 trucks operating and 1 truck spare would be required to haul the planned tonnage on a one shift per day, 7 days per week basis.



**FIGURE 6-2 OFF HIGHWAY TRUCKING SYSTEM
THE DEVELOPMENT OF THE VANGORDA PLATEAU ORE DEPOSITS**

That identical units were working successfully at similar latitudes was considered to be an advantage of this system. Scheduled daily ore commitments could be maintained despite temporary reductions in equipment availability by simply extending the operating times of the remaining vehicles.

The feature common to all alternatives considered, other than the off-highway system was the provision of an additional primary crusher and crushed ore storage facility at the Vangorda Plateau. Thus, while capital and operating costs compared most favourably with other alternatives, the off-highway arrangement did not reduce the risk of production loss that has resulted during shut-downs of the primary crusher. Such disruptions have occurred during scheduled major overhauls of the unit, and when handling wet or frozen ore.

Certain disadvantages were attributed to the system due to the fact that no such equipment is currently in use at the Faro pit. Thus additional operator training programs would be required and warehouse inventory values would increase. Pit ramp slopes would generally be designed at grades lower than those that could be efficiently handled by conventional haulage trucks to reflect the inferior climbing capabilities of the tractor/trailer configuration.

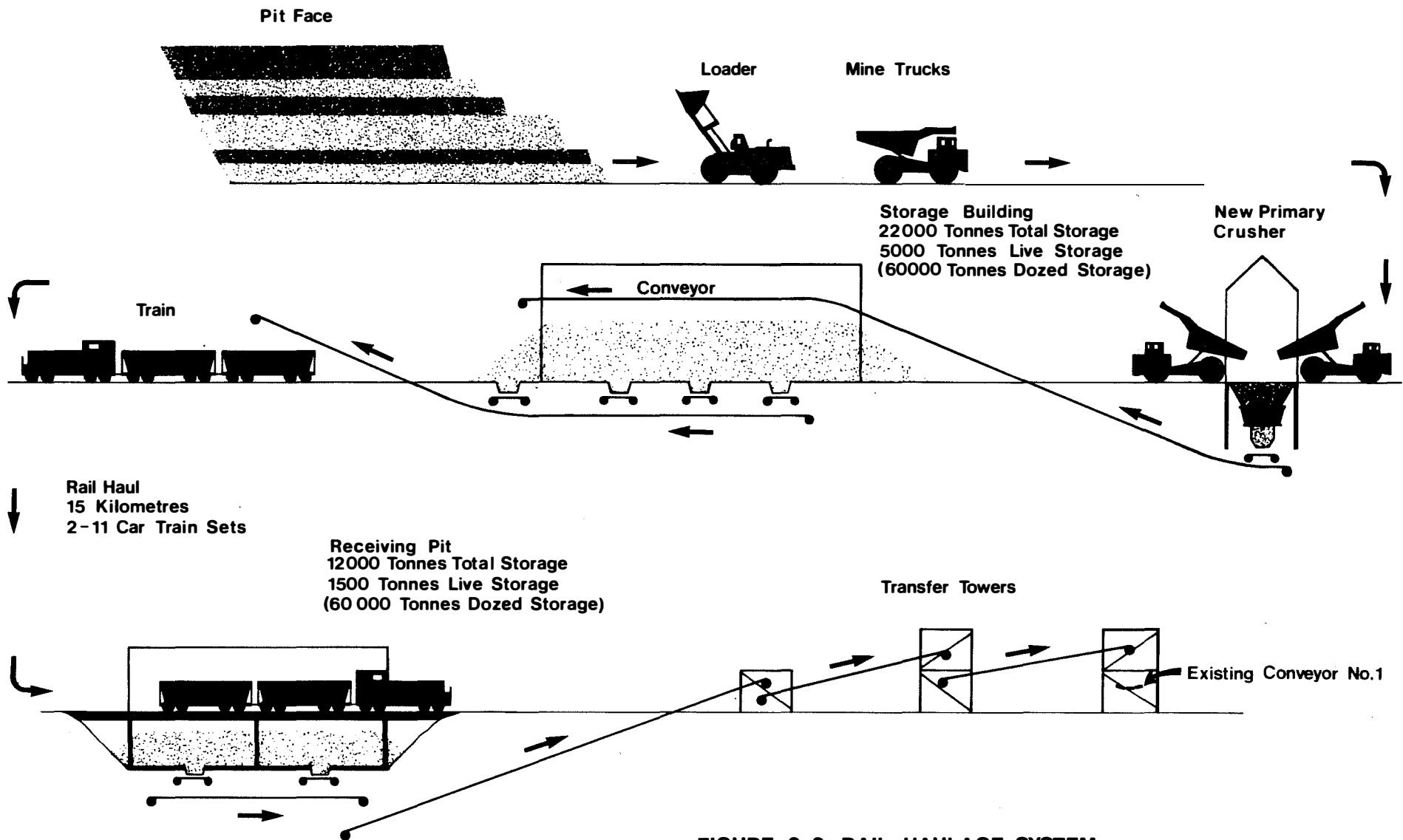
The schist and phyllite waste rock moved during the normal course of the mining, does not exhibit the ideal physical characteristics required of road surfacing material. More suitable material is available locally but at additional expense. Experience has demonstrated that normal trucking operations may be impaired by adverse climatic conditions less likely to affect rail and conveyor haulage systems.

Finally, effective control was considered difficult to maintain over a number of individually operated haulage units traveling over long distances, thus creating the potential for system inefficiencies.

Despite the disadvantages of the off-highway arrangement, the favourable capital and operating costs demand that more detailed studies be conducted to more thoroughly evaluate this generally accepted mode of ore transportation.

6.22 RAIL TRANSPORTATION

The rail system required that conventional haulage trucks be loaded at the face and discharged into a primary crusher located at the Grum minesite. The crushed ore would be delivered to a covered 5,000 tonne stockpile from which



**FIGURE 6-3 RAIL HAULAGE SYSTEM
 THE DEVELOPMENT OF THE VANGORDA PLATEAU ORE DEPOSITS**

material would be drawn by a conveyor belt to load standard gauge, bottom dump rail cars of 80 tonne capacity. (Figure 6-3).

Since the proposed rolling stock included two 800 HP diesel electric locomotives, the system offered flexibility in the selection of train configurations. Thus it would be feasible for each locomotive to pull 11 cars constituting one train or alternatively both locomotives could be operated in tandem to haul one 22 car train. In either case adequate time would be available in one shift to haul the scheduled ore commitments.

The planned rail alignment consisted of a 14.4 kilometre track placed on a 7.3 metre wide rail bed. The line was of favourable grade over most of its length with the exception of a 1.0 km 1 percent adverse grade located at the West end of the line.

The rail cars discharge into a 2,000 tonne capacity stockpile at a trestle dumping station located to the Southwest of the concentrator from whence material was transported by conventional conveyor belt systems and introduced into the existing crusher circuits. The stockpiles were designed to facilitate the removal and replenishment of ore from the system to permit extra-ordinary storage of large volumes of crushed ore prior to major scheduled overhauls of a primary crusher.

The capital cost provided for three spare ore cars and all the track maintenance equipment deemed necessary to support an efficient railroad operation. The rail transportation system offered many tangible advantages in addition to the favourable capital and operating costs. Such systems are simple, well-proven and currently operating successfully in cold climates. Since the proposed locomotives are widely used by major railroad companies across Canada, spare parts are readily available. The rail alternative included provision for the second primary crusher and stockpile facilities and was less prone to disruptions caused by adverse climatic conditions. Supervisory control of the system was considered to be more readily achievable when compared with the off-highway alternative.

Since railroad rolling stock, track structures and ties are normally amortized over a 25-30 year period, there exists an additional cost benefit that is not evident in this report which only considers open pit operations up to 1997. Net present value calculations conducted over extended periods of time to include future underground ore developments could thus tend to favour the rail transportation over the off-highway system.

Disadvantages of the rail alternative include the need for

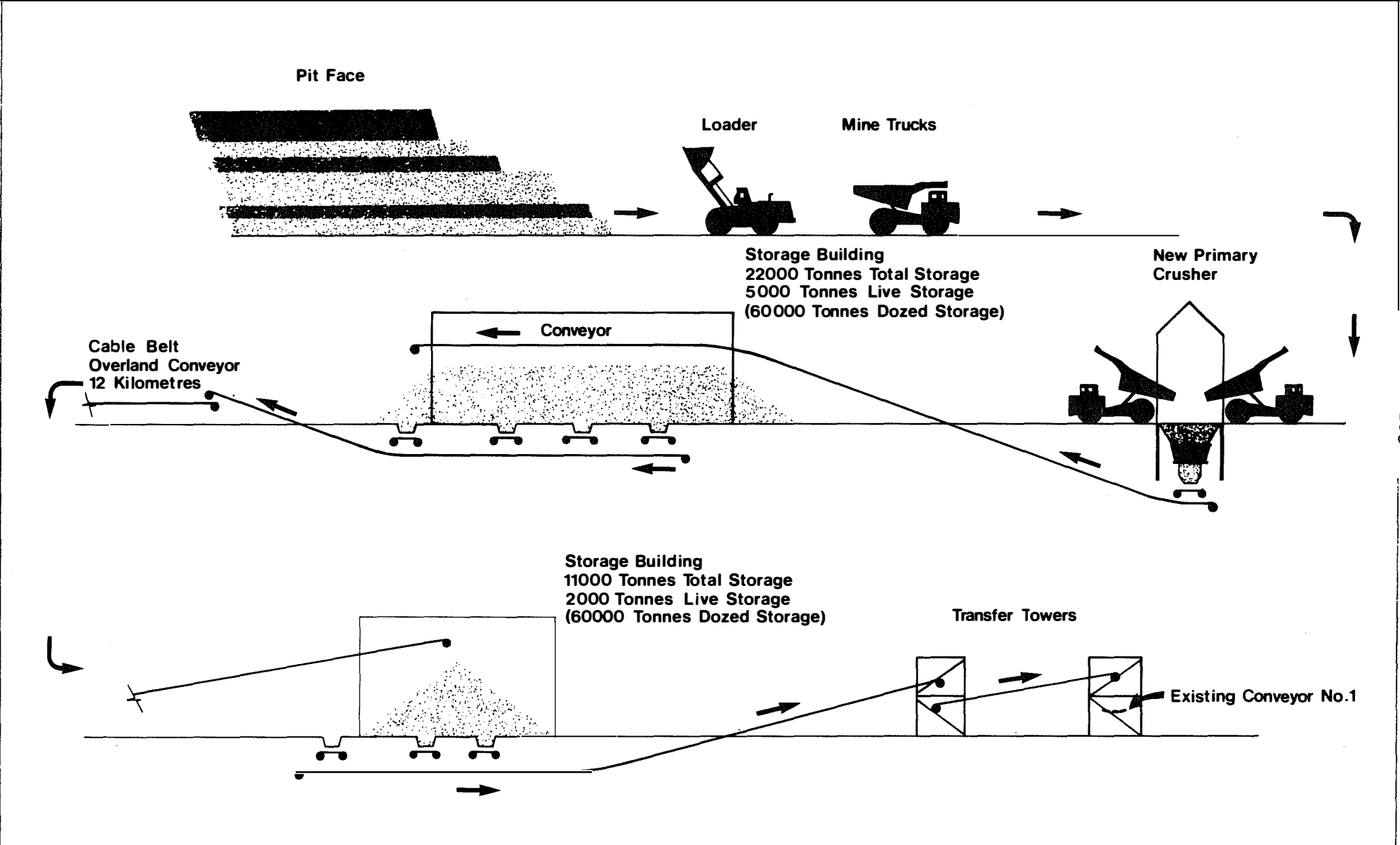
additional training programs and warehouse inventories generated by implementing a new system. Further, the restraints imposed on railroad development by natural topography would almost certainly preclude the extension of the proposed system in an Easterly direction toward the DY and Swim deposits.

6.23 THE CABLE BELT SYSTEM

The cable belt system was developed in England in the early 1950's to meet the need for higher conveyor horsepower than could be obtained with the then standard fabric belt-on-idler conveyors.

Since their introduction, cable belt conveyors have been installed in generally long-haul mining applications in many countries, including the United Kingdom, South Africa, Australia, Canada, Jamaica, Germany and Brazil.

The unique feature of this system is the separation of the driving (tension) medium from the material carrying medium. In conventional systems, the belt must be capable not only of carrying the material load, but also able to transmit the driving tension. In the cable belt system, the material is



**FIGURE 6-4 CABLE BELT HAULAGE SYSTEM
 THE DEVELOPMENT OF THE VANGORDA PLATEAU ORE DEPOSITS**

carried on a transversely stiffened but longitudinally flexible belt, riding on two endless loops of wire rope that transmit the driving tension. The ropes are supported at intervals by ball bearing pulleys. Molded rubber grooves on the belt grip the wire rope and prevent belt slippage. The wire ropes are driven by Koepe friction wheels at the drive unit, which incorporate a differential to allow for slight inequalities in rope movement. Because the ropes carry the driving tension, only enough tension to prevent folding is applied to the belt.

The mine haulage, crushing and stockpiling facilities included in this system were identical to those described in the rail haulage alternative. Thereafter, the 4,660 tonnes of ore per day would be carried by the 12.8 kilometre long, 76.2 centimetre wide conveyor to a 2,000 tonne covered surge pile. Two 800 HP electric motors would drive the belt at approximately 213 metres per minute.

The conveyor belt systems were found to be less labour intensive than the rail and off-highway alternatives. The relative high operating costs applied to the cable belt were based upon pessimistic estimates of rope life. It is probable that the detailed engineering studies proposed will result in a reduction of these operating costs to levels closer to those reported by cable belt users.

When compared to a conventional conveyor over long distances, the cable belt generally offered reduced maintenance costs, system simplicity and proven reliability. Since the belt itself does not transmit the driving tension, the potential for extensive longitudinal belt rips and the time required to perform low tension belt splices, is minimized. The overall rolling resistance is reduced in the conveyor belt system by eliminating belt flexibility over troughing idlers and reducing the total number of bearings. The net effect of these differences results in a lower power consumption.

There exist two potential disadvantages of the cable belt system when compared with the rail and off-highway trucks. First, the cable belt system is unique and solely dependent upon the performance of one conveyor. Although cable belts have demonstrated high availability at other mines complete spare parts modules must be maintained at the minesite to ensure the rapid change-out of worn or damaged components. Extensive lead times would be required for the purchase of all major mechanical components other than normal operating supplies.

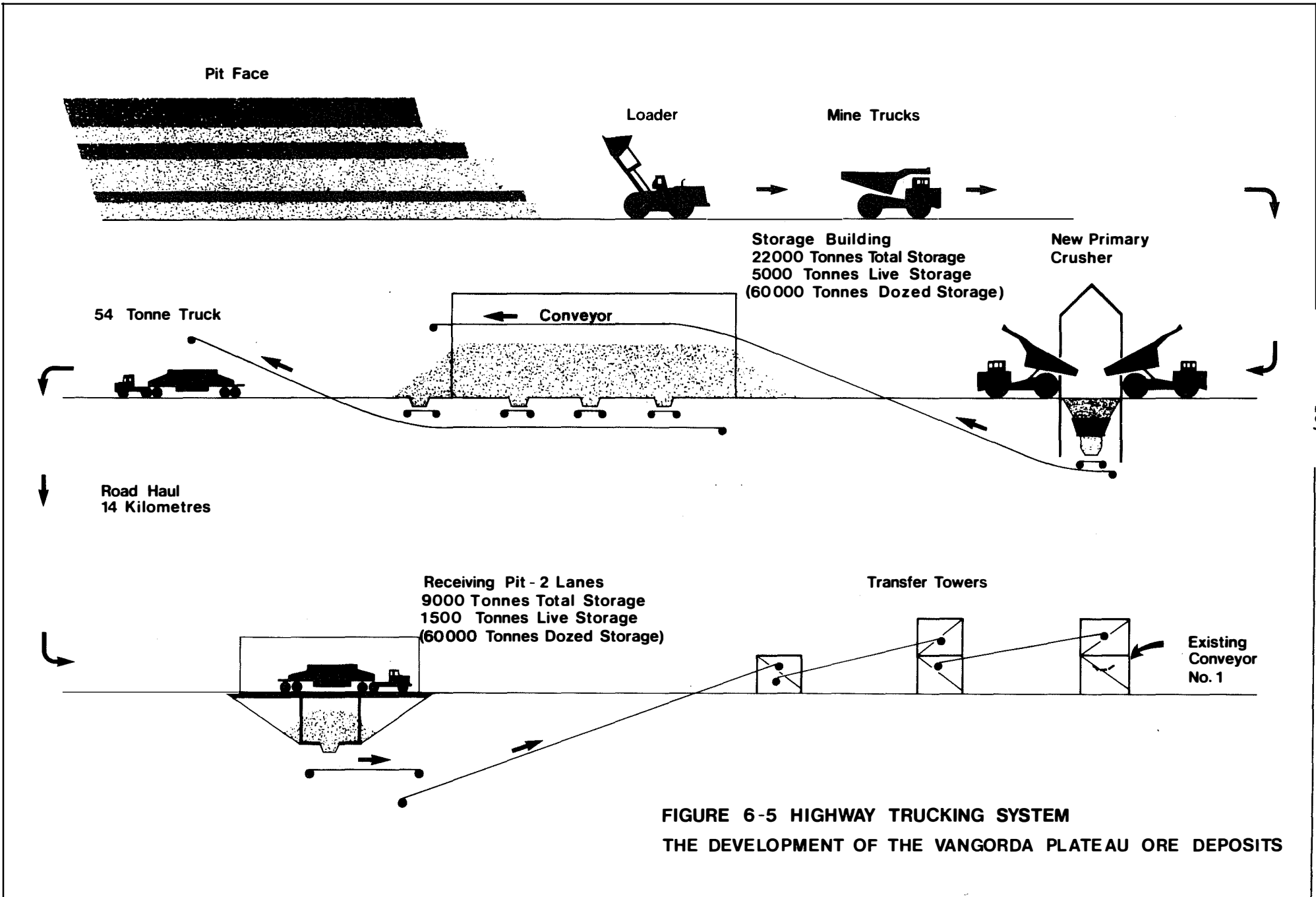
The second potential disadvantage relates to the operation of the system in sub-arctic climates. Despite the universal

acceptance of the cable belt for moving bulk materials over long distances there is no known installation that experiences the cold temperatures that prevail in the Yukon winter. Although information to date would suggest that the system is capable of providing satisfactory service under all seasonal conditions, an extensive analysis of the system will be conducted to satisfy these concerns.

6.24 HIGHWAY TRUCKS

This alternative required that off-highway pit trucks be loaded at the face and discharge their loads into a primary crusher located to the South of the Grum deposit. The crushed ore would be delivered to a stockpile from which material would be drawn by a conveyor belt to load trucks, each of which would be capable of hauling 54 tonnes. The trucks would proceed along a 15.2 metre wide road bed to a dumping station located to the East of the concentrator. Ore would be reclaimed by conveyor and thus introduced into the existing crushing circuit. This haulage system would require 12 units operating to deliver the planned tonnage of ore. Figure 6-5.

While it might be considered that the larger number of trucks offered improved system flexibility, it should be noted that



**FIGURE 6-5 HIGHWAY TRUCKING SYSTEM
 THE DEVELOPMENT OF THE VANGORDA PLATEAU ORE DEPOSITS**

under no circumstances could these units be deployed in the Faro pit to be loaded directly from the face. Further the problems discussed previously relating to supervisory control, road maintenance, fuel and tire costs, were also disadvantages of this scheme.

6.25 THE CONVENTIONAL CONVEYOR

As was the case when considering the cable belt and highway trucking, the conventional conveyor system required that pit run ore be hauled to the crusher located at the Grum minesite. Subsequent to crushing and stockpiling, the ore would be delivered to the conventional conveyor. Due to the distance involved, the haulage would be achieved by utilizing two conveyors in series, each of which would be 6.4 kilometres long. The final belt would discharge onto the covered surge pile from which ore would be drawn to be introduced into the existing crushing circuit. Figure 6-6.

The high risk involved in operating conventional conveyor systems over long distances in cold weather negated further consideration of this alternative.

6.3 THE SELECTION OF THE ORE HAULAGE SYSTEM

Detailed engineering studies are now in progress to evaluate the off-highway, rail and cable belt conveyor systems. Based upon the results of this work, the input from operating personnel at the minesite and appropriate plant visits, a comprehensive decision analysis will be conducted by mid 1980 to select the transportation system that will haul ore from the Vangorda Plateau to the Mill.

7
MILL MODIFICATIONS

Vangorda lead concentrates will be characterized by relatively low lead concentrate grades due to extremely fine crystal intergrowths. The concentrates will also exhibit relatively high levels of arsenic, silver and gold.

7.23 FARO ZONE III

Despite the medium to fine grained mineral composition of the Zone III material, laboratory testwork conducted by Lakefield Research on samples of this ore demonstrated that acceptable metallurgical results could be attained under certain conditions. The results of one test series are shown below.

FIGURE 7-6

LABORATORY FLOTATION TEST RESULTS - FARO ZONE III ORE

SOURCE	CONCENTRATE	ASSAYS %		% DISTRIBUTION	
		Pb	Zn	Pb	Zn
Cycle Test No. 18	Lead Zinc	61.5	52.0	91.2	87.9
Predicted Metallurgy from Laboratory Work	Lead Zinc	62-68	52-54	83-91	87-90

Note: Tests performed at medium-fine grind with
a P₈₀ 70-75 microns. Data source L.R. 2082.

In conjunction with this work at Lakefield, extensive laboratory testwork was carried out by the metallurgical staff at Faro, (C.A.M.C.) and in Kamloops (K.R.A.L.) on various samples of Faro ores. The objectives of the programs were to confirm that finer grinding improved overall metallurgical performance.

FIGURE 7-7

METALLURGICAL IMPROVEMENTS WITH FINE GRINDING FARO ORES

DATA SOURCE	GRIND RANGE (P ₈₀ microns)	INVESTIGATED (%-325#)	METALLURGICAL IMPROVEMENTS ACROSS RANGE			
			LEAD		ZINC	
			GRADE	RECOVERY	GRADE	RECOVERY
Rougher Tests KRAL-78	135 - 40	50 - 85	7.0	-	2.50	-
Rougher Tests CAMC 78-79	125 - 37	45 - 90	11.3	-	5.9	-
Cleaner Tests KRAL-79	125 - 45	45 - 80	2.5	7.0	2.1	9.5
Cleaner Tests CAMC-79	125 - 40	45 - 85	3.2	5.2	4.4	4.0
Plant Test Nov.13-17/78	125 - 60	45 - 70	3.0	5.8	3.0	4.0
Cleaner Tests KRAL-79	145 - 30	30 - 90	-	9.6	-	12.0

Notes: a) - signifies that results were adjusted to a constant grade or recovery for the purposes of analysis of data.

As a result of the encouraging bench scale test data, it was decided to conduct a pilot plant test on ores typical of Zone III material. Two discrete samples consisting primarily of 4E ore types weighing 200 tonnes and 40 tonnes respectively, were selected from the Faro pit and shipped to Lakefield in September 1979.

The primary objectives of the pilot plant were to establish the level of grind and the flowsheet that produced the optimum metallurgical performance, and also to generate data that could be used for predicting the metallurgical results that would be achieved by the modified plant.

Test results generated in this program were adversely affected by oxidation of the samples during the transportation of the two ore samples to the Lakefield facility. The larger sample

The predicted lead and zinc plant metallurgical performance was based upon pilot plant results obtained when treating ores at a grind of 50 microns, adjusted to compensate for the measured degree of sample oxidation.

The pilot plant results as recorded, and also adjusted for oxide content are shown below. The predicted plant metallurgy is compared with the 1978, 1979 plant performance.

FIGURE 7-9

PLANT METALLURGY COMPARED WITH PILOT PLANT RESULTS - FARO ZONE III ORE

DATA SOURCE	LEAD		ZINC	
	GRADE % Pb	RECOVERY %	GRADE % Zn	RECOVERY %
Pilot Plant Results	69.1	75.8	52.5	88.8
Adjusted Pilot Plant Results	68.4	86.9	52.1	90.4
Predicted Plant Metallurgy	67.0	87.5	53.5	88.5
1978-79 Plant Performance	61.1	84.0	50.4	80.0

- Notes: a) Pilot plant data refers to sample No. 1 only at the optimum grind of 50 microns P₈₀: Test No. 9.
- b) Adjusted data involves an empirical correction for the oxide content of the test sample.
- c) Plant performance data is an arithmetic average over two years.

The predicted plant metallurgical performance, including metal distribution is shown below.

FIGURE 7-10

PREDICTED PLANT METALLURGY - FARO ZONE III ORE

ORE SOURCE	CONC.	ASSAYS				METALLURGY		DISTRIBUTION			
		Pb	Zn	Au	Ag	Hg	As	Pb	Zn	Au	Ag
Faro-Zone III	Lead	67	*	0.6	600	40	0.03	87.5	*	33	65
	Zinc	*	53.5	*	*	300	0.01	*	88.5	*	*

Gold and silver recoveries were deduced from pilot plant and laboratory results. Using silver and gold concentration in the mill feed, predicted by the computer model, the precious metal concentrations in the lead concentrate were calculated. It is probable that, due to the sporadic occurrences of gold in the orebody, that some shipments of lead concentrate will contain payable quantities of gold.

7.3 PLANT DESIGN CRITERIA

The modified plant was designed to be capable of milling all Grum, Vangorda and Faro Zone III ores, individually or concurrently at planned throughput rates to achieve optimum overall metallurgical performance. Due to differing hardness and metallurgical characteristics of each ore type identified within the three deposits, it could be reasonably argued that no one constituent ore type in any blend of mill feed could yield its unique, optimum metallurgical performance. However, since such fundamental operating criteria as grind, retention times, pulp densities and reagent consumptions are similar for these ore types, the total plant performance will represent an acceptable metallurgical compromise.

7.31 OPTIMUM GRIND LEVEL

An instantaneous mill throughput rate of 450 tonnes per hour was used in all grinding calculations to ensure that planned annual mill throughput rates will be attainable under normal circumstances while achieving the target grind of about 50 microns in the flotation feed.

Several hypothetical economic models were constructed and evaluated by varying levels of grind and regrind to reduce

capital and operating costs. Metallurgical performance parameters were assigned to each model based upon laboratory and pilot plant test results at the various grind levels. A summary of the appropriate net present value determinations is tabulated below in Figure 7-11.

FIGURE 7-11
PLANT OPTIMUM ECONOMIC GRIND LEVEL

CASE	PRIMARY H.P.	REGRIND H.P.	TOTAL H.P.	GRIND TARGET P ₈₀	CAPITAL COST \$x10 ⁶	OPERATING COST INCREASE \$x10 ⁶	RELATIVE NET PRESENT VALUE \$x10 ⁶
1	11,700	1,350	13,050	50	43.0	6.8	153.9
2	9,200	2,350	11,550	70	43.1	5.1	129.8
3	7,700	1,850	10,550	100	38.6	4.3	112.7
4	5,200	1,350	6,550	130	0	0	117.4

- Notes: a) Reference - Memo Brown to Taggart Dec. 16, 1979 "Optimum Grind Calculations".
 b) Capital cost includes power plant: Clearly case 4 is with no expansion.
 c) Operating cost includes manpower, steel and reagents.
 d) Data assumes milling a 50:50 blend of Grum and Anvil Zone III ore.

The reported net present values are not absolute, but rather provide a relative comparison between the various flowsheets considered. It was concluded that the flowsheet designed to produce optimum metallurgical performance, also provided the most favourable financial alternative.

7.32 GRINDING CIRCUIT DESIGN

Mill design calculations were based upon standard Bond methods to determine installed horsepower requirements. These calculations indicated that in addition to the existing grinding

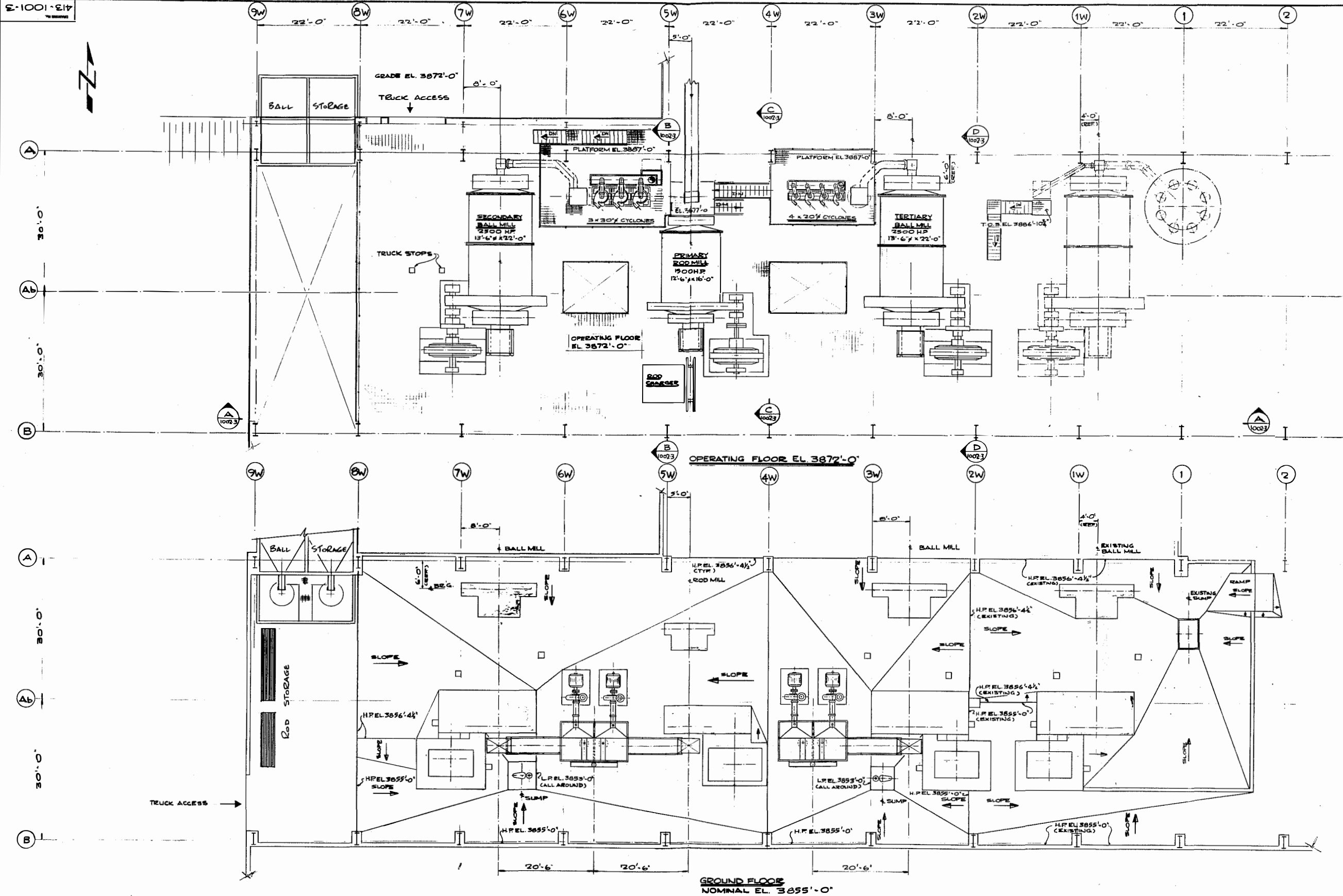


FIG. 7-12

TITLE
MODIFIED MILL GRINDING AREA GENERAL ARRANGEMENT

circuit one new rod mill with a 1500 HP motor, and two in-series ball mills each driven by a 2500 HP motor, would be capable of achieving the target grind of 50 microns at planned throughput rates. All calculations were based on a work index value of, 13.2 kW hr/tonne, the highest value reported during grindability testwork.

Regrind mill capacities will be just sufficient to achieve the required mineral liberation. Ore will be supplied to the new grinding circuit from two additional bins that will effectively supplement the marginal capacity of the existing fine ore storage. Figure 7-12.

7.33 FLOTATION CIRCUIT DESIGN

Results of testwork and experience at other operations has demonstrated that, in addition to fine grinding, certain other factors significantly affect metallurgical performance. Specifically, flotation pulp densities must be reduced and retention times extended when compared with current practice, to create an environment conducive to the efficient selective flotation of the finer minerals.

To achieve both of these objectives, the existing induced air 100 cubic foot flotation cells will be replaced with 1350 cubic

foot supercharged machines that will serve as lead and zinc roughers and first cleaners. The existing 200 cubic foot supercharged flotation cells will be converted to second and third stage cleaner circuits for both circuits. The net effect of these changes is summarized below.

FIGURE 7-13
FLOTATION CELL CAPACITY REQUIREMENTS

CIRCUIT	TOTAL CELL CAPACITY (ft ³)	CAPACITY/TONNE (ft ³ /tonne)
Anvil Present	29,200	3.22
Anvil Modified	55,200	6.09

The grinding pulps will be aerated prior to lead roughing and conditioners will prepare the mineral surfaces for zinc flotation. The aerators and conditioners form integral sections of their respective rougher flotation cell banks.

Reagents will be received, stored and mixed in a new reagent handling facility to be located immediately to the North of the fine ore storage bins. The plant will offer a much greater degree of environmental security than the existing systems. Basic instrumentation will ensure consistent reagent solution strengths and provide adequate warning of any undesirable condition in the new reagent plant.

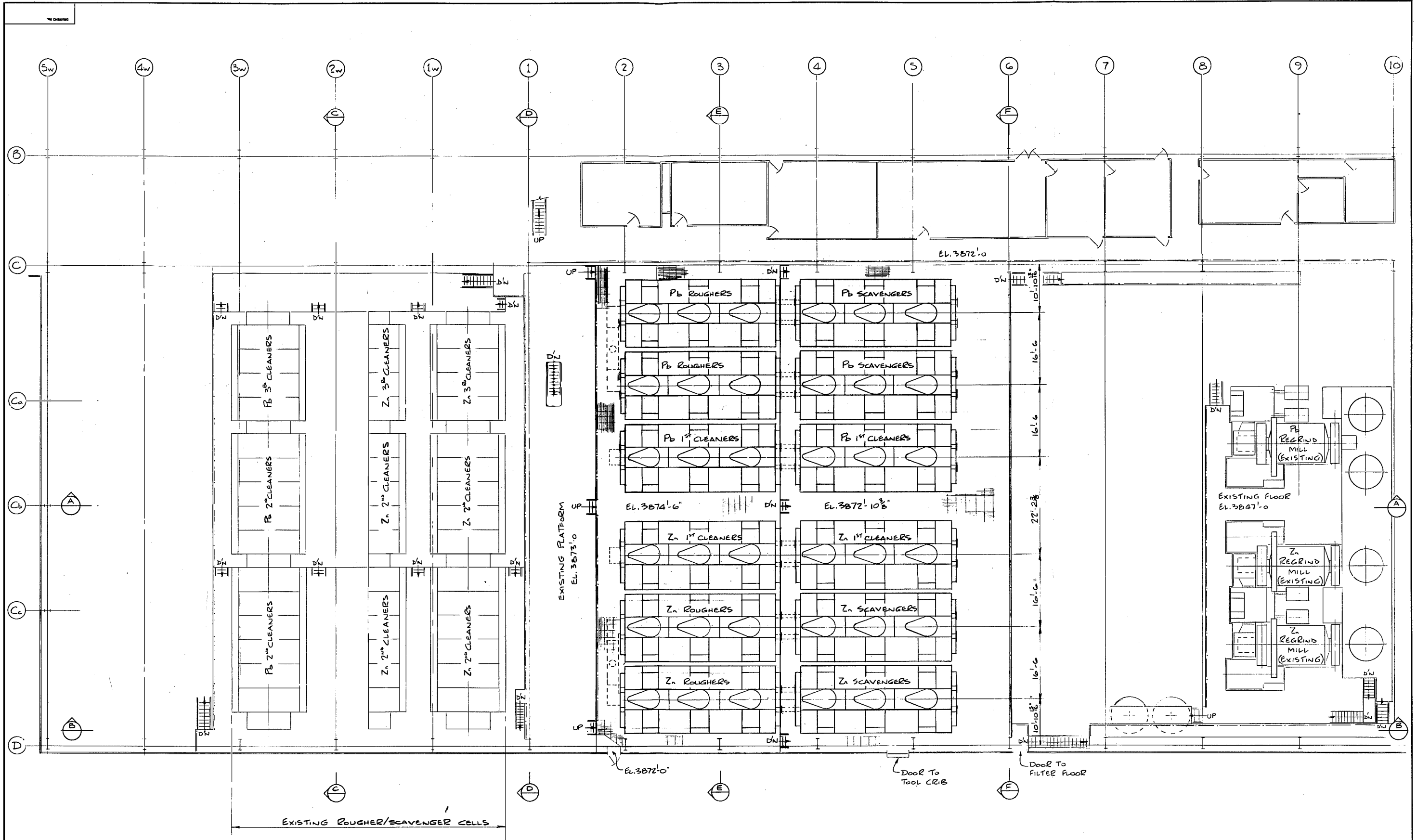


FIG 7-14

TITLE
MODIFIED MILL FLOTATION & REGRIND GENERAL ARRANGEMENT

7.34 INSTRUMENTATION

The modified plant will contain some sophisticated but field proven instrumentation to monitor and control some of the key process functions. The equipment selected will provide the minimum information required to control the process and will also form the basis for any new automatic control strategies. Provision of automatic control systems, will be delayed until the necessary strategies are formulated; usually this occurs two or three years after start-up of an on-stream analyzer system.

The principal component of the new instrumentation system will be the Courier 300 on-stream fluorescence analyzer. This unit is capable of measuring the concentration of four elements which will include lead, zinc and iron, in each of fourteen process streams. In addition the unit will measure the pulp density of each of the streams, and print-out all the data on a high speed typewriter.

A particle size monitor of the PSM-200 type will be installed on the lead circuit feed. This unit measures mean particle size and pulp density.

Key reagent flows will be monitored by employing magnetic flow

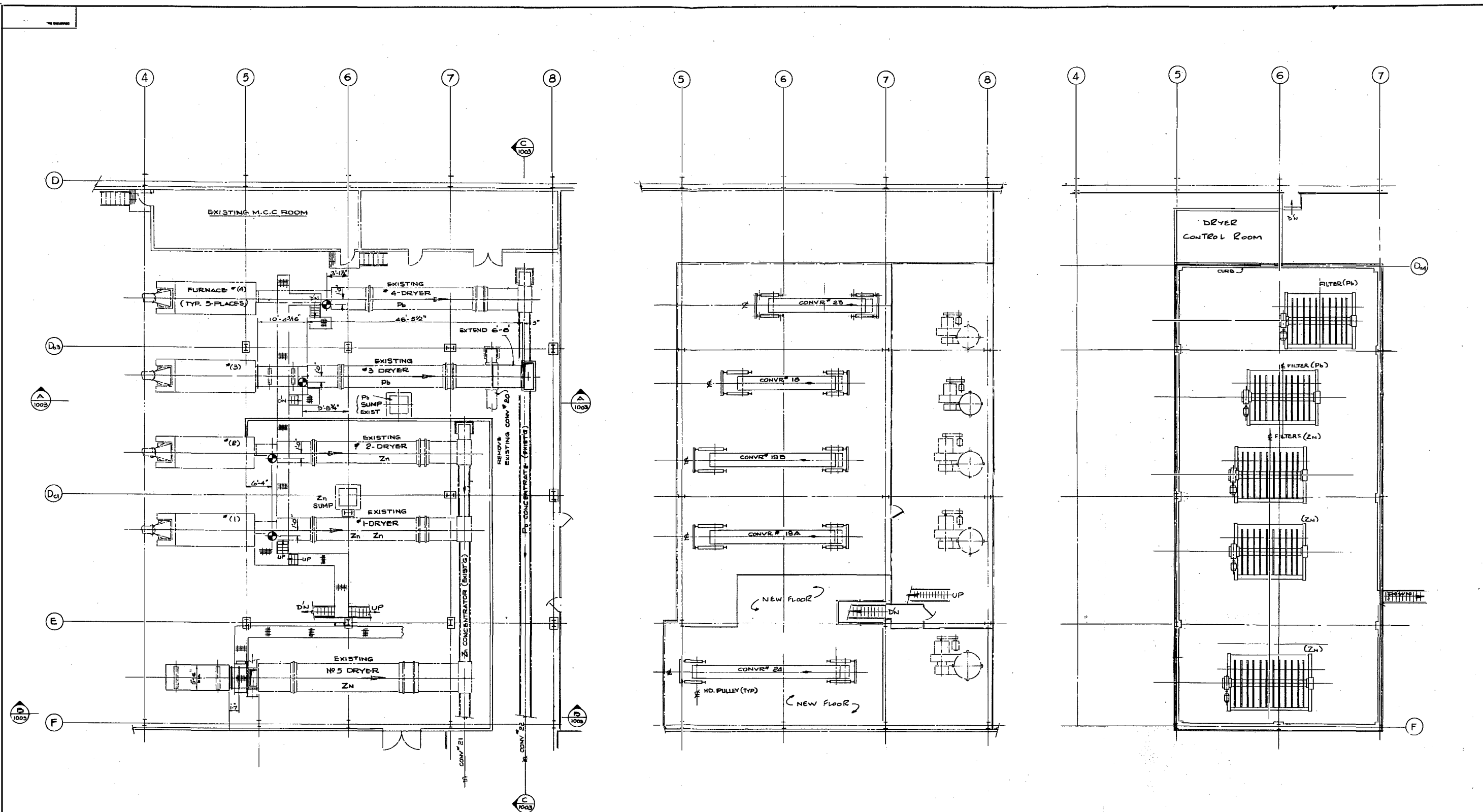
monitoring devices on certain critical reagent lines - e.g. cyanide, soda ash solution, collector and copper sulphate. These flows will be displayed on strip charts and totalized. pH control will be achieved by feed-back systems on the soda ash and lime pressure loops, from pH sensor probes located in the flotation cells.

Mass flow of material into the lead and zinc cleaner circuits will be measured and, using assay data, the circulating cleaner circuit load will be determined.

7.35 DEWATERING CIRCUIT DESIGN

Each concentrate will be thickened and a clarifier used to treat the thickener overflow. The clarifier overflow will be returned to the reclaim water system for re-use. Thickener underflow density control will be effected by means of variable speed diaphragm pumps which eliminate wide fluctuations in filter feed densities.

The filter feed pulps will be heated to improve filtering efficiency. The elevated pulp temperatures effectively reduce surface tension, thereby facilitating improved cake drainage on the filter. The existing filters will be replaced with larger



EXISTING CONCENTRATE DRYERS
BASEMENT FLOOR

NEW FILTER CAKE CONVEYORS
FIRST FLOOR

NEW FILTERS
SECOND FLOOR

FIG. 7-15

TITLE
MODIFIED MILL
FILTERING & DRYING
GENERAL ARRANGEMENT

units to increase the available filter media area by a factor of three to permit adequate time for cake formation and drainage.

Two additional 5000 CFM vacuum units, identical to the three presently in use will be installed to service the additional filter capacity. An additional 1200 CFM compressor is included in the design to provide air for the filter snap-blow systems and other purposes.

The elimination of bulk concentrates greatly simplifies the layout and thus the operation of the dewatering plant. Contamination between concentrates will be minimized by reducing the number of conveyors, and by dividing the existing basement into two discrete areas.

The allocation of dryers to specific functions is based upon theoretical design calculations that indicate that the existing units can dry the maximum anticipated concentrate production to acceptable moisture contents. The plan figures below are based upon milling planned tonnages of ore for 1984. This year was chosen since the highest annual concentrate output is predicted for 1984.

FIGURE 7-16
THE DEWATERING PLANT CAPACITY

PRODUCT	PLANNED OPERATING RATES (DMT/OPERATING HR)	DESIGN OPERATING RATES (DMT/OPERATING HR)
Lead concentrate Production	21.2	25.2
Zinc concentrate production	36.7	53.2

Grinding circuit availability 92%
Dewatering circuit availability 85%

Day to day changes in plant feed grades require some provision to dewater concentrate above planned levels for short periods of time. To obtain this essential "reserve capacity", dryer slopes have been steepened and the fire box configuration on number 5 dryer has been improved to maximize dryer throughput rates.

New weightometers are to be installed on the loadout belts to accurately monitor the dewatering plant production rates.

8.
POWER SUPPLY

8.1 CYPRUS ANVIL POWER REQUIREMENTS

The estimated power requirements to service the modified mill and mine development programs were calculated by applying the same load factor as presently measured to the designed connected horsepower load for determining peak demand and energy consumption criteria.

The modified mill equipment register and predicted mine equipment loads were used to develop the forecast connected load. For the purposes of this calculation it was assumed that a conveyor would be used to transport ore from the Vangorda Plateau to the mill site, since this alternative represents the worst case from an electrical load stand-point. The peak demand and annual energy consumption were calculated to be 25.0 MW and 155 GW hrs respectively.

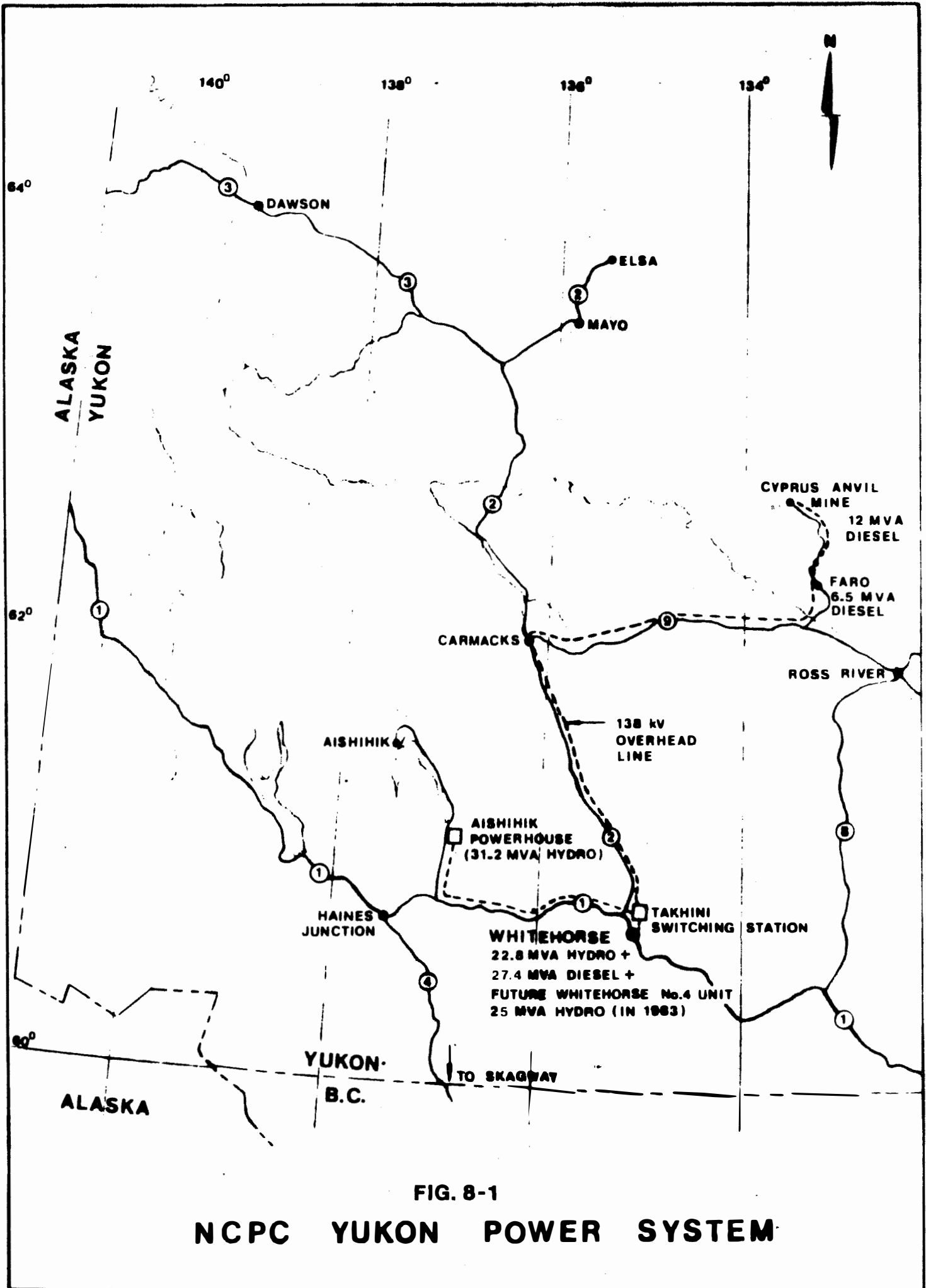


FIG. 8-1

NCPC YUKON POWER SYSTEM

8.2 THE N.C.P.C. POWER GENERATING CAPABILITIES

The N.C.P.C. electrical distribution grid provides power to Faro and the minesite, and also services Whitehorse, Carmacks, Ross River, and a number of smaller communities. (Figure 8-1). The total capacity of the present system is 77.7 MW. Following the installation of a fourth hydroelectric turbine at the Whitehorse Rapids plant in 1983, the system capabilities will be increased to 97.7 MW, exclusive of the proposed local generating capacity. The Figure 8-2 below summarizes the N.C.P.C. generating capabilities and includes the small diesel unit located at Faro, installed primarily to provide emergency domestic power to the communities of Faro and Ross River in the event of a power outage.

FIGURE 8-2

N.C.P.C. GENERATING CAPACITY

SOURCE	PRESENT CAPACITY (MW)	POST MID 1983 CAPACITY (MW)
Hydro: Aishihik	31.0	31.0
Whitehorse Rapids	<u>20.0</u>	<u>40.0</u>
Sub-Total	51.0	71.0
Diesel: Faro Plant	5.1	5.1
Whitehorse Rapids	<u>21.6</u>	<u>21.6</u>
Sub-Total	26.7	26.7
TOTAL	77.7	97.7

Appropriate utility system reserve capacities are normally computed by adding 5 percent of the anticipated peak demand to the capacity of the largest single generator that could be taken "off-line"; in

this case one of the two hydroelectric turbines (15.5 MW) located at Aishihik. The forecast system peak demand 1980-81 is 55.5 MW. Thus:

$$\begin{aligned} \text{Reserve capacity (MW)} &= \text{capacity largest unit} + (0.05 \times \text{peak demand}) \\ &= 15.5 + (0.05 \times 55.5) \\ &= \underline{18.3 \text{ MW}} \end{aligned}$$

As shown in figure 8-3 below the system has adequate capacity to satisfy the current requirements. The additional 9.0 MW load imposed by the development programs however, will result in a 10.0 MW shortfall in system capacity, which could be largely offset by the installation of a 9 MW thermal generating facility. The temporary reduction in reserve capacity is not sufficient to justify the installation of additional generating equipment, particularly when considering the excess system capacity that will exist once the new hydroelectric turbine is installed and operating by mid 1983.

FIGURE 8-3
N.C.P.C. SYSTEM CAPACITY vs. REQUIREMENTS

CASE	PERIOD	PEAK DEMAND MW	CALCULATED RESERVE MW	REQUIRED GENERATING MW	ACTUAL CAPABILITY MW	SURPLUS (SHORTAGE) MW
1	Forecast 1980/81	55.5	18.3	73.8	77.7	3.9
2 *	Forecast plus Vangorda Development Load	68.8	18.9	87.7	77.7	(10.0)
3	As for 2 plus 9 MW Power Plant	68.8	18.9	87.7	86.7	(1.0)
4	As for 2 plus Additional Hydro Unit at Whitehorse	68.8	18.9	87.7	106.7	19.0

* Includes provision for normal load growth.

From this analysis of the peak demand criteria it was concluded that a 9 MW increase in capacity will be required to satisfy the projected load in 1982 and at least for the first 6 months of 1983. Delays in commissioning the additional 20 MW turbine in Whitehorse would extend the dependency on the generating plant.

Similarly a study of the forthcoming energy production capabilities indicated that sufficient hydroelectric energy would be available to satisfy the system requirements in total by 1984, Figure 8-4 below.

FIGURE 8-4
LOCAL ELECTRICAL ENERGY REQUIREMENTS (GW hrs)

YEAR	1980	1981	1982	1983	1984	1985	1986
C.A.M.C. Requirement	100	100	145	145	145	155	155
N.C.P.C. Contribution	100	100	100	123	145	155	155
Local Generation Requirement	-	-	45	22	-	-	-

The above data assumes that the new hydroelectric turbine will be in service by mid 1983 and will be capable of producing 80 GW hrs/year. This may only be achieved following the resolution of winter and spring problems in the Marwell area of Whitehorse. The data above also assumes that the Whitehorse Copper Mine curtails production in 1983 as scheduled. Delays in a shut-down of this operation for any reason, would extend the dependency of Cyprus Anvil on locally generated energy.

8.3 SUPPLEMENTARY POWER GENERATION

Network analyses of the system were integrated with predicted total grid loadings to establish the need for an additional 9 MW generating facility, that would be required for at least the first two years of operation subsequent to the start-up of the modified mill circuit. A number of power generating alternatives were considered including, coal fired steam generators, hydroelectric generating systems, gas turbines, and diesel engine generators.

A preliminary feasibility study was conducted by Montreal Engineering Ltd. to investigate the viability of coal fired steam generators, for providing short and long term energy supply. The investigation indicated that such generation is worthy of further study in the future as coal quality and reserves are better defined. A coal fired power station could not be commissioned in the time required by the development schedule.

Hydroelectric generating potential in the immediate area was found to be limited. Nevertheless, studies are scheduled to commence in the near future to develop an inventory of possible sites and identify their respective generating potentials.

Gas turbines were found to be cheaper than stationary diesel

generating units in terms of capital costs. However, their inferior fuel efficiency characteristics, render these machines more suitable for stand-by and peaking service.

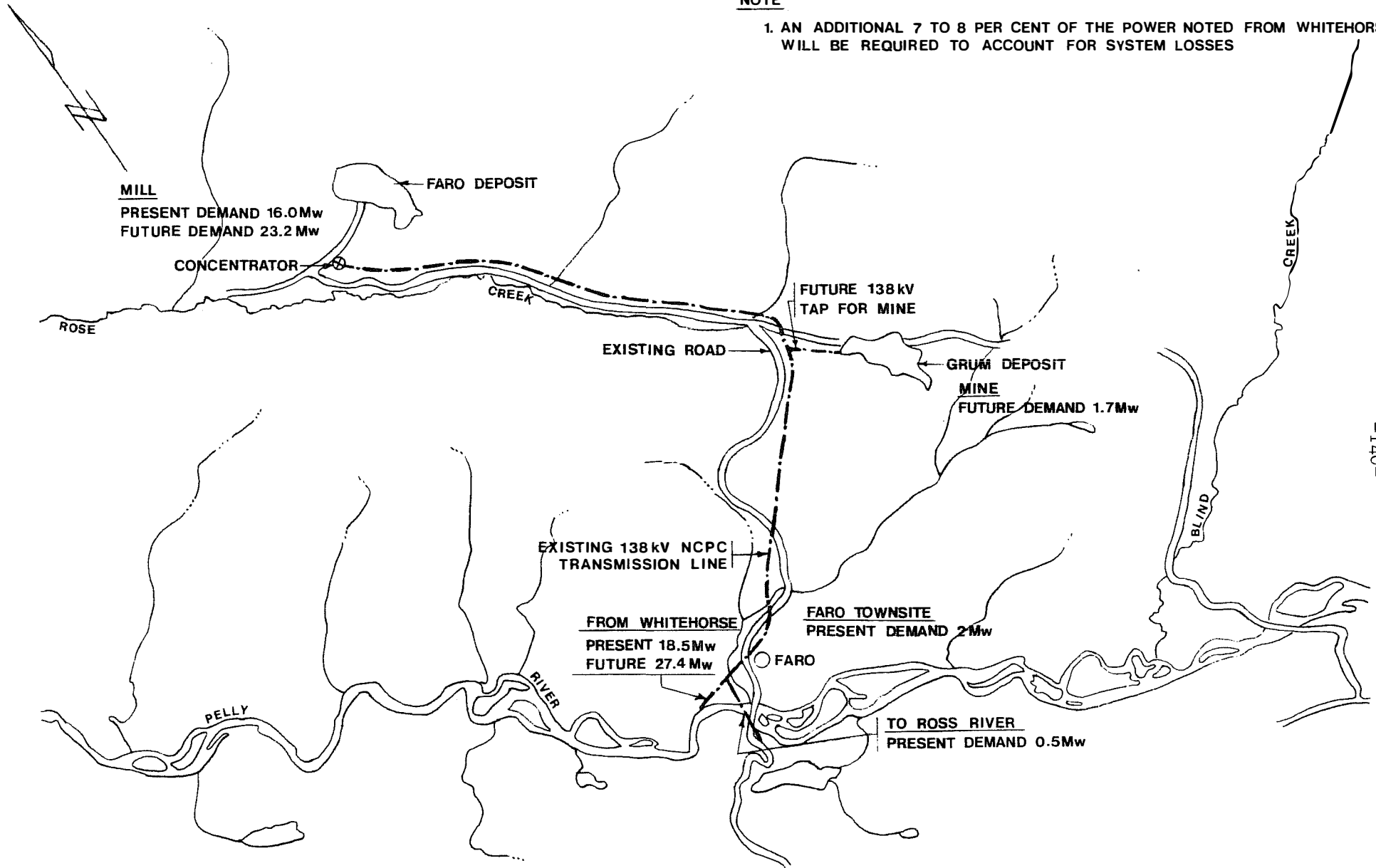
Diesel engine power generating units are normally favoured to supply long term energy needs. These units require a higher initial capital investment, however this disadvantage is offset by the improved reliability and low unit cost of energy produced.

The final plant design is currently in progress to select the most cost efficient and reliable generating system that would provide the incremental power requirements until adequate and cheaper hydro-electric energy is available. Both diesel engine and gas turbine alternatives are under consideration. For this purpose it was assumed that the power plant would be capable of generating up to a maximum of 10 MW.

Despite the installation of suitable compensating and control equipment, line losses in the order of 16 percent were predicted if the additional energy were generated in Whitehorse. Further study proved that it would be cheaper to transport fuel to the Faro area to a plant closer to the load centre, than to incur such substantial transmission losses.

NOTE

1. AN ADDITIONAL 7 TO 8 PER CENT OF THE POWER NOTED FROM WHITEHORSE WILL BE REQUIRED TO ACCOUNT FOR SYSTEM LOSSES



-071-

FIG. 8-5

N. T. S.

POWER DISTRIBUTION REQUIREMENTS FARO AREA

Power will be provided to the Vangorda Plateau minesite by means of a branch line taken off the existing 138 kV transmission line between the Town and the Faro minesite. A transformer and sub-station will be located at the Grum minesite.

The power generation and modified distribution system provides for an additional step-down transformer to parallel the 16 MVA unit presently in service. The total cost of the generating station transformers and transmission line to the Grum minesite will be approximately \$12.0 million.

8.4 THE COST OF ELECTRICAL ENERGY

The figure below summarizes the annual minesite energy requirement by year and identifies the respective energy sources.

FIGURE 8-6
TOTAL ENERGY PRODUCTION AND COST BY YEAR

YEAR	1980	1981	1982	1983	1984	1985	1986
Total Energy Required (GW hrs)	100	100	145	145	145	155	155
N.C.P.C. Energy Available (GW hrs)	100	100	100	123	145	155	155
Additional Generation Requirements (GW hrs)	-	-	45	22	-	-	-
Total Energy Cost (\$ million)	4.61	4.61	8.32	7.71	6.68	7.15	7.15
Unit Energy Cost (¢/KWH)	4.61	4.61	5.74	5.32	4.61	4.61	4.61

Total energy costs were derived by calculating the weighted average value for locally generated energy and that supplied by the existing grid.

8.5 LONG TERM POWER SUPPLY

The N.C.P.C. is presently considering a number of potential hydroelectric sites within the Yukon with a view to commencing staged development programs to provide sufficient energy for long term territorial growth. Areas currently under study are listed below with their respective potential capacities.

FIGURE 8-7
POTENTIAL HYDROELECTRIC DEVELOPMENTS

POTENTIAL SITE	POTENTIAL CAPACITY MW
Eagle Rock	75
Francis River	70
Teslin River	45
Little Salmon River	15

In view of the high transmission losses referred to earlier, and the high cost of thermal generated energy, there will be considerable advantage to Cyprus Anvil if any one of these sites could be developed.

In addition to these studies conducted by the N.C.P.C., Cyprus Anvil will continue to evaluate the feasibility of local hydroelectric and thermal power generating systems.

9.1 INTRODUCTION

The protection of the natural environment and the improvement in working conditions were vital considerations in the design of the long term development program. There are three principal areas of concern in this regard, namely the levels of airborne particulates, of noise in the working environment, and the potential adverse impact future mining developments could impart to the flora, fauna, water quality and aesthetic beauty of the natural surroundings.

9.2 AIRBORNE PARTICULATES

The potential to generate excessive levels of airborne particulates is inherent in the basic processes of crushing, grinding, flotation and concentrate drying. Dust may be generated directly by the process or indirectly by emissions from material spillages that have accumulated in the plant. While all levels of dust are undesirable, the so called "respirable dust", ranging in size from zero to five microns, is the size range deemed most harmful to health.

Significant improvements have been achieved during the last five years in reducing the concentrations of these undesirable, ultra--fine particles. These changes have been realized through the implementation of more effective plant ventilation.

Certain features have been incorporated in the new plant design that will further reduce airborne dust levels. Thus all new flotation cells will be covered and vented to minimize ultra-fine dust generation to atmosphere from flotation froth surfaces.

The most prolific dust source in the filter dryer area has been the transfer conveyor system feeding the dryers. The number of conveyor belt transfer points in the modified dewatering plant has been significantly reduced. In addition a solid floor will be laid

directly above the dryers to effectively isolate the dryer section and divide that part of the building into individually ventilated areas. Improved filter and dryer control systems will minimize periods of over-drying and hence dusting conditions, while reducing overall product moisture. Each of the above measures will contribute to much improved air quality and working environment in the dewatering section.

The design of the modified plant will do much to reduce process spillage which is not only unsightly but may also expose employees to elevated levels of dust. The principal sources of process spillage are the grinding and flotation section basements. There is no doubt that the redistribution of mill feed within the expanded grinding circuit, the redesigned flotation launders and improved circuit control facilities will do much to alleviate this problem.

At present the reagent mixing plant is centrally located in the concentrator. Chemical dusts emanating from this vicinity that are not exhausted by the local ventilation system, migrate through the flotation section and the mill mechanical workshop exposing employees to inhalation of this material. The modified plant design provides for a new reagent receiving and mixing facility, physically separated from the operating floors and serviced by a dedicated heating and ventilation system, thus minimizing employee exposure to these potentially harmful chemical dusts.

The existing lunchroom is small, poorly located and difficult to keep clean. Dust carried into the room on work clothing may accumulate on table surfaces and ultimately contaminate food. The modified plant incorporates central air conditioned and pressurized lunchroom facility and a new washroom. Provision is made to hang work coats and coveralls outside the lunchroom to prevent the involuntary transportation of dust and contaminants into the areas where food is consumed.

As a result of the work carried out over recent years, and the measures incorporated in this most recent design to reduce levels of airborne dust, the new plant has the capability of meeting all generally accepted environmental standards.

9.3 NOISE

Certain mineral processing functions typically generate noise levels above that at which hearing protection is required when employees are subjected to prolonged exposures during their normal working shift. Mine safety regulations require that hearing protection be worn by those employees who are exposed to time weighted averages in excess of 85 decibels. Whilst preventive action can be taken to minimize the adverse effects of noise, the wearing of protective devices is frequently uncomfortable and inconvenient. The adverse effect on the overall working environment inevitably results in reduced morale and job interest.

Noise levels will be reduced in the modified mill by the general reduction in the number of small high speed motors, belt-driven sheaves in the flotation area and the increased use of sound proofing materials.

9.4 FRESH WATER CONSUMPTION

The existing water license limits the annual consumption of fresh water at the minesite to 2.0 billion imperial gallons. In order to ensure compliance with this limit, and provide sufficient water to achieve the reduced flotation densities, an internal water recirculation system has been incorporated into the plant design. Thus water overflowing the lead and zinc clarifiers will be collected and used in the grinding and flotation processes. It is estimated that about 2,000 imperial gallons per minute may be recirculated within the modified mill, which would reduce the total fresh water requirement.

This reduction in fresh water consumption should be considered the first step in the long term management of fresh water usage. Engineering studies, in conjunction with laboratory testwork in progress at the minesite, are proceeding to develop methods by which further reductions in water consumption may be realized to the mutual benefit of the process and the environment.

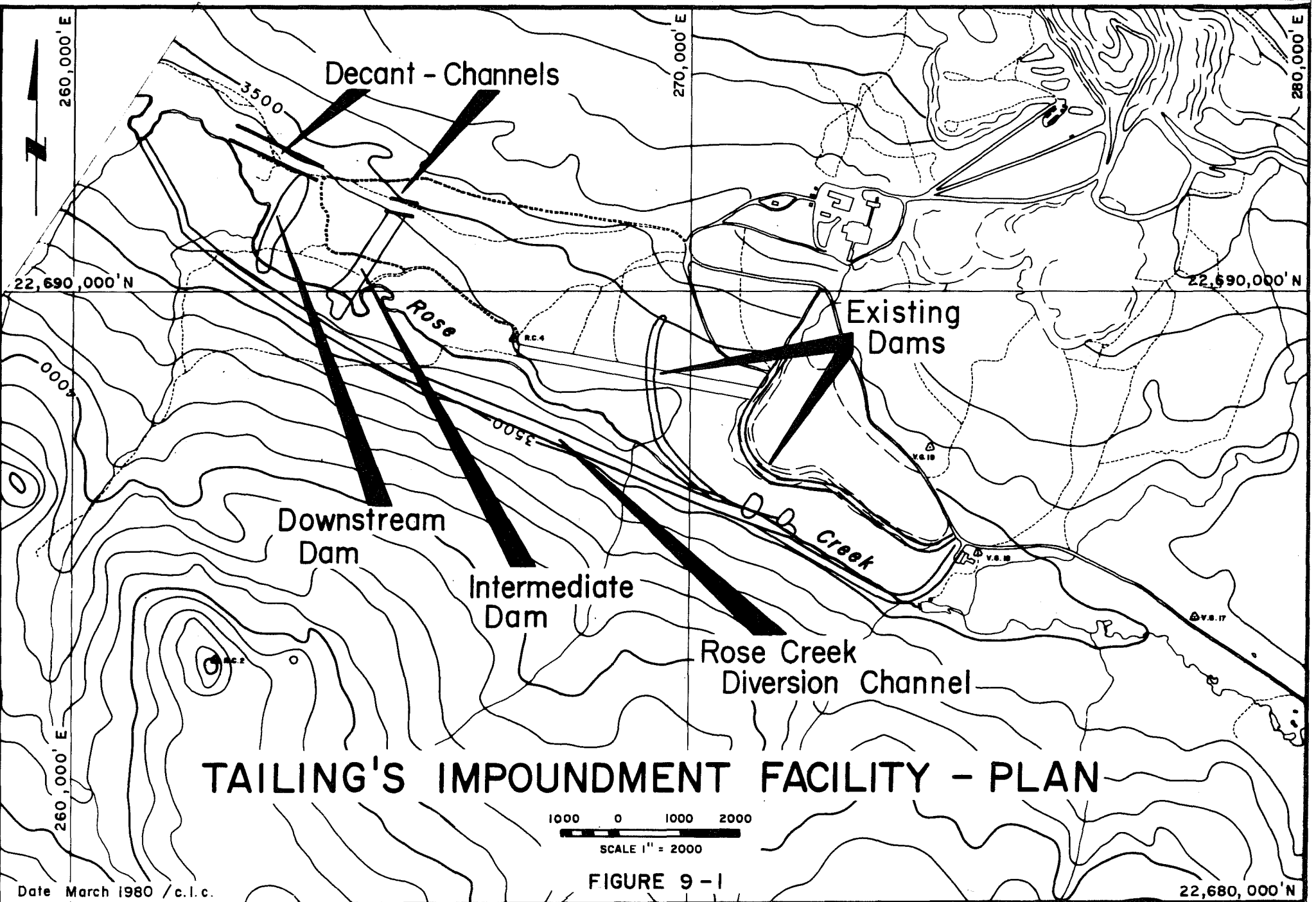
9.5 TAILINGS DISPOSAL

It will be necessary to construct new tailings impoundment facilities to accommodate the increased volumes of tailings produced when milling ore from the Vangorda Plateau, in addition to feed from the Faro pit.

The finer grind will exert constraints on the overall design of the facility. The physical size of the ponds will be increased not only to accommodate larger volumes of tailings, but also to provide increased retention times for effective settling of the finer suspended particulates. The proposed design reflects the lower ultimate deposition densities of the finer tailings caused by higher levels of fluid entrapment. Finally, since the angle of repose of the tailings will be lower, the expanded pond design provides for increased volumes of material to be stored beneath the water level.

The new tailings disposal facilities shown in Figure 9-1 will provide sufficient storage volume for an additional fifteen years production, during which time the two new dam structures will be raised in 1986 and again in 1990. The existing Rose Creek diversion ditch will be extended along the south side of the valley for approximately 3.2 kilometres. The impoundment area will be

contained by two new earth-fill dams. The area up-stream of the intermediate dam will provide storage for the solid tailings. The volume contained between the intermediate dam and the downstream dam will provide sufficient retention time for supernatant clarification to ensure that the final effluent will conform to all pertinent regulatory requirements.



TAILING'S IMPOUNDMENT FACILITY - PLAN

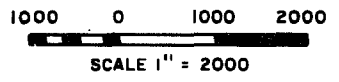


FIGURE 9 - 1

9.6 THE BIOPHYSICAL ENVIRONMENT

The elevation at the Anvil minesite is 1,070 metres and the climate is characterized by long cold winters and short cool summers. The mine is situated on the south flank of the Anvil Range, an area of rounded mountains cored by granite which reach a maximum elevation of 1,980 metres. Hillsides support an open forest of small white and black spruce above which alpine tundra predominates. Major wildlife species in the area are moose, Dall sheep, woodland caribou, grizzly bear and black bear. Streams support indigenous populations of grayling and provide spawning beds for chinook salmon.

Environmental baseline studies have been designed and are being expanded to assist in the complete understanding of the undisturbed natural environment. The studies are logically divided into specific areas of investigation.

9.61 HYDROLOGY:

Limited stream flow data is available for the Vangorda and Rose Creeks. Continuous recording stations will be constructed to accurately monitor these volumes to provide data for future

engineering purposes.

9.62 WATER QUALITY:

Most existing water quality data is concerned with flows in the vicinity of the mine. A regional program of water quality sampling was started in 1979 and includes sites on all watersheds in the Anvil Range, which could be affected by mining developments in the foreseeable future. Sampling has been carried out at approximately 25 sites, twice during 1979 and will be carried out four times per year henceforth. Stream sediments were also sampled during 1979 and will continue to be sampled every year to monitor possible accumulations of heavy metals.

A benthic sampling program will be instituted in co-operation with the Environmental Protection Service in the three major affected drainages in the Anvil Range. Benthic sampling provides a very sensitive method of detecting deteriorations in aquatic environment.

9.63 VEGETATION:

Vegetation mapping has been conducted in a general way (1:50,000 scale) over most of the affected areas of the Anvil

Range to provide an adequate level of detail for most purposes. More intensive studies of vegetation will be carried out to determine species composition and structure of the plant communities and growth rates of tree species for potential use in revegetation. Work commenced in this regard during 1979.

9.64 WILDLIFE:

Low key studies will commence, to monitor fish and ungulate populations in those areas that could be affected by future mining development. Of particular concern is the potential adverse affect, mining activities in Vangorda Plateau may impose upon the resident herd of sheep that have traditionally migrated over this land when travelling between Mount Mye and Sheep Mountain, their respective summer and winter habitats.

All long term production plans will endeavour to minimize detrimental effects upon the indigenous species in this area.

FIGURE 10-1
CYPRUS ANVIL MINING CORPORATION
FINANCIAL EVALUATION OF VANGORDA PLATEAU DEVELOPMENT
Cdn. \$ (Millions)

	<u>CASH 1</u>	<u>4B-V</u>	
	<u>Net Cash Flow available for distribution</u>	<u>Net Cash Flow available for distribution</u>	<u>Difference to Case 1</u>
1980	30.538	11.686	(18.852)
81	21.258	8.063	(13.195)
82	18.837	37.794	18.957
83	77.366	76.833	(.533)
84	41.374	38.208	(3.166)
85	39.751	64.206	24.455
86	42.283	46.447	4.164
87	49.023	59.761	10.738
88	40.253	68.625	28.372
89	17.341	72.823	55.482
90		45.527	45.527
91		54.991	54.991
92		60.625	60.625
93		33.927	33.927
94		29.807	29.807
95		24.234	24.234
96		24.551	24.551
97		30.647	30.647
TOTAL	<u>378.024</u>	<u>788.755</u>	<u>410.731</u>
		DCF/ROI	<u>36.6%</u>

CASE PRINT OUTS

FIGURE 10-8 CASE I CASH FLOW REPORT
(CON'T)

	39	1990	1991	1992	ACCUM
1. SALES LESS CONVERSION	130	0.000	0.000	0.000	1408.698
2. + LOAN DRAWDOWN	15	0.000	0.000	0.000	0.000
3. - LOAN REPAYMENTS	135	0.000	0.000	0.000	0.000
4. + BUYERS RECD. ADJUSTMEN	102	0.000	0.000	0.000	18.830
5. + OPENING CASH ON HAND	103	0.000	0.000	0.000	28.457
6. CASH AVAILABLE	117	0.000	0.000	0.000	1455.985
USE OF CASH					
7. PRODUCTION COSTS	104	0.000	0.000	0.000	605.375
8. ORE BODY ROYALTY	119	0.000	0.000	0.000	0.000
9. GENERAL AND ADMN. COSTS	105	0.000	0.000	0.000	130.615
9.5 RECLAMATION	400	0.000	0.000	0.000	0.000
10. INTEREST - TERM DEBT	31	0.000	0.000	0.000	0.000
11. - HOUSING	222	0.000	0.000	0.000	-0.109
12. PRINCIPAL HOUSING MORTGAGE	108	0.000	0.000	0.000	4.934
13. CAPITAL EXPEND. - ANVIL	391	0.000	0.000	0.000	43.840
14. V+G-RELATED - OTHER	389	0.000	0.000	0.000	0.000
15. EXPLORATION +FEASIBILITY	207	0.000	0.000	0.000	6.050
16. PRE-PRODUCTION STRIPPING	225	0.000	0.000	0.000	0.000
17. TORRENS SHARES	110	0.000	0.000	0.000	.454
18. YUKON ROYALTY	221	0.000	0.000	0.000	52.570
19. FED. INCOME TAX	99	0.000	0.000	0.000	206.565
20. DIVIDENDS	111	0.000	0.000	0.000	6.126
21. PREPAID EXPENSES	113	0.000	0.000	0.000	1.905
22. FLOAT ADJUSTMENT	257	0.000	0.000	0.000	0.000
23. TOTAL	114	0.000	0.000	0.000	1059.963
24. CLOSING CASH ON HAND	115	0.000	0.000	0.000	18.000
25. CASH AVAIL. FOR DISTRIB.	116	0.000	0.000	0.000	378.023
DISCOUNTED NCF					
26. 10 PERCENT	49	0.000	0.000	0.000	228.777
27. 12 PERCENT	42	0.000	0.000	0.000	209.428
28. 15 PERCENT	38	0.000	0.000	0.000	184.654
CUMULATIVE NPV					
29. 10 PERCENT	321	228.777	228.777	228.777	
30. 12 PERCENT	324	209.428	209.428	209.428	
31. 15 PERCENT	320	184.654	184.654	184.654	
32. PRICLS - LEAD (US C/LB)	418	0.000	0.000	0.000	32.731
33. ZINC (US C/LB)	419	0.000	0.000	0.000	37.171
34. SILVER (US \$/OZ420)		0.000	0.000	0.000	15.692
35. GOLD (US \$/OZ421)		0.000	0.000	0.000	312.000
36. CND. DOLLAR PER U.S. DOL	422	0.000	0.000	0.000	.798

